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Description of supported metal structure sensitivity by a geometric approach

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Abstract

A series of Pt/Al₂O₃ catalysts with uniform Pt particle sizes ranging from 0.95 to 2.62 nm was synthesized using the refilling method to control the growing of Pt nanoparticles and evaluated in propane dehydrogenation. An effect of particle size on the initial propane activity and TOF was demonstrated, the smallest particles being the most active. A geometric model was developed to quantify the surface site concentration for any fcc metal particle size. Comparing the evolution of initial activity for propane dehydrogenation with the different surface site concentrations, it was shown that the active sites of Pt/Al₂O₃ catalysts corresponded to the combination of corner and edge atoms. To get further, the model was confronted with numerous data extracted from literature demonstrating that it is an efficient tool to predict the structure-activity relationship of fcc metal catalysts and determine the exact nature of active sites for a wide range of reactions and metals.

Keywords: Platinum; Geometric model; Truncated octahedron; Controlled particle size synthesis; Size effect; Propane dehydrogenation; Surface site concentration; Structure-activity relationship; fcc metal.

1. Introduction

Metallic catalysts are of great importance in various fields such as synthesis chemistry, energy production but also environment processes [1, 2, 3, 4]. The most common metals (supported or not) used in heterogeneous catalysis belong to groups 8 to 11 (Fe, Ru, Co, Rh, Ir, Ni, Pd, Pt, Cu, Ag and Au). For decades, the complexity of unsupported metallic catalysts has motivated

fundamental investigations with simple model catalysts. In the 1970's, the works of Somorjai [5] based on the ultrahigh vacuum techniques investigated single crystals of metal determining both the exact surface structures by low energy electron diffraction (LEED) and their compositions by Auger electron spectroscopy (AES). This experimental approach provided impactful determinations of structure–property relationships of metallic catalysts. The results of such investigations showed how catalytic reaction activities vary from one metal crystal face to another [5]. Single crystals models provide incisive information about the effects of surface structure and composition on catalysis, but they provide no information about support effects and only limited, indirect information about supported metal particle size effects (the results are limited by any assumption that variation of crystal face and density of step, edge, kink, terrace, etc. sites accounts for crystallite size effects in supported metals). Single crystals also cannot accurately represent the smallest particles (particles with diameters less than about 1 nm), which may lack metallic character and may have unique structures and resemble molecules rather than two-dimensional extended solids [6].

Because of the limitations of single crystal models, researchers have worked toward simple models of supported metal catalysts.

Size and shape of the metal particles are the main characteristics which influence their electronic properties and so the catalytic activity of these supported nano-objects [7]. These specific properties are generally attributed without distinction to all surface atoms (called active sites) by opposition to bulk atoms of the particles [8]. Theoretical analyzes by Van Hardeveld and Hartog [9] on ideal geometric structures clearly showed the reliance of the fraction of the different types of crystallographic sites (corner, edge, faces) present on the surface with the size of the particles. In the case of ideal structures, the proportion of the atoms constituting the edges and the corners *versus* the quantity of surface atoms becomes larger as the nanocrystals become smaller. The size effects are mainly due to a not insignificant proportion of weakly coordinated sites (such as corner and edge atoms). In an ideal setting, size conditions the nature of the sites on the surface. Therefore, particle size can normally be correlated with catalytic activity.

However, reactions in heterogeneous catalysis can be split into two groups: those that are not sensitive to the size and the shape of the catalyst particles and for which each surface atom of the catalyst is supposed to be equally active; and structure sensitive reactions for which specific size and/or particular shape of metallic particles can greatly enhance the catalytic activity [10].

As far as structure sensitive reactions are concerned, the knowledge of the type of active sites is the key point to design an optimal catalyst for a given reaction. However, the determination of these active sites requires complex and time consuming calculations in order to predict the interaction energies between reactants and metallic surface atoms [11,12]. One reason of this complexity is due to the diverse types of surface metallic atoms differing in coordination number. A considerable simplification, called scaling model [13], allows a quite easily determination of this interaction energy even for complex reactants once the adsorption energy of the considered atom linked to the metal is known.

However, this methodology does not take into account the structure sensitivity and can therefore not well describe the global activity of a real catalyst. Recently, Calle-Valljo et al. [14,15] have gone deeper in the scaling model by integrating the geometry of the active site, which can be simply described by the number of neighbour atoms. These general scaling models thus allow to determine the optimum composition of the catalyst and its surface structure for a given reaction. However, this methodology requires theoretical skills and tools, and thus can only be used by experts in the field.

Development of a simple and affordable methodology allowing to mimic the type(s) of active sites for a given metallic nanoparticle would be a diagnostic tool of great interest for the heterogeneous catalysis community, which would save a tremendous amount of time for the design of catalytic materials.

Depending on the molecules involved in the reaction, dehydrogenation reactions may be either sensitive or insensitive to the structure. Propane dehydrogenation (denoted PDH) on Pt-based catalysts has often been considered as a structure sensitive reaction [16], although this aspect was not really studied. In 2008, Holmen and co-workers reported for the first time a Pt particle size effect for Pt-SBA15 catalysts, those with the smaller metallic particles, around 3 nm diameter, being more active for propane dehydrogenation than those with larger particles of 21 nm diameter, with also an effect on the selectivity to propylene and on coke formation [17]. Thereafter, a more in depth study performed on a series of platinum catalysts supported on hydrotalcites with nearly monodispersed sizes, ranging from 1 to 10 nm, clearly demonstrated, by combining kinetic analysis with density functional theory calculation and isotopic experiments, that Pt catalysts present a strong structure sensitive behavior for PDH reaction [18]. These results were very recently confirmed on a series of more classical Pt/Al₂O₃ catalysts with nanoparticles ranging from atomically dispersed Pt to ca. 12 nm of diameter, by varying

the Pt content from 0.05 to 5 wt.%, and applying thermal treatment for the highest Pt content in order to sinter Pt nanoparticles [19].

In this context, the objective of the present study is to develop an easy tool to determine the active sites for a given structure sensitive reaction using a simple geometric approach. For that purpose, propane dehydrogenation is chosen as test reaction and a series of monometallic Pt/Al₂O₃ catalysts is prepared using a specific preparation technique, the refilling method, developed in our laboratory by Barbier and co-workers many years ago and allowing to easily control the growing of supported metal nanoparticles starting from a parent catalyst [20].

2. Experimental

2.1. Catalyst preparation

2.1.1. Parent catalyst

The parent catalyst (denoted Pt/Al₂O₃(R0)) was prepared by impregnation of a γ -alumina support (GOD200, Axens) with a surface area of 200 m² g⁻¹. First, the support was calcined in flowing air (60 mL min⁻¹), for 4 h at a temperature of 450 °C. Secondly, the support was crushed and sieved to obtain a granulometry between 250 and 100 μ m. Then, the support was wet with an ammonia solution at pH 11 and a solution of diammineplatinum (II) nitrite (Pt(NH₃)₂(NO₂)₂, 1.7 wt.% of Pt, Alfa Aesar) was added in order to obtain a metal loading of 1 wt.%. The suspension was stirred for one night at 150 rpm and water was removed by drying at 110 °C for another night. Then, the catalyst was calcined under air (60 mL min⁻¹) for 4 h at 450 °C, and reduced under H₂ (60 mL min⁻¹) at 650 °C during 4 h. The final powder was sieved between 250 and 100 μ m. A blank alumina support, corresponding to the support submitted to the same treatment as the one used for the preparation of the R0 sample, but without the addition of the platinum salt, was also prepared.

2.1.2. Refilling method

The Pt/Al₂O₃(R_j) catalysts (where j represents the number of refill, j=1, 2 or 3) were prepared by deposition of j Pt layer(s) on the R0 parent catalyst by a surface redox reaction, namely the refilling method.

The Pt/Al₂O₃(R1) catalyst was prepared by the following procedure: a given amount of the Pt/Al₂O₃(R0) catalyst was placed in a reactor, outgassed with N₂ and then reduced under H₂ (60 mL min⁻¹) during 1 h at 450 °C. Then, the catalyst was cooled down to room temperature under

N₂. A volume of water was added to moisten the Pt/Al₂O₃(R0) catalyst. The suspension of Pt/Al₂O₃(R0) catalyst was at first maintained under H₂ flow in order to preadsorb hydrogen on the platinum surface (Eq.1) and then placed under N₂ flow for 15 min to remove dissolved or weakly adsorbed hydrogen in solution and on the catalyst, respectively. Afterwards, a chloroplatinic acid solution was added and let under N₂ flow in contact with the parent catalyst for 1 min (Eq.2). The refilling process based on a redox reaction between the hydrogen atoms adsorbed at the surface of the Pt parent catalyst and the oxidized Pt species in solution can be schematized as the following:



with Pt_S corresponding to surface Pt atoms.

Then the solution was filtered out to obtain the Pt/Al₂O₃(R1) catalyst. This procedure was repeated 3 times, in order to obtain the Pt/Al₂O₃(R2) starting from R1, and then Pt/Al₂O₃(R3) starting from R2. Finally, the Pt/Al₂O₃(Rj) sample was dried at 100 °C for one night under N₂, and then reduced under H₂ (60 mL min⁻¹) during 1 h at 650 °C.

2.2. Catalyst characterizations

2.2.1. Determination of the metal content

Inductively coupled plasma optical emission spectroscopy (ICP-OES) was used for the determination of the actual metal content of each sample. The measurements were performed with a Perkin Elmer Optima 2000DV spectrometer. The samples were previously digested in an acidic mixture of HNO₃ and HCl under microwave heating.

2.2.2. Transmission electron microscopy

Transmission electron microscopy (TEM) analysis was performed with a JEOL 2100 UHR microscope equipped with an energy dispersive X-ray (EDX). Reduced catalysts were suspended in ethanol under sonication for 5 min and loaded on holey carbon film Cu grid (300 mesh). A minimum of four hundred particles was counted to calculate the average particle size (denoted \bar{d}_{TEM}), according to the methodology used in the Ref. [21].

2.2.3. Hydrogen chemisorption

Hydrogen chemisorption measurements were performed at 30 °C using a Micromeritics Autochem 2920II apparatus. The catalyst (0.050–0.100 g) was introduced between two quartz wool balls into a quartz U-shaped tube reactor and reduced for 1 h at 650 °C (5 °C min⁻¹ heating rate) under a flow of hydrogen (30 mL min⁻¹), kept at this temperature for 1 h, then purged with argon (30 mL min⁻¹) at the same temperature for 1 h. The reactor was cooled down under argon to the adsorption temperature, and the measurements were undertaken through pulse injections (0.0551 mL) of 10%H₂/Ar until saturation. Hydrogen consumption was monitored using a thermal conductivity detector (TCD). The particle size (\bar{d}) and the dispersion (D) were determinate with the following equations (see Ref. [22] for more details):

$$\bar{d} \text{ (nm)} = \frac{1}{-0.138 \times \left(\frac{H}{Pt}\right)^5 + 0.794 \times \left(\frac{H}{Pt}\right)^4 - 1.469 \times \left(\frac{H}{Pt}\right)^3 + 0.903 \times \left(\frac{H}{Pt}\right)^2 + 0.703 \times \left(\frac{H}{Pt}\right)} \quad (\text{Eq.3})$$

$$D \text{ (\%)} = -29.230 \times \left(\frac{H}{Pt}\right)^5 + 134.647 \times \left(\frac{H}{Pt}\right)^4 - 201.198 \times \left(\frac{H}{Pt}\right)^3 + 70.105 \times \left(\frac{H}{Pt}\right)^2 + 98.611 \times \left(\frac{H}{Pt}\right) \quad (\text{Eq.4})$$

where H/Pt represents the experimental atomic ratio obtained by chemisorption.

