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# Effect of ultrasound on the induction time and the metastable zone widths of potassium sulphate

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## Abstract

A study of cooling crystallisation of a potassium sulphate solution in a batch reactor is described in this paper. The effect of ultrasound on primary nucleation was investigated by measures of induction time and metastable zone width of unseeded solutions. The appearance of crystals is detected by conductivity measurements.

The experimental results show that ultrasound has an effect on the primary nucleation of potassium sulphate. Ultrasound allows induction time and metastable zone width to be significantly reduced.

**Keywords:** Induction time; Metastable zone; Ultrasound; Potassium sulphate; Nucleation

## 1. Introduction

Crystallisation is an important process used in many domains, such as chemical, pharmaceutical and petrochemical industries. Works on the influence of ultrasound in crystallisation/precipitation processes have been published for several years [1–3].

The aim of our study is to determine if ultrasound has an effect on primary nucleation. Ultrasound is used only as a tool to induce the nucleation. For this, we carried out experiments of cooling crystallisation. Potassium sulphate has been chosen as a model product because a lot of data is available in the literature, such as solubility, nucleation and growth kinetics [4–6]. This investigation was divided into two parts. First, the induction time has been measured both with and without ultrasound. In the second part, the metastable zone width has been determined at a constant cooling rate for potassium sulphate solutions saturated at 30 °C.

## 2. Theory

The primary nucleation occurs in the absence of solid particles of the crystallised substance. For homogeneous primary nucleation, no solid phase is required, while the

heterogeneous primary nucleation is catalytically initiated by any foreign surface, such as the reactor wall, the stirring rod or solid impurities.

The primary nucleation rate is defined as the number of nuclei generated per unit volume and per unit time. The homogeneous primary nucleation rate is generally expressed as the following classical relation [7,8]:

$$J_{\text{hom}} = K_{\text{hom}} \exp \left[ -\frac{4}{27} \frac{\gamma_s^3 V_m^2 \beta^3}{(T k_B v \alpha \ln S)^2} \right] \quad (1)$$

For the heterogeneous primary nucleation we have

$$J_{\text{het}} = K_{\text{het}} \exp \left[ -\frac{4}{27} \frac{\gamma_s^3 V_m^2 \beta^3}{(T k_B v \alpha \ln S)^2} f(\theta) \right] \quad (2)$$

where  $f(\theta)$  is a function of the angle of contact between the crystalline deposit and substrate

$$f(\theta) = \frac{[(2 + \cos \theta)(1 - \cos \theta)^2]}{4}.$$

### 2.1. Induction period

In order to characterise the primary nucleation, we can measure the induction period which is defined as the time elapsed between the creation of supersaturation and the appearance of crystals. Kashiev et al. proposed a general expression of induction time valid for all nuclei, which appear and grow in a saturated solution [9]:

$$t_{\text{ind}} = \frac{N_c}{J} + \left[ \frac{\alpha_0}{a_p J G^{p-1}} \right] \quad (3)$$

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## Nomenclature

$a_{\pm}$	solute activity
$a_{\pm}^*$	saturation solute activity
$A$	primary nucleation rate constant ( $\text{m}^{-3} \text{s}^{-1}$ )
$\dot{b}$	cooling rate ( $^{\circ}\text{C s}^{-1}$ )
$C$	concentration ( $\text{kg K}_2\text{SO}_4 \text{ kg}^{-1} \text{ water}$ )
$C^*$	saturation concentration ( $\text{kg K}_2\text{SO}_4 \text{ kg}^{-1} \text{ water}$ )
$\Delta C$	absolute supersaturation ( $\text{kg K}_2\text{SO}_4 \text{ kg}^{-1} \text{ water}$ )
$\Delta C_{\max}$	maximum supersaturation ( $\text{kg K}_2\text{SO}_4 \text{ kg}^{-1} \text{ water}$ )
$\Delta C_w$	absolute supersaturation at the inner wall ( $\text{kg K}_2\text{SO}_4 \text{ kg}^{-1} \text{ water}$ )
$e$	wall thickness (m)
$g$	linear growth rate order
$\Delta G_{\text{crit}}$	critical free enthalpy ( $\text{J mol}^{-1}$ )
$\Delta G_{\text{crit}}^{\text{hom}}$	homogeneous nucleation critical free enthalpy ( $\text{J mol}^{-1}$ )
$\Delta G_{\text{crit}}^{\text{het}}$	heterogeneous nucleation critical free enthalpy ( $\text{J mol}^{-1}$ )
$h_s$	thermal coefficient transfer wall-solution ( $\text{W m}^{-2} ^{\circ}\text{C}^{-1}$ )
$h_f$	thermal coefficient transfer wall-fluid ( $\text{W m}^{-2} ^{\circ}\text{C}^{-1}$ )
$J_n$	number nucleation rate (number $\text{m}^{-3} \text{s}^{-1}$ )
$J_m$	mass nucleation rate ( $\text{kg m}^{-3} \text{s}^{-1}$ )
$k_B$	Boltzmann constant ( $=1.38058 \times 10^{-23}$ ) ( $\text{J molecule}^{-1} \text{K}^{-1}$ )
$k_n$	primary constant nucleation rate ( $\text{kg}^{(n-1)} \text{m}^{(3n-3)} \text{s}^{-1}$ )
$K_J$	primary nucleation rate constant (s)
$n$	nucleation order
$N$	stirrer rate ( $\text{tr min}^{-1}$ )
$N_c$	crystals number
$P_{\text{diss}}$	dissipated ultrasonic power ( $\text{W g}^{-1} \text{ solution}$ )
$S$	supersaturation ration
$S_{\text{ext}}$	outer surface ( $\text{m}^2$ )
$S_{\text{int}}$	inner surface ( $\text{m}^2$ )
$\bar{S}$	mean surface ( $\text{m}^2$ )
$t_{\text{ind}}$	induction time (s)
$T$	solution temperature ( $^{\circ}\text{C}$ )
$T_b$	bath temperature ( $^{\circ}\text{C}$ )
$T_1$	solution temperature ( $^{\circ}\text{C}$ )
$T_{\text{lim}}$	limit temperature ( $^{\circ}\text{C}$ )
$T_{\text{sat}}$	saturation temperature ( $^{\circ}\text{C}$ )
$T_{\text{sol}}$	solution temperature ( $^{\circ}\text{C}$ )
$T_{\text{sol}}^w$	inner wall temperature ( $^{\circ}\text{C}$ )
$\Delta T_{\max}$	maximum undercooling ( $^{\circ}\text{C}$ )
$U$	global heat transfer ( $\text{W m}^{-2} ^{\circ}\text{C}^{-1}$ )
$V$	solution volume ( $\text{m}^3$ )
$V_m$	molecular volume ( $\text{m}^3 \text{molecule}^{-1}$ )

