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Novel single-ion conducting electrolytes based on polyvinylidene fluoride polymer for Lithium metal batteries

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Highlights

- SIPE based on PVDF was successfully prepared with possible scalability.
- Good conductivity, high Li⁺ transport number and excellent interfacial stability vs. Lithium were obtained.
- SIPE used as both electrolyte and cathode binder for high voltage LMP based battery demonstrated promising cell performance.

Abstract

A single-ion polymer electrolyte (SIPE) based on PVDF-based random copolymer (Li-PVDF) was synthesized in water from the radical copolymerization of vinylidene fluoride (VDF) with perfluoro -2-methyl-3-oxa-5-sulfonimido[-3-oxa-5-sulfonyl fluoride] vinyl ether (VEPFSIS) initiated by potassium persulfate. The purified polymer, characterized by ¹H and ¹⁹F NMR spectroscopy, ICP-MS, and size-exclusion chromatography, contains 96 mol% VDF with an average molar mass of 128 kg mol⁻¹. The Li-PVDF was cast into self-standing membranes and then swollen with a 50/50 v/v mixture of ethylene carbonate and propylene carbonate. The membrane was analyzed using DSC, TGA, pulse field gradient (PFG)-NMR and electrochemical methods. The solvent-doped membrane exhibited a lithium ion transport number close to 1 with lithium ion conductivities higher than 10⁻⁴ S cm⁻¹ at 30 °C, an electrochemical stability up to 4.3 V vs. Li⁺/Li and an excellent reversibility upon continuous lithium plating/stripping cycles. In addition, prototype Li/NMC battery cells using Li-PVDF as

both electrolyte and cathode binder in the NMC based composite cathode showed reversible cycling and good performance at 60 °C. The results demonstrated the promising potential of this new single-ion polymer family in intrinsically safe all solid-state lithium metal based batteries.

Keywords: Lithium metal; PVDF; polymer electrolyte; single-ion; NMC composite electrode.

1. Introduction

Nowadays, due to the increasing environmental issues in our modern society, the transition from traditional fossil fuel to renewable energy sources in combination with an electrified transport has become a necessity, but it requires more efficient energy storage and conversion technologies [1]. Lithium metal-based batteries (LMBs) are foreseen as the next battery technology beyond lithium-ion thanks especially to the lithium high theoretical specific capacity (3.8 Ah g^{-1}) and low redox potential (-3.04 V vs. SHE) [2–4] compared to currently used graphite or graphite/silicon based negative electrodes [5]. However, the practical use of Lithium metal remains limited especially by severe safety issues due to irregular lithium plating during the charging using liquid electrolytes [6], an issue for which polymer based electrolytes [7,8], poly(ionic liquid) [9] or organic/inorganic composite electrolytes [10–12] seem to be a promising alternative [13,14].

Among the studied polymer-based systems, besides the most common used polyethylene oxide (PEO) [15], poly(vinylidene fluoride) (PVDF) and its derivatives are also attractive thanks to their mechanical stability upon a broad temperature window up to 160 °C, and their high chemical and electrochemical stability (up to 4.5 V vs. Li^+/Li) [16–18]. Indeed, PVDF is a well-known binder of both negative and positive composite electrodes for Li-ion technology. However, PVDF and its derivatives are not able to insure a good ionic conductivity of the Li cation in a dried state due their low ability for solvation [19]. In addition, the high degree of crystallinity of PVDF based polymers, which provides a high mechanical resistance, reduces the effective ionic conductivity, limiting the amount of amorphous paths for ion transport [20]. Nevertheless, they can be plasticized using polar solvents such as carbonates, and therefore are largely studied as gel electrolytes [21]. The polymer membranes based on VDF [16,22–25], copolymers [26–31] or blends with other polymers [32–38], gelled with a liquid electrolyte made from carbonate solvents and lithium salt, exhibit a high conductivity of up to $10^{-3} \text{ S cm}^{-1}$ at 30 °C and a good electrochemical stability of up to 4.5 V vs. Li^+/Li [38,39]. However, the conductivity of these gels is mainly driven by the carbonate solvation of both cation and anion,

which leads to lithium transference number (t_{Li}^+) lower than 0.45 [40]. This induces the formation of ionic concentration gradients when the cell is under current, limiting the maximal power and leading to nucleation and growth of lithium dendrites during the recharge (lithium plating) [41,42]. To avoid these issues, single-ion conducting polymer structures (SIPE) *i.e.*, polymers in which the anion is covalently bounded to the immobile macromolecular backbone, leading to only one mobile ion, the Li^+ ion, were designed to suppress the formation of a gradient of ion concentration under current, and by consequence prevent lithium dendrite nucleation and growth [43–47].

