Viscosity, tribological and physicochemical features of ZnO and MoS₂ diesel oil-based nanofluids: An experimental study

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Abstract

In this research, two different diesel oil-based nanofluids were prepared and the influence of temperature and nanoparticle content were examined on viscosity, tribological, and physicochemical features of diesel oil. The kinematic viscosity of samples was experimentally evaluated based on standard ASTM D445. The greatest viscosity increment was diagnosed at 0.7 wt.% and 100°C for both of the prepared nanofluids. The anti-friction behavior of the nanofluids was studied utilizing a pin-on-disc tribometer. The acquired outcomes revealed that ZnO and MoS₂ nanoparticles (NPs) could promote the tribological characteristics of pure diesel oil. By analyzing the friction coefficient values and line roughness of the wear surface (Ra), an optimal concentration of ZnO and MoS₂ nanoparticles (NPs) were found to be around 0.4 wt.% and 0.7 wt.%, respectively. The friction factor and pumping power were also measured at diverse content of nanoparticles and flow rates showing that the pumping power was enhanced by the incorporation of nanoparticles.

Keywords: Viscosity; Tribological behavior; Physicochemical characteristic; Nano-ZnO; Nano-MoS₂; Diesel oil-based nanofluid

1 **Nomenclature**

2 A Cross section area (m^2)

3 D Pipe diameter (m)

4 f Friction factor

5 Q Flow rate ($\text{m}^3 \text{s}^{-1}$)

6 t Time (s)

7 u Velocity (m s^{-1})

8 V Volume (m^3)

9 Re Reynolds number

10 L Length (m)

11 wt Nanoparticle weight fraction (%)

12 m Mass (kg)

13 T Temperature ($^{\circ}\text{C}$)

14 d Diameter (m)

15 M Molecular mass (kg mol^{-1})

16 N Avogadro number (mol^{-1})

17 **Greek letters**

18 ν Kinematic viscosity ($\text{mm}^2 \text{s}^{-1}$)

19 ρ Density (kg m^{-3})

20 φ Volume fraction (%)

21 **Subscripts**

22 th Theoretical

23 exp Experimental

24 bf Base fluid

1 nf Nanofluid
2 np Nanoparticle

3 **1. Introduction**

4
5 The term nanofluid refers to the stable distribution of low concentrations of nanoparticles
6 (NPs) with sizes ranging from 1 to 100 nm in a liquid [1, 2]. Nanofluids have been widely used
7 due to their greater thermal behaviors in comparison with the base fluid. Furthermore, having
8 more substantial surface areas than micro-sized particles and letting more inconsiderable erosion
9 in comparison with the traditional liquid-solid blends can be mentioned as the benefits of
10 nanofluids [3-8]. This exceptional improvement in characteristics is associated with the size and
11 shape of the NPs and their nature [9]. Several kinds of nanoparticles including metallic and
12 nonmetallic, with various forms and dimensions, were utilized to prepare nanofluids, and some
13 inspiring outcomes have been evidenced; however, the usage of nanoparticles may lead to
14 accretion in viscosity of the nanofluids owing to their viscose nature [10-22]. Recently, ZnO NPs
15 have attracted remarkable research attention owing to their capacity for advancing
16 thermophysical qualities, tribological properties, and good dispersion traits [23-29]. MoS₂ NPs
17 have exhibited excellent anti-wear, mechanical, and thermophysical properties among various
18 types of nanoparticles. Their lubricity characteristics associate with the inherent structure namely
19 the vast space and weak Van der Waals forces that lead them to move easily on each other [30-
20 32].

21 Numerous comparisons have been performed to examine the anti-wear features and thermal
22 performances of nano-MoS₂ additive oil-based fluids. The outcomes confirmed that the
23 tribological and thermal aspects of the prepared nanofluids are strikingly enhanced by adding
24 nano-MoS₂ particles to the utilized fluid [30, 33-35]. Dinesh et al. [36] scrutinized the
25 tribological and thermophysical characteristics of engine oil comprising MWCNT and Zinc
26 Oxide NPs. The outcomes demonstrated that MWCNT and Zinc Oxide NPs were able to
27 advance the operational facets of the engine oil. Esfe et al. [37] analyzed the rheological
28 attributes of engine oil utilizing MWCNT and ZnO NPs. The conclusions showed that the
29 usability of the nano-additives in the engine oil can decrease the damages to motor sections in a
30 cold start of the vehicle. The tribological properties of different base oils using ZnO and CuO
31 NPs as additives have been studied by Alves et al [38]. They reported that by adding
32 nanoparticles to conventional oil, the anti-frictional features could be remarkably enhanced. A