## Greek letters

$\alpha$	volume shape factor
$\beta$	surface shape factor
$\gamma$	interfacial tension ( $\text{J m}^{-2}$ )
$\gamma_{\pm}$	saturation activity coefficient of $\text{K}_2\text{SO}_4$
$\lambda_e$	wall thermal conductivity ( $\text{W m}^{-2} ^{\circ}\text{C}^{-1}$ )
$\nu$	ion number
$\theta$	angle of contact ( $^{\circ}$ )

Assumptions can be made to simplify the expression of the induction time [8].

Three cases are possible:

1.  $t_n$  is much higher than  $t_g$ . The nucleation is predominant.
2.  $t_n$  is of the same size order as  $t_g$ . Nucleation and growth act upon the induction time.
3.  $t_n$  is much smaller than  $t_g$ . The growth mechanism of the nucleus to a detectable size is predominant.

We have tested these different models, the best fit of experimental data was obtained assuming  $t_n \gg t_g$ . Only the model representing a good correlation of our experimental results is presented here. In our case, we assume that the formation time of a stable nucleus is much higher than the necessary time for the nucleus to grow to a detectable size ( $t_n \gg t_g$ ). So the induction time can be considered as inversely proportional to the nucleation rate and the induction time is expressed with only the first term of Eq. (3).

Combining Eqs. (1) and (4) for the mechanism of primary homogeneous nucleation and taking the logarithm of the induction time, we obtained

$$\ln(t_{\text{ind}}) = \ln \left( \frac{N_c}{K_{\text{hom}}} + \frac{4}{27} \frac{\gamma_s^3 V_m^2 \beta^3}{k_B^3 \alpha^2 \nu^2 T^3} \frac{1}{\ln^2 S} \right) \quad (4)$$

where  $S$  is the supersaturation ratio calculated from the following equation:

$$S = \frac{a_{\pm}}{a_{\pm}^*} = \frac{\gamma_{\pm} C}{\gamma_{\pm}^* C^*} \quad (5)$$

The logarithm of activity coefficients has been estimated using the Brömley equation [10].

Eq. (4) suggests that for a given temperature, the plot of  $\ln(t_{\text{ind}})$  versus  $(\ln^2 S)^{-1}$  should be a straight line. In the literature, it has been shown that the plots of  $\ln(t_{\text{ind}})$  versus  $(\ln^2 S)^{-1}$  consist in two linear segments [11]. For high supersaturations (straightline (1)), the nucleation is predominantly homogeneous, and for low supersaturations (straightline (2)) the heterogeneous nucleation prevails (Fig. 1).

## 2.2. Metastable zone widths

This method consists in the determination of the maximum undercooling  $\Delta T_{\max}$ . A solution of known saturation temperature  $T_{\text{sat}}$  is cooled to a temperature  $T_{\text{lim}}$  at which

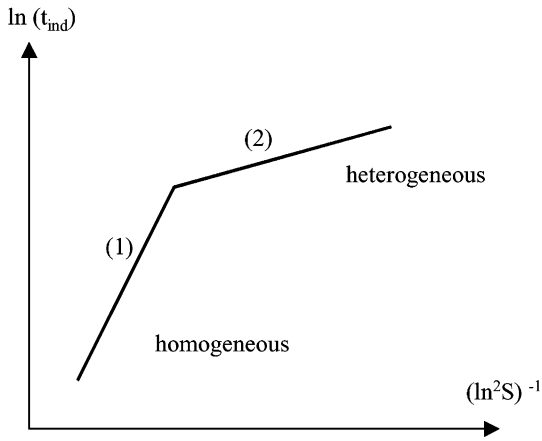


Fig. 1. Induction time as a function of initial supersaturation.

