

# Analysis of an anaerobic digestion model in landfill with mortality term

S. Ouchtout, Z. Mghazli, J. Harmand, Alain Rapaport, Z. Belhachmi

► **To cite this version:**

| S. Ouchtout, Z. Mghazli, J. Harmand, Alain Rapaport, Z. Belhachmi. Analysis of an anaerobic digestion model in landfill with mortality term. 2019. hal-02265820

**HAL Id: hal-02265820**

**<https://hal.archives-ouvertes.fr/hal-02265820>**

Submitted on 12 Aug 2019

**HAL** is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers.

L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.

# Analysis of an anaerobic digestion model in landfill with mortality term

S. OUCHTOUT

Interdisciplinary Laboratory for Natural Resources and Environment

Ibn Tofaïl University, Kénitra, Morocco

and

Laboratory of Mathematics, Informatics and Applications

University of Haute-Alsace, Mulhouse, France

Z. MGHAZLI

Interdisciplinary Laboratory for Natural Resources and Environment

Ibn Tofaïl University, Kénitra, Morocco

J. HARMAND

LBE

Univ. Montpellier, INRA, Narbonne, France

A. RAPAPORT\*

MISTEA

Univ. Montpellier, INRA, Montpellier SupAgro, Montpellier, France

Z. BELHACHMI

Laboratory of Mathematics, Informatics and Applications

University of Haute-Alsace, Mulhouse, France

August 12, 2019

## Abstract

We study a mathematical model of anaerobic digestion with biomass recirculation, dedicated to landfill problems, and analyze its asymptotic behavior. We show that the global attractor is composed of an infinity of non-hyperbolic equilibria. For non-monotonic growth function, this feature has impacts on the performances of the bioprocess.

**Key-words.** bioprocesses, biogas production, ordinary differential equations, Barbalat's Lemma, Center Manifold Theorem.

**AMS classification.** Primary: 37N25, 93D20; Secondary: 34C11, 34D35.

---

\*corresponding author

# 1 Introduction

The anaerobic digestion process is a natural biological process of decomposition of organic matter by microorganisms (bacteria) that are activated under anaerobic conditions, that is to say without oxygen. It is characterized by a succession of complex reactions both in parallel and in series. In the long term, the organic matter is transformed into biogas, a mixture mainly composed of methane and carbon dioxide. The main stages of this process are hydrolysis, acidogenesis, acetogenesis and methanogenesis. Models such as the "ADM1" allow a detailed description of this process, cf. [14]. However, such complex models are not well suited for mathematical analysis. It is why a number of simpler models have been investigated in the literature over these last years [8, 11, 22, 12, 20, 21]. When dealing with the digestion of wastewater, it is recognized that the limiting step is the methanogenesis. In such a case, modelling include one-, two- or three-steps models. Of particular interest is the model by Bernard et al., 2001 ([6]) which proposes to model the anaerobic digestion process as a two-steps process involving both the acidogenesis (using a Monod kinetics) and the methanogenesis processes (using a Haldane kinetics). This model, for which the mathematical analysis has been conducted by Benyahia et al., 2012, cf. [5], is very popular, notably for control purposes, since it remains of moderate complexity while being quite easy to calibrate to predict process behaviour with satisfying performances, [9, 2] or still [15]. It has also been the basis for proposing a systematic way to link simple models to ADM1 predictions, cf. [14]. In this work, we consider the model proposed by M. Rouez [22]. He is considering the anaerobic process in two steps that are Hydrolysis and Methanogenesis. Such description is well suited as long as the acidogenesis is not the limiting step, which is the case for the digestion of solid waste, as considered in this paper. In landfills, there is always a part of the raw material that has no access to oxygen. In addition, we consider here mortality. When a biological process is running in continuous mode, it is the rule rather than the exception not to consider mortality terms, cf. for instance [16] or [17], and such term can have a great influence on the process behaviour, cf. for instance [13]. However, when working in a closed environment - as it is the case in landfills - the mortality can no longer be neglected: part of the mortality of microorganism then returns to the slowly biodegradable material, itself being further hydrolyzed in rapidly biodegradable material. The role of the mortality term and the growth function on the performances of the overall process, notably in terms of biogas production, is of primer importance in landfill applications. The main objective of the present paper is to give deeper insights and predictions of this role with the help of a mathematical model.

The paper is organized as follows. In the next section, model and assumptions are presented and discussed. Then, the dynamics is mathematically analyzed in the following section. In particular, we show that there exists an infinity of equilibria to which solutions converge, depending on initial conditions. Finally, numerical simulations with different value of the death rate and various initial conditions are presented in a dedicated section, before discussions and

conclusions are drawn.

## 2 Model and assumptions

The hydrolysis step of transformation of organic matter of concentration is an important phase in the biodegradation process because it is a substrate preparation step. It is modeled by the first order equation

$$\frac{dX}{dt} = -K_h X \quad (1)$$

where  $X(t)$  is the concentration of organic matter at time  $t$  and  $K_h$  is the hydrolysis constant.