2.3. Catalytic test

Propane dehydrogenation reaction was carried out in a conventional fixed-bed reactor. The mass of sample was adjusted in order to obtain a constant Pt loading in the reactor (0.3 mg). A mass of blank alumina was added to the sample in order to maintain a total mass (catalyst + blank alumina) of 100 mg for each experiment. Then, the mixture was mixed with carborundum (SiC) (total catalytic bed of 3 cm height) and *in situ* prereduced under H₂ (60 mL min⁻¹) at 650 °C for 1 h. After reduction, the reaction gas mixture was introduced at 575 °C at a flowrate of 100 mL min⁻¹. The gas mixture was composed of 50% C₃H₈, 45% N₂ and 5% H₂ corresponding to a molar ratio of 10:9:1. The flowrate at the outlet was measured on line using a Ritter Gas Meter. The outlet gas composition was analyzed by an online Agilent 7820A gas chromatography equipped with an FID and HP-Al₂O₃/KCl capillary column. Propane conversion (X), activity in propane conversion ($A_{C_3H_8}$), propane turn over frequency ($TOF_{C_3H_8}$) and selectivity to each product C_xH_y ($S_{C_xH_y}$) in gas phase were calculated as follows:

$$X \text{ (\%)} = \frac{F_{C_3H_8in} - F_{C_3H_8out}}{F_{C_3H_8in}} \times 100 \quad (\text{Eq.5})$$

$$A_{C_3H_8} \text{ (mol h}^{-1} \text{ g}_{Pt}^{-1}) = \frac{X \times F_{C_3H_8in}}{m_{cata} \times \%Pt} \quad (\text{Eq.6})$$

$$TOF_{C_3H_8} \text{ (s}^{-1}) = \frac{A_{C_3H_8} \times MPt}{D \times 10^{-2} \times 3600} \quad (\text{Eq.7})$$

$$S_{C_xH_y}(\%) = \frac{x \times F_{C_xH_y}}{\sum(x \times F_{C_xH_y})} \times 100 \quad (\text{Eq.8})$$

where $F_{C_3H_8}$ corresponds to the molar flowrate (mol h⁻¹) of propane, and $F_{C_xH_y}$ refers to the molar flow rate (mol h⁻¹) of all the products identified at the outlet (C₃H₆, C₂H₆, C₂H₄ and CH₄); *in* and *out* are associated to the molar flowrate at the inlet and at the outlet, respectively; *x* and *y* are the number of carbon and hydrogen atoms in the molecule, respectively; m_{cata} is the mass (g) of catalyst and % Pt the Pt content (wt.%) in the catalyst; D represents the metal dispersion (%) and M_{Pt} the molar weight of platinum (g mol⁻¹).

3. Results and discussion

3.1. Description of the model and determination of surface site concentration

3.1.1. Relationship between the crystallite shape, the metallic crystallite size and the parameter *m*

As in our last paper based on the same geometric approach [23], the shape of the Pt crystallites was assumed to be a fcc perfect truncated octahedron (denoted TO, see figure in Table 1). The perfect truncated octahedron is the most common shape admitted in the literature for a crystallized fcc structure of metals like Pt [12, 15]. The perfect TO presents 14 faces divided in two types, 8 hexagonal faces with a (111) symmetry and 6 squares with a (100) symmetry. For a given size, the TO is characterized by a parameter *m*. This parameter *m* ($m \geq 2$) is the number of atoms lying on an equivalent edge, corner atoms included, of the chosen crystallite. For example, the value of the parameter *m* for truncated octahedron represented in Table 1 is 3. Knowing the value of the parameter *m*, it is possible to obtain directly the crystallite size (denoted *d* in Table 1), or conversely knowing the value of *d*, it is possible to obtain directly the value of parameter *m* with the equations given in Table 1 [23]. However, these definitions are true only if the studied particle sizes allow to obtain an integer for the *m* parameter. This problem is easily circumvented by using the average particle size (denoted \bar{d}) by assuming that it is a distribution of *k* particles with different sizes (denoted d_k) of m_k integer parameters.

The average particle size is then obtained using the following equation:

$$\bar{d} = 3 \times d_{Pt} \times (\bar{m} - 1) \quad (\text{Eq.9})$$

$$\text{with } \bar{m} = \sum_{k=1}^n (x_k \times m_k)$$

where, \bar{m} and x_k represent the average *m* parameter and the relative number of *k* particles enumerated in the total population.

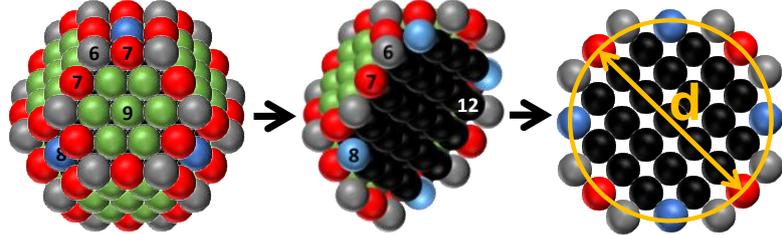
Knowing the value of \bar{d} , it is possible to obtain directly the value of \bar{m} parameter with Eq.10.

$$\bar{m} = \frac{\bar{d}}{3 \times d_{pt}} + 1 \quad (\text{Eq.10})$$

3.1.2. Relationship between the crystallite shape, the atom population and the parameter m

Based on the works of Van Hardeveld and Hartog [9], we developed a simple model to describe the evolution of the surface structure (corners, edges, faces (100) and faces (111)) for unsupported perfect fcc crystallites with the evolution of the crystallite size, as already described in our reference [23]. Each size is characterized by different atom populations: the total number of atoms (denoted N_T), the number of surface atoms (denoted N_S), the number of bulk atoms (denoted N_B) and the number of atoms with i coordination (denoted N_{C_i} and corresponding to the atoms occupying the corners, edges and faces, respectively). The N_T and N_B values are given by third order polynomial in m , whereas N_S is given by a second order polynomial in m . In addition, the N_{C_i} are given by a zero, first or second order polynomial in m . All the N_T , N_S , N_B and N_{C_i} formulas, for the TO, are listed in Table 1.

Table 1. Formulae used to calculate all parameters required to describe the geometrical model based on truncated octahedron ($d_{Pt} = 0.279 \text{ nm}$, $M_{Pt} = 195.08 \text{ g mol}^{-1}$; H: hexagonal and S: square). Illustration: truncated octahedron with parameter $m = 3$; numbers 6 (gray), 7 (red), 8 (blue), 9 (green) and 12 (black) represent the coordination numbers of the atoms located in the corners, edges (100), faces (100), faces (111) and bulk, respectively.



Parameter	Symbol	Formula	Location	Ref.
Particle size (nm)	d	$3 \times d_{Pt} \times (m - 1)$	-	[23]
Parameter m	m	$\frac{d}{3 \times d_{Pt}} + 1$	-	
Total number of atoms	N_T	$16 \times m^3 - 33 \times m^2 + 24 \times m - 6$	-	[9]
Total number of surface atoms	N_S	$30 \times m^2 - 60 \times m + 32$	Surface	
Number of bulk atoms	N_B	$16 \times m^3 - 63 \times m^2 + 84 \times m - 38$	Bulk	
Number of surface atoms	N_{C6}	24	Corner	
	$N_{C7}^{(H-H)}$	$12 \times (m - 2)$	Edge H-H	
	$N_{C7}^{(H-S)}$	$24 \times (m - 2)$	Edge H-S	
	N_{C8}	$6 \times (m - 2)^2$	Face (100)	
	N_{C9}	$8 \times (3 \times m^2 - 9 \times m + 7)$	Face (111)	
Fraction of accessible surface atoms	θ_{C6}	$1 - \frac{SA_{C6}}{4\pi}$	Corner	[24]
	$\theta_{C7}^{(H-H)}$	$1 - \frac{DA_{C7}^{(H-H)}}{2\pi}$	Edge H-H	
	$\theta_{C7}^{(H-S)}$	$1 - \frac{DA_{C7}^{(H-S)}}{2\pi}$	Edge H-S	
	θ_{C8}	$\frac{1}{2}$	Face (100)	
	θ_{C9}	$\frac{1}{2}$	Face (111)	
Solid angle (sr)	SA_{C6}	π	Corner	[23]
Dihedral angle (rad)	$DA_{C7}^{(H-H)}$	$2 \tan^{-1}(\sqrt{2})$	Edge H-H	
Dihedral angle (rad)	$DA_{C7}^{(H-S)}$	$\pi - \tan^{-1}(\sqrt{2})$	Edge H-S	
Number of accessible surface atoms	N_{C6acc}	$N_{C6} \times \theta_{C6}$	Corner	[23]
	$N_{C7acc}^{(H-H)}$	$N_{C7}^{(H-H)} \times \theta_{C7}^{(H-H)}$	Edge H-H	
	$N_{C7acc}^{(H-S)}$	$N_{C7}^{(H-S)} \times \theta_{C7}^{(H-S)}$	Edge H-S	
	N_{C8acc}	$N_{C8} \times \theta_{C8}$	Face (100)	
	N_{C9acc}	$N_{C9} \times \theta_{C9}$	Face (111)	
Accessible surface atom concentration (mol g_{Pt}^{-1})	$[N_{C6acc}]$	$\frac{N_{C6acc}}{N_T \times M_{Pt}}$	Corner	New parameter introduced in this work
	$[N_{C7acc}^{(H-H)}]$	$\frac{N_{C7acc}^{(H-H)}}{N_T \times M_{Pt}}$	Edge H-H	
	$[N_{C7acc}^{(H-S)}]$	$\frac{N_{C7acc}^{(H-S)}}{N_T \times M_{Pt}}$	Edge H-S	
	$[N_{C8acc}]$	$\frac{N_{C8acc}}{N_T \times M_{Pt}}$	Face (100)	
	$[N_{C9acc}]$	$\frac{N_{C9acc}}{N_T \times M_{Pt}}$	Face (111)	

3.1.3. Relationship between the surface site concentration and the crystallite size

For each crystallite size, it is possible to determine the fraction of accessible surface atoms for each i coordination (denoted θ_{Ci} and expressed in fraction of sphere) [24] using the equations listed in Table 1, where SA_{C6} and DA_{C7} represent the solid angle subtended at corner atoms and the dihedral angle corresponding to the intersection between two faces on a given edge, respectively. The solid angle (expressed in steradians) and the dihedral angle (expressed in radians) are obtained from the equations listed in Table 1 [24].