the birth of the first crystals is detectable. The maximum undercooling  $\Delta T_{\max}$  is defined as the difference between the saturation temperature  $T_{\text{sat}}$  and the temperature  $T_{\text{lim}}$ . The maximum undercooling can be expressed in terms of the maximum supersaturation,  $\Delta C_{\max}$  by the equation

$$\Delta C_{\max} = \left( \frac{dC^*}{dT} \Delta T_{\max} \right) \quad (6)$$

Nyvtl proposed a correlation between the mass of nuclei generated per unit mass of solution and the absolute supersaturation [12]

$$J_m = k_n \Delta C_{\max}^n \quad (7)$$

The nucleation rate can be expressed in terms of the cooling rate  $\dot{b}$

$$J_m = \left( \frac{dC^*}{dT} \dot{b} \right) \quad (8)$$

Eqs. (6)–(8) yield

$$\ln(\dot{b}) = d_1 \ln \left( \frac{dC^*}{dT} \right) + \ln(k_n) + d_2 \ln(\Delta T_{\max}) \quad (9)$$

where  $\dot{b}$  is the cooling rate and  $d_1$  and  $d_2$  are constants. These constants depend on the apparent orders of nucleation or growth.

This is a very general relation. However, different assumptions on the physical mechanisms to be taken into account lead to different interpretations of constants  $d_1$  and  $d_2$ . For instance, Nyvtl or Kubota assumed that only nucleation occurs before the crystals are detected: constants  $d_1$  and  $d_2$  are thus, simply related to the apparent order of nucleation,  $n$  [12,13]. For Söhnel and Nyvtl, constants  $d_1$  and  $d_2$  depend on the apparent orders of nucleation and growth [14]. If crystal growth is supposed to have a significant contribution, constants  $d_1$  and  $d_2$  are functions of the apparent order of growth,  $g$  [15].

The determination of the nucleation rate constant  $k_n$  and the kinetic apparent order of nucleation rate  $n$  and the linear

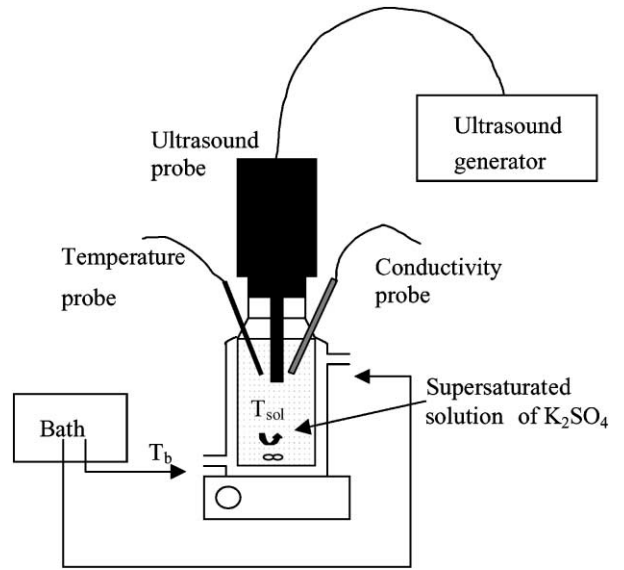


Fig. 2. Experimental apparatus.

growth rate order  $g$  are derived from the plot of maximum undercooling  $\Delta T_{\max}$  and cooling rate  $\dot{b}$  on logarithmic co-ordinates.

### 2.3. Ultrasound

We used power ultrasound with a frequency equal to 20 kHz. When high energy pressure waves are applied to a liquid, cavitation bubbles made of vapour and dissolved gas are created. The cavitation consists in the formation, growth and implosion of these bubbles. The violent implosion of bubbles is called collapse and can induce very high local temperatures and pressures.

The dissipated power of ultrasound reported in the text has been estimated by calorimetry. These dissipated powers represent about 40% of the electrical power consumed by the generator.

## 3. Experiments

Aqueous solutions are prepared from potassium sulphate crystals (purity > 99%) and distilled water. The experimental apparatus used for the determination of induction time and metastable zone widths is represented in Fig. 2. It consists of a thermostated reactor (200 ml) stirred with a magnetic rod at a constant rotation speed of about 500 rpm. Ultrasound is applied at the top of the reactor by a stainless ultrasound transducer with a titanium tip. Two ultrasonic power levels have been used: 0.05 and 0.12 W g<sup>-1</sup> solution. The conductivity and the solution temperature are respectively measured with instrumental resolutions  $\pm 0.1 \text{ mS cm}^{-1}$  and  $\pm 0.01^\circ\text{C}$ . We consider that the appearance of crystals is detected when there is a sudden decrease of the conductivity.

