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# Capture of magnetic nanoparticles on ordered magnetizable arrays: A parametric study

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**Abstract.** This work is devoted to the experimental study of the magnetic separation of medium sized nanoparticles (40-70 nm) which are separated from the suspending fluid when the suspension flows through a micropillar array magnetized by an external magnetic field. The nanoparticle accumulation around micropillars is visualized and described by the capture efficiency and retention capacity, which are analysed in function of different dimensionless parameters, such as Mason number, dipolar coupling parameter, nanoparticle volume fraction, orientation of the flow with respect to the magnetic field and array's geometry. The role of these parameters is interpreted in terms of the interplay between hydrodynamic and magnetic interactions, as well as taking into account possible field-induced phase separation. The results could be useful for the development of the microscale magnetic separators for biomedical applications.

## 1 Introduction

Small scale magnetic separation of magnetic particles has found numerous biomedical applications, such as cell separation [1], protein purification [2], control drug delivery and release [3] and immunoassays [4]. In most of these applications, micron sized beads bearing appropriate chemical groups on their surface are used, while the use of nanoparticles is limited because of strong Brownian motion hindering attractive interactions with magnetized collectors. However, phase separation or aggregation induced by an applied magnetic field have been found to significantly enhance these interactions leading to stronger magnetophoretic mobility of particles [5] and better separation efficiency [6]. The reason is that the magnetic force experienced by micron-sized aggregates is much larger than that of individual nanoparticles. This will likely allow replacement of microbeads by nanoparticles in aforementioned applications for which high specific surface and good colloidal stability are unconditional advantages of nanoparticles with respect to microbeads.

In our previous work, we have demonstrated an efficient capture of magnetic nanoparticles of a mean size about 80 nm on an ordered array of nickel micropillars incorporated into a microfluidic channel [7]. The micropillars were magnetized by an external uniform magnetic field of an intensity 6-10 kA/m. However, the capture efficiency  $\Lambda$  (related to the ratio of the inlet-to-outlet particle concentration) appeared to be a strongly decreasing function of the flow speed and of

the Mason number:  $\Lambda \propto Ma^{-1.78}$  that was explained by flow-induced rupture of the particle aggregates.

To optimize the capture efficiency keeping low values of the applied magnetic field, we have to establish and understand the effects of numerous parameters (other than  $Ma$ ) on the nanoparticle capture, such as dipolar coupling parameter, nanoparticle concentration, magnetic field orientation and geometry of micropillar arrays. This work is dedicated to an extensive parametric study of the magnetic separation process on ordered magnetizable arrays. To this purpose, we visualize the process of accumulation of magnetic nanoparticles around the micropillars when the nanoparticle suspension flows across the micropillar array in the presence of an externally applied magnetic field. Growth of the nanoparticle deposits with time allows analyzing the capture efficiency as function of numerous dimensionless parameters. In the next Section 2, we briefly describe the experimental setup and protocol. The results of the visualization experiments and parametric studies are presented in Section 3. The conclusions and perspectives are outlined in Section 4.

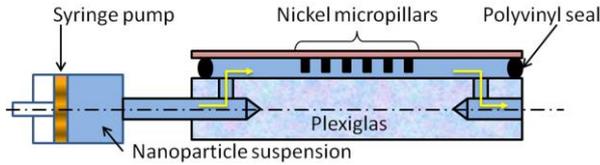
## 2 Experimental setup

A sketch of the microscale channel equipped with an array of nickel micropillars is presented in Fig.1. Briefly, micropillar arrays were created on a glass substrate by electroplating and soft photolithography, as described in [7]. Square and hexagonal arrays were used with the micropillar expected diameter, expected height and the distance between the pillar axes equal to  $d_m=50 \mu\text{m}$ ,

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$h=50\ \mu\text{m}$  and  $\Delta=150\ \mu\text{m}$ , respectively. The flow channel was created by squeezing a polyvinyl seal between a Plexiglas substrate and the glass cover bearing micropillars. The channel height was approximately adjusted to  $H\approx 2h=100\ \mu\text{m}$  by four screws pressing the glass cover to the Plexiglas substrate through an aluminium lid not shown in Fig.1. This design has an advantage of easy disassembling required for frequent cleaning of the cell, as opposed to permanently sealed microfluidic channel used in [7].