Knowing the values of N_{Ci} and θ_{Ci} , it is possible to calculate the number of accessible surface atoms (denoted N_{Ciacc} in Table 1) and the accessible surface atom concentration (denoted $[N_{Ciacc}]$ in Table 1). The $[N_{Ciacc}]$ values constitute a new parameter in our geometric model approach.

The surface site concentrations (denoted $[site]$, where site = corner, edge, face(100) or face(111)) of one Pt particle with a given m value, can then be obtained using the following equations (Eqs.11-14):

$$[corner] = [N_{C6acc}] \quad (Eq.11)$$

$$[edge] = [N_{C7acc}^{(H-H)}] + [N_{C7acc}^{(H-S)}] \quad (Eq.12)$$

$$[face(100)] = [N_{C8acc}] \quad (Eq.13)$$

$$[face(111)] = [N_{C9acc}] \quad (Eq.14)$$

The evolution of surface site concentrations *versus* particle size is presented in Fig.1. For the smallest Pt particle size ($d = 0.84$ nm), the corner sites are the main sites present on the particle surface ($2428.2 \mu\text{mol } g_{Pt}^{-1}$). As the metal particle size increases, there is an obvious decrease of the concentration of corner sites in favor of the edges, face (100), and face (111) sites. One can see that the edge, face (111), and face (100) site concentrations reach a maximum value (647.1 , 714.1 and $107.9 \mu\text{mol } g_{Pt}^{-1}$, respectively) with Pt particle size equal precisely to 1.39 , 1.69 and 3.04 nm, respectively, whereas the corners concentration monotonously decreases.

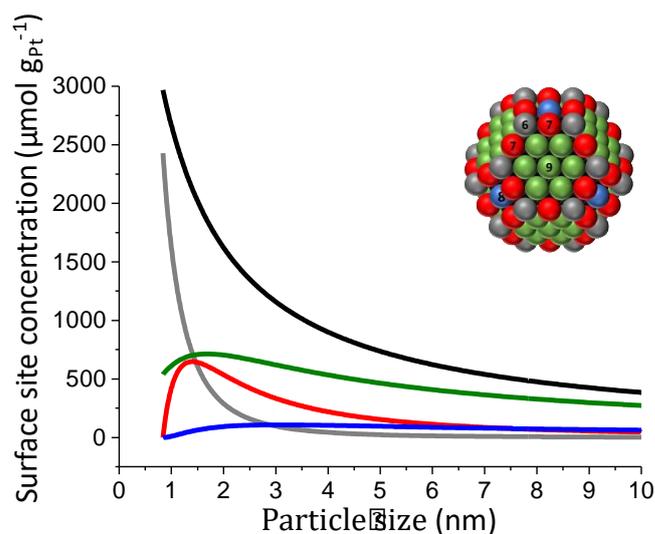


Fig.1. Evolution of the surface site concentration in function of the particle size for a fcc perfect truncated octahedron (black: all sites; grey: corners; red: edges; blue: faces (100) and green: faces (111)).

In terms of metal catalytic activity for a given reaction, it is expected that atoms with low coordination number (6 and 7 for corner and edge, respectively) are the most prone to chemisorb substrates since these atoms tend to complete their coordination to 12. In this sense, the surface site concentration presented in Fig.1 can be seen as a picture of a metallic catalyst activity per gram of metal. To validate this hypothesis, it is necessary to have available catalytic materials with particle size perfectly controlled and to evaluate them catalytically with a structure sensitive reaction, what will be the subject of the following.

3.2. Refilling method

3.2.1. Principle

Catalysts of various particle sizes are of great interest to understand the structure effects on activity, selectivity and deactivation of the metallic particles. Four decades ago, to achieve this purpose, our laboratory developed a preparation process named the refilling method [25]. This method consists in reducing Pt^{n+} ions by hydrogen preadsorbed on the metallic particles of a Pt/Al_2O_3 parent catalyst [20] (see Fig.2).

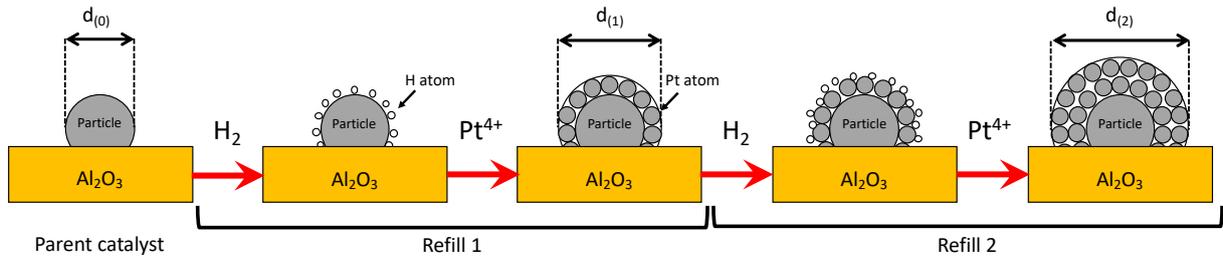


Fig.2. Principle of the refilling method.

By adding the appropriate Pt^{n+} amount (Pt^{4+} in our case), this surface reduction induces a uniform growth of the Pt particles. The expected diameter of these particles can be estimated using the following equation:

$$d_{(j)} = 2 \times j \times d_{Pt} + d_{(0)} \quad (\text{Eq.15})$$

where j and $d_{(0)}$ represent the number of refills ($j = 1, 2$ and 3 in this work) and the parent catalyst particle size, respectively.

Assuming that the shape of the particles is a TO, whatever the particle size, it is possible to calculate the expected amount of Pt^{4+} needed to form a monolayer around the particles of the parent catalyst. This expected amount of Pt^{4+} (denoted $m_{Pt^{4+}(j)}$) and the total expected amount of Pt on the catalyst (denoted $m_{Pt(j)}$) can be calculated using the Eq.16 and Eq.17.

$$m_{Pt^{4+}(j)} = m_{Pt(j-1)} \times \frac{N_{S(j)}}{N_{B(j)}} \quad (\text{Eq.16})$$

$$m_{Pt(j)} = m_{Pt(j-1)} + m_{Pt^{4+}(j)} \quad (\text{Eq.17})$$

where $N_{S(j)}$ and $N_{B(j)}$ represent the total surface atoms number and the bulk atoms number for one particle after the refill j ($N_{S(j)}$ and $N_{B(j)}$ are calculated with the formulae of Table 1 for a given $d_{(j)}$ and $j = 1, 2$ and 3 in this work).

An example of calculation is presented in Table 2.

Table 2. Predicted particle sizes and calculated amounts of Pt and Pt^{4+} for each j refill performed on 0.8 g of parent catalyst 1.07 wt.% Pt/ Al_2O_3 (R0).

Catalyst	j	$d_{(j)}$ (nm)	$\frac{N_{S(j)}}{N_{B(j)}}$	$m_{Pt(j)}$ (g)	$m_{Pt^{4+}(j)}$ (g)
Pt/ Al_2O_3 (R0)	0	0.95	-	$8.56 \cdot 10^{-3}$	-
Pt/ Al_2O_3 (R1)	1	1.51	1.82	$2.41 \cdot 10^{-2}$	$1.56 \cdot 10^{-2}$
Pt/ Al_2O_3 (R2)	2	2.07	1.13	$5.14 \cdot 10^{-2}$	$2.73 \cdot 10^{-2}$
Pt/ Al_2O_3 (R3)	3	2.62	0.82	$9.35 \cdot 10^{-2}$	$4.20 \cdot 10^{-2}$

3.2.2. Characterizations of the catalysts

All the characteristics of the various studied catalyst Pt/Al₂O₃(R_j) are reported in Table 3.

TEM images of selected fresh catalysts (the first and the last of the series) are presented in Fig.3. The measured metal content for Pt/Al₂O₃(R₀) (parent catalyst, 1.07 wt.%) is similar to the targeted one (1 wt.%). The particle size of the Pt/Al₂O₃(R₀) catalyst determined from H₂ chemisorption (0.95 nm) is quite close to the value determined from TEM images (1.30 nm), but lower. The measured metal content for Pt/Al₂O₃(R_j) catalysts (with j = 1, 2 or 3) increases with the j number of refills performed on the parent catalyst. The particle diameters of the refilled catalysts determined from H₂ chemisorption are between 1.44 and 2.62 nm, the value growing with the j number of refills. These results are in perfect agreement with the predicted d_(j) values (Table 2), clearly indicating the selective deposition of Pt allowing the formation of the monolayer.

Table 3. Characteristics of Pt/Al₂O₃(R_j) catalysts.

Catalyst	%Pt ^a (wt.%)	H/Pt ^b	\bar{d}^b (nm)	D ^b (%)	\bar{d}_{TEM} (nm)	\bar{d}_{TEM}^c (nm)
Pt/Al ₂ O ₃ (R ₀)	1.07	1.44	0.95	84.4	1.30	2.96
Pt/Al ₂ O ₃ (R ₁)	2.02	0.84	1.44	68.0	-	-
Pt/Al ₂ O ₃ (R ₂)	3.20	0.59	1.94	55.7	-	-
Pt/Al ₂ O ₃ (R ₃)	4.87	0.44	2.62	44.0	3.06	3.45

^a Pt content determined by ICP-OES, standard deviations lie in the $\pm 2\%$ range.

^b H/Pt ratio, average particle diameter and dispersion D determined by hydrogen chemisorption.

^c Average particle diameter determined by TEM after PDH reaction.

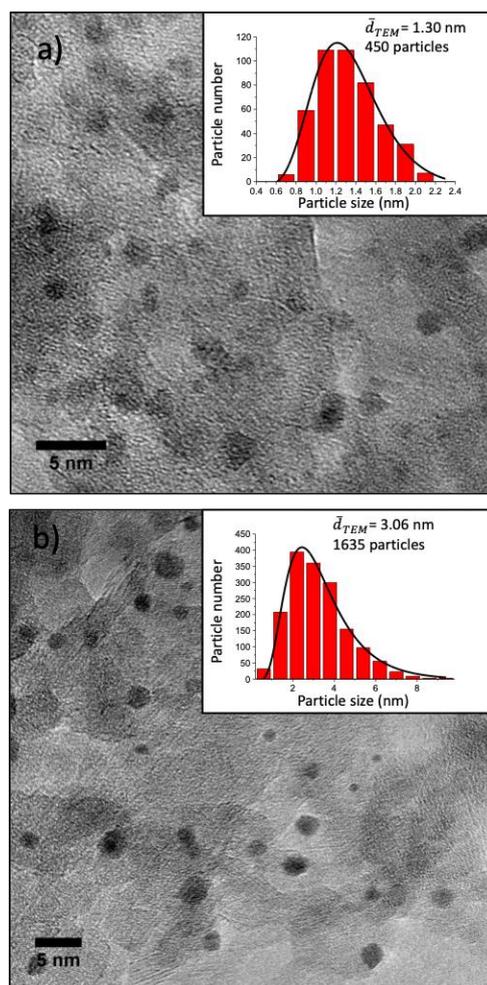


Fig.3. TEM images and particle size distributions of fresh Pt catalysts (a: Pt/Al₂O₃(R0) and b: Pt/Al₂O₃(R3)).

