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Solar Photovoltaic Powered On-Site Ammonia Production for Nitrogen Fertilization

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Abstract

Ammonia synthesis is the most important step for nitrogen-fertilizer production and consumes approximately 1% of the world’s energy production and energy-related greenhouse gas emissions. In addition to the concomitant emissions caused by ammonia and nitrogen fertilizer synthesis, centrally produced fertilizer that must be distributed to farms also harms the environment because of the embodied energy of transportation. An environmentally-optimal nitrogen fertilizer system would be distributed on farms themselves using only renewable inputs. Recent developments in solar photovoltaic technology and subsystems for ammonia production have made non-organic on-site ammonia production physically possible. This study provides a technical evaluation of the process for on-site nitrogen-fertilization of corn using solar photovoltaic electricity as the energy input. The system consists of a water electrolysis system to generate hydrogen and a membrane system to generate nitrogen needed as material inputs. Total power consumption for syngas preparation to generate a unit of ammonia is calculated. System total energy consumption is calculated while compensating syngas preparation with heat recovery. Five case-study locations are evaluated to determine their suggested nitrogen fertilizer addition (N-rate) for corn growth and the energy consumption for suggested N-rate is calculated. The System Advisor Model (SAM) is then used to simulate the PV system output for those five locations. Finally, the PV land use required as a fraction of the corn field area is determined. The results indicate that because PV is so much more efficient at solar energy conversion than organic methods, even the worst case evaluated in Indiana requires less than 1% of the corn field converted to a PV system to provide enough energy to generate sufficient amounts of ammonia for fertilizer for the remaining corn. The system was modeled to provide ammonia to fertilize for corn fields larger than 1079 acres with the worst soil conditions, the area of which applies to more than half of cropland in the U.S. in 2011. As the finiteness and emissions of fossil fuel production of nitrogen become more important, this renewable system should become economical and future investigations into its overall viability are warranted.
Keywords
Photovoltaic; Ammonia; Corn; Fertilizer; Electrolysis; Distributed generation; Distributed production

1. Introduction

Ammonia synthesis is the most important step for nitrogen-fertilizer production and consumes 1% of the world's energy production and resultant energy-related greenhouse gas emissions (Kitano et al., 1995). Ammonia consists only of nitrogen and hydrogen. Both hydrogen and nitrogen are widely available in earth’s atmosphere, but currently, according to U.S. Environmental Protection Agency (EPA) natural gas is used as a primary hydrogen generation source, and this process results in carbon dioxide (CO\textsubscript{2}) emissions (EPA, 2009). Carbon dioxide emissions have well-known environmental problems and there are efforts underway to replace fossil fuels with renewable sources of energy (Flavin, 1990; Steinberg, 1999; El-Fadel et al., 2003; Sims, 2004; Stern, 2006; Granovskii et al., 2007; Tsoutsos et al., 2008). In addition to the emissions caused by ammonia and nitrogen fertilizer synthesis, there are also negative environmental externalities caused by the transportation of the centrally produced good to distributed farms (Bretrup et al., 2004; Horvath, 2006; Facanha and Horvath, 2007; Pearce et al., 2007). Thus the environmentally optimal nitrogen fertilizer system would be distributed on farms themselves using only renewable inputs. Historically, the only means of doing this was with natural nitrogen fixation following the practices used by organic farmers (Havlin, et al. 1990; Drinkwater, et al., 1998; Badgley, et al., 2007). Unfortunately, this process has a significant productivity penalty with nonproductive (or less than optimal) crop rotations and potentially lower than optimal nitrogen levels. However, the nitrogen and hydrogen needed for ammonia synthesis can be obtained by using an air membrane system and water electrolysis, respectively. Commercial water electrolyzers can reach energy efficiency (higher heating value) as high as 73% (Ivy, 2004), making them feasible for hydrogen generation. Both of these methods—membrane and water electrolysis have the potential to be environmentally friendly as they use renewable natural resources as inputs (air and water); however, the sustainability is dependent on the energy used to run the processes. Solar photovoltaic (PV) technology, which converts renewable solar energy directly into electricity is a long-established sustainable energy technology (Pearce, 2002). As solar energy is available in all agriculturally relevant geographic locations, it represents a prime candidate for a sustainable solution for powering a distributed system for nitrogen fertilizer (N-fertilizer) production.