Water dispersions of iron oxide nanoparticles (ferrofluids) were synthesized by co-precipitation of iron salts in alkali medium and stabilized by a double layer of oleate ions, as described in detail in [8]. Using this method, instead of isolated nanoparticles (8-12 nm), permanent isotropic nanoclusters composed of numerous nanoparticles were obtained. These nanoclusters possessed an induced magnetic moment and had zero remnant magnetization. Since nanoclusters (40-70 nm) are the smallest structural units involved into magnetic separation process, they will be hereinafter called nanoparticles in order to avoid confusion with field-induced aggregates. The two synthesized ferrofluids, labelled as F1 and F2, contained nanoparticles of a mean diameter of  $d_n=68\ \text{nm}$  and  $42\ \text{nm}$ , respectively, as measured by dynamic light scattering and confirmed by transmission electron microscopy. The primary ferrofluids F1 and F2 were diluted at desired particle concentrations by distilled water.



**Fig. 1.** Microscale channel with a micropillar array

A dilute suspension of magnetic nanoparticles was pushed through the channel with a desired flow rate  $Q$  using a syringe pump Harvard PHD Ultra (United States). The flow velocity  $u$  was estimated as  $u=Q/S$ , where  $S$  is the channel cross-section. The channel was settled on the stage of an inverted microscope Diaphot (Nikon, Japan). Images were collected in transmission light with a four-fold objective and a CMOS camera PL-B742U (PixelLINK, Canada). An external uniform magnetic field was generated with a pair of Helmholtz coils equipped with iron yokes and placed around the microscope. The angle between the external field  $\mathbf{H}_0$  and the main flow was changed in the range  $\alpha=0-90^\circ$  by turning the flow cell on the microscope stage.

The following experimental protocol was adopted. First, the suspension was pushed through the channel at a desired velocity  $u$  in the absence of magnetic field for 5 minutes. Then, a magnetic field of a desired intensity  $H_0$  was applied. The nickel micropillars got magnetized and started to attract magnetic nanoparticles and separate them from the suspending liquid (water). Snapshots of nanoparticle accumulation around micropillars (such as shown in Fig.2) were taken every minute for 60 minutes from the moment of field application. For quantification

of the acquired time-lapses, we developed a macro under ImageJ to automatically segment the pillars and their neighbourhood. The macro measured the surface of nanoparticle deposits per pillar versus time. The relative deposit area was defined as the ratio of the whole area occupied by nanoparticle deposits to the whole area of the micropillar array. The image processing allowed obtaining experimental dependencies of the relative deposit area,  $s$ , versus the elapsed time  $t$ . In each case, the experimental  $s(t)$  curves were satisfactorily fitted to the following semi-empirical filtration law [7]:

$$s(t) = s_m \left[ 1 - \exp\left(-\frac{\phi_0 \Lambda u t}{\Phi s_m L}\right) \right] \quad (1)$$