As for the R0 sample, the size determined from H₂ chemisorption for the Pt/Al₂O₃(R3) sample is lower than that determined from the TEM images. This difference can be explained easily taking into account the discrepancy between the geometric model used for the determination of the size from H₂ chemisorption based on the distances between the center of Pt atoms, and the TEM diameter determined at the external surface of the particle. Thus, this difference is constant whatever the particle size and is of the same order as the diameter of one Pt atom as illustrated in Fig.4. Consequently, it is then possible to predict the diameter of the Pt nanoparticles knowing the number of refills, making sure that the particle diameters of the parent catalyst were determined according the same methodology. In the following, the used particle sizes will be those determined from H₂ chemisorption.

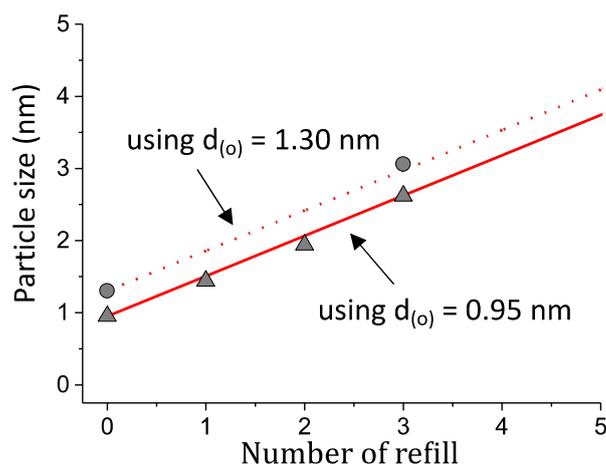


Fig.4. Evolution of the particle size in function of the j number of refill (triangle: size determined from H_2 chemisorption; circle: size determined from TEM; red line: predicted particle size with $d_{(0)} = 0.95$ nm; red dotted line: predicted particle size with $d_{(0)} = 1.30$ nm).

3.3. Effect of the platinum particle size on the propane dehydrogenation

The series of catalysts was evaluated in propane dehydrogenation at 575 °C. The activity as a function of time on stream, the initial TOF and the C_3H_6 selectivity as function of the particle size are presented in Fig.5.

Fig.5a shows the initial C_3H_8 activity decreases with the increase of particle size (139.2, 73.6, 41.8 and 26.0 mol h^{-1} g_{Pt}^{-1} for 0.95, 1.44, 1.94 and 2.62 nm, respectively), in accordance with the results of [17]. One can note that, for all the Pt catalysts, a deactivation is observed as a function of time on stream, characterized by a decrease of the C_3H_8 activity until a plateau, more severe on smaller particles (the same trend is observed for the conversion of propane, see Fig.S.1. in Supporting Information). The difference between the initial C_3H_8 activity and the plateau C_3H_8 activity (denoted $\Delta A_{C_3H_8}$) can be seen as a picture of the catalyst deactivation (see inserted figure in Fig.5a). $\Delta A_{C_3H_8}$ increases with the decrease of the particle size, indicating a coke deposit preferentially occurring on the corner and/or edge metal atoms [18], and/or a phenomenon of sintering on the smallest particles. TEM images of catalysts after PDH reaction are presented in Fig.S.2 (in Supporting Information). The values of particle size determined by TEM (listed in Table 3) show a sintering of the metal particles from 1.30 to 2.96 nm and 3.06 to 3.45 for the Pt/ Al_2O_3 (R0) and Pt/ Al_2O_3 (R3) samples, respectively, indicating the existence of a sintering preferentially more pronounced on the smallest particles. TEM and EDX analyses confirmed also the presence of carbon on the used catalysts.

In order to study the effect of particle size on PDH reactivity, it is absolutely necessary to get rid of the deactivation phenomenon (coke deposit and/or sintering), which would lead to errors of interpretation, and use the reactivity data referring exclusively to the initial time.

Fig.5b shows the initial $TOF_{C_3H_8}$ values and the initial C_3H_6 selectivity (denoted $S_{C_3H_6}$) obtained with the different catalysts. The initial $TOF_{C_3H_8}$ decreases with the increase of particle size (8.93, 5.86, 4.07 and 3.21 s^{-1} for 0.95, 1.44, 1.94 and 2.62 nm, respectively), indicating clearly that propane dehydrogenation is a structure sensitive reaction. However, no change in propylene selectivity (around 93-95 %) as a function of particle size is observed, unlike Zhu *et al.* results [18]. DFT results of Zhu *et al.* [18] shown that Pt particles of small sizes, with (211) dominating on the surface, have a lower dehydrogenation energy barrier and thus lead to higher activity than (111) and (100) surfaces. However, these authors observed higher selectivity toward propylene for large Pt clusters, for which the Pt(111) dominating results in a weakened binding strength of propylene and an increased energy barrier for the activation of C-H bonds, then lowering the possibility of deep dehydrogenation of propylene.

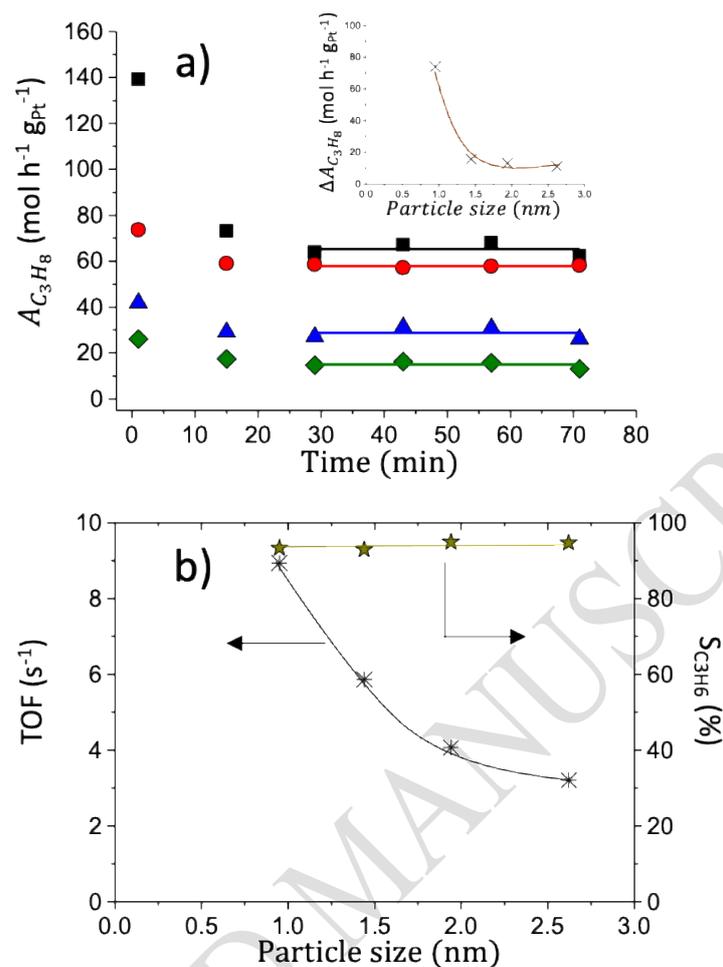


Fig.5. a): Evolution of the activity in function of the time on stream (square: Pt/Al₂O₃(R0); circle: Pt/Al₂O₃(R1); triangle: Pt/Al₂O₃(R2); lozenge: Pt/Al₂O₃(R3)); b) Evolution of the initial TOF and initial propene selectivity in function of the particle size.

3.4. Relationship between activity and surface site concentration

Activity of heterogeneous catalysts depends on the amounts of chemisorbed molecules, which themselves depend on the amount of surface sites. In this sense, the surface site concentrations presented in Fig.1 can be seen as a picture of a metallic catalyst activity per gram of Pt. As demonstrated by Calle-Vallejo *et al.* [14,15], all the energy considerations (adsorption, activation...) are intrinsically linked to the nature of the considered metal but also to the geometry of the active site. Assuming that the chosen surface sites have the same energetics for adsorption (whatever the metal particle size), and the adsorbed molecules do not interact with each other, the activity can then be expressed as a function of the surface site concentration (Eq.18).

$$A_{C_3H_8} = f([site]) \quad (\text{Eq.18})$$

To validate this hypothesis, we compared the evolution of the normalized initial activity (denoted $A_{C_3H_8}^{norm}$, determined with the Eq.19) with the normalized surface site concentration (denoted $[site]^{norm}$, determined with the Eq.20) in function of the particle size.

$$A_{C_3H_8}^{norm} = \frac{A_{C_3H_8}}{A_{C_3H_8}^{ref}} \quad (\text{Eq.19})$$

$$[site]^{norm} = \frac{[site]}{[site]^{ref}} \quad (\text{Eq.20})$$

where $A_{C_3H_8}^{ref}$ represents the reference activity corresponding to the one of the parent catalyst (in our case $139.2 \text{ mol h}^{-1} \text{ g}_{Pt}^{-1}$ for Pt/Al₂O₃(R0)), and $[site]^{ref}$ corresponds to the reference surface site concentrations associated to the particle size of the R0 sample, *i.e.* $\bar{d} = 0.95 \text{ nm}$ (see the highlighted values in Table 4 gathering the surface site concentrations calculated in function of the particle diameter).

Table 4. Surface site concentrations as function of the particle size and normalized values calculated for this study (using as reference the values highlighted in gray attributed to the parent R0 catalyst).