On the other hand, the methanogenesis is the last step in the anaerobic digestion process and leads to the production of biogas. Based on the principle of mass conservation and the fundamental relations of biological kinetic (that are the growth rate of bacteria and the use rate of the substrate), this step is modeled as follow

$$\begin{cases} \frac{dS}{dt} = -\frac{1}{Y}\mu(S)B \\ \frac{dB}{dt} = (\mu(S) - K_d)B \\ \frac{d[CO_2]}{dt} = (1 - f_2)\frac{1 - Y}{Y}\mu(S)B \\ \frac{d[CH_4]}{dt} = f_2\frac{1 - Y}{Y}\mu(S)B \end{cases} \quad (2)$$

where  $S(t)$  and  $B(t)$  represent the concentrations of soluble organic matter and methanogenic biomass at time  $t$ . The symbols  $\mu$ ,  $Y$ , and  $K_d$  are successively the specific growth rate, the rate of use of the substrate and the mortality rate. Parameters  $f_2$  and  $(1 - f_2)$  are the stoichiometric coefficients, representing the parts of soluble organic matter transformed into carbon dioxide and methane during methanogenesis step, of cumulative concentrations at time  $t$  denoted by the variables  $[CO_2](t)$  and  $[CH_4](t)$ .

In the present work, we consider that during the process the death of methanogenic bacteria constitute a substrate (given by a proportion  $\alpha K_d B$  of the death biomass, where  $\alpha$  is a constant parameter) to the hydrolysis step, which brings a source term in the equation (1). This means that only a fraction of the biomass mortality is used again as a substrate in the methanogenesis step, as described in [6, 4, 10]). This couples the hydrolysis and methanogenesis steps as represented in the model below, which makes the mathematical analysis of the model not straightforward. In addition, we introduce the stoichiometric coefficients  $f_1$  and  $(1 - f_1)$  to represent the parts of biomass  $X$  transformed into organic matter  $S$  and carbon dioxide  $CO_2$  during the "hydrolysis / acidogenesis" process. The overall process is depicted on Figure 1.

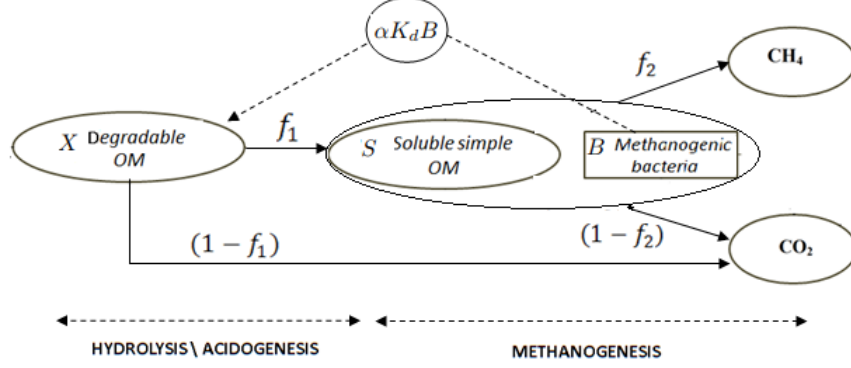


Figure 1: Overall scheme of the anaerobic degradation of organic matter

It is modeled by the following dynamic system (that was already proposed by Rouez in[22] but for a specific function  $\mu$  and coefficient  $\alpha = 1$ ).

$$\begin{cases} \frac{dX}{dt} = -K_h X + \alpha K_d B \\ \frac{dS}{dt} = f_1 K_h X - \frac{1}{Y} \mu(S) B \\ \frac{dB}{dt} = (\mu(S) - K_d) B \end{cases} \quad (3a)$$

$$\begin{cases} \frac{d[CO_2]}{dt} = (1 - f_1) K_h X + (1 - f_2) \frac{1 - Y}{Y} \mu(S) B \\ \frac{d[CH_4]}{dt} = f_2 \frac{1 - Y}{Y} \mu(S) B \end{cases} \quad (3b)$$

The total biogas  $G(t)$  produced by the process at time  $t$  is the sum of carbon dioxide  $[CO_2](t)$  and methane  $[CH_4](t)$ . Notice that in absence of initial substrate  $S$  or initial biomass  $B$ , the model (2) does not produce any biogas. We shall see that this is not the case for model (3), provided that there is initial matter  $X$ .

The specific growth rate function satisfy the following properties.

**Hypothesis 1.** *The function  $\mu$  is  $C^1$  with  $\mu(0) = 0$  and  $\mu(S) > 0$  for  $S > 0$ .*

Many functions that satisfy this hypothesis are met in the literature. The most popular ones are (see Figure 2) :

1. the Monod law [18], which is related to a growth saturation or limitation :

$$\mu(S) = \frac{\mu_{max} S}{K_S + S} \quad (4)$$

where  $\mu_{max}$  is the maximum growth rate and  $K_S$  the half-saturation constant.

- the Haldane law [1], which is also characterized by an inhibition phenomenon for large values of the substrate concentration:

$$\mu(S) = \frac{\mu_m S}{K_S + S + \frac{S^2}{K_I}} \quad (5)$$

where  $K_I$  is the inhibition constant.

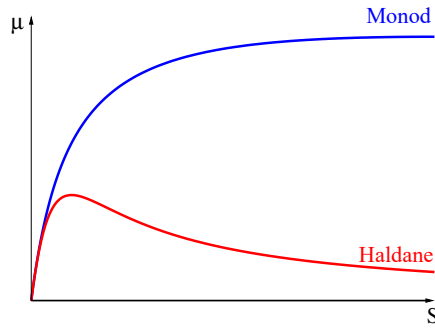


Figure 2: Graphs of Monod and Haldane functions

The Haldane expression is often considered to be more appropriate to the anaerobic process. Notice however that the Haldane function can be seen as a generalization of the Monod one on a fixed interval for large values of  $K_I$ .

