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Carbonation of hardened cement pastes: influence of temperature

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Abstract

The impact of temperature on carbonation was investigated in laboratory conditions using a device developed for this purpose. Two hardened cement pastes (CEM I and CEM V/A) were tested between 20°C and 80°C at different levels of relative humidity (RH). The carbonation rate of the CEM I increased with temperature, whereas that of CEM V/A reached a maximum at around 50°C.

Keywords: Carbonation (C) - Temperature (A) - Humidity (A) - Cement paste (D)

1. Introduction

Atmospheric carbonation involves a reaction between carbon dioxide (CO₂) and cementitious materials. Gaseous CO₂ present in the atmosphere diffuses through the concrete cover, dissolves in the pore solution, and then reacts with calcium ions to precipitate calcium carbonate (CaCO₃). The result of carbonation is the dissolution of calcium-bearing hydrates, the first of them being portlandite, Ca(OH)₂. This causes the pH of the pore solution to drop, which provides the ideal

conditions for the active corrosion of reinforcing steel. As carbonation has been studied for many years, the main mechanisms and influential parameters are well-known and efficient models are available to calculate the rate of the carbonation reaction [1–8]. Among all the influential parameters, the following are worth citing:

- Gaseous diffusion of CO₂: carbonation is driven by the gaseous diffusion of CO₂ in the ambient air through the carbonated layer to the calcium carbonate precipitation zone: the carbonated depth is proportional to the square root of time at steady-state [1,9,10].
- Concentration of solid phases which can be carbonated (and especially portlandite)
 [1,6,11].
- Moisture content: water is necessary for the chemical reactions to occur (reaction medium), but it is also hampers CO₂ diffusion. The higher the water content, the more likely the chemical reactions but the slower the diffusion rate. These two contradictory phenomena justify the existence of an optimal RH for carbonation around 40-60% [1,12–14].

In the field of radioactive geological disposal in France, reinforced concrete would be broadly used for waste packages, vaults, galleries or shafts that should remain stable during the operating period (up to 120 years) in order to ensure retrievability of the waste emplaced in the repository (reversibility). During this period, atmospheric carbonation would be one of the main phenomena concrete will have to cope with. Atmospheric carbonation is not expected to generate significant physical degradation by itself but rather through its major consequences (rebar corrosion). Due to the thermal output of some waste, the temperature in the vaults could be significantly higher than the ambient for several decades (it could reach 50 °C).

The effect of temperature is difficult to estimate because different contradictory mechanisms are at work. First, temperature modifies the solubility of the reactants: the higher the temperature, the lower the calcium [15,16] and CO_2 contents in solution [17,18]. This effect is expected to lessen the probability of reaction and thus inhibit carbonation. Dheilly *et al.* [19] used powdered

portlandite to check the influence of temperature between 10 and 40°C. They found that the higher the temperature, the lower the carbonation kinetics. The calcium carbonate crust formed around the portlandite grains was not found to inhibit carbonation [20,21] and the kinetic decrease with the temperature increase was therefore attributed to the decrease in the calcium solubility.

Temperature is also known to activate transport. Carbonation is a phenomenon driven by transport: a temperature increase is favourable to carbonation since it increases the diffusivity of CO_2 through the carbonated layer towards the $CaCO_3$ precipitation zone. In the same way, calcium ionic diffusion from the sound core to the precipitation zone is also enhanced. Transport can be described using the classical Arrhenius activation law with an activation energy of about 15-20 kJ/mol for CO_2 gas diffusion [22] and 44 kJ/mol for calcium diffusion [23,24].

Water retention is also affected by temperature: for a given RH, a temperature increase reduces the water retained at equilibrium [25–31]. Because the water content impacts both CO₂ diffusion and the chemical reactions, it is impossible to predict the influence of water retention modifications induced by temperature on carbonation. Moreover, temperature also impacts water transport; drying is faster when the temperature is increased [32–36]. From this perspective, the interaction between carbonation and water transport appears to be essential and even more important than at ambient temperature.