\bar{d} (nm)	Surface site concentration ($\mu\text{mol g}_{Pt}^{-1}$)							Normalized surface site concentration						
	Corner + Edge + Faces	Corner	Edge	Face (100)	Face (111)	Corner + Edge	Face (100) + Face (111)	Corner + Edge + Faces	Corner	Edge	Face (100)	Face (111)	Corner + Edge	Face (100) + Face (111)
0.84	2967.7	2428.2	0.0	0.0	539.6	2428.2	539.6	1.08	1.33	0.00	0.00	0.91	1.13	0.90
0.85	2941.5	2346.6	48.6	0.1	546.2	2395.2	546.2	1.07	1.29	0.15	0.02	0.92	1.11	0.91
0.86	2921.6	2286.4	83.8	0.3	551.1	2370.2	551.4	1.06	1.25	0.25	0.05	0.93	1.10	0.92
0.87	2901.9	2228.2	117.1	0.6	556.0	2345.3	556.6	1.05	1.22	0.36	0.11	0.94	1.09	0.93
0.88	2882.5	2171.9	148.8	1.0	560.8	2320.7	561.8	1.05	1.19	0.45	0.18	0.95	1.08	0.94
0.89	2863.2	2117.5	178.8	1.4	565.6	2296.2	567.0	1.04	1.16	0.54	0.25	0.95	1.07	0.95
0.90	2844.3	2064.8	207.2	1.9	570.3	2272.1	572.2	1.03	1.13	0.63	0.35	0.96	1.05	0.96
0.91	2825.5	2013.9	234.2	2.6	574.8	2248.1	577.4	1.03	1.10	0.71	0.47	0.97	1.04	0.97
0.92	2807.0	1964.7	259.8	3.2	579.4	2224.4	582.6	1.02	1.08	0.79	0.58	0.98	1.03	0.97
0.93	2788.7	1917.0	284.0	3.9	583.8	2201.0	587.7	1.01	1.05	0.86	0.71	0.99	1.02	0.98
0.94	2770.6	1870.8	307.0	4.7	588.1	2177.8	592.8	1.01	1.02	0.93	0.85	0.99	1.01	0.99
0.95	2752.7	1826.1	328.7	5.5	592.3	2154.8	597.9	1.00	1.00	1.00	1.00	1.00	1.00	1.00
0.96	2735.0	1782.8	349.3	6.4	596.5	2132.1	602.9	0.99	0.98	1.06	1.16	1.01	0.99	1.01
0.97	2717.6	1740.9	368.8	7.3	600.6	2109.7	607.9	0.99	0.95	1.12	1.33	1.01	0.98	1.02
0.98	2700.3	1700.2	387.3	8.3	604.6	2087.5	612.8	0.98	0.93	1.18	1.51	1.02	0.97	1.02
0.99	2683.3	1660.8	404.8	9.2	608.5	2065.6	617.7	0.97	0.91	1.23	1.67	1.03	0.96	1.03
1.00	2666.4	1622.6	421.3	10.3	612.3	2043.9	622.5	0.97	0.89	1.28	1.87	1.03	0.95	1.04
1.20	2366.5	1053.5	609.2	33.0	670.8	1662.7	703.8	0.86	0.58	1.85	6.00	1.13	0.77	1.18
1.40	2124.7	721.6	647.1	54.4	701.6	1368.7	756.0	0.77	0.40	1.97	9.89	1.18	0.64	1.26
1.60	1926.3	515.3	626.4	71.4	713.2	1141.7	784.6	0.70	0.28	1.91	12.98	1.20	0.53	1.31
1.80	1761.0	380.6	583.9	84.0	712.5	964.6	796.4	0.64	0.21	1.78	15.27	1.20	0.45	1.33
2.00	1621.3	289.0	535.4	93.0	703.9	824.4	796.9	0.59	0.16	1.63	16.91	1.19	0.38	1.33
2.20	1501.9	224.5	487.5	99.2	690.6	712.0	789.8	0.55	0.12	1.48	18.04	1.17	0.33	1.32
2.40	1398.6	177.9	442.9	103.4	674.5	620.8	777.9	0.51	0.10	1.35	18.80	1.14	0.29	1.30
2.60	1308.5	143.3	402.4	106.0	656.8	545.7	762.8	0.48	0.08	1.22	19.27	1.11	0.25	1.28
2.80	1229.2	117.1	366.2	107.4	638.5	483.3	745.9	0.45	0.06	1.11	19.53	1.08	0.22	1.25
3.00	1158.9	96.9	334.0	107.9	620.1	430.9	728.0	0.42	0.05	1.02	19.62	1.05	0.20	1.22
4.00	900.7	43.6	219.4	103.7	534.0	263.0	637.7	0.33	0.02	0.67	18.85	0.90	0.12	1.07
5.00	736.3	23.2	153.6	95.5	464.0	176.8	559.5	0.27	0.01	0.47	17.36	0.78	0.08	0.94
6.00	622.6	13.8	113.1	87.2	408.5	126.9	495.7	0.23	0.01	0.34	15.85	0.69	0.06	0.83
7.00	539.3	8.8	86.6	79.7	364.1	95.4	443.8	0.20	0.00	0.26	14.49	0.61	0.04	0.74
8.00	475.6	6.0	68.4	73.1	328.1	74.4	401.2	0.17	0.00	0.21	13.29	0.55	0.03	0.67
9.00	425.3	4.3	55.3	67.4	298.3	59.6	365.8	0.15	0.00	0.17	12.25	0.50	0.03	0.61
10.00	384.7	3.1	45.7	62.5	273.4	48.8	335.9	0.14	0.00	0.14	11.36	0.46	0.02	0.56

The evolutions of normalized activity and normalized surface site concentrations (all sites (Fig.6a), corner (Fig.6b), edge (Fig.6c), face (100) (Fig.6d), face (111) (Fig.6e), corner + edge (Fig.6f) and all faces (Fig.6g)) *versus* the particle size are presented in Fig.6. The best correlation between the experimental values of PDH activity and the surface site concentration predicted by the model is obtained for the [corner + edge] concentration (Fig.6f). The evolution of initial propane activity obtained with the four studied catalysts scales linearly with the [corner + edge] surface site concentrations, with an interception to zero (see Fig.6h). This result clearly evidences that the initial activity for PDH reaction is directly correlated with the quantity of corner + edge sites. The findings deduced from our approach based on a geometric model is in perfect accordance with the DFT results of Zhu *et al.* [18] which demonstrated that the catalyst with a higher fraction of Pt(211) on the surface (associated to corner + edge) would give rise to a lower dehydrogenation activation energy and thus to a higher activity.

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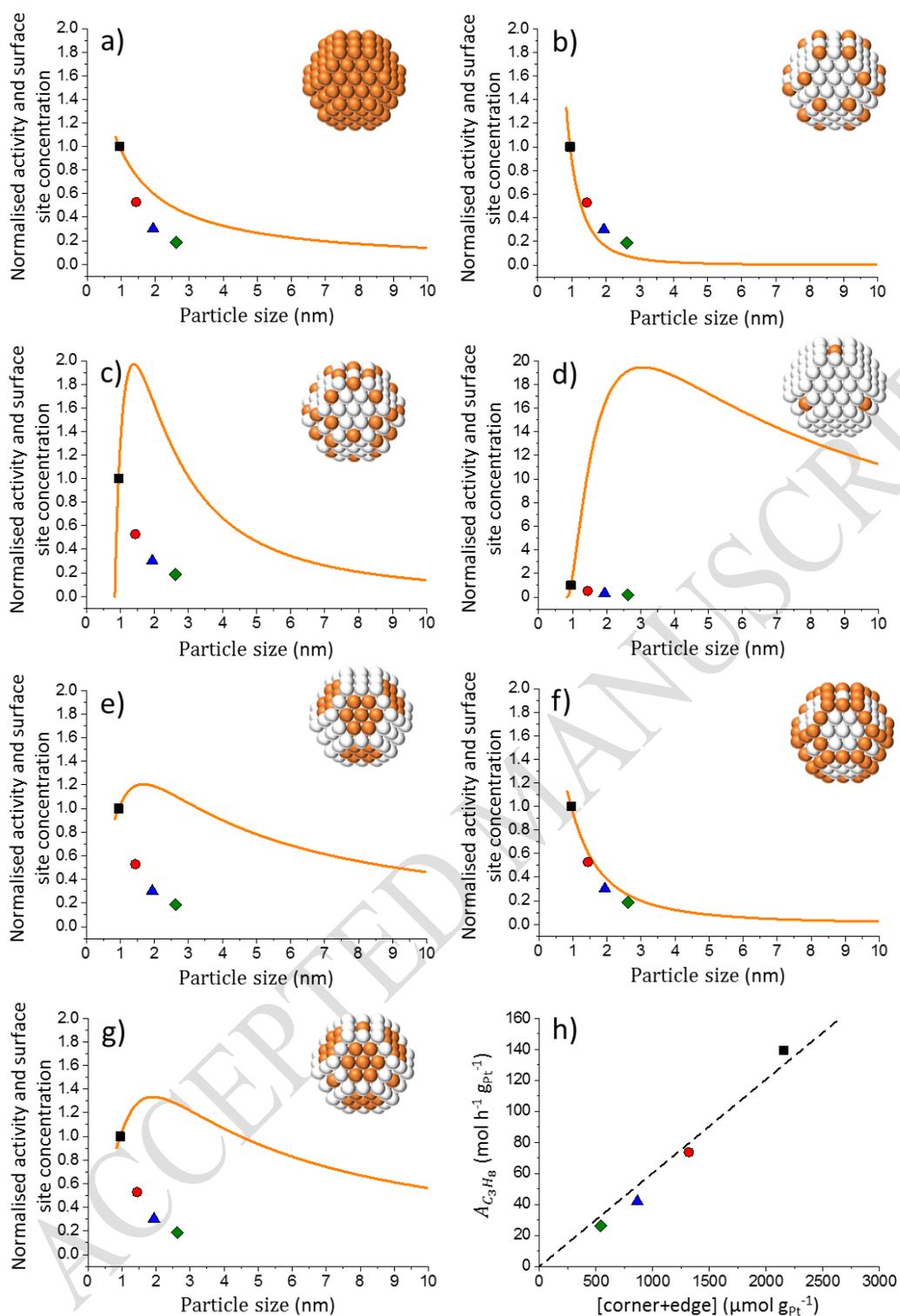


Fig.6. Evolution of the normalized activity for PDH (symbols) and normalized surface site concentrations (orange curves) versus the particle size: a) all sites; b) corner; c) edge; d) face (100); e) face (111); f) corner + edge and g) all faces; h) Evolution of the initial activity versus corner + edge surface site concentration. Square: Pt/Al₂O₃(R0) used as reference; circle: Pt/Al₂O₃(R1); triangle: Pt/Al₂O₃(R2); lozenge: Pt/Al₂O₃(R3)). Orange curves: results predicted with the model by using the particle size value of Pt/Al₂O₃(R0) ($\bar{d} = 0.95$ nm) for the normalization.