According to the United States Department of Agriculture (USDA), corn consumed 45.67% of N-fertilizer in United States in 2010 (USDA, 2013). Thus, corn fertilization in the United States is used as a case study here to determine the energetic feasibility for on-farm distributed N-fertilizer production using solar-generated electricity. First, the required N-fertilizer amounts are determined for five locations as the N-rate for corn strongly depends on the soil condition, which is greatly influenced by weather conditions (Fernández et al., 2012). Then the total power consumption for syngas preparation to generate a unit of ammonia is calculated. System total energy consumption is calculated while using heat recovery with syngas preparation for suggested N-fertilizer amounts. The System Advisor Model (SAM) is then used to simulate the PV system output for those five locations. Finally, the PV land use required as a fraction of the corn field area is determined. The results are presented and the technical and energetic viability of distributed on-farm nitrogen-fertilizeration production are discussed.
3. Methods

The proposed ammonia generation system is shown in Figure 1. The nitrogen membrane generator (2) works with the air compressor (1) to generate nitrogen, using air as source material. Hydrogen is generated from the water electrolyzer system (3). Hydrogen and nitrogen gases are then compressed and heated as syngas, which is combined in the ammonia converter (6). The heat generated in the converter will be recovered either to electrical energy or thermal energy, unconverted syngas will also be separated from ammonia and recycled as syngas again.
Figure 1. System diagram

The ammonia synthesis conversion rate is limited by temperature. Industrially the temperature used to speed up reaction is usually around 400°C to 500°C and the conversion rate is around 10% to 15% at this temperature (Lovell, 1980). However, unconverted syngas can be recovered, so the total conversion rate can eventually reach 97% (Barclay and Leigh, 2000). The primary criteria for selecting sub-components of the system was to achieve maximum energy efficiency.

2.1. Water electrolysis

To produce 1 lb (0.45 kg) of ammonia, 0.08 kg hydrogen needs to be produced. The Stuart IMET 1000 Series (Ivy, 2004) electrolyzer was selected as it generates hydrogen with purity higher than 99.997%. The energy consumption rate is 4.80 kWh/Nm$^3$ (N is "normal" in this context). This 0.08 kg of hydrogen is produced under a pressure of 360 psig. 4.43 kWh of electrical energy will be consumed to produce this amount of hydrogen.

2.2. Nitrogen membrane generator

An IGS Skidded Nitrogen Generators 7000 Series (IGS Generon, 2010) was selected, which produces nitrogen with a purity of 99.9%. With an inlet gas-flow rate of 129 ACFM (actual cubic feet per minute) under 100 psig, the nitrogen generator yields nitrogen at rate of 60.2 ACFM under 100 psig. This nitrogen generator itself requires no energy to operate, so the energy necessary to produce nitrogen depends on the power of an air compressor for the membrane system inlet gas. The FS-Circuit SE30 (Curtis-Toledo, INC., 2013) is a commercial gas compressor. To compress air to 100 psig at a flow rate of 129 ACFM, the air compressor works at 22.37 kW. The nitrogen consumption rate is given by:

$$E_N = (V_N / Q_N) \times P_N$$  \hspace{1cm} (1)

Where $V_N$ is volume of nitrogen, $Q_N$ is generation rate of membrane system, $P_N$ is power consumption of air compressor. Each pound of ammonia requires 0.38 kg of nitrogen in syngas at 97% conversion rate, which is 11.691 cubic feet at 0°C under 1 atm. Using equation (1), for the membrane system to generate this much nitrogen, the compressor consumes 0.130 kWh energy.

2.3. Ammonia synthesis

Conventional industry produces ammonia based on the Haber-Bosch method; the reaction equation is:

$$0.5N_2 + 1.5H_2 = NH_3; \Delta H = -46 \text{ kJ/mol}$$  \hspace{1cm} (2)

This is an exothermic reaction. At standard enthalpy, every pound of ammonia produced generates 0.340 kWh of thermal energy. The ammonia converter is usually operated at 400°C to 500°C under 140 to 210 atm; this is not the condition for standard enthalpy. However, syngas is close to standard enthalpy condition (25°C, 1 atm) before being compressed to required pressure and heated to conversion temperature. Upon application (after cooling from heat recovery), the generated ammonia will also be close to standard enthalpy conditions. According to Hess's law of constant heat summation, the total generated heat can be estimated as 0.340 kWh from the production of 0.45 kg of ammonia. The nitrogen required to produce 0.45 kg of ammonia is 0.37 kg; thus, the total energy $E$ (kWh) required to produce 0.45 kg of N can be given as:

$$E = (E_{\text{syngas}} - \eta \times E_{\text{exo}}) / 0.822$$  \hspace{1cm} (3)
Where $E_{\text{syngas}}$ (kWh) is the energy required to produce the correspondant hydrogen and nitrogen, $\eta$ is the total converter heat recovery rate. $E_{\text{exo}}$ (kWh) is the standard enthalpy to produce 0.45 kg of ammonia. 0.822 is nitrogen mass fraction in ammonia.