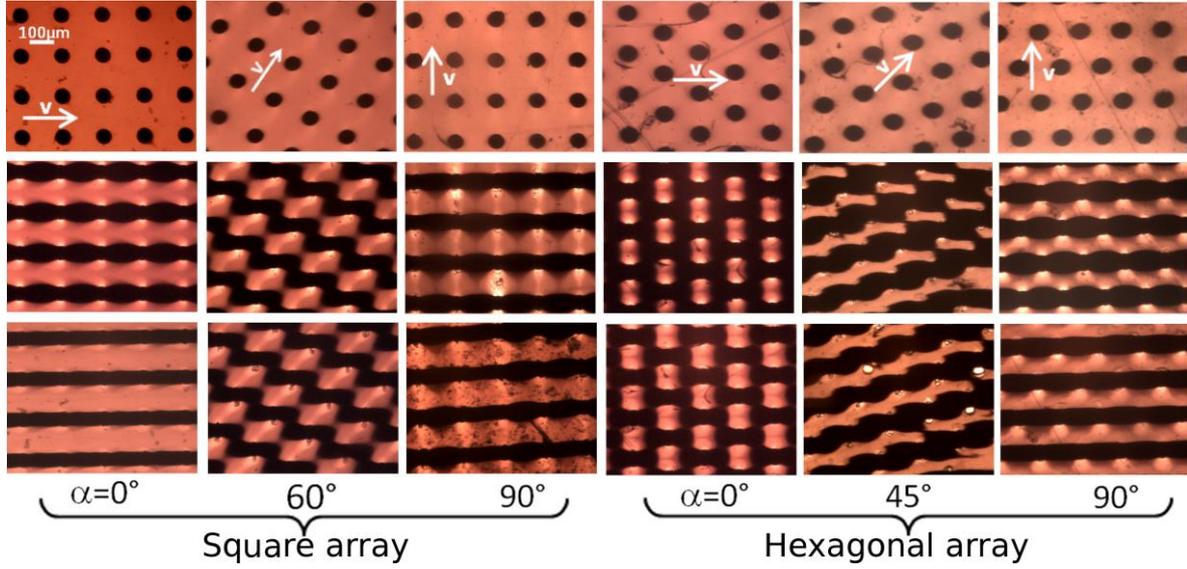
where  $\phi_0$  is the nanoparticle volume fraction at the channel inlet;  $\Phi\approx 0.70$  is the internal volume fraction of the deposit;  $L=1.3-1.5\ \text{mm}$  – array's dimension in the direction of flow;  $\Lambda=\ln(\phi_0/\phi_{out})$  is the capture efficiency in the beginning of separation ( $t=0$ ), this magnitude is related to the inlet ( $\phi_0$ ) and outlet ( $\phi_{out}$ ) nanoparticle volume fractions; and  $s_m$  is the maximum relative deposit area at long times ( $t\rightarrow\infty$ ), this magnitude characterizes the maximum amount of nanoparticles that the filter is able to capture and is hereinafter called the retention capacity. Typical  $s(t)$  curves have been presented in our previous work [7]. The magnitudes  $\Lambda$  and  $s_m$  are two fitting parameters depending on microscopic details of the particle capture. These magnitudes are analyzed in Section 3.2 as a function of different dimensionless parameters governing separation.

## 3 Results and discussion

### 3.1 Visualisation of particle deposits

Some snapshots showing nanoparticle deposits around the micropillars are shown in Fig.2. The upper row of the snapshots shows the top view of the micropillar arrays without captured nanoparticles, the middle and the bottom rows show nanoparticle deposits for the sample F1 at the flow speeds  $u=7.14\times 10^{-4}\ \text{m/s}$  and  $2.14\times 10^{-3}\ \text{m/s}$ , respectively, at an applied magnetic field  $H_0=13.5\ \text{kA/m}$ , inlet particle volume fraction  $\phi_0=0.3\%$  and elapsed time  $t=60\ \text{min}$ . Different columns correspond to different angles  $\alpha$  between the flow (whose direction is indicated by white arrows) and the magnetic field (horizontal for each snapshot). The three left columns show the capture on the square array, while the right three columns – on the hexagonal array.

In most of the snapshots, the nanoparticle deposits exhibit wavy patterns interconnecting the neighbouring micropillars and having a wavelength corresponding to the distance between them. In the beginning of the capture process (not shown in Fig.2), the nanoparticles are condensed in the vicinity of the micropillars and form concentrated elliptic deposits, which grow in the direction of the applied magnetic field until they touch each other. Percolation of primary elliptic deposits should explain wavy shape of the final deposits governed



**Fig. 2.** Snapshots of nanoparticles deposits around micropillars. The upper row shows naked micropillars without captured particles, the second and the bottom rows show nanoparticle deposits for the sample F1 at the flow speed  $u=7.14 \times 10^{-4}$  m/s and  $2.14 \times 10^{-3}$  m/s, respectively and for  $H_0=13.5$  kA/m,  $\phi_0=0.3\%$  and  $t=60$  min. The applied magnetic field is horizontal for each snapshot.