In order to validate the present geometric approach on other fcc metals and/or other reactions, it is necessary to find studies of the literature giving us access to values of catalytic activity, particle size and precise knowledge of the nature of the active sites for structure-sensitive reactions. So, we extracted numerous data from literature [21,26,27,28], listed in Table S.1 (in Supporting Information), and confronted them with the values determined from our model. Figs.S.3-6 displayed the normalized catalytic activities calculated from these data as function of the particle sizes for the four following respective reactions: ethane hydrogenolysis over Pt/SBA-15, water gas shift (denoted WGS) over Au/Al₂O₃, methane steam reforming (denoted MSR) over Rh/ZrO₂, and ethanol steam reforming (denoted ESR) over Co/C. For all reactions, the normalized activity decreases with the increase of particle size. Theoretical calculations by DFT over Pt(211) and Pt(111) surfaces supported the observed structure sensitivity for ethane hydrogenolysis on Pt catalysts, since the results of Watwe *et al.* [29] suggested that the active sites are defect sites such as the step edge of Pt(211). In the case of the WGS reaction, DFT calculations performed by Shekhar *et al.* [26] suggested that both corner and low-coordinated perimeter (atoms in contact with the support) sites are active sites on an Au/Al₂O₃ catalyst. The DFT results of Zhao *et al.* [30] obtained on Au/MgO catalysts clearly showed the critical role played by the metal/oxide interface in WGS catalysis (the effect of the support is not taken into account in our model). These authors observed that corner sites were at least of similar activity to the perimeter sites. For the MSR reaction over Rh/ZrO₂, Jones *et al.* [27] proposed, according to their DFT theoretical results, that the reactivity is dominated by steps and corners of the Rh particle. Finally, da Silva *et al.* [28] proposed, with the help of geometric model, that the effect of the cobalt particle size in the ESR reaction was attributed to the increasing fraction of edge and corner surface sites with decreasing size. For the four involved reactions, the evolution of the normalized surface site concentration displaying the best agreement with the normalized activity was gathered in Fig.7. Results clearly show that our geometric model accurately predicts the structure-sensitive dependence determined by theoretical approaches in each case, *i.e.* an activity directly proportional to the concentration of (i) edges for ethane hydrogenolysis on Pt catalysts as in ref [29] (Fig.7a), (ii) corners for WGS reaction on Au catalysts as in ref [26], (iii) corners + edges for MSR on Rh catalysts as in ref [27], (iv) edges for ESR on Co catalysts. In this last case, the correlation with the concentration of edge sites appears more favorable than the one with the corner + edge sites (Fig.S.6c compared to Fig.S.6f, R² correlation

coefficient equal to 0.9668 *versus* 0.9571, respectively). Nevertheless, the theoretical results obtained in ref [28] aren't challenged for all that.

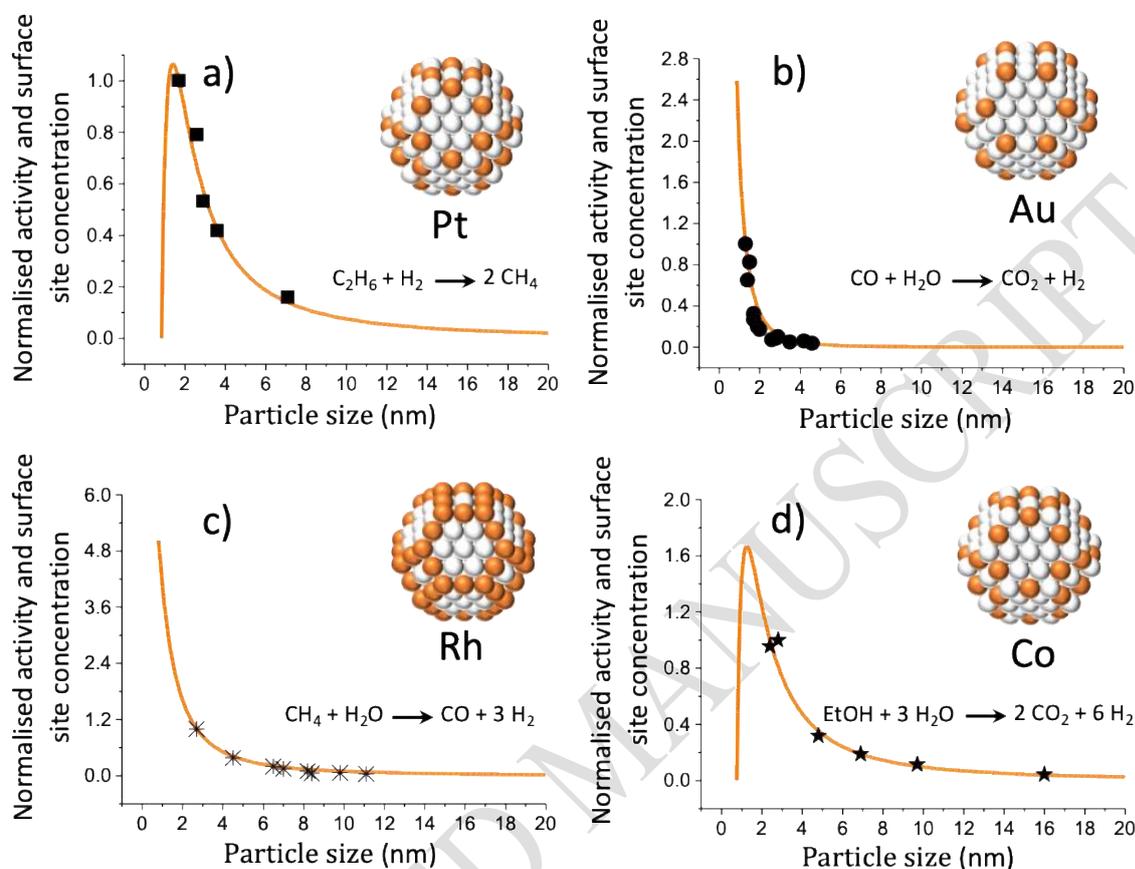


Fig.7. Evolution of the normalized activities calculated from literature data (square, circle, cross, star) and normalized surface site concentrations (orange curves) *versus* the particle size for: a) ethane hydrogenolysis on Pt/SBA-15 [21]; b) water gas shift on Au/Al₂O₃ [26]; c) methane steam reforming on Rh/ZrO₂ [27] and d) ethanol steam reforming on Co/C [28]. Orange curves: results predicted with the model by using the following particle size values for the normalization: $\bar{d} = 1.7$ nm for Pt/SBA-15, $\bar{d} = 1.3$ nm for Au/Al₂O₃, $\bar{d} = 2.7$ nm for Rh/ZrO₂ and $\bar{d} = 2.4$ nm for Co/C (with $d_{Pt} = 0.279$ nm, $M_{Pt} = 195.08$ g mol⁻¹, $d_{Au} = 0.288$ nm, $M_{Au} = 196.97$ g mol⁻¹, $d_{Rh} = 0.269$ nm, $M_{Rh} = 102.91$ g mol⁻¹, $d_{Co} = 0.250$ nm and $M_{Co} = 58.933$ g mol⁻¹).

4. Conclusion

To explain the particle size effect on metal catalyzed reaction, a geometric model (based on truncated octahedron shape) was developed to allow the quantification of surface site concentrations (corner, edge, face (100) and face (111)) for any fcc metal particle size. In the case of Pt, the model predicted that the effect of the particle size on the surface site concentration distribution was the most significant for particle sizes lower than 3.04 nm.

In order to validate the geometric model, a series of Pt/Al₂O₃ catalysts was prepared using a specific preparation technique, the refilling method, developed in our laboratory since 1978,

and allowing to easily and precisely control the growing of supported metal nanoparticles starting from a parent catalyst. The propane dehydrogenation activity was investigated on this Pt/Al₂O₃ catalysts series, with sizes ranging from 0.95 to 2.62 nm. The catalytic experiments showed that the initial activity and the initial $TOF_{C_3H_8}$ decreased with the increase of particle size, indicating that propane dehydrogenation is a structure sensitive reaction. Comparing the evolution of the normalized initial activity with the different normalized surface site concentrations (calculated from the geometric model), it was shown that the active sites corresponded to the combination of corner and edge Pt atoms (in accordance with the DFT results of Zhu *et al.* [18]). Moreover, the model has subsequently been confronted with numerous data extracted from literature (involving different fcc metal and reactions) and it has accurately predicted the structure-sensitive dependence and the nature of active sites determined by DFT approaches.

To conclude, the developed model based on surface site concentration is a powerful predictive tool for understanding the structure-activity relationship of fcc metal catalysts.

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Supporting Information

Description of supported metal structure sensitivity by a geometric approach

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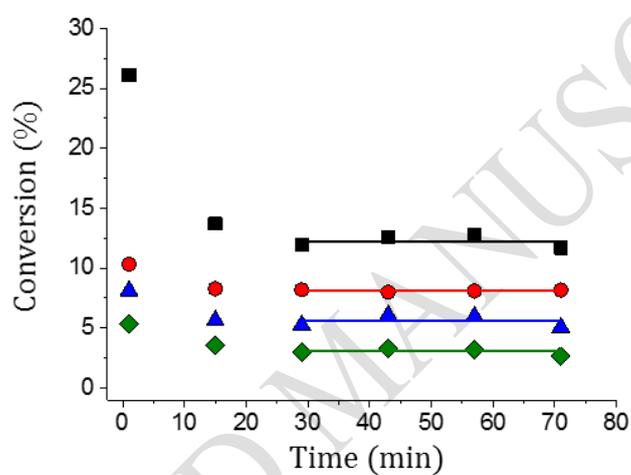


Fig.S.1. Evolution of the propane conversion in function of the time of stream (square: Pt/Al₂O₃(R0); circle: Pt/Al₂O₃(R1); triangle: Pt/Al₂O₃(R2); lozenge: Pt/Al₂O₃(R3)).

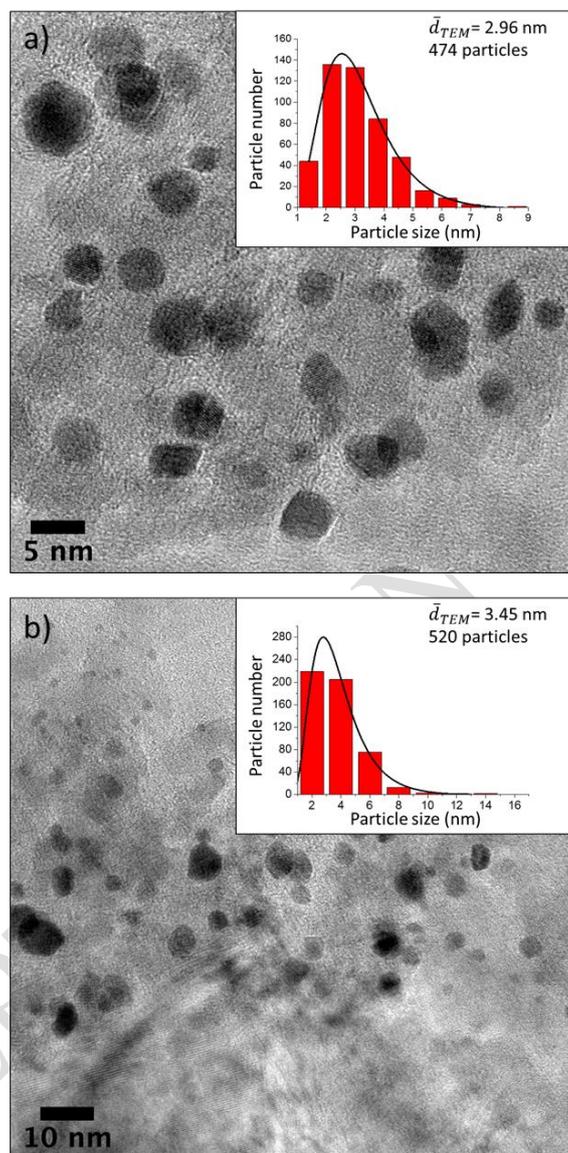


Fig.S.2. TEM images and particle size distributions of Pt catalysts after PDH reaction (a: Pt/Al₂O₃(R0) and b: Pt/Al₂O₃(R3)).