### 2.4. Case Study

For Indiana, a major corn-producing state in the United States, the suggested N-rate for corn growth is given directly for five different regions (Camberato and Nielsen, 2015). Therefore, a location was chosen in each of five regions in order to determine the N-rate for corn growth. Table 1 shows the results.

#### Table 1. N-rate for five locations

<table>
<thead>
<tr>
<th>Location</th>
<th>Indiana Region</th>
<th>N-rate (kg/hectare)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Evansville</td>
<td>Southwest (SW)</td>
<td>205</td>
</tr>
<tr>
<td>Grissom</td>
<td>North Central (NC)</td>
<td>212</td>
</tr>
<tr>
<td>Indianapolis</td>
<td>Central (C)</td>
<td>247</td>
</tr>
<tr>
<td>Fort Wayne</td>
<td>Northeast (NE)</td>
<td>254</td>
</tr>
<tr>
<td>Delaware</td>
<td>East Central (EC)</td>
<td>262</td>
</tr>
</tbody>
</table>

The suggested N-rate $R$ is also given in a formula by soil conditions (Shapiro et al., 2008):

$$ R = 35 + (1.2 \times E) - (8 \times N) - (0.14 \times E \times O) - C $$(4)

For this equation, $E$ is the expected yield (bu/ac), $N$ is the nitrate ppm in soil, $O$ is the percentage of organic matter in soil, $C$ accounts for N from all other sources in the current soil (lb./ac). According to this formula, suggested N-rate can range from 0 kg/ha to 353 kg/ha. It is known that, while more N-fertilizer is applied in greater quantities than suggested N-rate, there will be no additional increase in yield (Camberato and Nielsen, 2014). Thus, 353 kg/ha could be used to estimate the maximum N-rate for any expected yield.

### 2.5. PV system simulation

The National Renewable Energy Lab's System Advisor Model (SAM 2014.1.14) is used for simulation of the PV systems. The systems are simulated in the same five locations where the N rates are determined as listed in Table 1. PV modules (Suntech Power STP310-24/Vdx) with a nominal efficiency of 16% were chosen for all five locations. The arrays are designed to provide output of 200 kW dc. With inverter efficiency of 96.32%, the array provides a capacity of 448 kW per ha of total land area. According to this simulation, Table 2 shows the PV system energy/land rates for the five case-study locations. The total module area is 1,250 m², with 645 modules. Arrays have ground coverage ratio (GCR) of 0.3. At this configuration, arrays occupy total area of 1 acre (0.4 ha). Since PV modules degrade with time, the examination covers both the 1st- and 25th-year energy rates at degradation rate of 0.5% per year.

#### Table 2. Annual energy generation from PV system

<table>
<thead>
<tr>
<th>Location</th>
<th>PV energy rate (kWh/ac)</th>
<th>1st year</th>
<th>25th year</th>
</tr>
</thead>
<tbody>
<tr>
<td>Evansville</td>
<td>280,000</td>
<td>250,000</td>
<td></td>
</tr>
<tr>
<td>Grissom</td>
<td>250,000</td>
<td>220,000</td>
<td></td>
</tr>
<tr>
<td>Indianapolis</td>
<td>280,000</td>
<td>250,000</td>
<td></td>
</tr>
<tr>
<td>Fort Wayne</td>
<td>270,000</td>
<td>240,000</td>
<td></td>
</tr>
<tr>
<td>Delaware</td>
<td>250,000</td>
<td>220,000</td>
<td></td>
</tr>
</tbody>
</table>

3. Results

3.1. Required Energy as a Function of Heat Recovery

Using equation 3, the energy consumed for generating each pound of N from ammonia with respect to heat recovery rate can be calculated; this is shown in Figure 2.

![Figure 2](image_url). Energy consumption rate for unit N. Rate ranging from 5.12 kWh/lb (2.30 kWh/kg) to 5.56
kWh/lb (2.50 kWh/kg).