by the stress balance on their surface. The flow intensity and orientation influence the shape of the deposits which evolve to a straight stripe pattern with increasing speed in the case of the square array with  $\alpha=0^\circ$  [bottom left snapshot in Fig. 2] or to a honeycomb pattern in the case of the hexagonal array at  $\alpha=0^\circ$  [4<sup>th</sup> column from the left of Fig.2]. The last pattern with the highest deposit area is possible thanks to a gap of a thickness  $H-h \approx 50$   $\mu\text{m}$  between the end surface of micropillars and the bottom Plexiglas surface of the channel [Fig.1] allowing the liquid to pass through the channel.

When the flow makes some angle  $0^\circ < \alpha < 90^\circ$  with respect to the magnetic field  $\mathbf{H}_0$ , the nanoparticle deposits are no longer aligned with the applied magnetic field but show stair-like patterns making some angle with  $\mathbf{H}_0$  different from  $\alpha$ . Again, these patterns appear as a result of percolation of neighbouring deposits which find the optimal pathways for percolation depending on hydrodynamic drag and magnetic interactions between primary deposits. So, the descending stair-like pattern for the square array at  $\alpha=60^\circ$  is formed by linking primary deposits in the direction of flow [2<sup>nd</sup> column from the left in Fig.2], while ascending pattern for the hexagonal array at  $\alpha=45^\circ$  is formed by linking the deposits in the direction of the applied field [2<sup>nd</sup> column from the right in Fig.2]. In the case of the flow perpendicular to the magnetic field ( $\alpha=90^\circ$ ), the patterns are quite similar to those observed for the flow parallel to the field ( $\alpha=0^\circ$ ) except some asymmetry with respect to the horizontal axis (magnetic field direction) [3<sup>rd</sup> and the last columns of Fig.2].

Comparing the middle and the bottom rows of Fig.2, it is seen that the size of the deposits decreases with the flow speed because of the larger hydrodynamic stresses acting on the deposit surface and washing away nanoparticles. Comparing the left three columns with the right three right three columns, it is quite obvious that the hexagonal array generally captures more

nanoparticles than the square array. This can be explained by simple geometrical considerations. In fact, at the same distance between micropillars and at the same size of the primary elliptical deposits, the distance between the surfaces of primary deposits is closer for the hexagonal array allowing easier percolation and junction at several points, as in the case of honeycomb structure at  $\alpha=0^\circ$ . In summary, the array geometry and mutual orientation of the flow and of the magnetic field are crucial parameters defining the structure of the nanoparticle deposits and the retention capacity  $s_m$  [Section 2]. The parameters  $\Lambda$  and  $s_m$  quantifying magnetic separation will be inspected in details in the next Section 3.2.

### 3.2 Capture efficiency and retention capacity

Experiments show that the micropillars capture a small amount of nanoparticles in the absence of field, while the capture is significant in the presence of moderate magnetic fields  $4.8 \leq H_0 \leq 13.5$  kA/m. This signifies that colloidal interactions are negligible as compared to magnetic ones. In this case, the capture of magnetic nanoparticles is mostly governed by hydrodynamic ( $F_h$ ) and magnetic ( $F_m$ ) forces and can be affected by Brownian motion. Comparison of orders of magnitudes of these forces (or energies  $U$ ) allows definition of the three following dimensionless parameters: (a) Mason number  $Ma = F_h / F_m = 6\eta_0 u d_m / (\beta_n \mu_0 H_0^2 d_n^2)$ ; (b) dipolar coupling parameter  $\lambda = U_m / (k_B T) = \pi \beta_n^2 \mu_0 H_0^2 d_n^3 / (12 k_B T)$ ; and (c) Péclet number  $Pe = u d_m / D_n = 3\pi \eta_0 u d_n d_m / (k_B T) = 6\lambda Ma / \beta_n$ , where  $\eta_0 \approx 10^{-3}$  Pa·s is the suspending liquid (water) viscosity;  $\mu_0 = 4\pi \times 10^{-7}$  H/m is the vacuum magnetic permeability;  $\beta_n \approx 0.9$  is the magnetic contrast factor of nanoparticles;  $k_B T \approx 4 \times 10^{-21}$  J is the thermal agitation

energy; and  $D_n$  is the Brownian diffusion coefficient of nanoparticles.