Table S.1. Literature data used to calculate normalized activities according to the geometric model described in the present work (values highlighted in gray represent reference values used for the model, *i.e.* the particle size and activity of the reference catalyst for each series).

Catalyst			Characterization		Activity in Ref.				Reaction	Ref.	Calculated data in this work	
M	support	%wt	\bar{d} (nm)	D (%)	TOF (s ⁻¹)	Activity ($\mu\text{mol g}^{-1} \text{s}^{-1}$)	Activity ($\text{mol mol}_M^{-1} \text{s}^{-1}$)	Activity ($\text{mol g}_M^{-1} \text{s}^{-1}$)			Activity ($\text{mmol g}_M^{-1} \text{s}^{-1}$)	Normalised activity
Pt	SBA-15	0.73	1.7	-	-	0.159	-	-	Ethane hydrogenolysis	[1]	0.022	1.00
		0.90	2.6	-	-	0.155	-	-			0.017	0.79
		0.95	2.9	-	-	0.110	-	-			0.012	0.53
		1.0	3.6	-	-	0.091	-	-			0.009	0.42
		1.01	7.1	-	-	0.035	-	-			0.003	0.16
Au	Al ₂ O ₃	0.7	1.3	-	-	-	17.0 X 10 ⁻³	-	Water gas shift	[2]	8.6 X 10 ⁻⁵	1.00
		0.7	1.5	-	-	-	14.0 X 10 ⁻³	-			7.1 X 10 ⁻⁵	0.82
		0.7	1.4	-	-	-	11.0 X 10 ⁻³	-			5.6 X 10 ⁻⁵	0.65
		0.7	1.9	-	-	-	3.3 X 10 ⁻³	-			1.7 X 10 ⁻⁵	0.19
		0.7	2.9	-	-	-	1.7 X 10 ⁻³	-			0.9 X 10 ⁻⁵	0.10
		0.7	4.2	-	-	-	1.0 X 10 ⁻³	-			0.5 X 10 ⁻⁵	0.06
		1.4	1.7	-	-	-	5.5 X 10 ⁻³	-			2.8 X 10 ⁻⁵	0.32
		1.4	1.7	-	-	-	4.5 X 10 ⁻³	-			2.3 X 10 ⁻⁵	0.26
		1.3	2	-	-	-	2.9 X 10 ⁻³	-			1.5 X 10 ⁻⁵	0.17
		1.4	2.6	-	-	-	1.2 X 10 ⁻³	-			0.6 X 10 ⁻⁵	0.07
		1.4	2.8	-	-	-	1.4 X 10 ⁻³	-			0.7 X 10 ⁻⁵	0.08
		1.4	3.5	-	-	-	0.8 X 10 ⁻³	-			0.4 X 10 ⁻⁵	0.05
1.4	4.6	-	-	-	0.6 X 10 ⁻³	-	0.3 X 10 ⁻⁵	0.04				
Rh	ZrO ₂	1	2.7	32.3	12.5	-	-	-	Methane steam reforming	[3]	39.2	1.00
		1	8.4	10.6	1.8	-	-	-			1.9	0.05
		5	4.5	21	7.4	-	-	-			15.1	0.38
		5	8.2	11	3.6	-	-	-			3.8	0.10
		5	6.5	12.7	6.2	-	-	-			7.7	0.20
		5	7	12.8	4.7	-	-	-			5.8	0.15
		5	9.8	9.5	2.5	-	-	-			2.3	0.06
		5	11.1	7.6	2	-	-	-			1.5	0.04
Co	Carbon nanofibers	1	2.4	-	-	-	-	66 X 10 ⁻³	Ethanol steam reforming	[4]	66	1.00
		0.9	2.8	-	-	-	-	69 X 10 ⁻³			69	1.05
		3.5	4.8	-	-	-	-	22 X 10 ⁻³			22	0.33
		6.0	6.9	-	-	-	-	13 X 10 ⁻³			13	0.20
		9.7	9.7	-	-	-	-	8 X 10 ⁻³			8	0.12
		22	16	-	-	-	-	3 X 10 ⁻³			3	0.05

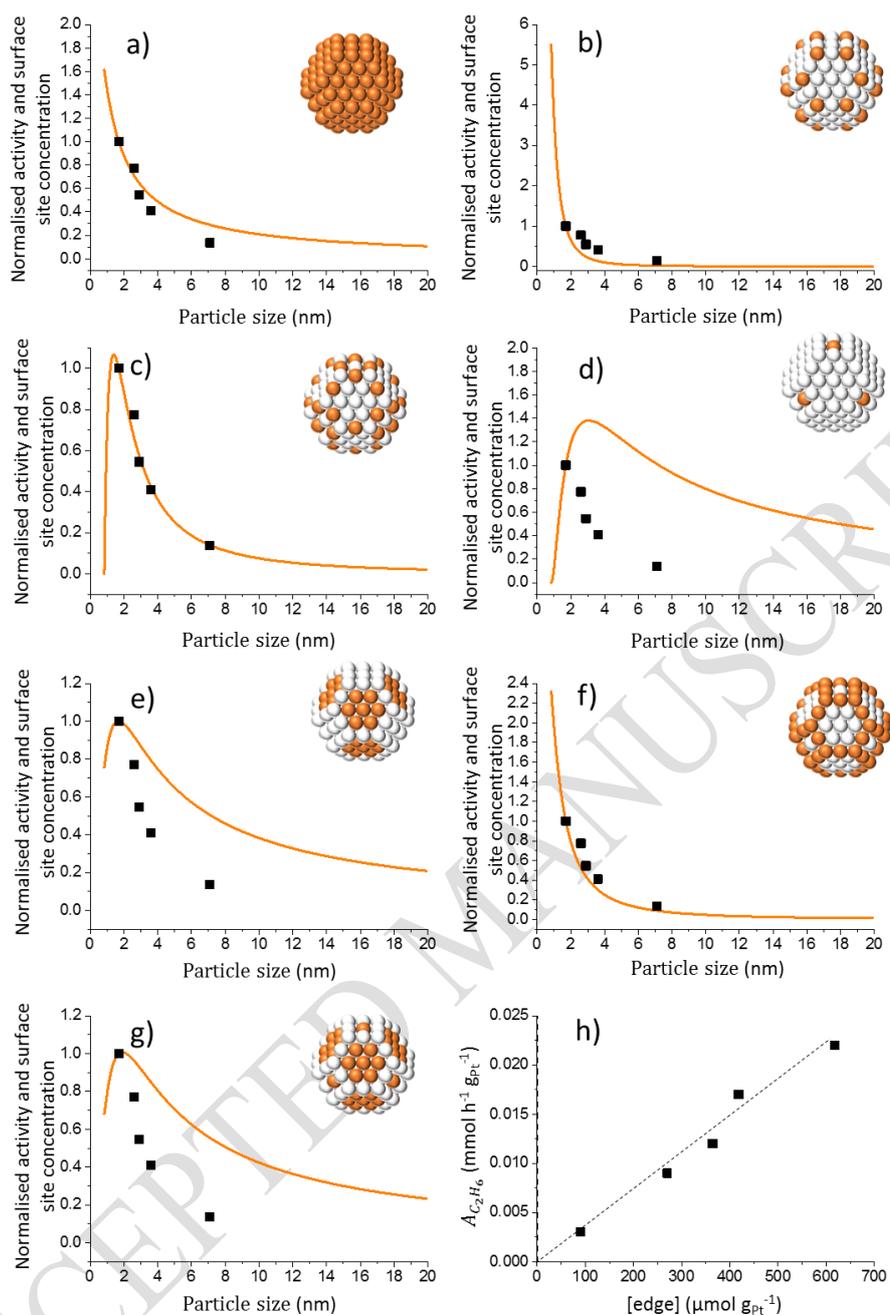


Fig.S.3. Evolution of the normalized ethane hydrogenolysis activity of Pt/SBA-15 catalysts (square, [1]) and normalized surface site concentrations (orange curves) versus the particle size: a) all sites; b) corner; c) edge; d) face (100); e) face (111); f) corner + edge and g) all faces; h) Evolution of the activity versus edge surface site concentration. Orange curves: results predicted with the model by using the particle size value $\bar{d} = 1.7$ nm for the normalization (with $d_{Pt} = 0.279$ nm, $M_{Pt} = 195.08$ g mol⁻¹).

