A generalized sample preparation method by incorporation of metal–organic compounds into polymers for electroless metallization

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ABSTRACT

Metallization of polymers is important for several technological and industrial applications. In this work, we demonstrate the influence of metallization bath parameters on LCP Vectra® 820i polymer samples prepared by incorporation of a small amount (<0.5 wt %) of metal-organic compounds (palladium, nickel or copper acetates) in the molten polymer. During blending, the acetates thermally decompose and yield the metallic particles (Pd, Ni or Cu) which are used as the activators for electroless copper deposition. After surface preparation, copper is deposited on LCP Vectra® 820i in an electroless bath including formaldehyde as reducer. The influence of metallization bath temperature and bath composition with respect to the copper deposition is investigated. The initiation of copper deposition is delayed for lower temperatures. In the temperature range of 35°C-55°C, after 60 min of deposition, the amount of deposited copper is similar for 35°C, 40°C and 45°C, and higher than that at 50°C and 55°C. The maximum rate of copper deposition is around 60 $\mu\text{g cm}^{-2} \text{ min}^{-1}$ for 35°C, 40°C and 45°C and higher than 50°C and 55°C. The mean diameter of deposited copper particles shifts to smaller values with increasing bath temperature. When the formaldehyde volume is increased in the metallization bath, the maximum deposition rate is higher, shifts to shorter deposition time and the mean particle diameter becomes smaller. The metallization reaction order with respect to formaldehyde and the activation energy of electroless copper deposition decreases with increasing deposited copper amount.

INTRODUCTION

The metallization of polymers is important for several industrial and technological applications [1], [2]. Liquid Crystal Polymer (LCP Vectra® E820i) is a high performance thermoplastic polymer and combines several interesting properties, like low moisture absorption, high heat resistance, high chemical and mechanical resistances, low coefficient of thermal expansion, low dielectric constant, excellent flow properties and dimensional stability [3]. These assets can be combined for numerous applications once it is metallized: in microelectronics for packaging [4], Microelectromechanical Systems (MEMS) [5] [6] and Molded Interconnect Devices (MIDs) [7].

The electrolytic process cannot be employed on non-conductors like polymers for their metallization. The electroless metal deposition is commonly used industrial processes on polymer surfaces [8] [9] due to its low cost, simple processing, uniform deposition layer on large surfaces, low temperature treatment and no requirement of vacuum system [10] [11]. Once a metal with enough thickness is electroless deposited on polymer surface, the electrolytic deposition can be further processed onto the electroless metal layer. Among the metals, copper is widely used metal in electrical connections associating low electrical resistivity, high electro migration resistance [12] and low-cost.

The traditional electroless copper deposition process on polymers involves commonly three steps: surface preparation/modification, surface activation (sensitizing or seeding), and electroless copper deposition [13]. The first step enables cleaning and modification of polymer surface in order to improve the adhesion of the forthcoming electroless metal layer. Several methods have been employed for this purpose including plasma surface modification [14] [15], laser treatment [16], surface grafting [17] [18], silane modification [19] and chemical etching [20]. The principal advantages of the chemical etching process are its low cost, simplicity and easy application without sophisticated tools. After carrying out the chemical etching, it is possible to produce the micro cavities and then increase the surface roughness. Such a rough surface favors the mechanical interlocking of the electroless deposited copper particles.