Thermal-electrical recovery rate is usually around 30%, while thermal-thermal recovery rate is usually much higher, around 90%. Any hybrid heat recovery system recovers heat to both thermal energy and electrical energy will have efficiency between 30% and 90%, so it's necessary to examine energy rate in this interval. At heat recovery of 30%, energy consumption rate is 2.46 kWh/kg N, while at 90%, it lowers to 2.32 kWh/kg N.

3.2. Annual Energy Consumption for N Fertilizer per Acre of Corn Field

At a given heat recovery rate, an annual energy consumption per unit corn field is linear with its suggested N-rate. Figure 3 shows the results, regarding suggested N-rate ranging from 0 kg/ha to 315 354 kg/ha. Both results at heat recovery rate of 30% and 90% are given, hybrid recovery systems should provide a result between these two limits.
Figure 3. Annual energy consumption rate as a function of annual N consumption rate. At 0 kWh/ac, there are high quantities of organic matter and nitrate concentrations in the soil with low yield expectation. At the highest yield expectation of 270 bushels/ac (16,700 kg/ha) and with the worst soil conditions and no organic matter nor nitrate, energy rate can reach as high as 14230 kWh/ha (30% recovery rate) or 4030 kWh/ha (90% recovery rate).

For suggested N fertilizer rates at the five case-study locations, the energy rate per acre is calculated for a sensitivity between 30% and 90% heat recovery rates. Table 3 summarizes the results of this calculation.

Table 3. Energy consumption rates for adequate N fertilizer for case-study locations

<table>
<thead>
<tr>
<th>Location</th>
<th>Energy Consumption Rate (kWh/ha)</th>
<th>30% Heat Recovery Rate</th>
<th>90% Heat Recovery Rate</th>
</tr>
</thead>
<tbody>
<tr>
<td>Evansville</td>
<td>2451</td>
<td>2335</td>
<td></td>
</tr>
<tr>
<td>Grissom</td>
<td>2570</td>
<td>2437</td>
<td></td>
</tr>
<tr>
<td>Indianapolis</td>
<td>2965</td>
<td>2817</td>
<td></td>
</tr>
<tr>
<td>Fort Wayne</td>
<td>3039</td>
<td>2891</td>
<td></td>
</tr>
<tr>
<td>Delaware</td>
<td>3114</td>
<td>2965</td>
<td></td>
</tr>
</tbody>
</table>

3.3. Land Required for Distributed N-Fertilizer Production with PV

Dividing the energy consumption rate of each location by its corresponding PV system energy rate gives the land occupation. Figure 4 illustrates the results. To determine the worst case scenario the following assumptions were made: Of all five case-study locations, the PV system in Delaware yields the worst energy rate so this location was used. Then, the worst soil condition is assumed to be present in Delaware; therefore, the energy consumption rate is assumed to be 4230 kWh/ha (30% recovery rate) or 4030 kWh/ha (90% recovery rate).

At heat recovery rate of 30% (shown in Figure 4.a), in 25 years, land of the PV in Evansville varies from 0.35% to 0.40%, in Grissom from 0.41% to 0.46%, in Indianapolis from 0.43% to 0.48%, in Fort Wayne from 0.46% to 0.51%, in Delaware from 0.51% to 0.57%, and worst case land of the PV in Delaware varies from 0.70% to 0.78%.
Figure 4. PV land usage after 25 years of degradation for systems with a) a heat recovery rate of 30%
and b) a heat recovery rate of 90%  

At a heat recovery rate of 90% (shown in Figure 4.b), in 25 years, the PV land usage in Evansville varies from 0.34% to 0.38%, in Grissom from 0.39% to 0.43%, in Indianapolis from 0.40% to 0.45%, in Fort Wayne from 0.43% to 0.49%, in Delaware from 0.48% to 0.55%, and worst case PV land use in Delaware varies from 0.66% to 75%. As can be seen from Figure 4, in all cases the land area necessary to provide the PV electricity for the necessary N-fertilizer was less than 1% of the total. Thus, the land required for the solar photovoltaic collectors is significantly smaller penalty than organic techniques of producing nitrogen.

4. Discussion and Future Work  

The results indicate that the systems are technically and energetically viable. As shown in Figure 4, even the worst case requires no more than 0.78% of the corn field to provide enough energy to generate sufficient amounts of ammonia for fertilizer. However, it should be pointed out that further experimentation is needed to verify these numbers as some factors in ammonia production, such as CO₂ removal from syngas, may influence these results, potentially leading to lower yields. However, these factors will not significantly affect the energy consumption rate and the PV area needed. The feasibility of using PV systems to provide energy for on-site ammonia production will still be viable. For shade-tolerant crops, the PV panels may be able to be placed above the crops in “agrivoltaic systems” (Goetzberger and Zastrow, 1982; Marrou et al., 2013; Dinesh and Pearce, 2015), leading to even smaller impacts on the farming system.