1 more constant tribo-film had made on the worn surface, which was adequate for the further
2 decreased friction. Cabaleiro et al. [39] assessed the thermal features of multiple TiO_2
3 nanofluids. They observed that the prepared nanofluids increased thermal conductivity in
4 comparison with pure fluids. Probes of the lubricating, rheological, and thermal performances of
5 ZnO NPs demonstrated that adding nano zinc oxide particles to the pure fluid can develop the
6 mentioned traits [40-46]. Hu et al. [47] conducted a tribological comparison between three
7 different types of MoS_2 in various greases. The results explicated that any MoS_2 enhanced the
8 wear resistance of the three greases in most cases under the chosen measurement conditions.
9 Zawawi et al. [48, 49] studied thermal conductivity and viscosity behaviors of three diverse
10 mixtures of nanoparticles in the base lubricant (PAG composite nano-lubricants) at diverse
11 nanoparticle volume levels and temperatures. They found that the usage of nanoparticles in the
12 pure lubricant improved the thermophysical traits such as thermal conductivity and dynamic
13 viscosity. Coelho et al. [50] analyzed the thermophysical qualities of CuO nanofluids. The results
14 declared that both permittivity and electrical conductivity developed with the addition of nano-
15 CuO particles. Ding et al. [51] conducted a study for understanding the tribological features of
16 silica NPs water-based lubricants. They published that the silica NPs can significantly improve
17 the tribological performances when added to the base lubricant. Empirical research of the
18 thermal characteristics of Al_2O_3 /water nanofluid proved that adding Al_2O_3 NPs as an additive
19 can substantially raise the thermal traits of the nanofluid [52-56]. Karimi et al. [57] estimated the
20 thermal conductivity acts of NiFe_2O_4 nanofluids at diverse concentrations. They noticed that the
21 thermal conductivity of the samples raised with the increasing temperature and content. Minea et
22 al. [58] conducted a study to compare the thermophysical qualities of diverse nanofluids. The
23 outcomes manifested that adding alumina to the ionic liquid can exceptionally enhance
24 thermophysical properties. Research performed by Zhengfeng et al. [59] proved that the addition
25 of three kinds of nano-montmorillonite as additives in the grease can enhance the lubricity
26 attributes. Lou et al. [60] researched to examine the lubricity aspects of the Al_2O_3 oil-based
27 nano-lubricants. The outcomes exposed that adding nano- Al_2O_3 particles to the pure oil can
28 notably enhance tribological properties; moreover, the pure oil containing 0.1 wt.% nano- Al_2O_3
29 particles had the lowest friction coefficient. Grecov et al. [61-66] investigated the effect of
30 cellulose and liquid crystals as an additive on the tribological and rheological properties of both
31 aqueous-based and oil-based lubricants. The results proved that the used additives had great

potential in friction reduction applications. Wu et al. [67] prepared MoS₂ nanosheets decorated by zinc borate (ZB) NPs and applied them as additives to assess the anti-frictional behavior of lubricating oil, confirming that they can dramatically advance the tribological characteristics. Sanukrishna et al. [68] examined the impressions of nano-TiO₂ particles (0.07~0.8% volume fractions) on rheological properties and thermal conductivity on PAG nano-lubricant at diverse temperatures, showing that the utilized nanoparticles can develop the examined properties. Sharif et al. [69] studied thermophysical behaviors of the Al₂O₃/polyalkylene glycol nano-lubricants at different content of additives and temperatures exhibiting that the measured quantities enhanced with utilizing the additives. Khairul et al. [70] studied the stability and thermal characteristics of different prepared nanofluids. They showed that the efficiency of the system developed with the usage of the nanoparticles. Jabbari et al. [71] reviewed the thermophysical qualities of various nanofluids, confirmed that the thermophysical attributes of nanofluids increased with raising nanoparticle volume fraction.

According to the conducted literature review, the preponderance of examinations in the aforementioned area announces a positive impact on the rheological, anti-friction, and thermal features of different types of additives. Based on the investigations in the field of nanofluids, comprehensive examinations have been carried out on nanofluids namely turbine meter oil, engine oil, grease, water-based nanofluids, and other nanofluids, while limited consideration has been paid to the area of diesel oil. Consequently, in this article, the impact of ZnO and MoS₂ NPs on viscosity, tribological, and physicochemical qualities were studied. It is worth stating that this work is a continuation of the previous one [72] to complete the characterization and demonstrate the potential of nano-lubricants considering different measurements.