The activation step permits to apply an appropriate catalyst on polymer surfaces. These catalysts (activators) which are mainly transition metals [8] [21] [22] [23] [24] initiate the metal deposition. Among the transition metals, palladium is a commonly utilized catalyst for activating the electroless metal plating process [25]. The most common industrial method is the use of SnCl_2 and PdCl_2 solutions or mixed Sn/Pd colloids where the metallic palladium seed is deposited on a polymer surface after reaction with Sn(II). However, the high cost of palladium forces its replacement with cheaper metals. Different processes have been performed for applying these catalysts on the polymer surfaces. But these methods sometimes need several steps [26] [27] [28] [29] [30] [31] and modern set-up. For example, a thin palladium acetate/acetone film was deposited on polyimide surfaces, then illuminated by an UV lamp and irradiated by a laser beam for patterning [27]. Copper was coated on PET films by using a silver mask exposed to oxygen plasma treatment [32]. Byeon et al. [28] have deposited copper on a palladium aerosol activated polymer membrane in the presence of ultrasounds. Zhou et al. [33] have prepared the polymer samples by mixing the polycarbonate (PC) with copper powder. After injection of the mixture as plates, they have activated samples by a 1064 nm laser beam and have deposited the electroless copper on the sample surface. A cheap and simple method to prepare polymer samples by incorporation of a small amount of metal-organic compounds (acetates of palladium, nickel or copper) in LCP Vectra® E820i polymer has been demonstrated [34]. During blending, since polymer was kept at sufficiently high temperature, the acetates were thermally decomposed resulting the metallic particles of Pd, Ni and Cu that are used as catalysts for electroless deposition [34].

The third step is the electroless deposition of copper in a bath containing a salt of copper and a reducing agent. This electroless metallization reaction is spontaneous since Cu^{2+} is reduced to Cu by the reducing agent (frequently formaldehyde, HCHO) on the active sites obtained during the activation step on polymer surfaces. This spontaneous reaction is initiated by the activator that lowers the activation energy for metal plating [35].

Electroless copper deposition on metal-organic compounds (Pd, Ni or Cu acetates) incorporated LCP Vectra® E820i samples has been previously investigated for a fixed composition of metallization bath at 45°C [34]. In this previous work, the electroless copper deposition on 0.15 wt % Pd incorporated LCP Vectra® E820i was more efficient compared to the deposition on 0.4 wt % Ni and 0.4 wt % Cu incorporated LCP Vectra® E820i, even the Pd amount was smaller [34]. In this work, we then studied the influence of bath temperature and bath composition on the most efficient samples *i.e.* palladium acetate incorporated LCP Vectra® E820i in order to optimize the electroless copper deposition process. The incorporated final Pd amount was around 0.15 wt % as measured by Inductively Coupled Plasma Mass Spectrometry (ICP-MS). The metallization bath included commercial ENPLATE LDS Cu100, deionized water and 37% diluted formaldehyde (used as reducing agent) with a typical ratio of 40 mL:160 mL:2 mL, respectively. The influence of composition (formaldehyde concentration) and temperature of the metallization bath on the copper deposition process is studied. The deposited copper amount was measured by weighing samples with a micro balance. The evolution of electroless copper amount and copper deposition rate with time is studied as a function of metallization bath temperature and formaldehyde volume. The size distribution of the electroless deposited copper particles was also studied for different parameters from Scanning Electron Microscope (SEM) images.

EXPERIMENTAL

Materials and sample preparation method have been detailed elsewhere [34]

Materials

LCP Vectra® E820i, a special grade of LCP with 40 % mineral filler is provided from Celanese.

Palladium is purchased from Acros Organics with a purity of 99.9 %.

The conditioner PM-925 from Dow Chemicals was employed for polymer etching. It is an alkaline solution, with a pH around 13 and includes KOH, [34]. The commercial ENPLATE LDS Cu100 product (from Enthone Company) was used for the preparation of the electroless copper metallization bath.

The supplier indicates that this solution contains copper sulfate and sodium hydroxide. It probably also includes ethylenediaminetetraacetic acid (EDTA) as complexing agent in order to avoid the copper precipitation [34].

Sample preparation

The samples were prepared by blending the commercially available LCP Vectra® E820i pellets with acetate of palladium as detailed previously [34]. The initial palladium acetate mass fraction was calculated in a way that the final metal particle amount remains very small. A very small amount of acetate incorporation is preferred, not only for the price of palladium but, particularly, to avoid the drastic modification of some polymer properties (mechanical, electrical, thermal).