**Hypothesis 2.** *Coefficients  $\alpha$ ,  $K_d$ ,  $Y$ ,  $f_1$  and  $f_2$  fulfill the following conditions.*

- The proportion of nutrient recycling  $\alpha$  cannot exceed 1

$$0 < \alpha \leq 1 \quad (6)$$

- The mortality rate  $K_d$  is a positive parameter which is below the maximum growth rate

$$0 < K_d < \max_s \mu(s) \quad (7)$$

- The rate of use of the substrate is a strictly positive parameter such that

$$0 < Y < 1 \quad (8)$$

- The stoichiometric coefficients parameters  $f_1$  and  $f_2$  are strictly positive and satisfy

$$0 < f_1 < 1 \quad \text{and} \quad 0 < f_2 < 1 \quad (9)$$

Condition (7) means that the choice of bacteria and operating conditions, which impact the growth and death rates (such as temperature, pH...), are such that the bacterial growth is possible. For convenience, we define the set

$$\mathcal{E} := \{s \in \mathbb{R}_+ ; \mu(s) \leq K_d\}$$

which has non-empty interior, under Hypotheses 1 and 2. For the Monod expression, one has

$$\mathcal{E} = [0, \lambda] \text{ with } \lambda = \frac{K_d K_S}{\mu_{max} - K_d}$$

and for the Haldane expression, the set  $\mathcal{E}$  has two connected components:

$$\mathcal{E} = [0, \lambda^-] \cup [\lambda^+, +\infty) \text{ with } \lambda^\pm = \frac{\mu_m - K_d \pm \sqrt{\Delta}}{2K_d/K_I} \quad (10)$$

where

$$\Delta = \mu_m^2 - 2\mu_m \cdot K_d + \left(1 - 4\frac{K_S}{K_I}\right) \cdot K_d^2$$

which is positive under Hypothesis 1.

### 3 Study of the asymptotic behavior

The dynamics (3) has a cascade structure. We thus begin by the study the asymptotic behavior of the sub-system (3a).

**Proposition 1.** *Under Hypotheses 1, 2, for any non-negative vector  $(X_0, S_0, B_0)$ , the solutions of system (3a) for the initial condition  $(X(0), S(0), B(0)) = (X_0, S_0, B_0)$  are non-negative, bounded and verify*

$$\lim_{t \rightarrow +\infty} X(t) = \lim_{t \rightarrow +\infty} B(t) = 0$$

and

$$\lim_{t \rightarrow +\infty} S(t) = S^* \leq S_0 + \frac{X_0 + \alpha B_0}{\alpha Y}$$

Moreover, when  $X_0$  or  $S_0$  is non null, one has  $S^* > 0$ .

*Proof.* On the edges of the positive orthant  $\mathbb{R}_+^3$ , one has

$$\begin{aligned} X = 0 &\Rightarrow \frac{dX}{dt} \geq 0 \\ S = 0 &\Rightarrow \frac{dS}{dt} \geq 0 \\ B = 0 &\Rightarrow \frac{dB}{dt} = 0 \end{aligned}$$

from which we deduce by uniqueness of solutions of the Cauchy problem that the solution  $(X(t), S(t), B(t))$  is non-negative when  $(X_0, S_0, B_0) \in \mathbb{R}_+^3$ .

We show now the system (3a) is dissipative. Consider the "storage" function

$$V(t) = X(t) + \alpha B(t) + \alpha Y S(t). \quad (11)$$

From equations (3a), one has

$$\frac{dV}{dt} = K_h(\alpha Y f_1 - 1)X. \quad (12)$$

By Hypothesis 2, one has  $\alpha Y f_1 < 1$  and as  $X(\cdot)$  is non-negative, we deduce that  $V$  is non-increasing. Being bounded from below by 0,  $V(t)$  converges to a limit  $V_\infty \geq 0$  when  $t$  tends to  $+\infty$ . This implies that the variables  $X(t)$ ,  $S(t)$  and  $B(t)$  are bounded. Moreover, one has

$$\frac{d^2V}{dt^2} = K_h(\alpha Y f_1 - 1)(-K_h X + \alpha K_d B)$$

from which we deduce that  $d^2V/dt^2$  is bounded and thus  $dV/dt$  is uniformly continuous on  $\mathbb{R}_+$ . By Barbalat's Lemma [3], we obtain that  $dV(t)/dt$  converges to 0 when  $t$  tends to  $+\infty$ . Therefore, we obtain

$$\lim_{t \rightarrow +\infty} X(t) = 0.$$

Similarly,  $d^2X/dt^2$  is bounded, thus  $dX/dt$  uniformly continuous and by Barbalat's Lemma,  $dX(t)/dt$  converges to 0 when  $t$  tends to  $+\infty$ , which gives

$$\lim_{t \rightarrow +\infty} B(t) = 0.$$

Finally, as  $V(t)$  converges to a limit when  $t$  tends to  $+\infty$ , we obtain