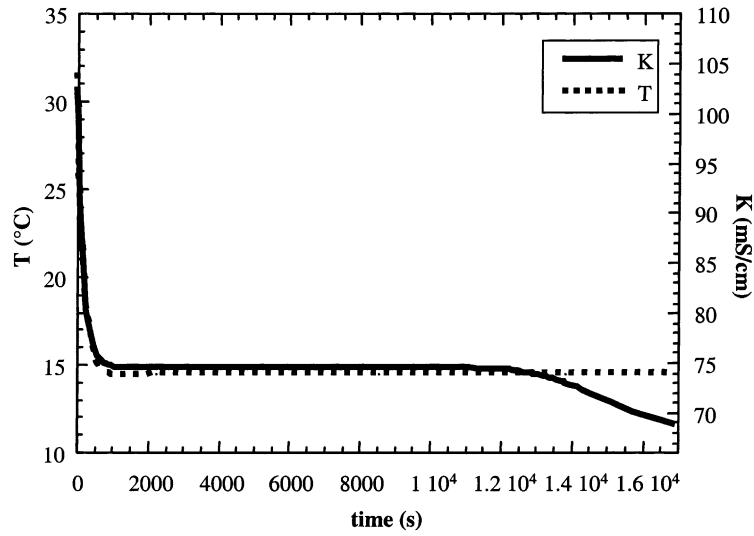


Fig. 3. Solution temperature and conductivity for an absolute supersaturation of  $0.0156 \text{ g K}_2\text{SO}_4 \text{ g}^{-1}$  water.

Before each experiment, in order to dissolve all crystals, solutions are warmed to a temperature higher by 5 or  $10^\circ\text{C}$  than the saturation temperature  $T_{\text{sat}}$  for 1 h.

For all experiments, the saturation concentration of potassium sulphate in water solutions is calculated from the following equation [16]:

$$C^* = 6.7 \times 10^{-2} + 2.3 \times 10^{-3} \times T - 6.0 \times 10^{-6} \times T^2 \quad (10)$$

For induction time measurements, the initial saturation temperatures ( $T_{\text{sat}}$ ) ranged from  $22$  to  $25^\circ\text{C}$  for experiments without ultrasound, and from  $19.5$  to  $23^\circ\text{C}$  for experiments with ultrasound. The solutions are rapidly cooled to a temperature  $T_1$  comprised between  $14$  and  $16^\circ\text{C}$ . Ultrasound is applied at the end of the cooling phase. The induction time is

measured as soon as the temperature  $T_1$  is reached or when ultrasound is applied.

Measurements of metastable zone widths are carried out for a saturation temperature ( $T_{\text{sat}}$ ) equal to  $30^\circ\text{C}$ . The cooling rates  $\dot{b}$  of solutions range from  $5$  to  $20^\circ\text{C h}^{-1}$ . The solution is insonified at the beginning of the cooling phase.

## 4. Results and discussion

### 4.1. Induction time

The appearance of potassium sulphate crystals is detected by a drop in the conductivity of the solution. The time corresponding to the crystallisation corresponds to the time where

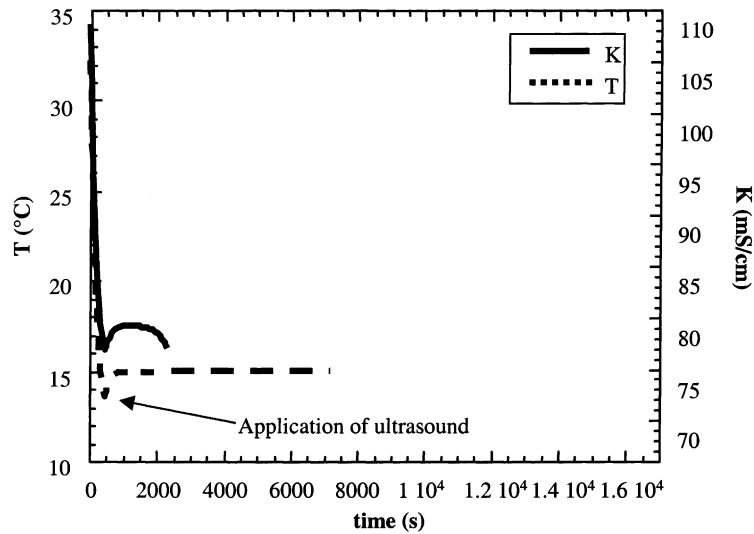


Fig. 4. Solution temperature and conductivity for an absolute supersaturation of  $0.0156 \text{ g K}_2\text{SO}_4 \text{ g}^{-1}$  water and an ultrasound power equal to  $0.05 \text{ W g}^{-1}$  solution.