Several studies are available in the literature that address the effect of temperature on carbonation [1,37–44]. In these studies, carbonation was mainly characterized through the variations in the carbonated depth versus time using phenolphtalein projection. Papadakis *et al.* [1] observed limited increase in the carbonation kinetics between 22 and 42°C (about 15-20%) in their study using concretes (w/c=0.65). Similar results were obtained by He [42], Jae-Dong *et al.* [39] and Loo *et al.* [40] over small temperature ranges (between 15 °C and 40°C). Mori *et al.* [37] found that the carbonated depth at 40°C was twice the value obtained at 20°C. In the same way, Uomoto and Takada [38] reported a multiplication factor of 1.7 between 10 and 30°C,

Matsuzawa *et al.* [43] obtained a factor 2 between 20 and 60°C. and Li *et al.* [44] obtained a factor 3 between 10 and 60°C. The compilation of these results is shown in Figure 1. Despite some discrepancies and uncertainties, the trend is clear: the carbonation rate increases with temperature.

The results of Liu et al. [41] were quite different. They used samples prepared by compaction of recycled autoclaved lightweight concrete (ALC) and water to achieve target water content. It must be recalled here that 11 Å-tobermorite (C/S = 5/6) is the main component of ALC. The samples were carbonated at temperatures ranging from 20 to 100°C with 100% CO₂ which was introduced into the chamber after bubbling into water to prevent sample drying. Between 20 and 60°C, the amount of adsorbed CO_2 strongly increased. Yet beyond 60°C, it decreased by about 30% (between 60 and 100°C, Figure 2). It therefore seemed that 60°C was the optimal temperature for carbonation, *i.e.* the temperature at which the carbonation rate was maximal. According to the authors, the fall in absorbed CO₂ above 60°C was attributed to the temperatureinduced decrease in solubility (Ca²⁺ and CO₂). This unexpected result was supported by the modelling study of Ishida and Li [45]. They accounted for the temperature influence on CO₂ dissolution and transport as well as on the solubility of calcium-bearing phases. Performing simulations between 10 and 50°C, they obtained an increase in the carbonation rate between 10 and 30°C and a decrease for higher temperatures. The value of 30°C itself is not significant because it depends on the input data. It is in fact important to consider that the two opposite effects of temperature can theoretically result in an optimal temperature for the carbonation rate.

At a first glance, all these results may appear contradictory, but it remains impossible to confirm this because most of them were obtained at temperatures below 60°C *i.e.* lower than the optimal temperature proposed by Liu *et al.* [41]. Moreover, all these experiments were not conducted using similar protocols (in terms of preconditioning, CO₂ concentration) or materials, and sometimes the preliminary drying was questionable as it can generally be said that most of the samples were probably not in equilibrium at the beginning of carbonation. The results might

therefore have inadvertently included the contribution of drying. For this reason, the main goal of this paper is to study the impact of temperature on the carbonation of two hardened cement pastes up to 80°C.

2. Materials and methods

2.1. Materials

We used two hardened pastes prepared using commercial cements, which were selected for their potential use in radioactive waste management in France:

- CEM I (ordinary Portland cement including at least 95% clinker) from Lafarge, Val d'Azergues factory, France
- CEM V/A (clinker with 22 wt% slag and 22 wt% fly ash) from Calcia, Airvault factory, France.

These two cements were selected by the French Radioactive Waste Management Agency (Andra) as references for all R&D studies. The water-to-binder ratio (w/b) of the pastes was fixed to enable comparison between the two pastes. We chose a w/b ratio of 0.40 because the properties of fresh paste seemed suitable, i.e. good workability, with neither visible segregation nor bleeding. The elementary composition of each paste is given in Table 1.

All the samples were cast in laboratory conditions in seven consecutive batches spanning over two days. The fresh paste was poured into cylindrical moulds (Ø35 × H60 mm) and vibrated. The samples were then kept seven days at ambient temperature in their closed moulds. After unmoulding, they were immersed three months in a small volume of solution in an airtight container to prevent carbonation. The curing solution composition was designed to prevent calcium and alkalis leaching [46,47].

The composition of the curing solution was determined by i) expression of the inner solution [48,49] of samples kept three months in sealed bags, and ii) analysis using ionic chromatography

(Table 2). The curing solution compositions were also determined before the samples were added and then at the end of the curing process: only small changes could be observed, which confirmed that there was no significant leaching.