$$\lim_{t \rightarrow +\infty} S(t) = S^* = \frac{V_\infty}{\alpha Y}.$$

Let us show that  $S^*$  cannot be equal to 0 when  $X_0$  or  $S_0$  is non null. If not,  $S(t)$  has to tends to zero and therefore there exists  $T > 0$  such that  $\mu(S(t)) \leq f_1 Y \alpha K_d$  for any  $t > T$ . Then one has

$$\frac{d}{dt} (f_1 X(t) + S(t)) \geq 0, \quad t > T.$$

When  $f_1 X(0) + S(0) > 0$ , the variables  $X(\cdot)$ ,  $S(\cdot)$  cannot reach 0 in finite time (by uniqueness of the solutions of the Cauchy problem), and one has then  $f_1 X(t) + S(t) \geq f_1 X(T) + S(T) > 0$  for any  $t > T$ , which is in contradiction with the fact that  $f_1 X(t) + S(t)$  tends to 0 when  $t$  tends to  $+\infty$ .  $\square$

Let us now characterize the set of equilibria that can be reached by positive solutions.



**Proposition 2.** *Under Hypotheses 1, 2, the solution of (3a) for an initial condition in  $\mathbb{R}_+^3$  with  $X_0 > 0$  and  $B_0 > 0$  converges asymptotically to an equilibrium  $(0, S^*, 0)$  where  $S^* > 0$  belongs to  $\mathcal{E}$ .*

*Proof.* If there exists a solution of (3a) such that  $S(\cdot)$  converges asymptotically to  $S^* > 0$  that does not belong to  $\mathcal{E}$ , there exists  $T > 0$  such that one has

$$\mu(S(t)) - K_d > \eta := \frac{\mu(S^*) - K_d}{2}, \quad t > T,$$

but then the solution  $B(\cdot) > 0$  verifies

$$\frac{dB(t)}{dt} > \eta B(t), \quad t > T.$$

With standard comparison theorem for differential inequalities (see e.g. [23]), we conclude that  $B(\cdot)$  cannot converge asymptotically to 0, and thus a contradiction with the results of Proposition 1.  $\square$

The system (3a) admits an infinity of equilibria which are not hyperbolic. One cannot conclude about their stability by studying the single linearization of the dynamics. However, one has the following result.

**Proposition 3.** *Assume that Hypotheses 1 and 2 are fulfilled. For each steady state  $E = (0, S^*, 0)$  with  $S^* \in \text{int } \mathcal{E}$ , there exists an invariant one-dimensional manifold  $\mathcal{M}$  in  $\mathbb{R}_+^3$  such that any solution of (3a) with initial condition in  $\mathcal{M}$  converges asymptotically to  $E$ .*

*Proof.* Let us fix  $S^* > 0$  such that  $\mu(S^*) < K_d$  and consider the variable

$$Z(t) = f_1 X(t) + (S(t) - S^*) + \beta B(t)$$

with

$$\beta := \frac{\mu(S^*)/Y - f_1 \alpha K_d}{\mu(S^*) - K_d}.$$

A direct computation gives

$$\frac{dZ}{dt} = -\gamma(\mu(S) - \mu(S^*))B,$$

with

$$\gamma := \frac{K_d(1 - Y f_1 \alpha)}{Y(K_d - \mu(S^*))} > 0.$$

We can then write the system (3a) in  $\mathbb{R}_+^3$  equivalently on the domain

$$\mathcal{D} := \{(Z, X, B) \in \mathbb{R} \times \mathbb{R}_+^2; Z \geq f_1 X + \beta B - S^*\}$$

as follows

$$\frac{dZ}{dt} = -\gamma g(Z, X, B) \quad (13a)$$

$$\frac{d}{dt} \begin{bmatrix} X \\ B \end{bmatrix} = \underbrace{\begin{bmatrix} -K_h & \alpha K_d \\ 0 & \mu(S^*) - K_d \end{bmatrix}}_A \begin{bmatrix} X \\ B \end{bmatrix} + \begin{bmatrix} 0 \\ g(Z, X, B) \end{bmatrix} \quad (13b)$$

with

$$g(Z, X, B) := \left( \mu(S^* + Z - f_1 X - \beta B) - \mu(S^*) \right) B.$$

Notice that the matrix  $A$  is Hurwitz and  $g$  verifies  $g(0) = 0$  and  $Dg(0) = 0$ . We are then in position to apply the Center Manifold Theorem [7], which states that there exists an invariant manifold  $\mathcal{M}$  of dimension one that contains the equilibrium 0. Consider an initial condition in  $\mathcal{M}$ . We know from Proposition 1 that  $X(t)$  and  $B(t)$  converge to 0 when  $t$  tends to infinity, and that  $S(t)$  admits a limit. Consequently,  $Z(t)$  has to converge to a certain  $Z^*$  when  $t$  tends to  $+\infty$ , and  $(Z^*, 0, 0)$  is an equilibrium of (13) in  $\mathcal{M}$ . If  $Z^*$  is non null, there exists an orbit  $\{(\tilde{Z}(t), \tilde{X}(t), \tilde{B}(t)), t \in \mathbb{R}\}$  in  $\mathcal{M}$  that connects in forward time the equilibrium  $(0, 0, 0)$  to  $(Z^*, 0, 0)$ , that is with

$$\lim_{t \rightarrow -\infty} (\tilde{Z}(t), \tilde{X}(t), \tilde{B}(t)) = (0, 0, 0).$$