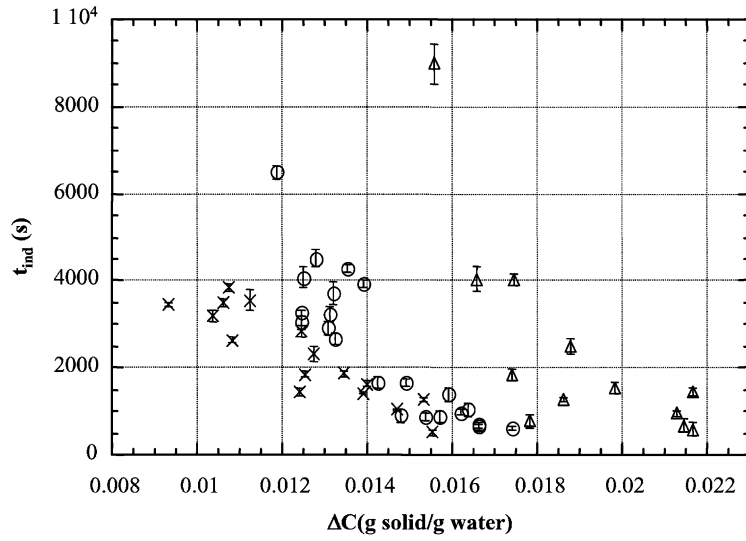


Fig. 5. Influence of ultrasound on the induction time of aqueous potassium sulphate solutions: ( $\Delta$ ) without ultrasound, ( $\circ$ )  $P_{\text{diss}} = 0.05 \text{ W g}^{-1}$  solution, ( $\times$ )  $P_{\text{diss}} = 0.12 \text{ W g}^{-1}$  solution.

the derivative of the conductivity versus the time becomes negative.

Figs. 3 and 4 present the variation of the solution temperature and conductivity for an absolute supersaturation of  $0.0156 \text{ g K}_2\text{SO}_4 \text{ g}^{-1}$  water. We can observe that the induction time without ultrasound is about 9000 s whereas with ultrasound it is about 1000 s. Moreover, the conductivity decreases faster with ultrasound than without ultrasound. As the conductivity is proportional to the potassium sulphate concentration, this difference suggests that more crystalline surface is formed with ultrasound.

All results obtained for the variation of the induction time versus absolute supersaturation are presented in Fig. 5 and Table 1. The absolute supersaturation is calculated as the

difference between the actual concentration and the saturation concentration. The maximum cooling time for experiments without ultrasound is about 900 s and for experiments with ultrasound it is about 450 s. The mass error for the absolute supersaturation error is about  $10^{-4} \text{ g K}_2\text{SO}_4 \text{ g}^{-1}$  water. The maximum error on the determination of the induction time is equal to 15% for experiments without ultrasound, to 11% for experiments at  $0.05 \text{ W g}^{-1}$  solution and to 12% for experiments and  $0.12 \text{ W g}^{-1}$  solution.

We obtained the same type of curve with and without ultrasound. The induction time decreases when absolute supersaturation increases. This behaviour agrees with classical results on crystallisation. However, we can observe that ultrasound has a significant effect on induction time,

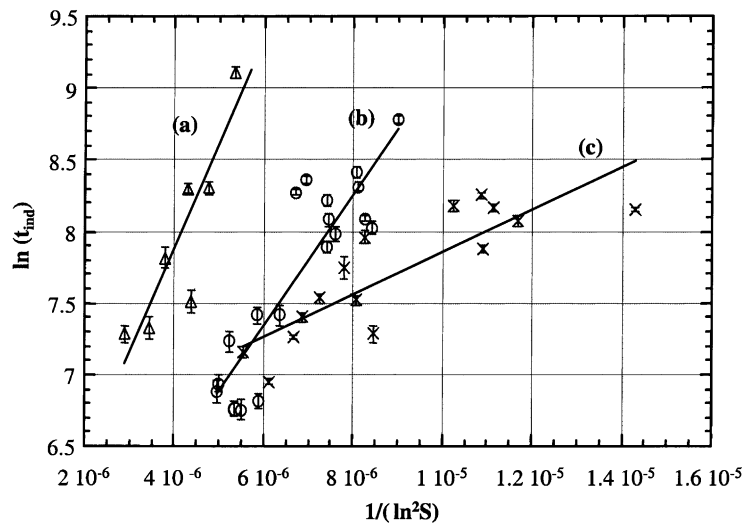


Fig. 6. Induction time as a function of final temperature and ratio supersaturation for potassium sulphate crystallisation: (a) without ultrasound, (b)  $P_{\text{diss}} = 0.043 \text{ W g}^{-1}$  solution and (c),  $P_{\text{diss}} = 0.114 \text{ W g}^{-1}$  solution.

Table 1  
Values of the induction time measurement

$\Delta C$ (g K <sub>2</sub> SO <sub>4</sub> g <sup>-1</sup> water)	$t_{\text{ind}}$ (s)	Measure error ( $\pm s$ )
Without ultrasound		
0.0156	8978	340
0.0166	4040	200
0.0174	1830	140
0.0175	4029	135
0.0179	769	70
0.0186	1276	45
0.0188	2476	175
0.0198	1520	120
0.0213	959	65
0.0215	672	100
0.0217	591	70
0.0217	1459	85
$P_{\text{diss}} = 0.05 \text{ W g}^{-1}$ solution		
0.0119	6493	150
0.0124	3053	150
0.0125	3261	60
0.0125	4080	125
0.0128	4506	200
0.0131	2915	150
0.0131	3235	155
0.0132	3715	150
0.0132	2668	120
0.0136	4275	100
0.0139	3920	85
0.0142	1658	120
0.0148	910	50
0.0149	1655	90
0.0154	858	50
0.0157	869	45
0.0159	1382	100
0.0162	975	75
0.0164	1032	60
0.0166	689	60
0.0166	648	65
0.0174	616	60
$P_{\text{diss}} = 0.12 \text{ W g}^{-1}$ solution		
0.0093	3464	50
0.0104	3204	135
0.0106	3505	85
0.0108	3837	80
0.0108	2643	75
0.0112	3560	150
0.0124	1453	90
0.0125	2857	135
0.0125	1841	65
0.0127	2308	175
0.0135	1863	55
0.0139	1421	25
0.0140	1635	50
0.0147	1044	20
0.0153	1281	45
0.0156	520	62

especially at low absolute supersaturations ( $<0.014 \text{ g K}_2\text{SO}_4 \text{ g}^{-1} \text{ water}$ ). This effect is less significant at high supersaturation when nucleation is very fast anyway.