The polymer pellets were dried in a furnace at 170°C during 8 hours before blending. The polymer and palladium acetate blend was prepared in a Brabender blender at 360 °C. The acetate of Pd was gradually added into the molten LCP Vectra® E820i previously put in the mixer bowl of 35 cm³ in volume. The torque generated by two rotating blades with adjustable speed was recorded as a function of time during blending and the blades were kept at constant torque for approximately 10 min once the torque was stabilized. Three to four batches yielded enough material to inject a dozen samples. After preparation of blend, the obtained pads were grinded and injected as small rods of 4 mm x 10 mm x 100 mm by using an ARBOURG AllRounder 270S injection mold with a screw of 18 mm in diameter. The typical temperatures during injection molding were 335–350 °C, with the mold temperature set to 80 °C. The injection pressure was 1800 bars with an injection time around 10 seconds.

0.15 wt % Pd incorporated LCP Vectra® E820i samples were prepared and labelled as LCP-0.15 w% Pd. The initial mass of metal-organic compound was calculated in a way that the final mass fraction was 0.15 wt % of Pd.

Palladium acetate was selected in relation with the melting and degradation temperatures of polymer. Precisely, the thermal decomposition temperature of palladium acetate should be higher than the melting temperature of polymer but lower than its degradation temperature. In such a way, palladium acetate can be thermally decomposed into the molten polymer during blending of polymer-acetate mixture. The melting temperature of LCP Vectra® 820i is 335 °C after the technical datasheet of supplier [36]. The decomposition temperature of palladium acetate in air is in the range of 214–276 °C depending on the heating rate as analyzed by TGA [37]. The TGA experiment has been performed in air while in our case the Pd acetate was decomposed in a polymer environment (LCP Vectra® E820i). The environment can modify the decomposition route and the final products. It was supposed that the palladium acetate was decomposed during the blending process yielding some metallic active sites for electroless Cu deposition.

Bath conditions

Three main steps were employed in the electroless copper deposition process: etching, neutralization and metallization. After each main step, an intermediate rinsing bath with deionized water was employed. Deionized water was also used to prepare all the baths.

The PM-925 product was used as a first cleaning/etching step for the surface treatment of LCP Vectra® E820i at 82 °C for 8 min. The etching process improves the mechanical adhesion of deposited copper by increasing the roughness of the polymer surface. The bath was slowly stirred with a polytetrafluoroethylene (PTFE) covered magnetic stirrer. After etching, the samples were rinsed in a deionized water bath at 50 °C followed by another deionized water bath at room temperature.

The neutralization step was performed by dipping the samples during 5 minutes into a neutralization bath including diluted sulfuric acid (5 vol %) and deionized water. The pH of the neutralization bath was 5.5. The aim of this step is to remove the traces of alkaline PM-925 in the first etching step. A fast stirring of the bath is employed. After neutralizing, the samples were rinsed in deionized water and dried by compressed air.

The electroless copper deposition bath was prepared by using ENPLATE LDS Cu100, deionized water and 37 % diluted formaldehyde with appropriate volume proportion. The typical metallization bath volume was around 200 mL including thus 40 mL: 160 mL: 2 mL of ENPLATE LDS Cu100, deionized water and formaldehyde respectively (volume proportion of 20:80:1). The pH of the metallization bath was around 12. The usual bath temperature was 45 °C. Moreover the influence of the bath composition and bath temperature on the electroless copper deposition process was investigated. The formaldehyde proportion was varied from 1 mL to 6 mL (1mL, 1.5 mL, 2mL and 6 mL) while the ENPLATE LDS Cu100 and deionized water amount set fixed (40 mL and 160 mL respectively, i.e. a ratio of 20:80:1 to 20:80:3) in the metallization bath kept at 45 °C. In the case of the fixed metallized bath composition including 40 mL of ENPLATE LDS Cu100, 160 mL of deionized water and 2 mL of formaldehyde (proportion 20:80:1), the metallization of LCP-0.15 wt % Pd samples was studied with different bath temperatures changing from 35 °C to 55 °C (35°C, 40°C, 45°C, 50°C and 55°C) . The metallization bath was not stirred during the metallization process.