One has then

$$\lim_{t \rightarrow -\infty} \mu(S^* + \tilde{Z}(t) - f_1 \tilde{X}(t) - \beta \tilde{B}(t)) - \mu(S^*) = 0,$$

and thus there exists  $T < 0$  such that

$$\mu(S^* + \tilde{Z}(t) - f_1 \tilde{X}(t) - \beta \tilde{B}(t)) - \mu(S^*) < \eta := \frac{1}{2}(K_d - \mu(S^*)), \quad t < T$$

which implies that one has

$$\frac{d\tilde{B}(t)}{dt} < -\eta \tilde{B}(t), \quad t < T$$

in contradiction with  $\lim_{t \rightarrow -\infty} \tilde{B}(t) = 0$  (by standard comparison theorem for differential inequalities, see e.g. [23]).  $\square$

Propositions 2 and 3 together allow to state the following result.

**Corollary 1.** *Under Hypotheses 1 and 2, the set  $\{0\} \times \mathcal{E} \times \{0\}$  is a forward attractor of the dynamics (3a).*

Finally, let us consider the sub-system (3b).

**Proposition 4.** *Under Hypotheses 1, 2, for any non-negative vector  $(X_0, S_0, B_0)$ , the solutions of (3) verify*

$$\lim_{t \rightarrow +\infty} [CO_2](t) = a(X_0 + \alpha B_0) + b(S_0 - S^*) \quad (14)$$

$$\lim_{t \rightarrow +\infty} [CH_4](t) = c(X_0 + \alpha B_0) + d(S_0 - S^*) \quad (15)$$

where  $S^*$  is the asymptotic value of  $S(\cdot)$  and the coefficients  $a, b, c, d$  are positive numbers given by the following expressions.

$$a = \frac{1 - f_1 + f_1(1 - f_2)(1 - Y)}{1 - \alpha Y f_1}, \quad b = \frac{(1 - f_1)\alpha Y + (1 - f_2)(1 - Y)}{1 - \alpha Y f_1}$$

$$c = \frac{f_1 f_2(1 - Y)}{1 - \alpha Y f_1}, \quad d = \frac{f_2(1 - Y)}{1 - \alpha Y f_1}.$$

*Proof.* Consider again the function  $V$  defined in (11). Equation (12) gives

$$V(t) = V(0) + K_h(\alpha Y f_1 - 1) \int_0^t X(\tau) d\tau.$$

As  $V(\cdot)$  is bounded, we obtain

$$\int_0^t X(\tau) d\tau < +\infty. \quad (16)$$

From the first equation of (3a), we obtain also

$$X(t) = X(0) - K_h \int_0^t X(\tau) d\tau + \alpha K_d \int_0^t B(\tau) d\tau$$

and with (16), we obtain

$$\int_0^t B(\tau) d\tau < +\infty. \quad (17)$$

Then, from the last equation of (3a), one has

$$B(t) = B(0) + \int_0^t \mu(S(\tau))B(\tau) d\tau - K_d \int_0^t B(\tau) d\tau,$$

from which we get with (17)

$$\int_0^t \mu(S(\tau))B(\tau) d\tau < +\infty. \quad (18)$$

We conclude, from equations (3b), that  $[CO_2](t)$  and  $[CH_4](t)$  converges asymptotically to finite values.

The integration of equations (3a) between  $t = 0$  and  $t = +\infty$  leads to the following system of equations

$$\begin{aligned} K_h \int_0^{+\infty} X(\tau) d\tau - \alpha \int_0^{+\infty} \mu(S(\tau))B(\tau) d\tau &= X_0 + \alpha B_0 \\ Y f_1 K_h \int_0^{+\infty} X(\tau) d\tau - \int_0^{+\infty} \mu(S(\tau))B(\tau) d\tau &= Y(S^* - S_0) \end{aligned}$$

whose solution is unique, given by the expressions

$$\begin{aligned} \int_0^{+\infty} X(\tau) d\tau &= \frac{X_0 + \alpha Y(S_0 - S^*) + \alpha B_0}{K_h(1 - \alpha Y f_1)} \\ \int_0^{+\infty} \mu(S(\tau))B(\tau) d\tau &= Y \frac{f_1 X_0 + (S_0 - S^*) + \alpha f_1 B_0}{1 - \alpha Y f_1} \end{aligned}$$

because  $1 - \alpha Y f_1 > 0$  under Hypothesis 2, which provide the formulae (14), (15).  $\square$

**Remark 1.** *One can check that when  $B_0 = 0$ , there is no production of methane (as expected) because the trajectory stays on the half line*

$$\{(X, S, B); f_1 X + S = f_1 X_0 + S_0, B = 0\}$$

and one has then  $cX_0 + d(S_0 - S^*) = 0$ . The production of dioxide is then equal to  $(a + \alpha b)X_0$  whatever is  $S_0$ .

When the set  $\mathcal{E}$  is not connected, as an union of intervals  $\mathcal{E} = I_1 \sqcup I_2 \sqcup \dots$ , the state space can be split into a family  $\{\mathcal{B}_i\}$  of attraction basins of the subsets  $\{0\} \times I_i \times \{0\}$ . These basins conduct the system to different levels of performances. For instance, with the Haldane law, there are two basins  $\mathcal{B}^-$ ,  $\mathcal{B}^+$  leading to equilibria with  $S^*$  in  $[0, \lambda^-]$  or in  $[\lambda^+, +\infty)$ . The separating surface  $\mathcal{S}$  of  $\mathcal{B}^-$  and  $\mathcal{B}^+$  is numerically investigated in the next section.