Among all SIPEs, those based on PVDF have not been widely reported due to the difficulty of synthesis. Up to now, most of the SIPEs were synthesized by covalently grafting the lateral ionic chain onto the VDF backbone by irradiation [48] or reaction with amines [49]. For example, by ^{60}Co γ -ray irradiation, Ding *et al.* [48] successfully synthesized new PVDF based SIPE by grafting hexafluorobutyl methacrylate (HFMA) and 2-acrylamido-2-methylpropanesulfonic acid (AMPS) onto the PVDF backbone. Polymer electrolytes prepared from sulfonated PVDF soaked in EC/DMC (v/v = 1/1) presented a conductivity of $2.08 \times 10^{-5} S cm^{-1}$ at 30 °C combined with a Li^+ transference number of 0.93. This SIPE was used as a binder for preparing $LiFePO_4$ cathode, allowing a better cycling compared to the PVDF binder alone. Generally, $LiFePO_4/Li$ cell with sulfonated PVDF SIPE as both binder and electrolyte provides stable charge/discharge cycling with a capacity of 142 mAh g^{-1} at 0.1 C at room temperature [48]. On the other hand, lithium sulfonate-grafted PVDF-HFP polymer was successfully synthesized by direct grafting of taurine onto PVDF backbone and was used as binder for $LiFePO_4$ cathode [49]. The use of grafted SIPE allows a better solid electrolyte interface and faster charge transfer, resulting in better battery performance and higher capacity retention compared to cathode with PVDF binder. However, these methods of synthesis cannot be easily scaled up due to either the use of radioactive source, or the difficulty to control the amount and position of grafted anions onto the PVDF backbone.

Recently, Ameduri *et al.* have developed a new method of synthesis of SIPE based on PVDF from the radical copolymerization of VDF and a functional monomer, which allows them to control both composition and structure of the single-ion copolymers [50]. These SIPEs were studied in proton exchange membrane fuel cells. Herein, based on such synthetic methodology, a new kind of SIPE promising for lithium batteries has been synthesized by radical copolymerization of VDF with a perfluoroalkylsulfonimide vinyl ether lithium sulfonate and fully characterized by means of NMR spectroscopy and size exclusion chromatography. The membrane cast from this new copolymer has been soaked, for different

times, in an ethylene/propylene carbonates mixture (50/50 in vol.). The transport (conductivity and transference number) and thermodynamic properties of the resulting membranes have been thoroughly studied. The best composition has been used for the assembly of Li/SIPE/Li symmetrical cells to check its ability to reversibly plate and strip lithium metal. Their electrochemical window has also been analyzed. Finally, composite cathode electrode based on lamellar $\text{LiNi}_{0.33}\text{Mn}_{0.33}\text{Co}_{0.33}\text{O}_2$ (NMC 111) as active material and SIPE as both co-binder and electrolyte were formulated and cycled in coin cells (Li/SIPE/composite cathode) at 60 °C.

2. Experimental section

2.1. Materials

Dimethylformamide (DMF) and potassium persulfate were purchased from Aldrich and used as received. Vinylidene fluoride (VDF) and perfluoro -2-methyl-3-oxa-5-sulfonimido[-3-oxa-5-sulfonyl fluoride] vinyl ether (VEPFSIS) were kindly provided by Arkema (France) and Juhua (China) companies, respectively.

2.2. Li-PVDF synthesis

The PVDF based SIP was synthesized in water by following the same protocol as described in a previous work [50] by radical copolymerization of two monomers, vinylidene fluoride (VDF) and VEPFSIS, in presence of potassium persulfate as the initiator (KPS) (**Scheme 1**). The VEPFSIS introduces two anions, *i.e.*, sulfonimide and sulfonate anions (VEPFSIS-Li), the last one being obtained by the hydrolysis of fluorosulfonic function in presence of LiOH [51,52].

Scheme 1. Radical copolymerization of vinylidene fluoride (VDF) and VEPFISIS, and modification of SO_2F into SO_3Li with the formation of single-ion conducting copolymer, Li-PVDF.

In a typical synthesis, Li-PVDF was prepared in a 100 mL Hastelloy Parr autoclave equipped with a bourdon pressure gauge, a rupture disk and inlet and outlet valves. First, the autoclave was purged with 30 bars of nitrogen pressure to prevent any leakage. Then, a 20 mm Hg vacuum was operated for 15 min. The reactants including potassium persulfate (KPS) as initiator (36 mg, 0.04 mol%), perfluorinated vinyl ether monomer bearing both a sulfonyl fluoride and sulfonimide (VEPFISIS) (15.41 g, 6 mol%) and water (55 mL) as solvent were inserted into the autoclave through a funnel tightly connected to the vessel. After cooling, VDF (20 g, 94 mol%) was transferred by double weighing (*i.e.*, the difference of weight before and after transferring VDF) into the autoclave. The reactor was gradually heated up to 70 °C and the pressure in the autoclave reached a maximum of 85 bars. The reaction was stopped after 16 h and showed a good VDF conversion since the pressure went down to 14 bars ($\Delta P = 71$ bars). Then, the autoclave was cooled down to room temperature using an ice bath and the unreacted VDF was vented off. After opening the autoclave, the resulting total product mixture was dissolved in DMF, then precipitated from cold water. The copolymer (15.48 g, 1eq.) was then suspended in a water-methanol mixture (300 mL, 1/1, v/v) and LiOH (0.65 g, 1eq.) was added to modify the SO_2F into SO_3Li [51,52]. The reaction mixture was stirred for 48 h at

room temperature. Li-PVDF (copolymer poly(VDF-VEPFSIS-Li)) in form of white powder was recovered by filtration then dried under high vacuum at 80 °C until constant weight. In order to remove any trace of non-reacted VEPFSIS or inorganic salts such as LiOH, LiF, the polymer was immersed in a large excess of deionized water under stirring for 2 h and then filtered. This operation was repeated several times until the pH of washing water was 7. To ensure the non-reacted VEPFSIS was totally removed, the purified copolymer was characterized by ¹⁹F NMR spectroscopy and the absence of signal at -134 ppm (assigned to CFO in F₂C=CFO- of this monomer) is a good evidence. After filtration, the polymer was dried under vacuum (10⁻³ mbars) at 80 °C until constant weight to produce 12.4 g of copolymer as a white solid powder (80 wt.% yield)