Distributed production of nitrogen fertilizer may also be useful for directly reducing fertilizer effects on the environment. Farmers often over apply fertilizer. For example, in 2010, 31% N-based fertilizer applied to corn was in excess of the suggested N-rate (Ribaudo et al., 2012). Over nitrogen fertilization can contaminate groundwater and cause other environment problems (Power and Schepers 2003). A dedicated on-site ammonia production system, like the one proposed for the first time here, may efficiently help nitrogen management by producing just enough N-fertilizer for a given area by design. As the farmers would also be the nitrogen fertilizer synthesizers it may lead more careful application and low-cost open-source nitrate testing equipment (Wittbrodt, et al., 2015) based off of open-source colorimeters and water testing apparatuses (Anzalone et al., 2013; Wijnen, et al., 2014). There is some evidence from related distributed production (e.g. with solar PV), that more environmentally responsible behavior is created simply by exposure to the green technology (Schelly, 2014a, 2014b); however, future field work is needed to see if such an effect would transfer to the farm community.

The technologies evaluated in this study are still on a relatively large scale. In this case, the commercial membrane system is able to generate nitrogen at 95 Nm³/hr, while the water electrolyzer is able to generate hydrogen at 60 Nm³/hr. Since three times the volume of hydrogen is required as nitrogen (see equation 2), five hydrogen generators can be coupled with one nitrogen generator. Then the hydrogen generators could be run at 95% utilization. Working continuously, at conversion rate of 97%, one set of these generators can provide syngas for ammonia to fertilize 436 ha of corn field that has the worst soil condition. Farms that have cropland area larger than 404 ha occupy 53.7% of total U.S. croplands in 2011 (MacDonald et al., 2013). Research is needed in developing efficient sub-components with
smaller throughputs. This could open up the technology to the other approximately half of farms in the U.S. Furthermore, this approach may work for smaller farms if they teamed up to share a system until the components are miniaturized.

To put the size of the PV system in perspective, on a 1000 acre (404 ha) farm, the PV array would take up less than 7.8 acres (3.2 ha) and produce more than 1.7 GWh electrical energy. Energy wise, the proposed system can provide nitrogen an energy intensity of 2.32 kWh/kg to 2.46 kWh/kg ammonia; this is fairly competitive with modern industrial energy intensity of 1.40 kWh/kg (Schlögl, 2003). The land use of the equipment is likely to be much smaller than the PV.

The results of this study are promising and indicate a potential for the technology of distributed PV-powered nitrogen fertilizer production. However, this study is only the foundation of the needed work to develop this into a laterally scalable distributed farming system. Further, more granular studies are needed to examine the possibility of building experimental systems and a careful examination of the economic viability must be determined.

There are also technical challenges that must be addressed. First, industrial production requires a stable ammonia converter condition to maintain a high energy efficiency. However, for a PV system, maintaining continuous stable energy output is a challenge without storage. Additional energy storage systems and special energy distribution methods may be needed to maintain stable energy input. This may not be prohibitively expensive as not only has the levelized cost of PV-generated electricity dropped radically (Branker et al., 2011), but with recent advances at Tesla, battery costs have also declined sharply (Tesla, 2015). Second, all calculations in this paper are based on a commercial product since a specialized water electrolyzer or nitrogen generator for ammonia production is not available, and both selected generators produce gas above 1 atm, which makes the energy efficiency lower. A recent study has shown an energy conversion rate (given by efficiency of PV system times energy efficiency of electrolysis) greater than 18% to produce hydrogen (Licht et al., 2001). This is much higher than the total hydrogen production energy conversion rate considered here of 12%. Future work should investigate coupling these more efficient systems, as water electrolysis occupies 82% of the total energy consumption before heat recovery, improving its efficiency will greatly impact the overall system efficiency.

Conclusions

The results of this study indicate that it is technically feasible for nearly half of the agricultural area in the U.S. to have individual farms producing their own nitrogen fertilizer using direct solar energy with current technology that is already commercially available. The land required for the solar photovoltaic collectors is less than 1% of the total land area, a much significantly smaller penalty than organic techniques of producing nitrogen. As the finiteness and emissions of fossil fuel production of nitrogen become more important, this renewable system should become economical and future investigations into its overall viability are warranted.
Acknowledgments

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