## 4 Application

Proposition 4 shows that the production of the total biogas  $G$  is impacted by the final value  $S^*$  of the remaining soluble matter, which is itself related to the death rate  $K_d$  (as  $S^*$  belongs to the set  $\mathcal{E}$ ).

For the Haldane growth function, the process leads either to a relatively large production of biogas (when  $S^* < \lambda^-$ ) or to a relatively small production of it (when  $S^* > \lambda^+$ ), depending on the initial condition. The difference between these two situations get larger when the death rate  $K_d$  is small, differently to the Monod case which is more robust.

Because the Haldane function is often more realistic (and the Monod function can be seen as a particular case for large values of the parameter  $K_I$ ), we

$K_h$	$Y$	$f_1$	$f_2$	$\alpha$
0.176	0.05	0.7	0.76	0.9

Table 1:

present here simulations only for the Haldane one, with  $\mu_m = 0.3$ ,  $K_S = 160$  and  $K_I = 10$  and other model parameters reported in the following Table.

With these parameters, the corresponding Haldane function is plotted in Figure 3.

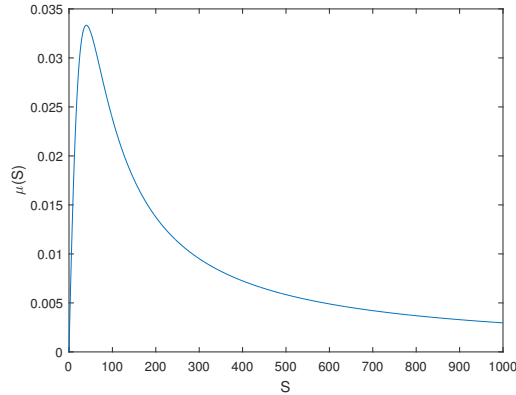


Figure 3: Graph of the Haldane function considered in the example

Let us fix the death rate  $K_d = 0.02$ . For such value, we obtain  $\lambda^- = 12.5$  and  $\lambda^+ = 127.4$  (see equations (10)). Consider  $S_0 = 0$  and  $B_0 = 2$ . Depending on the initial condition of  $X$ ,  $S$  converges either towards a value smaller than  $\lambda^-$  or larger than  $\lambda^+$ . Such a behaviour can be seen with five initial conditions of  $X$  in Figure 4 ( $X_0 = 340$  to  $X_0 = 360$  with an increment of 5). As expected, there is a sudden change on the asymptotic value of  $S$  when  $X_0$  passes a threshold: for  $X_0 = 340, 345$  and  $350$ ,  $S$  converges towards values smaller than  $\lambda^-$  while it converges towards values larger than  $\lambda^+$  for  $X_0 = 355$  and  $360$ .

As  $K_d$  increases,  $\lambda^-$  increases while  $\lambda^+$  decreases and for very small values of  $K_d$ ,  $\lambda^+$  may be very large. In Figure 5, we plotted the value of the threshold on  $X_0$  for which the asymptotic value  $S^*$  is under  $\lambda^-$  or over  $\lambda^+$  for a range of values of  $K_d$  between 0.005 and 0.03. One can observe that it is a decreasing function of the  $X_0$  threshold.

The biogas production can be seen as an increasing function of  $X_0$  as long as  $S$  converges under  $\lambda^-$  (since asymptotically there remains a low amount of

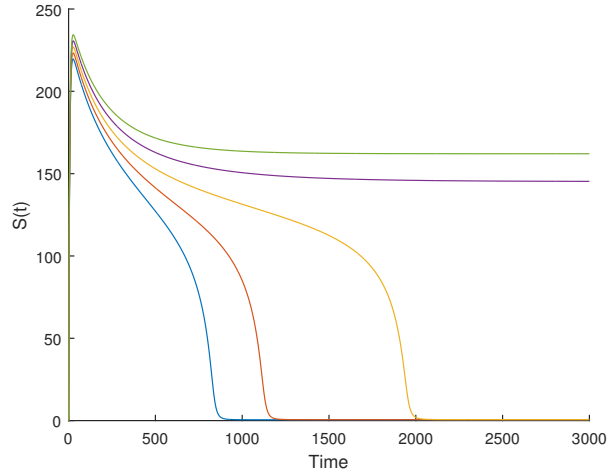


Figure 4: Graph of  $S(\cdot)$  for initial conditions  $X_0 = 340$  to  $X_0 = 360$  with a step of 5