In Fig. 6, the plots of  $\ln(t_{\text{ind}})$  versus  $(\ln^2 S)^{-1}$  for experiments with and without ultrasound are represented. The values corresponding to an induction time lower than 1400 s

Table 2  
Calculation of the absolute supersaturation at the wall

$P_{\text{diss}}$ (W g <sup>-1</sup> solution)	$\Delta T = T_{\text{sol}} - T_{\text{sol}}^w$ (°C)	$\Delta C_w$ (g K <sub>2</sub> SO <sub>4</sub> g <sup>-1</sup> water)
0.00	0.28	$\Delta C + 0.0006$
0.05	0.89	$\Delta C + 0.0019$
0.12	1.23	$\Delta C + 0.0026$

for experiments without ultrasound and lower than 700 s for experiments with ultrasound are not taken into account because the cooling time is too high in comparison with the induction period. The corresponding equations are

$$P_{\text{diss}} = 0.00 \text{ W g}^{-1} \text{ solution,}$$

$$\ln(t_{\text{ind}}) = (3.69 \times 10^{-2} \pm 0.06 \times 10^{-2})(\ln^2 S)^{-1} + (4.85 \pm 0.11) \quad (11)$$

$$P_{\text{diss}} = 0.05 \text{ W g}^{-1} \text{ solution,}$$

$$\ln(t_{\text{ind}}) = (2.35 \times 10^{-2} \pm 0.05 \times 10^{-2})(\ln^2 S)^{-1} + (4.42 \pm 0.12) \quad (12)$$

$$P_{\text{diss}} = 0.12 \text{ W g}^{-1} \text{ solution,}$$

$$\ln(t_{\text{ind}}) = (0.91 \times 10^{-2} \pm 0.02 \times 10^{-2})(\ln^2 S)^{-1} + (6.12 \pm 0.06) \quad (13)$$

The numerical values of the slopes are low, suggesting that the main mechanism is heterogeneous primary nucleation [11]. When ultrasound is applied or when ultrasound power increases, the slope decreases. This change of slope suggests that ultrasound modifies the product  $[\gamma_s^3 f(\theta)]$  (Eq. (1)) [17]. Ultrasound seems to change the activation energy to act on either the surface energy crystal-solution or the contact angle. So, ultrasound may decrease the critical radius.

For experiments at  $0.12 \text{ W g}^{-1}$  solution, there seems (Fig. 6) to be a break for  $(1/\ln^2 S)$  contained between 160 and 200. This change corresponds to the low values of the induction time. This break could correspond to a change in the nucleation mechanism.

However, when ultrasound is applied to the solution, a lower wall temperature is required to maintain the same reactor temperature in order to allow the ultrasound power to be removed by the jacket. Therefore, the absolute supersaturation at the wall is higher when ultrasound is applied, and this could result in a shortening of the induction time. In order to distinguish between the specific contributions of ultrasound and of this thermal effect, we have estimated the wall temperature as a function of the solution temperature and ultrasound power (see Appendix A). We can then calculate the absolute supersaturation at the wall  $\Delta C_w$ , as a function of the bulk absolute supersaturation  $\Delta C$ , for experiments with and without ultrasound (see Table 2). The difference between both supersaturations (bulk and wall) is negligible in experiments without ultrasound, but increases

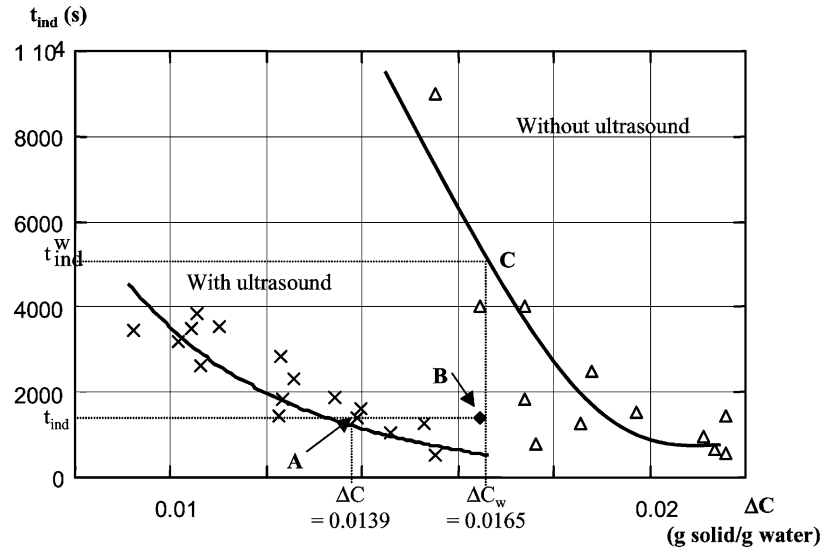


Fig. 7. Induction time as a function of supersaturation with and without for an ultrasound power of  $0.114 \text{ W g}^{-1}$  solution.

significantly with ultrasound power: one might suspect that the observed effect of ultrasound could be simply due to this artefact.