After the cure, the top and bottom parts of the samples were cut off and discarded, resulting in Ø35×H50 mm samples which were assumed to be homogeneous. It was verified that the samples were fully saturated (no water uptake after 48 hours in water and a vacuum): no additional procedure was used to ensure initial saturation.

2.2. Specimen preparation and preconditioning

Once cured, the samples were divided into different sets (including at least four samples for each formulation), which were preconditioned at 20, 50 and 80°C with different RHs using airtight containers and saturated salt solutions. Table 3 summarises the solutions used for the three temperatures.

The containers were regularly opened and the samples weighed to compute their relative mass variation according to:

$$\left(\frac{\Delta m}{m}\right)(t) = \frac{m(t) - m_0}{m_0},\tag{1}$$

where m_0 and m(t) are the initial mass and the mass measured at the time *t* respectively. The deviation from equilibrium was estimated using the following equation:

$$\varepsilon(t) = \frac{\left(\frac{\Delta m}{m}\right)(t+1) - \left(\frac{\Delta m}{m}\right)(t)}{\left(\frac{\Delta m}{m}\right)(t)}.$$
(2)

The pastes were assumed to be at equilibrium when ε became lower than 0.05%. These results (mass at equilibrium) were used to assess the water retention curves; see [31] for more details. The cylinders were covered with overlapping adhesive aluminium foils [50], leaving only the top side accessible to carbonation and to ensuring that one-dimensional CO₂ diffusion could occur. The samples were then put back in the containers from which they were taken seven days before being submitted to carbonation. Note that all the sample sets were not used for accelerated carbonation (see after).

2.3. Accelerated carbonation

A specific device was designed to conduct accelerated carbonation experiments under controlled environmental conditions (Figure 3). It was composed of different components with different purposes. First a commercial climatic chamber was used to control temperature and RH in the volume used for the experiments (340 L). The chamber made it possible to perform experiments between 20 and 90°C and between 20 to 95% RH. A device was added to analyse and regulate the CO₂ content within the chamber. It was composed of a commercial CO₂ analyser (making use of infra-red absorption), together with a complex system of pumps and servo-valves to remove the gas from the chamber, transferring it to the CO₂ analyser and back to the chamber. When the CO₂ content in the chamber was lower than the target, pure CO₂ was injected until both of them corresponded. The analyser was automatically calibrated using ambient air (0,04% CO₂) and pure CO₂ (100%). A gas cooling system (Peltier effect) was added between the chamber and the analyser to prevent penalising water condensation inside the analyser.

A thermo-hygrometer and a CO_2 sensor were introduced into the chamber to monitor the conditions during the experiments. Figure 4 presents the results of a preliminary test conducted at 80°C, 70% RH and using 50% CO_2 . Despite the increased variability of the environmental conditions induced by the addition of dry CO_2 into the chamber (on day 1), the environment was regulated correctly and the CO_2 content revealed the fact that the variations remained limited. These variations were much smaller than those defined in the French standard for the accelerated carbonation test (NF P18-458), i.e. \pm 3°C for temperature and \pm 5% for RH and the CO_2 content.

Accelerated carbonation tests were conducted at 50% CO_2 for seven days (168 hours) using the environmental conditions in which the samples were at equilibrium. A period of 7 days appeared as the best compromise between the time needed to test different configurations (temperature and RH) and the time needed for each test. After the test, the CO_2 regulation system was shut down and the CO_2 withdrawn from the chamber by injection of compressed air. The chamber could then be opened and the samples taken out for characterization.

It must be noted that accelerated carbonation using 50% CO_2 is known to be unduly aggressive and not representative of natural carbonation in terms of the consequences [51]. In this study, using 50% CO_2 made it possible to perform all the carbonation tests in a reasonable time, however, readers must keep in mind that the transposition of some of the results and conclusions to natural carbonation is arguable. For more carbonation results on these pastes at lower CO_2 concentration, the readers are referred to [52,53].

2.4. Characterization methods

After carbonation, the specimens were cut along their vertical axis. One part was sprayed with phenolphthalein and the carbonated depth was measured. The other part was cut into thin slices (about 500 μm thick) that were used for X-ray diffraction (XRD) and thermo-gravimetric analysis (TGA).