Preparation of single ion conducting polymer electrolyte (SIPE)

In a typical protocol, the Li-PVDF membrane was cast from a solution of 10 wt% Li-PVDF in DMF. The solution was prepared at room temperature, filtered over a 0.45 µm filter, degassed under vacuum and cast in a Petri dish, then the solvent was evaporated at 60 °C for 2 days. The resulting membrane was further immersed during 24 h in water in order to eliminate the residual DMF. Then, the washed membrane was dried at 80 °C under vacuum for 24 h. The dried membranes were stored in an argon filled glovebox (Jacomex, O₂, H₂O < 1 ppm) for at least one week before use.

Solvent uptake was conducted in glove box using a mixture of 50/50 by volume of ethylene carbonate/propylene carbonate (EC/PC). The solvent mixture was previously dried with 3 Å molecular sieves until the water content was lower than 5 ppm (by Karl Fisher) before used. Samples were weighed before and after soaking in solvent after different immersion times. Before each weight measurement, the excess solvent on the membrane surface was removed using a Kimtech paper. Swelling tests were conducted three times and error bars come from the standard deviation of the measures. The results are presented in **Fig. 1**.

For the purpose of clarity, these membranes are denoted Li-PVDF-x in which x is the weight per cent of solvent calculated from the following equation:

$$x (\%) = \frac{m_{\text{EC/PC}}}{m_{\text{EC/PC}} + m_{\text{Li-PVDF}}} \times 100\% \quad (\text{Eq. 1})$$

where $m_{\text{EC/PC}}$ and $m_{\text{Li-PVDF}}$ are the weights of solvent and Li-PVDF membrane, respectively.

2.3. Characterization

NMR analysis was conducted with a Bruker AVANCE III HD spectrometer at frequencies of 400.15 MHz for ^1H and 376.52 MHz for ^{19}F . Data treatment was performed on the software MestRe-C 2.3a.

Thermogravimetric analysis (TGA) was carried out from 25 to 600 °C at a heating rate of 10 °C min $^{-1}$ under a nitrogen flow of 50 mL.min $^{-1}$ using a thermogravimetric analyzer (TGA, 1 STARe System from Mettler-Toledo).

The molecular weight was measured by size exclusion chromatography (WATERS 515 HPLC) coupled with multi-angle light laser scattering Wyatt Dawn EOS detector (SEC-MALLs-) using a 10 AGILENT 2xPLgel-Mixed-D as column and DMF (Alfa Aesar – HPLC grade 99.7%) with NaNO_3 (0.1 M) as solvent. A solution of around 1 wt% of polymer was injected through the polypropylene filter of 0.45 μm under solvent flow rate of 1 mL min $^{-1}$. Received data from refractometer and MALLS (**Fig. S3**) were analyzed by using ASTRA software provided by Wyatt.

ICP-MS

Inductively coupled plasma mass spectrometry (ICP-MS) was carried out on a Perkin Elmer Nexion 2000c device. Lithium concentration of Li-PVDF membrane was determined using standard solutions of 0, 2, 5, 10, 20 and 50 ppb relative to an invariable quantity of internal standard (2.5 ppb of Rh). Li-PVDF polymer was degraded in extra pure acid nitric and diluted with ultrapure water in order to obtain a concentration in the calibration range. The obtained data are processed using Syngistix software.

Self-diffusion coefficients of lithium and fluorine were assessed by pulse field gradient (PFG)-NMR using a 9.4T Bruker Avance 400 with a diffusion probe of 5 mm. The magnitude of the pulsed field gradient was varied from $0 \leq g \leq 1000 \text{ G cm}^{-1}$; Δ was set at 200 ms and δ was set between 1 ms and 5 ms, depending on the diffusion coefficient of the mobile species. SIPEs containing 50 wt% EC/PC were cut in bands and introduced into an NMR tube (diameter 4 mm) hermetically sealed inside the glovebox. The measurements were carried out at $70.0 \pm 0.5 \text{ }^\circ\text{C}$.

The Li^+ transference number of polymer electrolyte can be determined either by PFG-NMR or electrochemical methods. In the former method, the Li^+ transport number (t_{NMR}^+) can be

calculated using the diffusion coefficients measured by NMR of the Li and the anion (Fluorine) following **Eq. 2**:

$$t_{NMR}^+ = \frac{D_{Li}}{D_{Li} + D_F} \quad (\text{Eq. 2})$$

By the second method, $t_{\text{electrochem.}}^+$ can also be estimated using a coupling technique of DC polarization with chronoamperometric (CA) measurement, and Electrochemical Impedance Spectroscopy on Li/Li symmetric cells. The experiment has been carried out on VMP300 potentiostat (Biologic). The Li^+ transport number was then calculated from Watanabe [53] (**Eq. 3**) approaches:

$$t_{\text{electrochem.}}^+ = \frac{R_b}{\left(\frac{\Delta V}{I_s} - R_s\right)} \quad (\text{Eq. 3})$$

in which ΔV is the static voltage of the cell, I_s is the current obtained at the steady state, R_b is the bulk electrolyte resistance, and R_s the steady-state resistance of the lithium electrode/electrolyte interface. The advantage of the Watanabe's approach [53] compared to the classical Bruce and Vincent's [54], is to use directly the measured electrolyte resistance by EIS instead of calculating it thanks to the initial current value after imposing the voltage which strongly depends on the response time of the potentiostat used.