During a metallization experiment, the sample was dipped into the metallization bath and was taken off after some metallization time for weighing then put again in the same metallization bath. Since the samples can retain some residue of etching or neutralization bath, which can destroy the subsequently deposited copper layer over time, the samples were thoroughly rinsed in deionized water, dried by compressed air and weighed. The final rinsing and drying steps are necessary in order to have a dry sample before the sample mass gain measurements. The metallization bath was not renewed during a metallization experiment.

Sample characterization

The samples were characterized as discussed elsewhere [34].

The samples were weighed by a Mettler AE166 Delta range microbalance in order to determine the electroless deposited copper amount.

The amount of Pd was around 0.15 wt % in LCP as measured by ICP-MS technique carried out in an external subcontracted laboratory.

A Philips XL30i Scanning Electron Microscope (SEM) was used for the observation of the deposited copper particles on LCP Vectra® E820i sample surfaces.

RESULTS AND DISCUSSION

Some results on the metallization of Pd, Ni and Cu incorporated LCP Vectra® E820i have been presented elsewhere [34]. As said previously, the LCP-0.15 wt % Pd sample was more efficient for electroless copper deposition compared to LCP-0.4 wt % Ni and LCP-0.4 wt % Cu, even though the palladium amount was smaller.

In the present work, we then investigated the influence of the metallization bath temperature and bath composition on the electroless deposition of copper on LCP-0.15 wt % Pd samples for optimizing the electroless process.

Two series of electroless copper deposition experiments were carried out on 0.15 wt % Pd filled LCP Vectra® E820i samples. The first series of metallization was performed in the metallization baths with different temperatures (35°C, 40°C, 45°C, 50°C and 55°C) by keeping the bath in a fixed composition (40 mL of ENPLATE LDS Cu100, 160 mL of deionized water and 2 mL of formaldehyde *i.e.* a proportion 20:80:1). The second series of experiments were realized in a metallization bath with different volumes of formaldehyde (1 mL, 1.5 mL, 2 mL or 6 mL formaldehyde poured in 40 mL of ENPLATE LDS Cu100 and 160 mL of deionized water) by keeping the bath temperature at 45°C.

Electroless copper deposition on LCP-0.15 wt% Pd with different bath temperatures

Figure 1 shows the LCP-0.15wt % Pd samples with different copper deposition temperatures. The deposited copper was at the bottom part of the rod shaped samples.

Figure 1. Copper deposition on LCP-0.15 wt % Pd samples at different bath temperatures (from left to right: 35 °C, 40 °C, 45 °C, 50 °C, 55 °C).

The amount of deposited copper on LCP-0.15wt % Pd samples was plotted as a function of cumulative dipping time into the metallization bath at: 35 °C, 40 °C, 45 °C, 50 °C and 55 °C (Figure 2).

Figure 2. Amount of deposited copper per unit area (mg cm^{-2}) on LCP-0.15 wt % Pd samples as a function of cumulative dipping time into the metallization bath kept at different temperatures: 35 °C, 40 °C, 45 °C, 50 °C and 55 °C.

The deposited Cu amount initially increases with time for all temperatures and arrives rapidly to a plateau for 50 °C and 55 °C on LCP-0.15 wt % Pd samples. The amount of deposited copper at the end of the experiment at 50 °C and 55 °C is relatively low, compared to the deposition at lower temperatures (35 °C, 40 °C and 45 °C). We remind that, for a given temperature, the same metallization bath was used without bath renewing until the end of the experiment. The difference in color of the deposited copper layers in Figure 1 probably originated from the difference in the thickness and the irregularities of the copper layer which reflects the light differently.

At lower temperatures, the initiation of copper deposition was delayed compared to the higher bath temperatures. Nevertheless, the copper quantity was very similar after 60 minutes of deposition at 35 °C, 40 °C and 45 °C, *i.e.* around 2.5 mg cm^{-2} . The reaction continued and the deposited copper amount was even more important after 80 min at 35 °C when compared to 40 °C and 45 °C.