XRD was used to characterize the mineralogical changes during carbonation. Data was collected using a PANalytical X'Pert diffractometer with an X'Celerator detector (CuK α , λ = 1.5405 Å). The analyses were performed directly on the disk surface [54]. The disks were scanned between 5 and 65° with a step size of 0.017°, for a total duration of 20 minutes. Plotting the diffracted intensity of the main peak of a phase versus depth provided a mineralogical profile from the surface exposed to CO₂ to the noncarbonated core that was used to identify the presence of the considered phases in the mineralogical assemblage. The XRD results were processed to estimate the polymorphic abundance of calcium carbonate (calcite, aragonite and vaterite) in the carbonated zone. To this end, we tried to use Rietveld refinement but the results were not satisfactory because suitable model structures could not be found for the C-S-H [55] and the alternative methods such as PONCKS or that of Snellings [56] could not be easily used here because of carbonation itself. Rather, we found easier and more straightforward to use a modified version of the method proposed by Chung [57,58]: it is presented in Appendix 1. It was used to estimate the weight fraction in the carbonated zone of vaterite (v) and aragonite (a) relative to that of calcite (c) using:

$$\frac{\overline{x}_v}{\overline{x}_c} = \left(\frac{k_c}{k_v}\right) \frac{\int I_v dv}{\int I_c dv}$$
(3)

$$\frac{\overline{x}_a}{\overline{x}_c} = \left(\frac{k_c}{k_a}\right) \frac{\int I_a d\nu}{\int I_c d\nu}$$
(4)

with:

- \overline{x}_i mean value of the weight fraction of compound *i* in the carbonated zone
- *I_i* is the diffracted intensity for the compound *i*
- *k_i* ratio of intensity of the compound *i* to that of corundum.

TGA was used to quantify the amount of portlandite and calcium carbonate. Some disks were powdered and then introduced into a Netzsch STA 409 analyser. The sample (120 mg ± 1 mg) was left in the device for 72 hours at ambient temperature under a dry nitrogen flowrate (80 mL/min) to remove all evaporable water before it was heated from 25°C up to 1150°C at 10°C/min under a constant nitrogen flow (80 mL/min). The amount of portlandite and calcium carbonate was computed using the mass loss recorded between 400 and 550°C and between 600 and 900°C respectively.

3. Results

3.1. Initial state

The mineralogical assemblage obtained at 20°C and characterized using XRD (Figure 5) was considered usual for those binders. Portlandite, ettringite and C-S-H (broad peak around 29°) [59–63] were detected for CEM I, as well as traces of anhydrous compounds (C₄AF and C₂S). The CEM V paste was similar to that of CEM I with monosulfoaluminate and traces of mullite and quartz. Table 5 lists some of the properties of the non-carbonated pastes obtained elsewhere [31].

The first desorption isotherms obtained at 20°C (Figure 6) are of type IV according to the classification originally proposed by Brunauer [64,65]: the monomolecular layer edification at low RH is clearly visible, as is the presence of a plateau near saturation (CEMV) representative of capillary condensation within a meso-porous medium. Whatever the paste, a temperature increase led to a significant reduction in the water retained at equilibrium with any arbitrary RH. After the preconditioning period, the mineralogical assemblage at 50 and 80°C was more or less the same as that of 20°C: for PV (CEM V/A) katoite (Ca₃Al₂(SiO₄)(OH)₈, see [66]) was detected at the expense of ettringite and monosulfoaluminate [67–69] (Table 6). Results of TGA tests conducted on CEM I samples preconditioned at 20 and 80°C showed that the portlandite content remained stable (around 5.8 mol/L of paste) whatever the RH (Figure 7). This indicates that the 3-month cure was long enough for the CEM I paste to reach maturity. Conversely, the portlandite content of the CEM V/A samples kept at 80°C decreased when the RH increased. This was assumed to be an indication of ongoing hydration (due to pozzolanic reactions) during the preconditioning. We believe that this may have impacted the results of the CEM V/A pastes, but we did not attempt to quantify it.