Differential scanning calorimetry (DSC) was performed on a 1 STARe System from Mettler-Toledo under nitrogen flow (50 ml min^{-1}) and a heating rate of $10 \text{ }^\circ\text{C min}^{-1}$. Each sample was evaluated through two heating and one cooling cycles from $-100 \text{ }^\circ\text{C}$ to $180 \text{ }^\circ\text{C}$ for dry samples and from $-150 \text{ }^\circ\text{C}$ to $180 \text{ }^\circ\text{C}$ for the plasticized samples. The T_g values were assessed from the mid-point in the heat flow jump, while the melting points were determined from the onset temperature of the melting peak. The crystallinity degree (χ) of Li-PVDF can be calculated by applying **Eq. 4**:

$$\chi = \frac{\Delta H_m}{\Delta H_o} \times 100\% \quad (\text{Eq. 4})$$

where ΔH_o (104.5 J g^{-1}) corresponds to the melting enthalpy of a 100% crystalline PVDF [55,56] and ΔH_m is the melting enthalpy of the copolymer (determined by DSC in J g^{-1}), respectively.

Concerning plasticized samples, the enthalpy and degree of crystallinity were calculated by subtracting the weight of the EC/PC solvent uptake.

Ionic conductivity of the Li-PVDF membranes was determined by electrochemical impedance spectroscopy using an impedance analyzer (Hewlett Packard 4192A) with an excitation voltage amplitude of 20 mV in the frequency range from 5 Hz to 13 MHz. The temperature range probed was from 0 to $80 \pm 0,1$ °C thanks to a climatic chamber (Vötsch VC4018). Data were recorded every 10 °C after a stabilization time of 1 h minimum. Dry and plasticized membranes were sandwiched between two stainless steel blocking electrodes and sealed in Swagelok®-type cells inside the glovebox before measurement. Same measurement was conducted twice for the same amount of contained solvent and the average values with 5% error were presented in **Fig. 2**. The conductivity was calculated from the following equation:

$$\sigma = \frac{L}{R \times S} \quad (\text{Eq. 5})$$

where L, S and R stand for the electrolyte membrane thickness, the electrode surface area and the bulk membrane resistance (determined from Zview fitting the Nyquist's plot, *e.g.* **Fig. S7**), respectively.

The conductivity data were fitted using the Vogel–Tammann–Fulcher equation [57–59]:

$$\sigma = \frac{A}{\sqrt{T}} \exp \left(\frac{-E_a}{R(T-T_0)} \right) \quad (\text{Eq. 6})$$

where σ is the ionic conductivity (S cm^{-1}), the pre-exponential term A is a constant proportional to the amount of ionic mobile charges, E_a is a pseudo-activation energy (J mol^{-1}), R is the perfect gas constant ($8.314 \text{ J mol}^{-1} \text{ K}^{-1}$) and $T_0 = T_g - 50$ is the ideal glass transition temperature.

Electrochemical stability of the electrolyte membranes was determined using cyclic voltammetry (CV) carried out in a coin cell prepared by sandwiching the electrolyte membranes between a lithium disk and a blocking stainless steel electrode. Measurements were conducted on a VMP3 potentiostat (BioLogic) using a slow sweep rate of 0.1 mV s^{-1} in a voltage ranging from -0.5 to +5 V *vs.* Li^+/Li . In addition, the lithium plating and stripping coulombic efficiency was calculated from the area ratio of the lithium plating peak area over the lithium stripping peak area obtained around 0 V *vs.* Li^+/Li .

Evaluation in symmetric Li/Li. Lithium stripping/plating experiments were performed by sandwiching the electrolyte membranes between two lithium disks ($\varnothing = 12 \text{ mm}$), assembled in coin cells, and applying selected current densities from ± 0.02 to $\pm 0.4 \text{ mA cm}^{-2}$ for 30 min per interval (with 5 min rest between each step) using a VMP3 potentiostat (BioLogic).

Battery performance. Battery cycling was performed in prototype coin cells using a lithium foil as the anode and standard lamellar $\text{LiNi}_{0.33}\text{Mn}_{0.33}\text{Co}_{0.33}\text{O}_2$ (NMC 111) as the cathode material. The NMC composite cathode was prepared by solution casting onto an aluminum foil of a well-dispersed slurry mixture of 60 wt% NMC, 10 wt% carbon black (C65) and 30 wt% of polymer binder, *i.e.*, 25 wt% Li-PVDF and 5 wt% PVDF in NMP. After NMP evaporation at 60 °C for 24 h, the cathode was pressed at 120 °C to reduce the porosity ($\leq 10\%$) before being swollen in EC-PC to reach a similar SIPE composition to the electrolyte membrane. The areal capacity of the prepared electrode is 0.33-0.36 mAh cm^{-2} giving a theoretical accessible capacity at 4.2 V vs. Li^+/Li for NMC 111 of 160 mAh g^{-1} [60]. Charge and discharge tests were performed at 60 °C using the galvanostatic cycling with potential limitation (GCPL) technique in a VMP3 potentiostat from Biologic over a voltage range from 2.8 to 4.2 V.