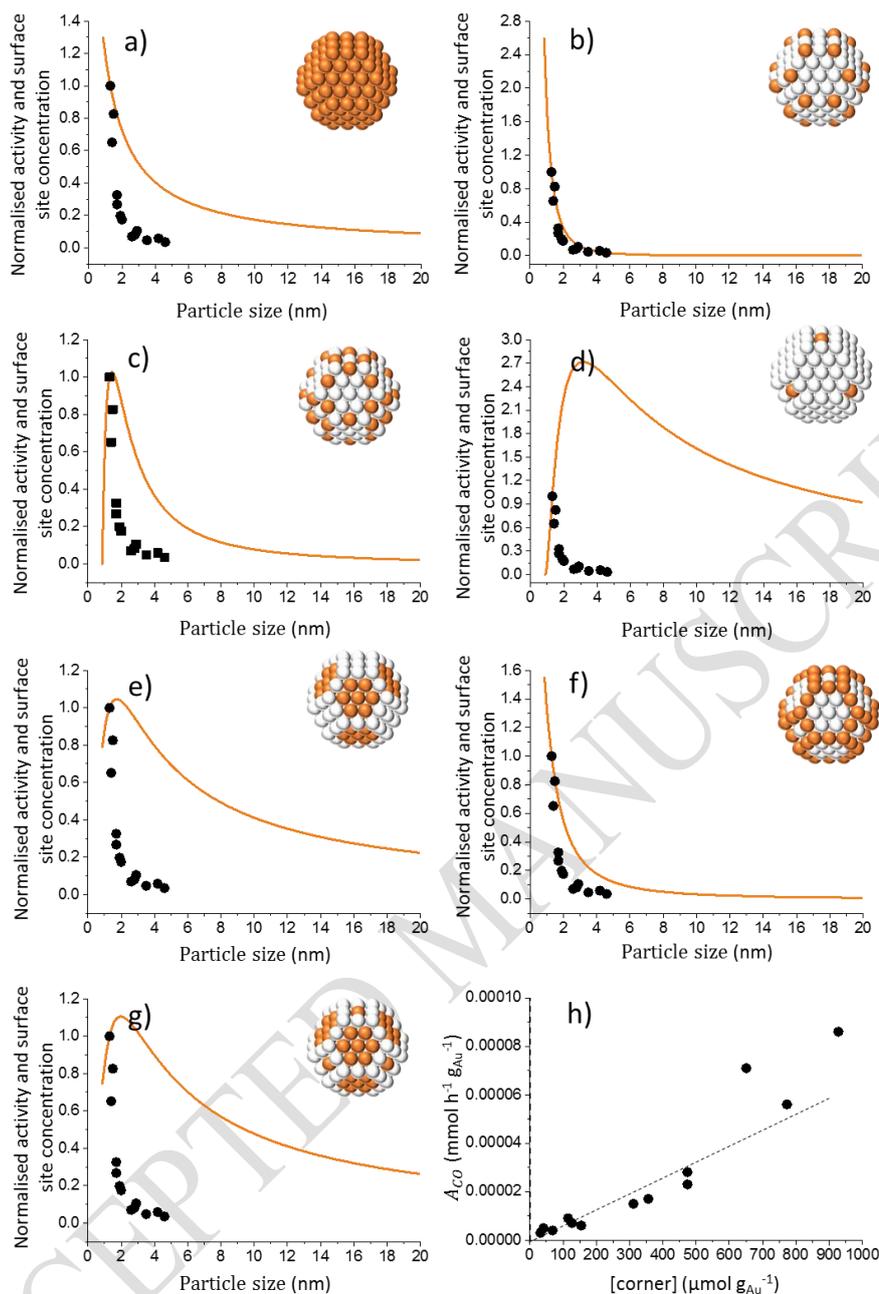


Fig.S.4. Evolution of the normalized water gas shift activity of Au/Al₂O₃ catalysts (circle, [2]) and normalized surface site concentrations (orange curves) versus the particle size: a) all sites; b) corner; c) edge; d) face (100); e) face (111); f) corner + edge and g) all faces; h) Evolution of the activity versus corner surface site concentration. Orange curves: results predicted with the model by using the particle size value $\bar{d} = 1.3$ nm for the normalization (with $d_{Au} = 0.288$ nm, $M_{Au} = 196.97$ g mol⁻¹).

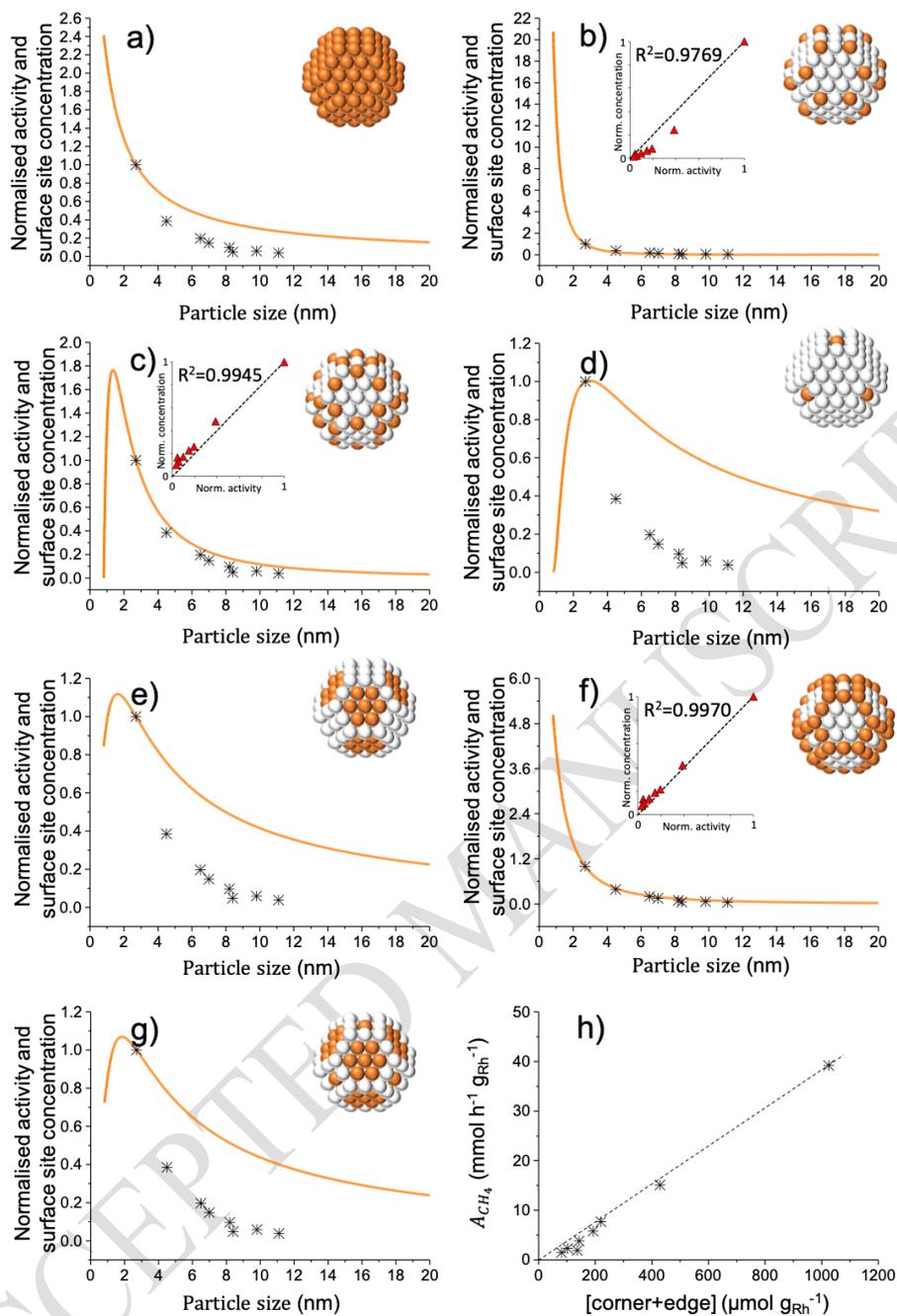


Fig.S.5. Evolution of the normalized methane steam reforming activity of Rh/ZrO₂ catalysts (cross, [3]) and normalized surface site concentrations (orange curves) versus the particle size: a) all sites; b) corner; c) edge; d) face (100); e) face (111); f) corner + edge and g) all faces; h) Evolution of the activity versus corner + edge surface site concentration. Orange curves: results predicted with the model by using the particle size value $\bar{d} = 2.7$ nm for the normalization (with $d_{Rh} = 0.269$ nm, $M_{Rh} = 102.91$ g mol⁻¹).

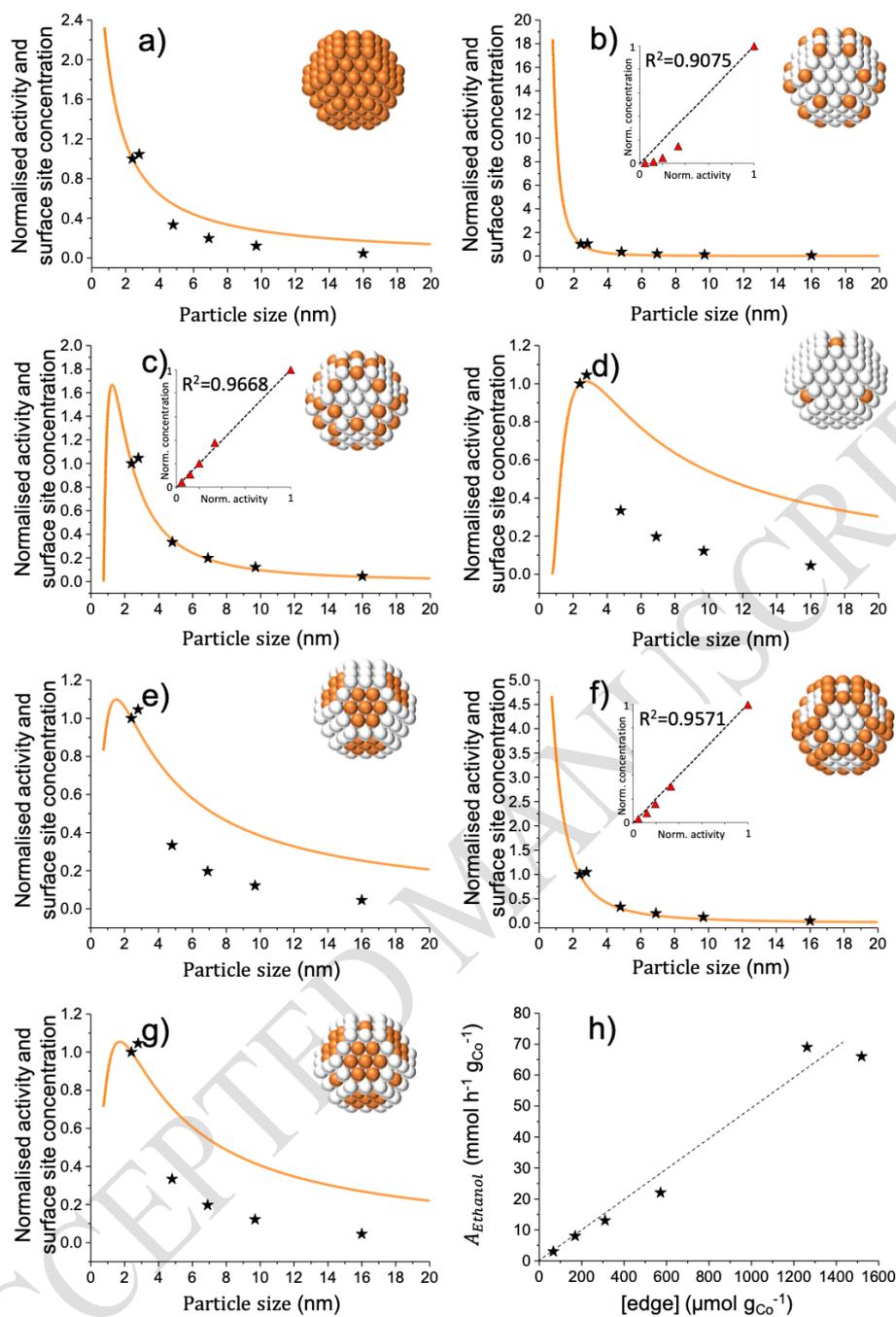


Fig.S.6. Evolution of the normalized ethanol steam reforming activity of Co/C catalysts (star, [4]) and normalized surface site concentrations (orange curves) versus the particle size: a) all sites; b) corner; c) edge; d) face (100); e) face (111); f) corner + edge and g) all faces; h) Evolution of the activity versus edge surface site concentration. Orange curves: results predicted with the model by using the particle size value $\bar{d} = 2.4$ nm for the normalization (with $d_{Co} = 0.250$ nm and $M_{Co} = 58.933$ g mol⁻¹).

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