3.2. Impact of carbonation on mineralogy

Regardless of the temperature and RH, the XRD results (Figure 8) showed the precipitation of the three usual polymorphs of calcium carbonate, *i.e.* calcite, aragonite and vaterite [70,71], at the expense of portlandite. In most cases, portlandite was not completely depleted in the carbonated zone. It was believed (but not verified) that the precipitation of calcium carbonate around the crystals of portlandite tended to inhibit the dissolution of portlandite [72–75] (Table 7).

Using TGA (Figure 9), a carbonation profile (portlandite and calcium carbonate concentrations versus depth) was determined for the CEM I paste carbonated at 80°C and 65% RH. The resulting profile was very similar to that obtained using XRD (Figure 8), thus confirming that XRD could be used in a semi-quantitative approach [76]. The decrease in the mass loss between 25°C and 200°C observed on DTG (Figure 10) was attributed to the carbonation of C-S-H [77,78]. The decomposition of calcium carbonate appeared to be characterized by different peaks ranging from 550 to 900°C as has already been observed in the past [6,77,79,80]. This was assumed to be due to the presence of aragonite and vaterite (and perhaps also to amorphous calcium carbonate) in addition to calcite [79–81]. It sometimes proved hard to distinguish the decomposition peak of portlandite from those of calcium carbonate, rendering the quantification process difficult.

Using the modified RIR method, the mean value of the weight fractions of aragonite (\bar{x}_a) and vaterite (\bar{x}_v) relative to that of calcite (\bar{x}_c) could be computed. In most cases, the amounts of vaterite and aragonite increased when the RH decreased (Figure 11). At high RH, calcite was the major calcium carbonate (ratio close to zero), but it no longer appeared to be the major calcium carbonate at low RH. For instance, considering the CEM I paste carbonated at 80°C and 26% RH, the weight fraction of aragonite in the carbonated zone was four times that of calcite. Aragonite also always appeared in higher amounts than vaterite. The results obtained at 20°C for the CEM I

paste were quite different from all the others; they may not be reliable because of the very small carbonation depth (Figure 12).

These results were interpreted as follows. The presence of metastable forms of calcium carbonate (vaterite and aragonite) together with the stable form (calcite) was considered as an intrinsic feature of carbonation because it has been broadly observed for years [70,82,83] and because of the temperature increase in the present tests [84,85]. Aragonite and vaterite are generally obtained in the carbonation of C-S-H and sulfoaluminate phases [68,71,81,86–88]. The increase in the polymorphic abundance at low RH was believed to be due to the inhibition of the polymorphic transformation from the metastable state to the thermodynamically stable one [84,89,90] due to the lack of water in the pores [91].

3.3. Carbonation depth

Figure 12 shows the measured carbonation depths versus RH. The results depicted the wellknown bell curves for both pastes, with a maximum at around 50% RH [1,12–14]. It must, however, be noted that the 20°C-optimal RH of the CEM V paste was much lower: around 33%. This was believed to be due to its unusual type IV water retention curve (plateau at high RH) that required a very low RH (down to 26%) to desaturate the pore system (Figure 6) [31]. For CEM I, the fact that the optimal RH remained the same for all three temperatures tended to indicate that the temperature-induced modification of the water retention was minor for carbonation but this was not confirmed by the CEM V results that were clearly changed beyond 20°C. Whatever the temperature, the carbonation depth of the composite cement (CEM V/A) paste was greater than that of Portland (CEM I) as we already know [11,92–96].

Figure 13 compares the carbonation depth values measured using phenolphthalein and XRD. In the latter case, we used the mineralogical profiles to evaluate the depth at which the portlandite peak intensity became lower than the average obtained in the non-carbonated zone (Figure 8). Unlike the results of references [6,97,98], the comparison was quite good: all the data aligned along the equality line, although the carbonation depth obtained using XRD was almost always greater than that obtained using phenolphthalein. This was believed to be due to the short duration of the experiments (7 days) that helped reduce the difference between the two methods.