Theoretically a mass gain of 1 mg cm^{-2} corresponds to a copper thickness of $1.12 \text{ }\mu\text{m}$ if the layer is uniform [34]. For the bath temperatures of 35 °C, 40 °C and 45 °C, after 1 hour, the copper layer thickness was around $2.8 \text{ }\mu\text{m}$.

The copper deposition rate calculated from Figure 2 by taking the first derivative of the curves with respect to time, considering a piecewise linear function shown in Figure 3. The deposition rate was not constant. Since the bath was not renewed during an experiment, the available copper ions in the metallization bath decreased due to its continuous consumption in time. The deposition rate curves displayed a maximum at around $50\text{-}70 \text{ }\mu\text{g cm}^{-2} \text{ min}^{-1}$. The maximum rate seemed to shift to longer metallization times when the bath temperature decreased.

In the case of 55 °C, the deposition was very fast and took less than 15 minutes during which we could unfortunately have only very few experimental mass measurement points. This was the reason why the curves for 55 °C was not represented in Figure 3 and Figure 6 as well as its SEM picture in Figure 4.

Figure 3. Rate of electroless Cu deposition on LCP-0.15 wt % Pd for different metallization bath temperatures (35 °C, 40 °C, 45 °C and 50 °C).

The copper layers deposited on LCP-0.15 wt % Pd at constant temperatures (35 °C, 40 °C, 45 °C and 50 °C) were examined by SEM at the end of each experiment (Figure 4). The spherical particles were observed on all the surfaces. The size of copper particles seems to become smaller with increasing bath temperature since the SEM images were taken with the same magnification. As concluded from Figure 2, the higher the bath temperature (in the range of 35 °C-55 °C), the lower the final deposited amount of copper on LCP-0.15 wt % Pd sample surfaces on which the SEM observations were performed.

Figure 4. SEM observation of metallized copper layers on LCP-0.15 wt % Pd at different temperatures of metallization: a) 35 °C, b) 40 °C, c) 45 °C, d) 50 °C.

The diameter of the electroless deposited copper particles seems to obey a Gaussian distribution function as shown in Figure 5 (for example for a bath temperature of 40 °C) while the initial composition of metallization bath was kept constant. On Figure 5, the histogram represents the experimental probability density as a function of measured particle diameter with an interval of 1 μm (0-1 μm , 1-2 μm , etc... with an average value of 0.5 μm , 1.5 μm , etc. respectively). The scattered dots show the probability density against the measured particle diameter plotted by using a Gaussian distribution function and the continuous line is the full theoretical Gaussian function for guidance to the eye.

Figure 5. Probability density versus the diameter of copper particles deposited at 40 °C on LCP-0.15 wt % Pd sample.

In such a way, the copper particle diameter distribution was studied for different metallization bath temperatures (Figure 6) by keeping the initial bath composition constant. It appeared that the mean particle diameter shifted from around 8 μm to 2 μm and the distribution function curves were sharpened (standard deviation was twice at 35 °C compared to 50 °C) with increasing bath temperature. We keep in mind that the initial bath composition was same for each temperature *i.e.* 40 mL of ENPLATE LDS Cu100, 160 mL of deionized water, and 2 mL of formaldehyde with a volume ratio of 20:80:1.

Figure 6. Distribution of copper particle diameter measured on the pictures in Figure 4 for different bath temperatures: 35 °C, 40 °C, 45 °C, and 50 °C on LCP-0.15 wt % Pd.

Electroless copper deposition on LCP-0.15 wt% Pd with different formaldehyde volume in the metallization bath at 45°C

The concentration of formaldehyde in the metallization bath can also affect the copper deposition process on LCP-0.15 wt % Pd. Baths with different initial compositions were prepared while maintaining the metallization bath temperature at 45 °C. The formaldehyde volumes of 1mL, 1.5 mL, 2 mL and 6 mL were poured into baths including 160 mL of deionized water and 40 mL of ENPLATE LDS Cu100, i.e. the ENPLATE LDS Cu100, deionized water and formaldehyde with volume ratios of 20:80:0.5, 20:80:0.75, 20:80:1 and 20:80:3, respectively.