In the current investigation, diesel oil-based nanofluids were prepared using a two-step preparation technique with 0.1, 0.4, and 0.7 wt.% of ZnO and MoS₂ NPs, and the impact of nanoparticle concentration on the viscosity, tribological, and physicochemical features of the nanofluids was analyzed.

2. Experimental materials and methods

2.1 Materials

Zinc oxide (ZnO) and molybdenum disulfide (MoS₂) as the precursor, SAE-40 monograde diesel engine oil as the core fluid, and Triton X-100 as the surfactant were procured from US

Research-Nanomaterials, Sigma-Aldrich, Pars oil co, and Samchun, respectively. Table 1 presents the main features of the nanoparticles from the manufacturer data. Characteristics of the base fluid are shown in Table 2. SEM characterization (Zeiss, Germany) was performed for the analysis of ZnO and MoS₂ NPs. The crystalline form of the used nanoparticles was examined using powder X-ray diffraction (XRD, PHILIPS-PW1730, Netherlands) with Cu-K α radiation (λ = 0.14056 nm) at room temperature. The XRD patterns were performed at room temperature ranging in $2\theta = 7 - 80^\circ$ at a rate of 3° min^{-1} . The Debye–Scherrer’s formula was applied to compute the crystallite size of the nanoparticles, based on the XRD schema [73]:

$$D = \frac{0.9 \cdot \lambda}{\beta(\cos\theta)}$$

(1)

Where D , λ , β , and θ are the particle size perpendicular to the regular line of plane, the wavelength of X-ray, the entire width at the half summit of the diffraction peak, and the Bragg angle of the peak.

Table 1 Properties of the nanoparticles.

Properties	ZnO	MoS ₂
Color	White	Gray/Black
Purity (%)	99.9	99
Density (g/cm ³)	5.6	5.06
Size (nm)	30	90

Table 2 Characteristics of the diesel oil.

Base Fluid	Physical properties	Value
Monograde diesel oil (SAE-40)	Pour point, °C	-17.8
	Flash point, °C	238
	Density, Kg/cm ³ at 15 °C	0.893
	Kinematic viscosity, cSt at 40 °C	162.53
	Kinematic viscosity, cSt at 100 °C	14.62
	Viscosity Index (VI)	86.85

2.2 Preparation of nanofluids

The nano-ZnO and nano-MoS₂ particles were added to the diesel oil at 0.1, 0.4, and 0.7 wt.%. The nanofluids were prepared at different concentrations from 0.02 wt.% to 0.8 wt.%; however, there were no conspicuous differences between the results for each test at the concentration below the 0.1 wt.%. The most significant reason for this phenomenon is the fact that because of the high viscosity of the base diesel oil, nanoparticles could not strikingly affect the investigated parameters at lower concentrations—that is— below the 0.1 wt.%. To possess satisfying dispersibility, Triton X-100 (mass proportion of 1 to 2 with nanoparticle) as the surfactant was poured into the nanofluid mixture. The required value of nanoparticles and surfactant were accurately balanced employing a precision electronic balance and mixed with the diesel oil. The suspension was mixed using a mechanical stirrer at 900 rpm for about 3 hours and was agitated with an ultrasonic agitator (Parsonic 2600s, Iran) for about 45 min to provide a stable nanofluid. The sonication operated at a frequency of 28 kHz and a nominal power of 70 W at room temperature. Multiple concentrations were prepared to study the influence of the nanoparticle content.

2.3 Kinematic viscosity analysis

The kinematic viscosity was assessed based on ASTM D445. The kinematic viscosity was assessed using an Opaque viscometer (Accuracy: $\pm 0.3\%$) at atmospheric pressure. The viscometer bath was employed to control the temperature. All analyses were conducted three times. Kinematic viscosity of the prepared nanofluids was discovered at 40°C – 100°C.

2.4 Tribological analysis

The tribological features of the produced nanofluids at various concentrations were assessed and compared to the base diesel oil using a pin-on-disc tribometer based on the ASTM G99. The tribological experiments were carried out at 25°C with a sliding velocity of 150 rpm and a weight of 75 N. The analyses were carried out under various loading bars varying from 20 N to 75 N; however, because of the high viscosity of diesel oil, lower loading bars could not affect, and significant change was not seen in the recorder COF values. Thus, 75 N was considered as the loading bar. The sliding length was 1000 m. The material of the pins was hardened bearing steel (AISI 52100). The diameter and length of the pins were 5 mm and 50 mm, respectively. Before the tribological examination, the pin and disc were purified utilizing acetone. The normal force was applied applying load rings. The specimen is rotated at a selected speed. The rotation of the

sample and the sample holder were controlled by the motor. The examinations were done using the prepared nanofluids, and outcomes were compared with the pure diesel fluid. The friction coefficient values were reported; furthermore, the surface roughness R_a was measured. All tests were replicated at least three times, and the average value of each was determined.