For experiments with ultrasound, it can be verified that the measured induction time is always much shorter than the induction time, which would have been observed without ultrasound with a supersaturation equal to  $\Delta C_w$  (Fig. 7). For a bulk supersaturation  $\Delta C$  (point A), the corresponding wall supersaturation is  $\Delta C_w$  (point B). For this supersaturation, the induction time without ultrasound  $t_{\text{ind}}^w$  (about 5800 s, point C) remains much higher than the measured one (1421 s, point B).

As a result, we can conclude that ultrasound has a strong specific effect on nucleation, which can by no means be explained by the wall temperature effect.

#### 4.2. Metastable zone widths

The measurements of the metastable zone width with and without ultrasound are presented in Fig. 8 and in Table 3. Correlation equations of the data are

(a) Without ultrasound

$$\ln(\dot{b}) = (5.81 \pm 0.30) \ln(\Delta T_{\text{max}}) - (11.69 \pm 0.91) \quad (15)$$

(b) With ultrasound

$$\ln(\dot{b}) = (2.74 \pm 0.18) \ln(\Delta T_{\text{max}}) - (3.55 \pm 0.52) \quad (16)$$

(c) Nyvlt et al.  $\ln(\dot{b}) = 13.64 \ln(\Delta T_{\text{max}}) - 31.24 \quad (17)$

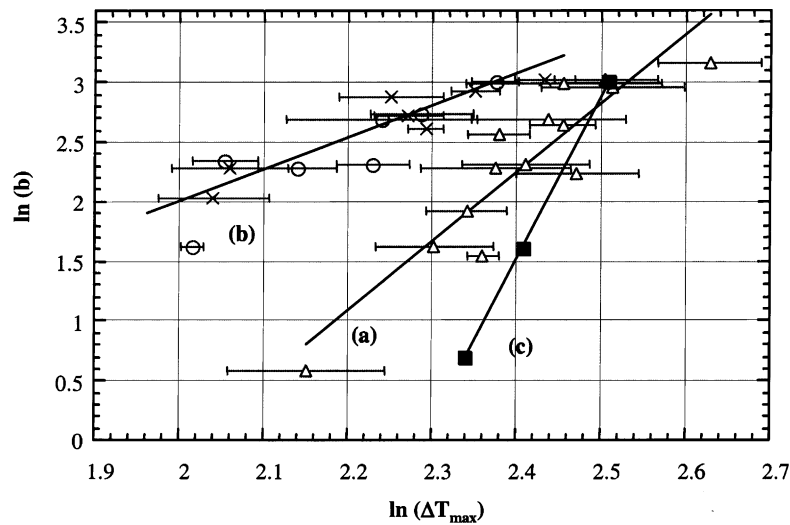


Fig. 8. Nucleation characteristics of potassium sulphate aqueous solutions which saturation temperature is  $30^\circ\text{C}$ : (a) without ultrasound, (b) with ultrasound and (c) Nyvlt et al.



Table 3

Average values of the measurement of the metastable zone width for a saturation temperature equal to 30 °C

$\bar{b}$ (°C h <sup>-1</sup> )	$\Delta T_{\max}$ (°C)	Total error (±°C)	Experiments number
Without ultrasound			
1.80	8.6	0.80	1
4.68	10.60	0.20	1
5.04	10.00	0.70	4
6.84	10.40	0.50	1
9.36	11.85	0.85	2
9.72	10.76	0.96	5
10.08	11.15	0.85	2
12.96	10.80	0.40	1
14.04	11.65	0.45	2
14.76	11.45	1.05	4
19.08	12.35	1.05	2
19.80	11.65	1.35	2
20.52	12.25	0.75	2
22.05	13.85	0.85	2
$P_{\text{diss}} = 0.05 \text{ W g}^{-1}$ solution			
5.04	7.50	0.10	1
10.44	7.80	0.30	1
9.72	8.50	0.20	2
10.08	9.30	0.40	1
14.76	9.40	1.10	2
15.48	9.85	0.60	1
20.16	10.75	0.30	1
$P_{\text{diss}} = 0.12 \text{ W g}^{-1}$ solution			
7.56	7.70	0.50	1
9.72	7.85	0.55	2
13.68	9.90	0.20	1
15.12	9.70	0.40	1
17.64	9.50	0.60	1
18.72	10.50	0.30	1
20.52	11.40	0.40	1

We can consider that our results obtained without ultrasound (a) are comparable with those of Nyvlt et al. (c) [15,18] with respect to the difficult control of the primary nucleation. This behaviour is strongly modified when ultrasound is applied; but we did not observe a significant difference between the two tested ultrasonic powers (0.05 and 0.12 W g<sup>-1</sup> solution). The slope of the  $\ln(\bar{b})$  versus  $\ln(\Delta T_{\max})$  line is strongly reduced with ultrasound, while the intercept point is increased. From Eq. (10) we can conclude that ultrasound decreases the apparent order of nucleation  $n$ .