As shown in Figure 7, the LCP-0.15 wt % Pd samples were metallized in these baths having different composition at 45 °C, which was the usually used bath temperature. The color of deposited layers was similar and had a typical metallic copper color.

Figure 7. Electroless copper deposited LCP-0.15 wt % Pd samples with different formaldehyde volume (1 mL, 1.5 mL, 2 mL and 6 mL) in the metallization bath including 160 mL deionized water and 40 mL ENPLATE LDS Cu100. Bath temperature was 45 °C. The pictures were taken at the end of the metallization experiments.

The amount of deposited copper on LCP-0.15 wt % Pd samples was plotted against cumulated dipping time in the metallization bath with different concentrations of formaldehyde. (Figure 8).

Figure 8. Evolution of copper amount deposited on LCP-0.15 wt % Pd with different formaldehyde volumes (1mL, 1.5 mL, 2 mL, 6 mL) in the metallization bath kept at 45 °C.

The copper amount (mg cm^{-2}) increased with cumulated dipping time for all metallization baths, regardless of the bath composition.

In the bath with the highest formaldehyde volume i.e. 6 mL, the reaction seemed to initiate before all baths with lower formaldehyde volumes. After 60 minutes of deposition, the deposited Cu amount was around $2\text{--}2.5 \text{ mg cm}^{-2}$ and similar on all LCP-0.15 wt % Pd samples.

As previously, the copper deposition rate was calculated by taking the first derivative of the curves with respect to time, considering a piecewise linear function and plotted as a function of dipping time for LCP-0.15 wt % Pd samples (Figure 9). We remarked that the bath with the highest volume of formaldehyde (6 mL) has a highest maximum rate and the maximum rate occurs in a shorter metallization time. In the bath with the lowest formaldehyde volume, i.e. 1 mL, the maximum deposition rate was the lowest, lying in a range between $35\text{ to }40 \mu\text{g cm}^{-2} \text{ min}^{-1}$ and seemed to be almost constant after 30-40 min of metallization time.

Figure 9. Rate of electroless Cu deposition on LCP-0.15 wt % Pd for different initial formaldehyde volumes in the metallization bath. The bath temperature was kept at 45 °C.

The SEM observations were performed on copper layers deposited on LCP-0.15 wt % Pd samples in the metallization baths with different formaldehyde volumes (Figure 10).

Figure 10. SEM observations on copper layers deposited on LCP-0.15 wt % Pd samples in the metallization baths with different volumes of formaldehyde: a) 1 mL, b) 1.5 mL, c) 2 mL, d) 6mL. The metallization baths were kept at a temperature of 45 °C.

The copper particle diameter distribution was studied by a Gaussian distribution function for different formaldehyde concentrations in the metallization bath (Figure 11). The mean copper particle diameter shifted to smaller values with increasing formaldehyde volume in the bath. The mean copper particle diameters were around 7 μm and 5 μm in metallization bath with 1 mL and 2 mL of formaldehyde, respectively, and decreased to around 3.9 μm in the bath with 6 mL of HCOH. The standard deviation increased from 0.96 to 1.4 with increasing formaldehyde concentration from 1mL to 6 mL, respectively.

Figure 11. Copper particle size distributions deposited on LCP-0.15 wt % Pd in the baths with different HCHO concentrations (1 mL, 1.5 mL, 2 mL and 6 mL) in a metallization bath kept at 45 °C.

Since the bath temperature and formaldehyde concentration were varied separately by keeping one of them constant, we can estimate the activation energy of electroless copper deposition and the order of reaction with respect to formaldehyde. For electroless copper deposition in the presence of formaldehyde as reducing agent and EDTA as chelating agent, the overall copper deposition reaction takes place [1]:

The rate, r , that determines the kinetics of the electroless copper deposition can be written [38]:

$$r = k[Cu^{2+}]^a [OH^-]^b [HCHO]^c (LIGAND)^d \quad (2)$$

where k is the temperature dependent rate constant and a, b, c, d are the orders of reaction.