2.5 Friction factor determination

The friction factor and the pressure drop of nano-lubricants in a copper tube were measured using an experimental setup described as follows. The system consisted of a pump to transport the working fluids at different velocities, a fluid tank, valves, pressure gauges, and a flow meter. Fig. 1 exhibits the schematic of the system.

Fig. 1. Design of the laboratory device.

3. Data and uncertainty analysis

The theoretical friction factor (f) for laminar flow and Reynolds number are obtained as [74, 75]:

$$f = \frac{64}{Re}$$

(2)

$$Re = \frac{uD}{\nu}$$

(3)

where D , u , ν and are the diameter of the pipe as a specific length, velocity, and kinematic viscosity, and Re is Reynolds number. Velocity and flow rate circumscribed by Eqs. (4) and (5), sequentially [76].

$$u = \frac{Q}{A}$$

(4)

$$Q = \frac{V}{t}$$

(5)

where t , V , A , Q and are time, volume, the cross-section area of the pipe, and flow rate.

Theoretical (ΔP_{th}) pressure difference was defined by Eq. (6) [77].

$$\Delta P_{th} = f \frac{L}{D} * \frac{\rho u^2}{2}$$

(6)

L and ρ are the pipe length and density of the fluid.

The pumping power was determined by utilizing Eq. (7).

$$W = Q \Delta P_{exp}$$

(7)

Considering the devices employed in this research have various precision and the parameters were estimated with these tools possess errors, it is essential to examine the impact of analysis error on these outcomes. If P is a function of empirical variables such as $x_1, x_2, x_3, \dots, x_n$, the subsequent formula is applied to assess the determination error of the parameter x_i [78]:

$$U_{P_i} = \frac{x_i}{P} \frac{\partial P}{\partial x_i} u_{x_i}$$

(8)

where x_i is the assessable quantity and u_{x_i} is the determination error. The highest error of parameter P is determined by merging the error of per parameter x_i utilizing the subsequent formula:

$$U_P = \pm \left\{ \left(\frac{x_1}{P} \frac{\partial P}{\partial x_1} u_{x_1} \right)^2 + \left(\frac{x_2}{P} \frac{\partial P}{\partial x_2} u_{x_2} \right)^2 + \dots + \left(\frac{x_n}{P} \frac{\partial P}{\partial x_n} u_{x_n} \right)^2 \right\}^{1/2}$$

(9)

As stated earlier, the Reynolds number is determined as $Re = \frac{uD}{\nu}$, and the generated error from the Reynolds number is proved as follows:

$$U_{Re} = \sqrt{(U_u)^2 + (U_D)^2 + (-U_\nu)^2} \quad (10)$$

Given that $u = \frac{Q}{A}$, U_U is computed as follows:

$$U_U = \sqrt{(U_Q)^2 + (-U_A)^2} \quad (11)$$

Additionally, the generated error by the volumetric flow rate is determined as $Q = \frac{V}{t}$ that is defined by Eq. (12).

$$U_Q = \sqrt{(U_V)^2 + (-U_t)^2} \quad (12)$$

The error of the friction factor ascertainment is similar to the error correlated with the Reynolds number.

$$U_f = U_{Re} \quad (13)$$

Hence, the highest friction factor error in the analyses reached 1.1%.

Errors for all measured parameters are calculated as follows:

The mass of base fluid: $U_{m_{bf}} = \pm \frac{0.001}{98.6} = \pm 1.014 \times 10^{-5}$

The mass of nanoparticle: $U_{m_{np}} = \pm \frac{0.001}{0.2} = \pm 5 \times 10^{-3}$

The nanoparticle weight fraction: $U_{wt} = \pm [U_{m_{bf}}^2 + U_{m_{np}}^2]^{1/2} = \pm 5 \times 10^{-3}$