3. Results and discussion

3.1. Characterization of Li-PVDF single-ion conducting polymer

The purity of the polymer was verified by ^1H and ^{19}F NMR spectroscopy and the composition of the final copolymer was calculated from ^{19}F -NMR spectra (**Fig. S1**) using the peak area ratio between the signals corresponding to the side chain and those assigned to PVDF segments (**Eq. 7**). The peaks appearing between -78 and -82 ppm are attributed to the 11 fluorine atoms of VEPFIS-Li, while those centered at -92, -110, -113 and -116 ppm are characteristic of VDF units [50]. The calculated ratios are gathered in **Table 1**. As expected from perfluorovinyl ethers, it is observed that the reactivity of the ionic monomer is lower than that of VDF monomer and its incorporation in the copolymer structure is lower than that in the initial ratio. From the resulting composition, we calculated the Li content (mequivLi/g copolymer) from **Eq. 8** considering that each side chain contains two Li cations, *i.e.*, one Li perfluorosulfonate and one perfluorosulfonimide (**Table 1**).

$$\text{VEPFIS-Li/VDF ratio by } ^{19}\text{F NMR} = \frac{\int_{-77}^{-83} I/11}{(\int_{-91}^{-96} I + \int_{-109}^{-110} I + \int_{-103}^{-115} I + \int_{-116.5}^{-117} I)/2} \quad (\text{Eq. 7})$$

$$n(\text{Li})/\text{g}_{\text{copolymer}} = \frac{n_{\text{VEPFIS-Li}} \times \text{number of Li per chain}}{m_{\text{Li-PVDF}}} = \frac{(100\% - \text{wt\% PVdF}) \times 2}{M_{\text{VEPFIS-Li}}} \quad (\text{Eq. 8})$$

where $M_{\text{VEPFIS-Li}}$ and M_{VDF} worth 815 g mol^{-1} and 64 g mol^{-1} , respectively.

The chemical composition of the synthesized SIPE was also determined by thermogravimetric analysis (**Fig. S2**). The polymer weight loss taking place at around 320-350 °C was associated to the degradation of lateral side chains according to Colpaert *et al.* (*i.e.*, only sulfonate and sulfonimide side chain PFSIS-Li) [50]. By assuming that this decomposition is complete, the chemical composition, *i.e.*, the weight fraction of PVDF segment in Li-PVDF, can be estimated using **Eq. 9**:

$$\text{wt\% PVDF by TGA} = 100\% - \text{wt\%}_{\text{VEPFSIS-Li}} = 100\% - \frac{\text{wt\%}_{\text{PFSISLi}} * M_{\text{VEPFSIS-Li}}}{M_{\text{PFSISLi}}} \quad (\text{Eq. 9})$$

where $M_{\text{PFSISLi}} = 734 \text{ g mol}^{-1}$.

The obtained results (**Table 1**) are in good agreement with those deduced from ^{19}F NMR spectroscopy, confirming the chemical composition of the synthesized SIP. The lithium content values calculated from NMR, TGA and ICP are very close (**Table 1**), which proves the high purity of ionic polymer.

The molar mass was determined thanks to size exclusion chromatography and was calculated from both laser diffusion and refractometer signal (**Fig. S3**). The obtained results (**Table 1**) show a high M_n of 128 kg mol $^{-1}$ and a dispersity (PDI) of 3, which is expected for a conventional radical copolymerization.

Table 1. Chemical compositions, IECs and molar mass of Li-PVDF powder.

SIP	Ratio VDF/PFVESIS		wt% PVDF (%)			Li concentration (mequiv g $^{-1}$)					Molar mass (kg mol $^{-1}$)		
	Theory	^{19}F NMR	Theory	^{19}F NMR	TGA	Theory	^{19}F NMR	TGA	ICP	Average ^a	M_n	M_w	$\text{PDI} = M_w/M_n$
Li-PVDF	94:6	96:4	55	66	65	1.09	0.83	0.86	0.82	0.84 ± 0.02	128	390	3.1

^a Average value from three experimental methods ^{19}F NMR, TGA and ICP.

3.2. Fabrication and characterization of SIPE membrane

The thermodynamic behavior of Li-PVDF analyzed by DSC (**Table 2**) shows two transition temperatures: the first one is around 110 °C, possibly attributed to specific relaxation temperature to PVDF copolymers, *i.e.*, the mid-temperature transition [61] while the second one, corresponding to the PVDF melting peak, appears at around 155 °C [62]. The melting of the PVDF crystalline phase in the Li-PVDF copolymer takes place at least 10 °C lower than

that of the pure PVDF, which suggests that the copolymer forms crystallites with smaller size [63]. The melting temperature has to be also affected by the presence of ca. 4 mol.% of bulky comonomer. This behavior is in agreement with a random copolymer structure [17,18]. From the data in **Table 2**, the crystallinity degree of Li-PVDF is around 26.5%, being at least 1.5 times lower than that of a membrane cast from standard pure high molar mass PVDF ($\Delta H > 40\text{-}50 \text{ J g}^{-1}$, $\chi_c = 38\text{-}48\%$) [62]. This phenomenon is due to the presence of side chains, which affects the crystallization of PVDF sequences, similarly to the case of poly(VDF-*co*-HFP) copolymers [26].