For calculating the order of reaction with respect to the formaldehyde, only the formaldehyde concentration was varied (1 mL, 1.5 mL, 2 mL and 6 mL) by keeping all other metallization bath

components (deionized water and ENPLATE LDS Cu100 fixed to 160 mL and 40 mL, respectively) and the bath temperature constant (45 °C).

The copper deposition rate would then be proportional to $[HCHO]^c$ for a given temperature. We can then rewrite the equation (2)

$$r = k' [HCHO]^c \quad (3)$$

where k' is another rate constant including all constants in equation (2).

The plot of $\ln r$ as a function of $\ln[HCHO]$ permitted to estimate the order of the reaction c with respect to formaldehyde for a given amount of deposited copper at 45 °C. The reaction order with respect to formaldehyde was around 0.6 at 0.2 mg cm⁻² of deposited copper and decreased to 0.17 at 0.8 mg cm⁻² (Figure 12).

Figure 12. Evolution of the order of copper deposition reaction with respect to formaldehyde with deposited copper amount at 45 °C on LCP-0.15 wt % Pd.

Our results show that the order decreases from 0.6 to 0.2 with increasing amount of deposited copper from 0.2 mg cm⁻² to 0.8 mg cm⁻². It has been pointed out that the influence of formaldehyde concentration was generally small during steady state (final) deposition i.e. reaction orders less than 0.1, however during initial stages, the reaction was found to be the first order with respect to formaldehyde [38]. The reaction order for formaldehyde has been reported 0.68 during the initial stage to 0 during the final stage [38]. Donahue and Shippey have found around 0.2 as the reaction order for formaldehyde [39]. Our results are in rather good agreement with the results found in the literature [38] [39].

The activation energy for electroless copper deposition was also estimated for different amounts of deposited copper on LCP-0.15 wt % Pd samples, supposing that the rate equation obeys the Arrhenius law *i.e.* $k = Ae^{-E/RT}$ in equation (2) where A is the pre-exponential factor, E is the activation energy, R and T are the universal gas constant and the temperature respectively. In our experiments, the bath temperature was changed from 35 °C to 55 °C and the formaldehyde volume was kept constant at 2 mL in a bath of 160 mL of deionized water and 40 mL of ENPLATE LDC Cu100. The plot of $\ln k$ as a function of $1/T$ permitted to estimate the activation energy for a given amount of electroless deposited copper. The variation of the activation energy with the amount of electroless deposited copper was shown in Figure 13. The activation energy decreased with increasing copper amount: around 45 kJ mol⁻¹ for 0.2 mg cm⁻² and around 26 kJ mol⁻¹ for 0.4 mg cm⁻² of deposited copper.

Figure 13. Activation energy of electroless copper deposition with different amounts of electroless deposited copper on LCP-0.15 wt % Pd. The bath included ENPLATE LDC Cu100, deionized water and formaldehyde with a volume ratio of 20:80:1, respectively.

Several values of activation energy have been found in the literature [38]. Schumacher et al. have calculated an activation energy of 60.9 kJ mol^{-1} [40]. This value was probably at the beginning of the deposition reaction since they have indicated that the reaction with respect to formaldehyde was the first order. For the electroless copper deposition process, an activation energy of 46 kJ mol^{-1} has also been reported by Molenaar et al. [41] in good agreement with our results.

The activation energies of $49\text{--}50 \text{ kJ mol}^{-1}$, 46 kJ mol^{-1} and 24 kJ mol^{-1} for the electroless copper process have been reviewed in the presence of Cu, Ni and Pd catalysts respectively [35].

Nevertheless, the nature of the catalyst is only important until the catalyst is covered by copper.