Inspecting dependencies of the capture efficiency  $\Lambda$  and retention capacity  $s_m$  on one of the parameters  $Ma$ ,  $\lambda$  and  $Pe$ , varying all other parameters, we realize that different data better collapse when plotted against Mason number. Thus, in what follows, the magnitudes  $\Lambda$  and  $s_m$  will be mostly analysed as function of Mason number.

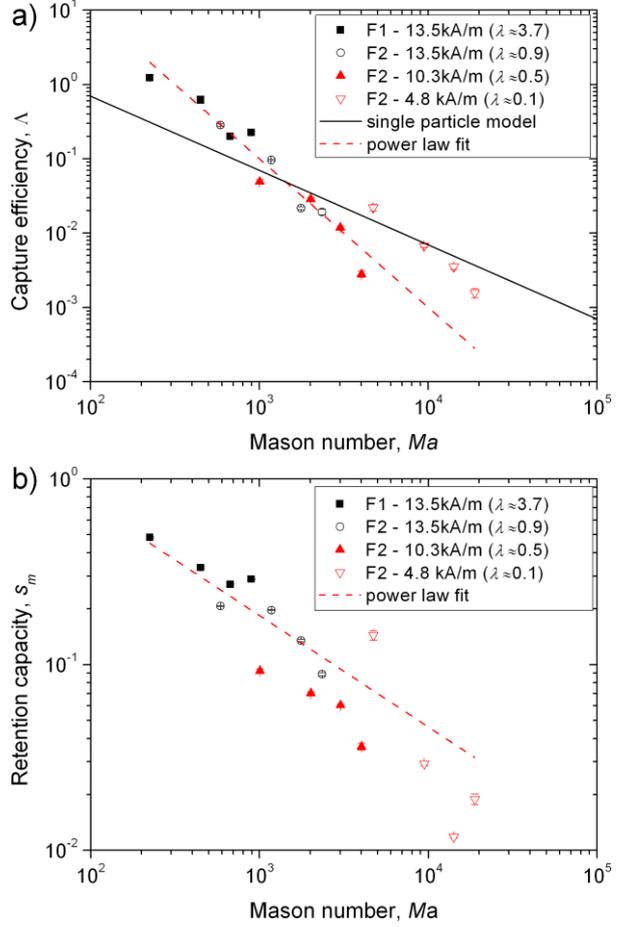
Mason number dependencies of  $\Lambda$  and  $s_m$  are shown in Fig. 3 for two different particle diameters  $d_n$  (samples F1 with  $d_n=68$  nm and F2 with  $d_n=42$  nm) and three different values of the applied magnetic field  $H_0$  while the particle concentration ( $\phi_0=0.3\%$ ), flow orientation ( $\alpha=0^\circ$ ) and arrays' geometry (square) are kept constant. Variations of  $d_n$  and  $H_0$  result in a variation of the dipolar coupling parameter in the range  $0.1 \leq \lambda \leq 3.7$ . Three experimental  $\Lambda$  versus  $Ma$  curves, corresponding to  $\lambda \geq 0.5$ , are gathered along a straight line in log-log scale and fitted by a scaling law  $\Lambda \propto Ma^{-2}$  (dashed line on Fig. 3a), while the fourth curve with  $\lambda \approx 0.1$  shows a weaker Mason number dependency. Experiments show that nanoparticle suspensions undergo phase separation with appearance of bulk aggregates at  $\lambda \geq 0.5$  and  $\phi_0=0.3\%$ <sup>1</sup>. Intense shear flows around the micropillars can disrupt nanoparticles from aggregates such that the aggregate size is expected to be a decreasing function of the flow speed  $u$  and of the Mason number. The combination of this effect with increasing convective flux washing away the aggregates from the micropillars could explain a strong decrease of the capture efficiency with Mason number ( $\Lambda \propto Ma^{-2}$ ) for  $\lambda \geq 0.5$ . The theoretical model assuming chain-like clusters instead of observed bulk needle-like aggregates predicts a quite similar behaviour ( $\Lambda \propto Ma^{-1.7}$ ) [7]. Furthermore, collapse of the experimental Mason number dependencies for  $\lambda \geq 0.5$  signifies that the capture is governed by the interplay between magnetic and hydrodynamic forces, while the Brownian motion of bulk aggregates is expected to be very weak. Nanoparticle suspensions do not exhibit phase separation at  $\lambda=0.1$  and  $\phi_0=0.3\%$ . In this case, the capture efficiency of individual nanoparticles is only defined by a compromise between convective, magnetophoretic and diffusive fluxes. A simple model neglecting diffusive flux predicts the following Mason number dependency in the limit  $Ma \gg 1$  [7]:

$$\Lambda \approx 16 \frac{cL}{(1-c)^2 d_m} Ma^{-1} \quad (2)$$

where  $c$  is the volume fraction of the micropillars with respect to the total array's volume;  $c \approx 0.09$  and  $0.10$  for the square and hexagonal arrays, respectively. The theoretical dependency [Eq. (2), solid line in Fig. 3a] agrees relatively well with experimental points for  $\lambda \approx 0.1$

<sup>1</sup> Field-induced phase separation is possible at such low values of  $\lambda$  because both samples F1 and F2 have relatively broad particle size distribution; the largest particles with the size above 100 nm are assumed to form the dense phase (aggregates) while the smallest ones remain in a dilute phase, as suggested in numerous works – see for example [9].

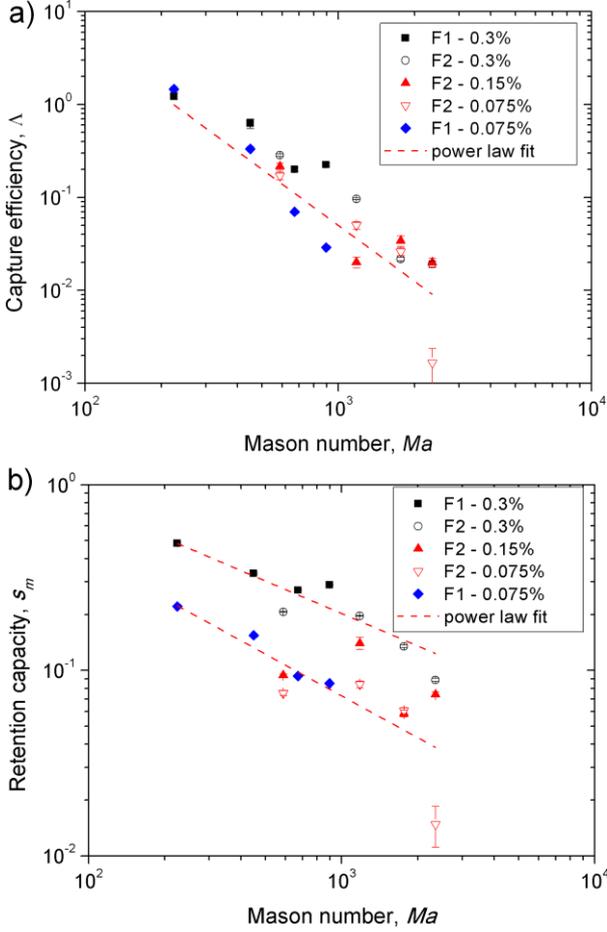
[open triangles] without adjustable parameters. Thus, the single particle model supports a smoother decrease of the capture efficiency with growing Mason numbers ( $\Lambda \propto Ma^{-1}$ ) at  $\lambda \approx 0.1$ , as opposed to the case of phase separating colloid ( $\Lambda \propto Ma^{-2}$ ) at  $\lambda \geq 0.5$ .