The carbonated zone appeared to be frequently cracked as has already been observed, see references [52,53,99–101]. Figure 14 illustrates the cracking patterns obtained at 80°C between 26% and 76% RH. For both cements, the cracking increased when the RH decreased: cracking was thus believed to be due to a combination of desiccation and carbonation shrinkage [14,102–104]. Furthermore, the CEM V/A pastes were generally cracked more severely than the CEM I. This was believed to be due to the greater amount of C-(A)-S-H in the CEM V/A paste, which induced more shrinkage when they were decalcified [103,105]

4. Discussion

Figure 15(a) reports the maximal carbonation depth obtained at a given temperature as a function of the test temperature. The latter appeared to increase the depth of carbonation, though not in the same way for both cements. Considering the CEM I paste, the carbonation depth increased almost linearly with temperature: the maximal carbonation depth increased threefold between 20 and 80°C. Obviously, the thermo-activation of CO₂ transport and chemical reactions controlled the temperature influence on carbonation. This was consistent with most of the results in literature [37–40,43,44] - see Figure 15(b). The results of the CEM V/A paste were quite different. The carbonation rate increased between 20 and 50°C, but decreased between 50 and 80°C; the rate at 80°C remained greater than that of 20°C. The results clearly show that temperature has an accelerating effect, but with a maximum at 50°C. This observation is consistent with the results of Liu *et al.* [41].

Such a difference between the two pastes was not expected because all the samples were submitted to the same test sequence. This difference was thought to result from the differences

in their mineralogical composition and properties (Table 5): less portlandite and more C-(A)-S-H for the CEM V paste with regards to CEM I. The reduced C/S ratio of the C-(A)-S-H in the CEM V paste [106–109] may also have played a prominent role, as the calcium concentration at equilibrium is known to be lower (whatever the temperature between 25°C and 85°C) [16].

5. Conclusion

In the field of radioactive waste management, the impact of temperature on the atmospheric carbonation of cement-based materials was investigated. Two hardened cement pastes made with CEM I and CEM V/A were carbonated at three temperatures ranging from 20 and 80°C. The tests were conducted at different RH with 50% CO₂ using a device that was specifically set up for this purpose. The device was designed to maintain the temperature, RH and CO₂ content over large ranges with great accuracy. Prior to carbonation, all the paste samples were brought as close to hygral equilibrium as possible. The pastes were carbonated 7 days and then the samples were tested using phenolphthalein, XRD and TGA.

The results showed that the carbonation process was not significantly impacted at temperatures higher than the ambient temperature: the calcium-bearing phases were dissolved to precipitate calcium carbonate. The two metastable forms of calcium carbonate (aragonite and vaterite) were always observed in varying amounts. Their presence was inferred to be an intrinsic feature of carbonation. Furthermore, the amount of metastable phases increased when the RH decreased: this indicates that the polymorphic transformation into calcite was inhibited due to the lack of water.

In terms of carbonation rate, temperature was found to accelerate carbonation though not in the same manner for the two pastes. The carbonation rate of the CEM I paste increased linearly with temperature between 20 and 80°C, whereas that of the CEM V/A paste reached a maximum at around 50°C. This disparity was thought to be due to differences in the mineralogical assemblage of the two pastes: less portlandite and reduced C/S ratio for the CEM V/A paste.

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Appendix 1: Extended RIR method

It was shown that when a sample is exposed to monochromatic X-rays, the intensity of the

diffracted X-rays depends on the composition [110]:

$$I_i = K_i \frac{x_i}{\rho_i \mu_m} \tag{5}$$

with:

- *I_i* is the intensity of the diffracted X-rays by a selected plane (*hkl*) of the compound *i*
- K_i constant that depends on compound *i* and diffractometer
- x_i weight fraction of compound *i* in the exposed sample
- ρ_i density of compound *i*
- μ_m mass absorption coefficient of the exposed sample.

Considering the carbonated area as a homogeneous zone (the mass absorption coefficient μ_m is assumed to be uniform), the mean value of the weight fraction \overline{x}_i of compound *i* in the carbonated zone is then given by:

$$\overline{x}_i = \frac{1}{V_c} \int x_i dv = \frac{1}{V_c} \int \mu_m \frac{\rho_i}{K_i} I_i dv = \mu_m \frac{\rho_i}{V_c K_i} \int I_i dv$$
(6)

where V_c is the volume of the carbonated zone.