After the catalyst is covered by copper, the reaction becomes autocatalytic, which means the deposited copper acts as a catalyst for further plating. In theory, there is no limit to the thickness of grown copper layer. In practice, however, side reactions will eventually become dominant, and bath lifetime is finite.

Our preliminary adhesion measurements determined from the pull up test by using a homemade device for sample holding on a tensile test machine resulted the stress values higher than 7 MPa on copper layers deposited during 2 hours on LCP-0.15 wt % Pd. The copper adhesion on LCP depends on the surface roughness [20], [42]. Ge et al. [42] have investigated the electroless copper deposition on the LCP films subjected to different surface treatments and measured a pull strength of around 5-7 MPa for electroless copper layer deposited on untreated and treated LCP surfaces by different processes. Our preliminary adhesion values of electroless deposited copper on LCP-0.15 wt % Pd are relatively high and are in line with those of Ge et al. [42]

CONCLUSIONS

The electroless copper deposition was studied on polymer samples prepared by the incorporation of a very small amount (< 0.5 wt %) of metal-organic compounds (palladium acetate) into the molten LCP Vectra® E820i. During blending, palladium acetate is thermally decomposed leading to the metallic particles on which the electroless deposition of copper is triggered. After blending, the samples are shaped in an injection mold. The samples were then etched in a bath permitting to increase the roughness and improving the mechanical interlocking of the electroless deposited copper particles.

The electroless copper deposition was performed in a bath including a commercial copper salt solution and formaldehyde as reducing agent.

The influence of the metallization bath temperature and bath composition on the electroless copper deposition was studied on LCP-0.15 wt % Pd. For a fixed bath composition, the copper deposition was investigated at the temperature range of 35 °C-55 °C. The formaldehyde concentration was also varied from 1 mL to 6 mL in the metallization baths including 40 mL of ENPLATE LDS100 and 160 mL of distilled water by keeping the bath temperature at 45°C. When the bath composition was kept constant, the deposited copper amount increased with cumulative dipping time into the

metallization bath for all studied temperatures but the final amount was very low at 50 °C and 55 °C when compared to the deposition at 35 °C, 40 °C and 45 °C. The deposition was also delayed at lower temperatures. After one hour of electroless deposition, the deposited copper amount was around 2.5 mg cm⁻² and the maximum deposition rate was around 60 µg cm⁻² min⁻¹ for the deposition temperatures of 35 °C, 40 °C and 45 °C. The diameter of the deposited copper particles follows a Gaussian distribution function. The mean particle size and standard deviation decreased with increasing bath temperature. The influence of the formaldehyde concentration (volume: 1 mL, 1.5 mL, 2 mL and 6 mL in a bath of around 200 mL) was also studied on LCP-0.15 wt % Pd by keeping the bath temperature constant at 45 °C. The deposition starts earlier in the baths with higher concentration of formaldehyde. The electroless deposited copper amount was similar after 60 minutes of deposition for all the baths, having different formaldehyde concentration. The maximum deposition rate was higher and situated at shorter time when the formaldehyde concentration is higher. The electroless deposited copper particles diameter obeys a Gaussian distribution. The mean particle diameter decreases but the standard deviation increases with increasing concentration of formaldehyde in the metallization bath on LCP-0.15 wt % Pd.

The reaction order with respect to formaldehyde was calculated around 0.6 at 0.2 mg cm⁻² of deposited copper and decreased to 0.17 for a deposited copper amount of 0.8 mg cm⁻². The calculated activation energy for electroless copper deposition decreased with increasing deposited copper amount: around 45 kJ mol⁻¹ for 0.2 mg cm⁻² and around 26 kJ mol⁻¹ for 0.4 mg cm⁻² of copper.

In summary, the influence of metallization bath parameters on the electroless copper deposition on LCP-0.15 wt % Pd samples prepared by a simple and cheap method was studied in order to optimize the electroless copper deposition process on polymers. Bath temperature and formaldehyde concentration affect the electroless deposited copper amount, copper deposition rate and the copper particle diameter.

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