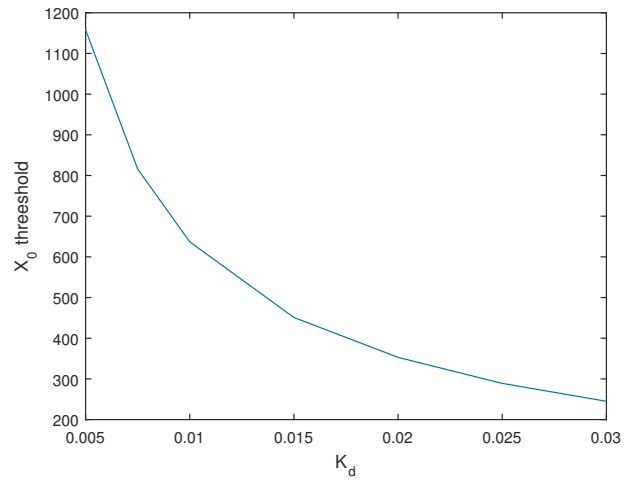


Figure 5: Threshold on  $X_0$  as a function of  $K_d$  for model parameters indicated in Table 1

substrate) and an increasing one as soon as the threshold on  $X_0$  is crossed over (when  $S$  converges over  $\lambda^+$ ). In Figure 6, we plotted the total production of biogas production for  $K_d = 0.02$  as a function of  $X_0$  from 300 to 400 (recall that in this case the threshold value for  $X_0$  is about 357), which shows the

discontinuity.

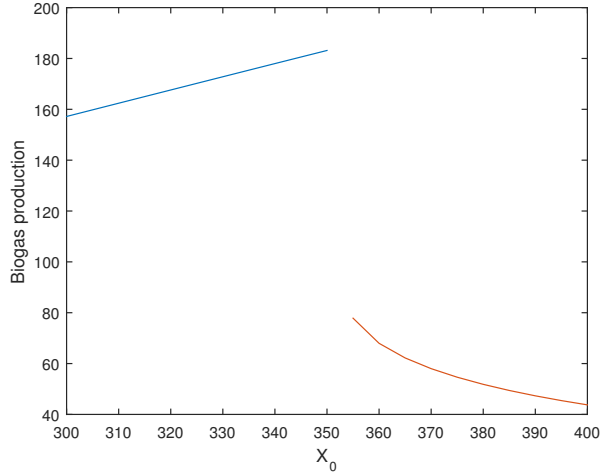


Figure 6: Biogas production as a function of  $X_0$  for  $K_d = 0.02$

Finally, we have plotted in Figure 7 the values  $\lambda^-$ ,  $\lambda^+$  as functions of  $K_d$ , which show the distance between the two attractors. In addition, the biogas productions obtained on both sides of the switching value of  $X_0$ , denoted by  $\text{Biogas}^-$  and  $\text{Biogas}^+$ , have been plotted. As expected, for small values of  $K_d$ , the difference between the two extremes values of the biogas productions are high.

This study reveals interesting insights for practitioners.

1. When  $S_0$  is small (or null), considering that an inhibition cannot occur because it concerns only high values of  $S^*$ , and adopting a Monod function instead of an Haldane one (or a large value of  $K_I$ ), could lead to wrong predictions. The biogas production could be poor under high initial concentration of organic matter  $X_0$ , because it conducts the system to large asymptotic values of  $S^*$  (see Figures 4 and 6).
2. When the death rate  $K_d$  is high (but not too much to fulfill condition (7)), the performances on biogas production are quite sensitive to the initial load of organic matter  $X_0$ , because the threshold on  $X_0$  is low (see Figure 5).
3. When the death rate  $K_d$  is low, the system has good performances on the condition that the initial load  $X_0$  does exceed the threshold, which is relatively large. However, if it is exceeded, the performances collapse dramatically (see Figure 7).

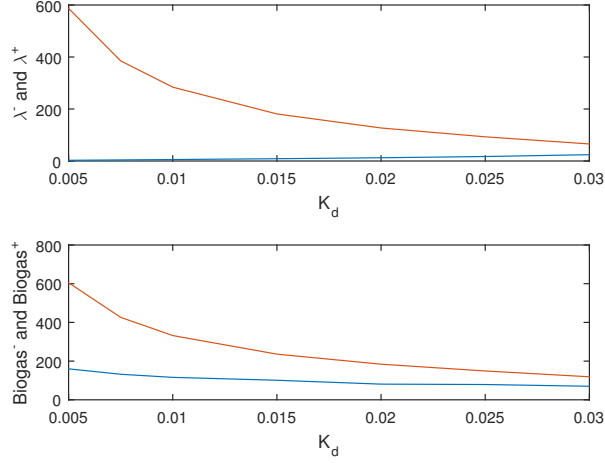


Figure 7:  $\lambda^-$ ,  $\lambda^+$  (on top)  $\text{Biogas}^-$  and  $\text{Biogas}^+$  (on bottom) as functions of  $K_d$

## 5 Conclusion

With the help of Barbalat's Lemma and the Center Manifold Theorem, we have shown that the trajectories of the system are bounded and converge to one of the non-hyperbolic equilibria. For non-monotonic growth functions, such as the Haldane function, the global attractor is non-connected. In this case, we have shown that the performances in terms of biogas production is discontinuous with respect to the initial condition.

For the Haldane law, a too high initial load of organic matter could be penalizing because there could be a significant quantity of residual soluble matter, especially when the death rate is small. A strategy could be then to fractionate the load of organic matter over the time, i.e. have a smaller initial load and re-introduce the remaining quantity of matter to be treated later (in one or several times). This leads to a control problem for choosing optimally the proportion of splitting and the corresponding re-introduction time(s) to obtain the best performances. This could be the matter of a future work. Another possibility is to play with the recirculation rate (in a completely mixed system), as in [19].