As for the determination of the absolute supersaturation at the wall, we can estimate the metastable zone width at the wall. For these measurements, the difference between the solution temperature and the inner wall temperature is not significant. The difference is about 0.16 °C without ultrasound and about 0.55 °C with ultrasound. The maximum undercooling at the wall  $\Delta T_{\max}^w$  with ultrasound is always lower than the maximum undercooling at the wall  $\Delta T_{\max}^w$  and in the solution  $\Delta T_{\max}$  without ultrasound. Thus, we observe only an effect of the ultrasound on the metastable zone width.

## 5. Conclusions

It has been shown that ultrasound can influence the primary nucleation of potassium sulphate.

Ultrasound reduces the induction time especially for low absolute supersaturation. For experiments with ultrasound, the predominant effect has been identified as a specific effect of ultrasound and not an effect of the lower wall temperature. The exploitation of the induction time models shows that the main mechanism is a heterogeneous primary nucleation mechanism. Using the different models of classical primary nucleation theory, ultrasound seems to decrease the activation energy so they can decrease the critical radius. However, these different models do not allow an explanation of the mechanism of the action of ultrasound.

The metastable zone width can also be reduced by the application of ultrasound. The apparent orders of nucleation or growth are decreased by ultrasound. Results indicate that it would be sufficient to apply a low ultrasonic power to decrease the metastable zone width. Hence, ultrasound decreases the apparent order of the primary nucleation rate and increases the rate of appearance of the solid.

It seems that ultrasound modified the mechanism of nucleation itself, since the apparent order of nucleation is strongly reduced in the presence of ultrasound.

Some explanations can be proposed on the action of ultrasound:

- Does ultrasound increase the heterogeneity of the system or does it create new nucleation sites?
- The increase of the nucleation rate could be explained by the presence of shock waves in the solution. These waves could increase the probability of collisions of a molecule and a molecular aggregate.

With this study, we have shown that ultrasound permits to set off nucleation at supersaturations lower than without ultrasound. In industrial crystallisation processes, ultrasound can induce nucleation in conditions where spontaneous primary nucleation cannot occur without ultrasound. Moreover, ultrasound could allow seeding to be avoided and thus avoiding the introduction of foreign particles into the solution.

## Appendix A

From classical relations of thermal transfer in a reactor we have calculated the difference  $\Delta T$ , between the solution temperature ( $T_{\text{sol}}$ ) and the wall temperature ( $T_{\text{sol}}^w$ ) (Fig. 9).

The transfer heat flux is expressed as

$$\phi = U \bar{S} (T_{\text{sol}} - T_f) \quad (\text{A.1})$$

$$\phi = h_s S_{\text{int}} (T_{\text{sol}} - T_{\text{sol}}^w) \quad (\text{A.2})$$

The overall heat transfer coefficient expression is given as

$$\frac{1}{U \bar{S}} = \frac{1}{h_s S_{\text{int}}} + \frac{1}{h_f S_{\text{ext}}} + \frac{e}{\lambda_p \bar{S}} \quad (\text{A.3})$$

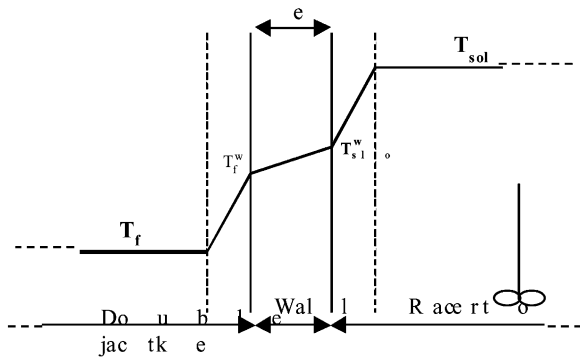


Fig. 9. Thermal transfer through an exchange wall during a cooling.

where  $\bar{S}$ ,  $S_{int}$  and  $S_{ext}$  are respectively the mean exchange surface, the inner exchange surface and the outer exchange surface.

Replacing the inner heat transfer, the overall heat transfer can be connected with the stirrer rate  $N$  by the following equation:

$$\frac{1}{U\bar{S}} = s \times N^{(-a)} + \frac{1}{h'S'} \quad (A.4)$$

where

$$\frac{1}{h'S'} = \frac{1}{h_f S_{ext}} + \frac{e}{\lambda_p \bar{S}} \quad (A.5)$$

Knowing  $e$ ,  $\lambda_p$  and the different surfaces, the heat transfer coefficient between the wall and the cooling fluid,  $h_f$  can be calculated from the intercept of Eq. (A.4) (i.e.  $N_c$  tends to infinity) from experimental overall heat transfer data against  $N$ .

Then, with the Eq. (A.3) we can determine the heat transfer coefficient between the wall and the solution,  $h_s$  and calculate the wall temperature (Eqs. (A.1) and (A.2)).

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