The conductivity of Li-PVDF was measured in the 50 – 80 °C temperature range. Due to its high T_g , Li-PVDF copolymer can only reach $10^{-6} \text{ S cm}^{-1}$ at 80 °C, which is not satisfactory for battery applications. In order to dissociate the ion pairs and to increase the Li mobility, Li-PVDF membranes were plasticized with a mixture of two high boiling and flash point carbonates [64], *i.e.*, 50/50 v/v EC/PC. The plasticization of PVDF by carbonate solvents is rather interesting for lithium-battery application [65,66] due to their high dielectric constant and electrochemical stability. The solvent uptake (eq. 1) as a function of soaking time of the Li-PVDF membranes is illustrated in **Fig. 1**.

Fig. 1. Solvent uptake versus soaking time of Li-PVDF.

SIPE membrane reached an equilibrium after only 100 s, which confirms the strong affinity of the matrix with the carbonate solvent with an uptake of $58 \pm 6 \text{ wt}\%$, slightly higher than the PVDF swelling ratio in solvent mixture such as EC/DEC or EC/DMC [67], due to the existence of ionic fraction and a lower crystallinity. The membrane containing 60% is solid and mechanically stable easy to handle, as shown in **Fig. S4**.

Lithium concentration (in mequiv/g) in plasticized Li-PVDF membranes (**Table 2**) can then be recalculated using the following equation:

$$n(\text{Li})/g_{\text{SIPE}} = \frac{n(\text{Li})}{m_{\text{Li-PVDF}} + m_{\text{EC-PC}}} = 0.84 \times (1 - x (\%)) / 100 \quad (\text{Eq. 10})$$

where 0.84 is the concentration in pure Li-PVDF and $x (\%)$ is the weight per cent of solvent in plasticized membrane. The increase of the solvent amount in the membrane induces a continuous decrease of the glass transition temperature (T_g) (**Table 2**), owing to the increase of the molecular dynamics of polymer segments swollen by the solvent [68]. After the incorporation of the solvent (up to 40 wt%) into Li-PVDF, SIPE displays slightly increased crystallinity and decreased melting point compared to the solvent-free membranes. This can be explained by solvent induced PVDF crystallization due to increase of molecular dynamics, which facilitates polymer chains reorganization [16] into crystallites. Indeed, this phenomenon has been already reported, *i.e.* an increase in polymer crystallinity by soaking it in a liquid-phase solvent, *e.g.* in the case of poly(ethylene terephthalate) [69]. However, their crystallite sizes become smaller with the increase of the solvent content because the melting point significantly decreased [70]. Above 40 wt% of solvent uptake, the presence of a second endothermic peak around 0 °C is observed by DSC analysis (**Fig. S5**). This second peak grows with the solvent content and may correspond to the crystallization of solvent rich domains, which are in poor interaction with the polymer, although the melting enthalpy and temperature of PVDF domains continue to decrease.

Table 2. Glass transition temperature (T_g), melting temperatures (T_m) and melting enthalpies (ΔH_m) of pure and plasticized Li-PVDF membranes as a function of the solvent content.

Solvent uptake (wt %)	Li (mequiv g ⁻¹)	T_g (°C)	$T_{m \text{ Li-PVDF}}$ (°C)	ΔH_m (J g ⁻¹)	ΔH_m (J g ⁻¹ SIPE)	$\Delta H_{m \text{ PVDF}}^b$ (J g ⁻¹ PVDF)	$\chi_c \text{ PVDF}$ (%)	$T_{m \text{ EC-PC}}$ (°C)	$\Delta H_{\text{EC-PC}}^c$ (J g ⁻¹)	$\chi_{c \text{ EC}}^d$ (%)
0	0.84	--	159	18 ± 2	18 ± 2	28 ± 3	26.5	--	--	--
15	0.71	-50	135	18 ± 2	22 ± 2	34 ± 3	32.2	--	--	--
20	0.66	-65	124	17 ± 2	21 ± 2	31 ± 3	30.0	--	--	--
33	0.56	-73	119	13 ± 2	19 ± 2	29 ± 3	27.8	--	--	--
44	0.46	-80	103	5 ± 1	9 ± 1	14 ± 1	13.2	4	23 ± 3	28.1
55	0.37	-97	99	3 ± 1	6 ± 1	8 ± 1	7.9	-4	34 ± 3	42.6
60	0.33	-99	96	2 ± 1	4 ± 1	7 ± 1	6.3	-5	36 ± 3	44.6

^{b, c} ΔH recalculated as a function of PVDF content in the membrane (**Eq. 4**).

^d $\Delta H_{\text{EC}} = 13.5 \text{ kJ mol}^{-1}$ (= 153.4 J g⁻¹ from reference [71]).