The temperature: $U_T = \pm \frac{0.02}{40} = \pm 5 \times 10^{-4}$

The kinematic viscosity: $U_\nu = \pm \frac{0.02}{40} = \pm 5 \times 10^{-4}$

4. Results and discussion

4.1 Materials: characterization

The SEM pictures of the nano-ZnO and nano-MoS₂ particles are displayed in Fig. 2. Based on the SEM pictures, the nano-ZnO and nano-MoS₂ particles have a nearly spherical form and platelet-like shape with an average diameter of 30 nm and 90 nm, respectively. The XRD

patterns of the nano-ZnO and nano-MoS₂ particles are displayed in Fig. 3. The XRD pattern of the ZnO NPs shows peaks at $2\theta = 31.88, 34.58, 36.43, 47.73, 56.73, 62.93, 66.83, 68.03,$ and 69.13 , which can be classified to the (100), (002), (101), (102), (110), (103), (200), (112) and (201) planes of ZnO. All diffraction peaks were in arrangement with the diffraction data of the standard card (JCPDS card number 36-1451) [79]. The XRD pattern of the MoS₂ NPs displays diffraction peaks at $2\theta = 14.63, 29.18, 32.88, 39.73, 44.38, 50.13, 60.48$ and 70.23 matching to the (002), (004), (100), (103), (104), (105), (112), and (200) crystal planes of the MoS₂ structure according to the source data of JCPDS card number 37-1492 [80]. No impurity peaks were identified. The crystallite sizes of ZnO and MoS₂ calculated according to the principal peak breadth in the XRD schema by Eq. (1) were 14.2 nm and 32.6 nm, respectively. The nanoparticles are presented with an agglomeration of several crystals; thus, in most cases, the average diameter of nanoparticles is higher than the crystallite size. Comparing the average diameter and crystallite size of nanoparticles, it can be concluded that ZnO NPs are more agglomerated.

Fig. 2. SEM images of (a) ZnO NPs, (b) MoS₂ NPs.

Fig. 3. XRD patterns of (a) ZnO NPs, (b) MoS₂ NPs.

4.2 Viscosity

Fig. 4. depicts the impact of the ZnO and MoS₂ NPs concentration and temperature on the kinematic viscosity of the diesel oil, at 40°C – 100°C. According to Fig. 4, it can be seen that the kinematic viscosity of all specimens including ZnO and MoS₂ NPs, has increased concerning the pure diesel oil. The increase was more substantial at greater concentrations because of the agglomeration of the increase in nanoparticles. While the temperature rises, the kinematic viscosity of all specimens was reduced since the intermolecular strengths are weakened by increasing the temperature. At each measured temperature, ZnO nanofluids showed higher viscosity values than diesel oil comprising nano-MoS₂ particles since the ZnO nanofluids are

more stable and the nano-ZnO particles are more coherent compared to the MoS₂ nanofluids. The maximum viscosity increment was obtained at 0.7 wt.% and 100 °C for both prepared nanofluids. Considering the results, it can be concluded that the ZnO nanofluids were more resistant to move in comparison with the MoS₂ diesel oil-based nanofluids.

Fig. 4. Variation of kinematic viscosity of diesel oil containing ZnO and MoS₂ NPs at different concentrations with temperature.

One of the commonly utilized formulas for evaluating the relation between the viscosity and temperature of the manufacturing oils is Walther function, which is characterized by Eq. (14) [81]:

$$W = \log(\log(v + \varepsilon)) = b - n \log T$$

(14)

Where v , ε , and T are the kinematic viscosity (mm²/s), 0.7 for the kinematic viscosity greater than 2 mm²/s, the temperature (K), and b and n attribute to fixed parameters that are specified

based on the oil sort. The parameters b and n obtained from Eq. (14) for different concentrations of the ZnO and MoS₂ NPs are gathered in Table 3. According to the R² values, it can be asserted that the aforementioned model can properly determine the changes in the kinematic viscosity of the ZnO and MoS₂ NPs with temperature in the studied range.

Table 3 Parameters acquired from the fitting of alteration in kinematic viscosity with temperature using the Walther function.