Let us consider the case of the pure compound i ($x_i^0 = 1$), the diffracted intensity I_i^0 is given by (μ_i is the mass absorption coefficient of the pure compound i):

$$I_i^0 = K_i \frac{x_i^0}{\rho_i \mu_i} = \frac{K_i}{\rho_i \mu_i}$$
⁽⁷⁾

Combining equations (6) and (7) helps flush out the cumbersome parameter K_i :

$$\overline{x}_{i} = \frac{1}{V_{c}I_{i}^{0}} \left(\frac{\mu_{m}}{\mu_{i}}\right) \int I_{i} dv$$
(8)

Let us now assume the presence of an internal reference f (of known concentration \overline{x}_{f}) in the carbonated zone that would be used to evaluate the fraction of the other compounds (flushing agent) [57]:

$$\overline{x}_f = \frac{1}{V_c I_f^0} {\binom{\mu_m}{\mu_f}} \int I_f dv \tag{9}$$

The weight fraction of the compound *i* in the carbonated zone is then:

$$\overline{x}_{i} = \overline{x}_{f} \frac{\mu_{f}}{\mu_{i}} \left(\frac{I_{f}^{0}}{I_{i}^{0}} \right) \frac{\int I_{i} dv}{\int I_{f} dv}$$
(10)

When corundum is used as a flushing agent, it was shown [57] that:

$$\frac{\mu_f}{\mu_i} \binom{I_f^0}{I_i^0} = \frac{1}{k_i} \tag{11}$$

where k_i is the reference intensity ratio (RIR) of the compound *i* [111]. This value is available in the powder diffraction file (PDF) of the International Centre for Diffraction Data¹ (ICDD).

$$\overline{x}_i = \overline{x}_f \left(\frac{1}{k_i}\right) \frac{\int I_i dv}{\int I_f dv}$$
(12)

In the absence of corundum in the sample, any other compound may be used as internal reference: calcite (*c*) was chosen here since it is the main product of carbonation. Eq. (12) then becomes [58]:

$$\frac{\overline{x}_i}{\overline{x}_c} = \left(\frac{k_c}{k_i}\right) \frac{\int I_i dv}{\int I_c dv}$$
(13)

¹ <u>http://www.icdd.com/</u>

List of figures



Figure 1: Impact of temperature on carbonation: compilation of literature results



Figure 2: impact of temperature on ALC compacts, redrawn after [41]



Figure 3: Device for accelerated carbonation tests



*Figure 4: Temperature, RH and CO*₂ *content during a preliminary test conducted at 20°C, 70% RH and 50% CO*₂*. The first reported number represents the average for each measurement, whereas the second represents the standard deviation.*



Figure 5: Diffractograms of the non-carbonated pastes after curing at 20°C (AFm = monosulfoaluminate; C_2S = dicalcium silicate; C_4AF = calcium aluminoferrite; C-S-H = calcium silicate hydrates; e = ettringite; m = mullite; p = portlandite; q = quartz)



Figure 6: Desorption isotherm of the hardened pastes as a function of temperature (the solid lines are provided as guidelines only) [31]



Figure 7: TGA: portlandite content versus RH (white=20°C; black=80°C)



Figure 8: XRD peak intensity profiles of CEM I and CEM V/A pastes at 80°C



Figure 9: Portlandite and calcium carbonate <u>contents</u> profile of the CEM I paste (80°C and 65% RH, <u>obtained using TGA</u>) to be compared to Figure 8



Figure 10: Typical thermograms of the PI and PV pastes during carbonation



Figure 11: Polymorphic abundance of calcium carbonate assessed using XRD and the RIR method: ratio $(\overline{x}_i/\overline{x}_c)$ as a function of temperature and RH



Figure 12: Carbonation depth versus RH



Figure 13: Comparison of carbonated depths measured by means of phenolphthalein or XRD



Figure 14: Cracking in the carbonated zone at 80°C: the pink line indicates the frontier between the non-carbonated and carbonated zones whereas the yellow lines represent the cracks



Figure 15: Impact of temperature on the carbonation rate (the lines are given as guidelines only)