3.3. Ionic transport properties

The diffusion coefficient of lithium (D_{Li}) in Li-PVDF-55 membrane at 70 °C, measured by PFG-NMR spectroscopy, was found to be $8 \times 10^{-11} \text{ m}^2 \text{ s}^{-1}$, while fluorine (D_{F}) was not measurable, which demonstrates that the Li^+ transport number is, as expected, close to 1 [46]. This value was also measured at 60°C by an electrochemical method using the Watanabe

approach [53] based on a potentiostatic polarization of lithium symmetric cell (the time dependent current response and the impedance obtained in steady state are shown in **Fig. S6**). Lithium transport number was calculated to be 0.87 ± 0.3 , which is comparable to other single-ion conducting systems reported in the literature [43,72,73] and in agreement with the results obtained from PFG-NMR results.

The ionic conductivities of Li-PVDF-x as a function of temperature for different solvent uptakes are plotted in Arrhenius coordinates in **Fig. 2a**. Generally, for all solvent contents, the data display a thermally activated conductivity with a characteristic curvature of VTF model assigned to the increase of free volume induced from the expansion of the polymer [33]. Interestingly, there is no drop of conductivity at high temperature, which means that the carbonates display sufficient affinity with the Li-PVDF matrix to avoid any evaporation.

Fig. 2. a) Conductivity as a function of temperature of Li-PVDF-x membranes containing different solvent contents (x) with their VTF fitting (best fitting parameters listed in **Table S1**); b) Isothermal conductivity at 25°C and pseudoactivation energy calculated from VTF fit of conductivity data as a function of solvent content in wt%; c) isothermal conductivity at 25°C

°C and pseudo-activation energy as a function of the number of moles of solvent (n_{solvent}) / number of moles of lithium (n_{Li}) ratio.

An increase in solvent content induces a continuous rise in conductivity, which could be explained by: (i) an enhanced ion-pair dissociation, *i.e.*, increasing number of free mobile charges, (ii) an increase of the molecular dynamics facilitating faster ion motions in agreement with the decrease of both the SIPE glass transition temperature, and (iii) a better percolation of the ionic domains [23,74,75]. The best ionic conductivity (*e.g.*, Li-PVDF-60 doped with 60 wt% of solvent) reaches $5 \times 10^{-4} \text{ S cm}^{-1}$ at 25 °C (**Fig. 2b**) [76]. **Fig. 2b** displays the evolution of the calculated conductivity at 25 °C and the pseudo-activation energy thanks to VTF fits as a function of solvent uptake. It shows two distinct behaviours for low and high solvent concentrations with a threshold at about 35–45 wt% (grey zone in **Fig. 2b**), corresponding to 6–8 molecules of solvent over one lithium cation (see **Fig. 2c**). In the low-EC/PC region below the threshold, an exponential increase in conductivity of almost 3 orders of magnitude (from $4 \times 10^{-8} \text{ S cm}^{-1}$ to $2 \times 10^{-5} \text{ S cm}^{-1}$) is observed. In parallel, the pseudo-activation energy decreases linearly (from 17 to 9 kJ mol⁻¹), which matches an easiest ionic transport. Above the threshold, the isothermal conductivity continues to increase, while E_a decreases but in a much slower manner.

These results are in good agreement with the DSC findings where, for a solvent content < 40 wt%, the solvent strongly interacts with the ionic moieties of the polymer, thus significantly contributing to the ion pair dissociation and polymer dynamics. Moreover, for $x > 40$ wt%, the membranes contain rich solvent domains, which also leads to an enhanced Li-ion mobility, presumably related to a reduced local viscosity and a further improved connectivity.

The plasticized Li-PVDF-60 membrane exhibits an excellent single-ion conductivity, which is higher than that of membrane blends of PVDF and liquid electrolytes. For example, a conductivity of *ca.* $10^{-4} \text{ S cm}^{-1}$ at room temperature was obtained for EC-PC doped PVDF containing LiBF₄ [19] or LiN(SO₂C₆H₄)₂ [14] or EC plasticized PVDF–LiCF₃SO₃ [74].

Further electrochemical characterizations were conducted on a Li-PVDF plasticized with 55 wt% EC-PC, denoted Li-PVDF-55, that exhibited the best compromise between conductivity and mechanical behavior.

3.4. Electrochemical stability

Electrochemical stability of plasticized Li-PVDF membranes was evaluated from cyclic voltammetry at 80 °C, and revealed an electrochemical stability window (ESW) spanning 4.3 V when employing stainless steel working electrode (WE), which is in agreement with the ESW of carbonate based electrolytes [77] (**Fig. 3**). Similar results were obtained from other groups when studying solvent doped salt-containing PVDF membranes, *e.g.*, PVDF plasticized with $\text{LiN}(\text{SO}_2\text{CF}_3)_2$ in PC [22] or LiPF_6 in EC/DMC/DEC solvent [25]. Tiny peaks can be noted around 1 V *vs.* Li^+/Li which may be due to intercalation/de-intercalation in the oxide layers on the stainless steel WE [78]. Two peaks at -0.5 V and +0.54 V *vs.* Li^+/Li , correspond to the reversible plating and stripping of lithium onto stainless steel working electrode [79,80] with high current density. Coulombic efficiency of lithium plating/stripping process of this PVDF membrane was calculated as 83%, which is rather high considering the known instability of carbonate based electrolytes on lithium electrode which generally present Coulombic efficiency lower than 80% [81].