## Acknowledgments

The authors are gratefully for the French-Moroccan exchange program "PHC TOUBKAL 17/47".



## References

- [1] J. ANDREWS, *A mathematical model for the continuous culture of microorganisms utilizing inhibitory substrates*, Biotechnology and Bioengineering, 10(6) (1968), 707–723.
- [2] J. ARZATE, M. KIRSTEIN, F. ERTEM, E. KIELHORN, H. MALULE, P. NEUBAUER, M. CRUZ-BOURNAZOU AND S. JUNNE, *Anaerobic Digestion Model (AM2) for the Description of Biogas Processes at Dynamic Feedstock Loading Rates*, Chemie Ingenieur Technik, 89(5) (2017) 686–695.
- [3] I. BARBALAT, *Systèmes d'équations différentielles d'oscillations non linéaires*, Rev. Math. Pures Appl. 4 (1959), 267–270.
- [4] G. BASTIN AND D. DOCHAIN., *On-line estimation and adaptive control of bioreactors*, *Dynamics of Microbial Competition* Elsevier Science Publishers, New-York (1991).
- [5] B. BENYAHIA, T. SARI, B. CHERKI AND J. HARMAND, *Bifurcation and stability analysis of a two step model for monitoring anaerobic digestion processes*, Journal of Process Control, 22(6) (2012), 1008–1019.
- [6] O. BERNARD, Z. HADJ-SADOK, D. DOCHAIN, A. GENOVESI AND J.P. STEYER, *Dynamical model development and parameter identification for an anaerobic wastewater treatment process*. Biotechnology and bioengineering, 75(4) (2001), 424–438.
- [7] J. CARR, *Applications of Centre Manifold Theory*, Springer-Verlag (1981).
- [8] D. CHENU, *Modélisation des transferts réactifs de masse et de chaleur dans les installations de stockage de déchets ménagers: application aux installations de type bioréacteur*. PhD thesis, Institut National Polytechnique de Toulouse, France (2007).
- [9] I. DIDI, H. DIB AND B. CHERKI, *A Luenberger-type observer for the AM2 model*, Journal of Process control, 32 (2015), 117–126.
- [10] D. DOCHAIN, *Automatic Control of Bioprocesses Control systems* , John Wiley and Sons (2010).
- [11] G. DOLLÉ, O. DURAN, N. FEYEUX, E. FRÉNOT, M. GIACOMINI AND C. PRUD'HOMME, *Mathematical modeling and numerical simulation of a bioreactor landfill using Feel++*. ESAIM: Proceedings and Surveys, 55 (2016), 83–110.
- [12] R. FEKIH-SALEM, *Modèles Mathématiques pour la compétition et la co-existence des espèces microbiennes dans un chémostat*. PhD thesis, Univ. Montpellier, France (2013).

- [13] J. HARMAND, C. LOBRY, A. RAPAPORT AND T. SARI, *THE CHEMOSTAT: MATHEMATICAL THEORY OF MICROORGANISMS CULTURES*, ISTE Wiley (2017).
- [14] S. HASSAM, E. FICARA, A. LEVA, J. HARMAND, *A generic and systematic procedure to derive a simplified model from the Anaerobic Digestion Model No. 1 (ADM1)*, *Biochemical Engineering Journal* 99 (2015), 193–203.
- [15] M. HMISSI, J. HARMAND, V. ALCARAZ-GONZALEZ AND H. SHAYEB, *Evaluation of alkalinity spatial distribution in an up-flow fixed bed anaerobic digester*, *Water Science and Technology*, 77(4) (2018), 948–959.
- [16] S.J. JANG AND J. BAGLAMA, *Nutrient-plankton models with nutrient recycling*. *Computers and Mathematics with Applications*, 49(2-3) (2005), 375–387.
- [17] M. LOREAU, *Material cycling and the stability of ecosystems*. *The American Naturalist*, 143(3) (1994), 508–513.
- [18] J. MONOD *La technique de la culture continue: Théorie et applications*, *Ann. Inst. Pasteur, Lille*, 79 (1950), 390–410.
- [19] A. RAPAPORT, T. BAYEN, M. SEBBAH, A. DONOSO-BRAVO AND A. TORRICO, *Dynamical modelling and optimal control of landfills*, *Mathematical Models and Methods in Applied Sciences*, 26(5) (2016), 901–929.
- [20] A. RAPAPORT, T. NIDELET, S. EL AIDA AND J. HARMAND. *About biomass overyielding of mixed cultures in batch processes*. Preprint hal (2019).
- [21] A. RAPAPORT, T. NIDELET AND J. HARMAND, *About biomass overyielding of mixed cultures in batch processes*, 8th IFAC Conference on Foundations of Systems Biology in Engineering (FOSBE), Valencia, Spain, 15-18 Oct. (2019).
- [22] M. ROUEZ, *Dégradation anaérobie de déchets solides: Caractérisation, facteurs d'influence et modélisations*. PhD thesis, Institut National des Sciences Appliquées, Lyon, France (2008).
- [23] W. WALTER, *Ordinary Differential Equations*, Springer (1998).

E-mails: `salih.ouchtout@gmail.com`  
`zoubida.mghazli@uit.ac.ma`  
`jerome.harmand@inra.fr`  
`alain.rapaport@inra.fr`  
`zakaria.belhachmi@uha.fr`