Concentration (wt.%)	b	n	R ²
0	9.23	3.56	0.99
0.1 ZnO	9.07	3.49	0.99
0.4 ZnO	9.02	3.47	0.99
0.7 ZnO	8.99	3.46	0.99
0.1 MoS ₂	9.08	3.50	0.99
0.4 MoS ₂	9.04	3.48	0.99
0.7 MoS ₂	9.02	3.47	0.99

Einstein proposed the dependency of viscosity on the volume portion of the nanoparticles. Einstein assumed that the particles were in very dilute suspensions, namely solid spheres without interactions, and the improvement in the shear makes the rotary movement of the particles; thus, raises the dispersal viscosity. The Einstein formula, which can be utilized for suspensions having a particle volume portion below 0.01 ($\varphi < 0.02$) is depicted as follows [82]:

$$\eta_{nf} = \eta_{bf}(1 + 2.5\varphi)$$

(15)

$$\varphi = \frac{\left(\frac{m}{\rho}\right)_{np}}{\left(\frac{m}{\rho}\right)_{np} + \left(\frac{m}{\rho}\right)_{bf}}$$

(16)

where η , φ , m , and, ρ are viscosity, the volume fraction of nanoparticles, mass, and density.

Many equations have been proposed to calculate the relative viscosity ($\eta_r = \frac{\eta_{nf}}{\eta_{bf}}$) using the volume portion of nanoparticles which are noted in Table 4. In equations, the diameter of the molecule of base fluid (d_f) was defined by Eq. (17).

$$d_f = 0.1 \left(\frac{6M}{N\rho_f} \right)^{1/3} \quad (17)$$

Where M , N , and ρ_f are the molecular mass of the diesel oil, Avogadro number, and the mass density of diesel oil calculated at temperature $T_0 = 293$ K. d_p is the diameter of the nanoparticles.

The calculated values of the relative viscosity applying various models at different volume fractions of MoS₂ nanofluids are listed in Table 5. The alteration of the relative viscosity for MoS₂ nanofluids using different models and also the comparison between these models with the experimental data are presented in Fig. 5. As can be noticed in these figures, the theoretical models could not foretell the relative viscosity-mass fraction of the nanoparticles relation since these models did not ponder the size, shape, sort of the nanoparticles, sort of base fluids, and agglomeration of the nanoparticles, as well as temperature, while above-mentioned factors have a significant impression on the viscosity of nanofluids. As it is shown, the Einstein model unpredicted viscosity and this model was only developed for sphere nanoparticles. Numerous studies have also asserted similar conclusions considering different nanofluids, in which empirical results are not agreeable with the considered models [83-86].

Table 4 Classic equations to calculate the relative viscosity.

Author	Equation
Corcione [87]	$\frac{\eta_{nf}}{\eta_{bf}} = \frac{1}{1 - 34.87 \left(\frac{d_p}{d_f} \right)^{-0.3} \varphi^{1.03}}$
Sharma [88]	$\frac{\eta_{nf}}{\eta_{bf}} = \left(1 + \frac{\varphi}{100} \right)^{11.3} \left(1 + \frac{T_{nf}}{70} \right)^{-0.038} \left(1 + \frac{d_p}{170} \right)^{-0.061}$

Table 5 Relative viscosity of MoS₂ nanofluids at diverse volume fractions.

Nanoparticle		MoS ₂		
Weight fraction (wt.%)		0.1	0.4	0.7
Volume fraction (φ %)		0.018	0.071	0.126
Relative viscosity	Einstein	1.00045	1.00178	1.00315
	Corcione	1.00034	1.00138	1.0025
	Sharma	0.98299	0.98305	0.98311

Fig. 5. Relative viscosity as a function of volume fraction for MoS₂ nanofluids.

4.3 Friction characteristics

Figs. 6 and 7 illustrate the recorded friction coefficients (COFs) vs time for the base sample, ZnO, and MoS₂ diesel oil-based nanofluids with various contents (0.1 ~ 0.7 wt.%) at rotating speed of 150 rpm and applied load of 75 N. The mean values of the COFs are also shown in Fig. 8. The performance of diesel oil without and with nanoparticles was assessed. The outcomes reveal that all the samples lead to an initial short running-in period and the COF stabilizes almost 300 seconds after the starting of the tribological analysis. Other researchers [89-91] also noticed similar conclusions concerning different nanofluids proving that the continuance of the run-in phase is reliant on various factors of the contact surfaces such as geometrical, chemical, and physical; moreover, the capacity of the lubricating fluid to produce a proper tribo-film. It is