Fig. 3. Cyclic voltammetry of Li-PVDF-55 membrane using Li/stainless steel cell from -0.5 to 5 V *vs.* Li^+/Li at a slow sweep rate of 0.1 mV s^{-1} . The figure on the right is the magnification of the current density *versus* 3-5 V range *vs.* Li^+/Li zone.

3.5. Evaluation of lithium plating/stripping efficiency

Lithium stripping/plating cycling tests coupled with impedance spectroscopy was conducted at 60 °C on symmetric Li/Li cells separated by the Li-PVDF-55 membrane (**Fig. 4**). The polarization of this cell is negligible at low applied current density of 0.01 mA cm^{-2} (2 mV) and it increases linearly with the stepwise applied current density up to 86 mV at 0.5 mA cm^{-2} (**Fig. 4c**), which shows an ohmic behavior, as expected for a single-ion electrolyte which presents high lithium plating/stripping kinetics. Indeed, the polarization is mostly due to the solid electrolyte interphase (SEI) on the lithium surface as shown in the Nyquist plot in **Fig.**

4d. These values are comparable with a recent study on EC-doped single-ion multi-block copolymer [46]. Finally, a reversible decrease of the polarization when current density is decreased to 0.2 mA cm^{-2} suggests a very stable SEI between the polymer electrolyte and the lithium electrode. This is confirmed by the galvanostatic impedance spectroscopy analysis along plating/stripping cycling measurements, which show that the interface resistance only varied slightly (but not monotonously) with the different applied current densities. This slight variation can be explained by the reorganization of the lithium/electrolyte interface upon continuous lithium stripping and plating [25,46]. These results demonstrate the good compatibility of our SIPE with lithium metal.

Finally, **Fig. 4b** shows a zoom on characteristic cycles (herein obtained at 0.1 , 0.3 and 0.5 mA cm^{-2} , respectively). The polarization upon the application of current density is immediately achieved, which further confirms the single-ion conductivity of our SIPE [54,82].

Fig. 4. Lithium plating/stripping cycling measurements obtained at 60°C in a symmetric Li/Li cell using Li-PVDF-55 membrane. (a) Effect of increasing current densities (0.01 , 0.1 , 0.3 , 0.4 , 0.5 mA cm^{-2}), followed by lowering the current density to 0.2 mA cm^{-2} . The duration of each lithium plating and stripping step is 30 min; (b) Magnification of characteristic plating/stripping cycles at 0.1 , 0.3 and 0.5 mA.cm^{-2} ; (c) Evolution of the polarization versus the applied current density; (d) Galvanostatic electrochemical impedance spectra of the Li/Li cell obtained for the different applied current densities (Nyquist plots).

3.6. Cycling performance of Li/NMC battery

To further demonstrate the interest of this new SIPE, the cycling performance at 60 °C of an Li/NMC battery in coin cell configuration has been tested. It is worth noting that the Li-PVDF-55 was used as both electrolyte separator and binder in the composite electrode. The cut off voltage of the charge was 4.2 V vs. Li^+/Li . The results are shown in **Fig. 5**.

The cycling is reversible (**Fig. 5b**), with 143 mAh g^{-1} at low C-rate of C/20 (D/20, D = discharge capacity), approaching theoretical capacity. After 20 cycles, the C-Rate C is increased to C/10 in charge and D/5 in discharge, which induces a drop of the capacity to 132 mAh g^{-1} (**Fig. 5a**) followed by about thirty very stable cycles. After 55 cycles the discharge rate is increased to D/3 (**Fig. 5a**), which leads to a slow decrease in discharge capacity from 132 to 120 mAh g^{-1} over the next 40 cycles. This value then remains very stable for the next 100 cycles (Fig5B). The faradic efficiency is 98%, and overall after 200 cycles the capacity retention is 80.16%. It can be noted that these cycle conditions are quite harsh since the C-rates are low and the temperature is high, which favors parasitic interfacial reactions, generally leading to a rapid decrease of the capacity in classical Li-ion technology. Therefore, these results show the promising potential of the SIPE designed on the basis of a PVDF skeleton instead of a PEO skeleton [15].

Fig. 5. Cycling performance of a NMC battery cell with Li-PVDF-55 as both electrolyte and cathode binder at 60 °C and various cycling rates: (a) Charge and discharge curves C/10, D/5 (cycle 20) and C/10 D/3 (cycle 55) and (b) Capacity versus cycle number.

4. Conclusion

A new lithium single-ion conducting PVDF-based copolymer was successfully synthesized by conventional and up-scalable radical copolymerization of VDF with a perfluorovinyl ether monomer bearing both sulfonimide and sulfonyl fluoride side-groups. The resulting copolymer had a molar mass of 128 kg mol^{-1} and contained 94 mol% of VDF. The

dry membrane was plasticized using a 50/50 v/v of EC and PC mixture to provide self-standing solid state electrolyte membranes combining high single-ion conductivity of 5×10^{-4} S cm^{-1} at 25 °C (with 60 wt% EC/PC), an electrochemical window spanning 4.3 V, an excellent reversibility of lithium plating/stripping in symmetric Li/Li cell, and very good capacity retention in high potential Li/NMC ASSB battery. This work paves the way for the design of new efficient SIPEs based on a PVDF backbone. Their promising performances open many perspectives for the development of solid-state batteries.

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