List of tables

Table 1: Composition of the pastes

Compound	CEM I	CEM V/A	Unit
OPC	1396	759	g/L
Limestone filler	-	-	g/L
Slag	-	298	g/L
Fly ash	-	298	g/L
Silica fume	-	-	g/L
Water	558	542	g/L

Table 2: Composition (in mmol/L) and pH of the interstitial and curing solutions (at the beginning and of the cure)

	CEM I		CEM V/A					
	Na+	K+	Ca ²⁺	рН	Na+	K+	Ca ²⁺	рН
Inner solution	47	452	2	13.7	87	533	2	13.7
Curing solution - beginning of cure	49	439	2	13.6	90	518	4	13.7
Curing solution - end of cure	54	455	3	13.6	85	474	2	13.7

Table 3: RH generated as a function of temperature [112–116]

Desiccant/saturated salt solutions		Temperature			
		20 °C	50 °C	80 °C	
Lithium chloride	LiCl	-	-	11%	
Magnesium chloride	$MgCl_2$	33%	31%	26%	
Magnesium nitrate	$Mg(NO_3)_2$	54%	-	-	
Sodium bromide	NaBr	-	51%	51%	
Urea	$CO(NH_2)_2$	-	62%	-	
Ammonium nitrate	NH_4NO_3	63%	-	-	
Potassium iodide	KI	70%	-	61%	
Sodium nitrate	NaNO ₃	-	-	65%	
Sodium chloride	NaCl	-	74%	76%	
Ammonium sulphate	$(NH_4)_2SO_4$	-	-	-	
Ammonium chloride	NH ₄ Cl	80%	-	-	
Potassium chloride	KCl	-	-	-	
Potassium nitrate	KNO ₃	-	85%	-	
Sodium carbonate	Na_2CO_3	-	-	85%	
Potassium sulfate	K_2SO_4	-	-	95%	

Table 4: Inter-reticular distance and RIR ratio

	Calcite	Aragonite	Vaterite
d(h,k,l)	3.04 Å	3.40 Å	3.57 Å
k_i	2.0	1.15	0.60

Table 5: Properties of the non-carbonated pastes [31]

Properties	CEM I	CEM V/A	Unit
Saturated density <i>d</i> _{sat}	2.04	1.93	g/cm ³
Porosity (80°C)	37.2%	38.9%	-
C-S-H content	5.1	7.0	mol/L of paste
Portlandite content	5.8	2.1	mol/L of paste
Specific surface area	190	297	m²/g
Permeability to water	2.0×10 ⁻²²	0.7×10 ⁻²²	m ²

Table 6: Mineralogy of the non-carbonated zone

Paste	Temp	Detected phases in the non-carbonated zone (XRD)	
	20°C	C-S-H + portlandite + ettringite + C_2S + C_4AF	
PI (CEM I)	50°C	C-S-H + portlandite + ettringite + C ₂ S + C ₄ AF	
	80°C	C-S-H + portlandite + C_2S + C_4AF	
2000		C-S-H + portlandite + ettringite + monosulfoaluminate + mullite +	
	20 C	$quartz + C_2S + C_4AF$	
PV (CEM V/A)	FOOC	C-S-H + portlandite + ettringite + monosulfoaluminate + katoite +	
	50 C	mullite + quartz + C_2S + C_4AF	
	80°C	C-S-H + portlandite + katoite + mullite + quartz + C ₂ S + C ₄ AF	

Table 7: Mineralogy of the carbonated zone

Paste	Temp	Detected phases in the carbonated zone (XRD)	
	20°C	Calcite + aragonite + vaterite + portlandite + ettringite + C ₂ S + C ₄ AF	
PI (CEM I)	50°C	Calcite + aragonite + vaterite + portlandite + C ₂ S + C ₄ AF	
	80°C	Calcite + aragonite + vaterite + portlandite + C ₂ S + C ₄ AF	
PV (CEM V/A)	20°C	Calcite + aragonite + vaterite + portlandite + monocarboaluminate + ettringite + mullite + quartz + $C_2S + C_4AF$	
	50°C	Calcite + aragonite + vaterite + portlandite +katoite + mullite + quartz + C_2S + C_4AF	
	80°C	Calcite + aragonite + vaterite + portlandite +katoite + mullite + quartz + C ₂ S + C ₄ AF	