determined that the average COFs of the nanofluids diminished with the content ranging from 0.1 wt.% to 0.7 wt.%. Fig. 6 shows that the friction coefficient diminished when the content of nano-ZnO particles was under 0.4 wt.%. However, when the content exceeded 0.4 wt.%, the friction coefficient increased. On the other hand, Fig. 7 shows that the friction coefficient values decreased by adding MoS₂ NPs. Based on Figs 6, 7, and 8, it can be understood that the COF values steadily decreased for MoS₂ nanofluids while for the ZnO nanofluids decreased first and then, gradually increased. Considering Fig. 8, it can be concluded that MoS₂ diesel oil-based nanofluids had a better anti-friction behavior compared to the ZnO nanofluids both in lower concentrations and higher concentrations. The lowest final COF in this research happened at a concentration of 0.7 wt.% MoS₂ nanofluids and the optimal content for ZnO NPs was 0.4 wt.%. Shape, size, morphology, and the inherent attributes of the nanoparticles play a vital role to develop the lubrication qualities of the nanofluids. Nanoparticles with lower diameter act better in anti-friction purposes in comparison with the greater ones in diameter. Nonetheless, in this investigation, the most influential factor in enhancing the lubricity performance of the MoS₂ nanofluids is the intrinsic structural features of the nano-MoS₂ particles which lead them to move easily on each other. Thus, the layers are located unitedly with low molecular forces and can readily move over each other.

Fig. 6. Friction coefficient (COF) of the ZnO nanofluids with various contents as a function of time.

Fig. 7. Friction coefficient (COF) of the MoS₂ nanofluids with various contents as a function of time.

Fig. 8. Average friction coefficient (COF) values of the nanofluids at various concentrations.

Fig. 9 presents the characterizations of the wear mark on the rubbing superfcies equal to the sliding path. The assessed line roughness R_a values of the worn surfaces before and after the test at varying contents of ZnO and MoS₂ nanofluids are tabulated in Table 6. Based on the computed surface roughness (R_a), it can be discerned that the worn surfaces became smooth after the friction experiment due to the polishing impact of the diesel oil. Moreover, the roughness average of surfaces (R_a) decreased with the addition of the nanoparticles to the diesel oil. Having considered the pure diesel oil, the reduction of the R_a values after the test was 3.64%, 21.33%, and 11.14% for 0.1 wt.%, 0.4 wt.%, and 0.7 wt.% ZnO nanofluids, respectively. Whereas the reduction of the R_a values was 12.82%, 43.95%, and 60.75% for 0.1 wt.%, 0.4 wt.%, and 0.7 wt.% MoS₂ nanofluids. Hence, MoS₂ nanofluids showed lower R_a values compared to those of ZnO nanofluids proving better anti-friction behavior of the MoS₂ NPs.

Fig. 9. Profile curve of wear scar of (a) pure diesel oil, (b) 0.1 wt.% ZnO nanofluids, (c) 0.4 wt.% ZnO nanofluids, (d) 0.7 wt.% ZnO nanofluids, (e) 0.1 wt.% MoS₂ nanofluids, (f) 0.4 wt.% MoS₂ nanofluids, (g) 0.7 wt.% MoS₂ nanofluids.

Table 6 The measured surface roughness (R_a) values of the worn surfaces before and after the test at different concentrations of ZnO and MoS₂ nanofluids.

Concentration (wt.%)	R_a (before test)/ μm	R_a (after test)/ μm	$\Delta R_a/\mu\text{m}$
0 (pure diesel oil)	6.922	5.136	1.786
0.1 ZnO	6.971	5.120	1.851
0.4 ZnO	5.942	3.775	2.167
0.7 ZnO	6.395	4.410	1.985
0.1 MoS ₂	4.601	2.586	2.015
0.4 MoS ₂	5.016	2.445	2.571
0.7 MoS ₂	5.279	2.413	2.866

4.4 Friction factor

The friction factor and the experimental pressure difference values were acquired using the devised laboratory at diverse flow rates for different nanofluids and the results were compared to the pure diesel oil. The variety of the friction factor at the measured flow rates, inlet velocity, Reynolds number, kinematic viscosity, the difference between the experimental and theoretical pressures at various content of nanoparticles are listed in Table 7. According to the data listed in Table 7, it can be concluded that the friction factor and Reynolds number had an opposite relation since the kinematic viscosity of the samples was increased by adding the nano-additives. At each flow rate, higher amounts of the friction factor were seen in comparison with the base fluid without nano-additives because by increasing the content of the nanoparticles, the kinematic viscosity of the nanofluids increased. By comparing the experimental and theoretical pressure values, it can be concluded that the laboratory had a proper performance. Based on the acquired outcomes, the pressure drops in the tube increased with the rising in the Reynolds number or inlet velocity. Recently, researchers have stated the identical trend for other nanofluids [31, 92]. The friction factor was raised in all contents of ZnO and MoS₂ NPs with the highest increment of 8.2 % and 8.3% for ZnO and MoS₂ nanofluids happening at 0.7 wt.% with the lowest inlet velocity.

Table 7 The difference of friction factor at diverse flow rates for different nanofluids.

Concentration (wt.%)	$Q \times 10^5$ (m ³ /s)	u (m/s)	Re	$v \times 10^6$ (m ² /s)	f	ΔP_{th}	ΔP_{exp}	Disparity (%)
0 (pure diesel oil)	1.022	0.161	6.18	234.065	10.36	14654.91	14130	3.58
	1.211	0.190	8.82	194.273	7.26	14302.62	13680	4.35
	3.614	0.568	29.67	172.341	2.16	38029.63	36150	4.94
	5.311	0.835	43.59	172.341	1.47	55932.20	52900	5.42
0.1 ZnO	1.022	0.161	5.90	245.058	10.84	15331.46	14980	2.29
	1.211	0.190	8.41	203.804	7.61	14989.75	14250	4.94
	3.614	0.568	28.24	181.016	2.27	39959.97	38710	3.13
	5.311	0.835	41.50	181.016	1.54	58586.32	55400	5.44
0.4 ZnO	1.022	0.161	5.85	247.333	10.95	15479.58	14600	5.68
	1.211	0.190	8.32	205.830	7.69	15140.03	14520	4.10
	3.614	0.568	27.96	182.889	2.29	40292.60	38350	4.82
	5.311	0.835	41.08	182.889	1.56	59318.58	57880	2.43
0.7 ZnO	1.022	0.161	5.71	253.322	11.21	15839.33	14830	6.37
	1.211	0.190	8.13	210.767	7.87	15486.79	14450	6.69
	3.614	0.568	27.31	187.248	2.34	41152.09	36505	11.29
	5.311	0.835	40.12	187.248	1.60	60809.62	57540	5.38
0.1 MoS ₂	1.022	0.161	5.95	243.190	10.76	15218.06	14725	3.24
	1.211	0.190	8.47	202.245	7.56	14891.01	14100	5.31
	3.614	0.568	28.46	179.629	2.25	39607.22	37970	4.13
	5.311	0.835	41.83	179.629	1.53	58204.90	56980	2.10
0.4 MoS ₂	1.022	0.161	5.87	246.436	10.91	15421.96	14750	4.36
	1.211	0.190	8.36	205.024	7.66	15079.92	14265	5.40
	3.614	0.568	28.07	182.141	2.28	40113.88	38985	2.81
	5.311	0.835	41.25	182.141	1.55	58934.26	57655	2.17
0.7 MoS ₂	1.022	0.161	5.70	253.585	11.22	15851.55	15150	4.43
	1.211	0.190	8.12	210.872	7.88	15504.60	15110	2.55
	3.614	0.568	27.30	187.278	2.34	41147.15	39880	3.08
	5.311	0.835	40.12	187.278	1.60	60802.32	58600	3.62

Fig. 10 exhibits the change of pumping power based on flow rates at various contents. Considering Fig. 10, it can be comprehended that the pumping power was enhanced by adding the nano-additives to the base fluid, as expected. The reason for this phenomenon is the fact that the pressure drops increased by increasing the flow rate, hence the increment in the pressure drop caused an augmentation in pumping power.

Fig. 10. Change of pumping power as a function of flow rate at different concentrations.

5. Conclusion

The effects of ZnO and MoS₂ NPs on the viscosity, tribological, and physicochemical attributes of diesel oil were evaluated. The following outcomes can be presented:

1. It was noticed that the kinematic viscosity and viscosity index of the samples raised with the incorporation of nanoparticles. Furthermore, the rise in kinematic viscosity grew by rising nanoparticle concentration. At each concentration of nanoparticles, ZnO nanofluids had higher kinematic viscosity compared to the MoS₂ nanofluids. The maximum rise in the kinematic viscosity was seen at 0.7 wt.% for each nanofluid. Walther equation

foretells well the kinematic viscosity–temperature relation. The selected theoretical models do not predict the relative viscosity enhancement with nanoparticle volume fraction.

2. Having fewer COF values and lower the roughness average of surfaces (R_a), it can be inferred that the ZnO and MoS₂ nanofluids had more desirable tribological characteristics. The optimal content of ZnO and MoS₂ NPs were 0.4 wt.% and 0.7 wt.%, respectively.
3. Evaluating the effect of the nanoparticles content on friction factor at the measured flow rates and inlet velocities showed that the friction factor increased by adding the NPs to the base fluid. In addition, the pumping power was enhanced by the incorporation of nanoparticles.

6. References

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