**Fig. 3.** Mason number dependency of the capture efficiency (a) and retention capacity (b) at different dipolar coupling parameter  $\lambda$  and fixed values of  $\phi_0=0.3\%$ ,  $\alpha=0^\circ$  and for the square array. Solid line in (a) stands for the prediction of the single particle model [Eq. (2)]. Dashed lines in (a) and (b) correspond to a power-law fit of the experimental data.

The retention capacity fits to an approximate scaling law  $s_m \propto Ma^{-0.6 \pm 0.1}$  but the data are much more dispersed around the fitting curve [dashed line on Fig. 3b]. The maximum size of deposits is expected to decrease with increasing diffusive nanoparticle flux responsible for nanoparticle “evaporation” from the deposit surface. This could explain generally lower retention capacities for lower dipolar coupling parameters  $\lambda$ , as observed in Fig. 3b.

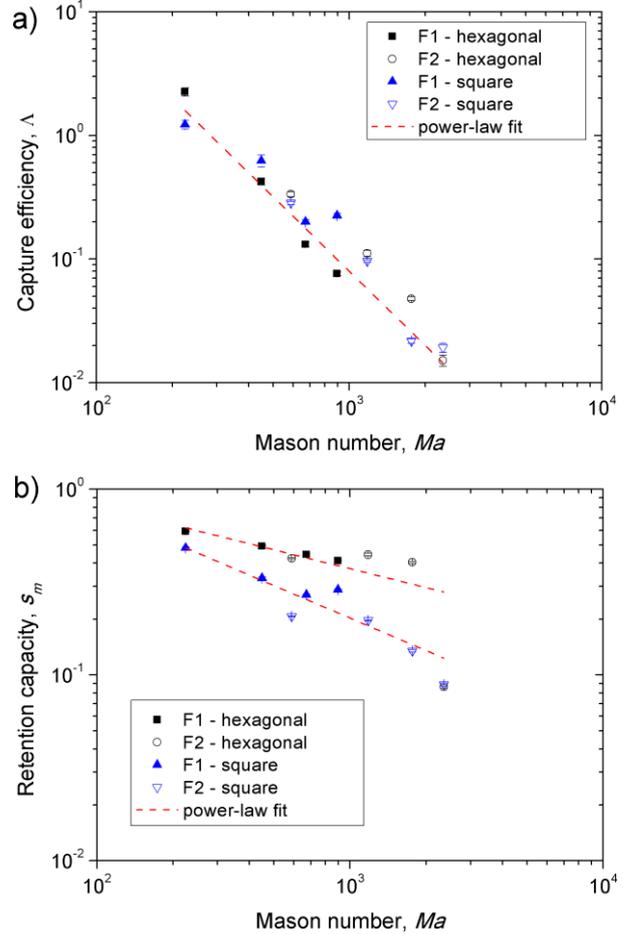
The effect of the particle volume fraction  $\phi_0$  is inspected in Fig. 4 where Mason number dependencies of  $\Lambda$  and  $s_m$  are shown for different values of  $\phi_0$  and for two samples F1 and F2 at constant magnetic field intensity ( $H_0=13.5$  kA/m), the flow orientation ( $\alpha=0^\circ$ ) and the array's geometry (square). Experiments show that the suspensions undergo phase separation for all the curves presented in Fig. 4. The Mason number dependencies of the capture efficiency are spread around a master curve



**Fig. 4.** The same as in Fig.3 but at different particle volume fractions  $\phi_0$  and for two different samples (F1 and F2) at fixed values of  $H_0=13.5$  kA/m,  $\alpha=0^\circ$  and for the square array. The dashed line in (a) corresponds to a fit of all the data by a single curve  $\Lambda \propto Ma^{-2}$ , while two dashed curves in (b) correspond to the fit of the data at  $\phi_0=0.3\%$  and  $\phi_0=0.075\%$  by two distinct curves having the same scaling behaviour  $s_m \propto Ma^{-0.6 \pm 0.1}$ .

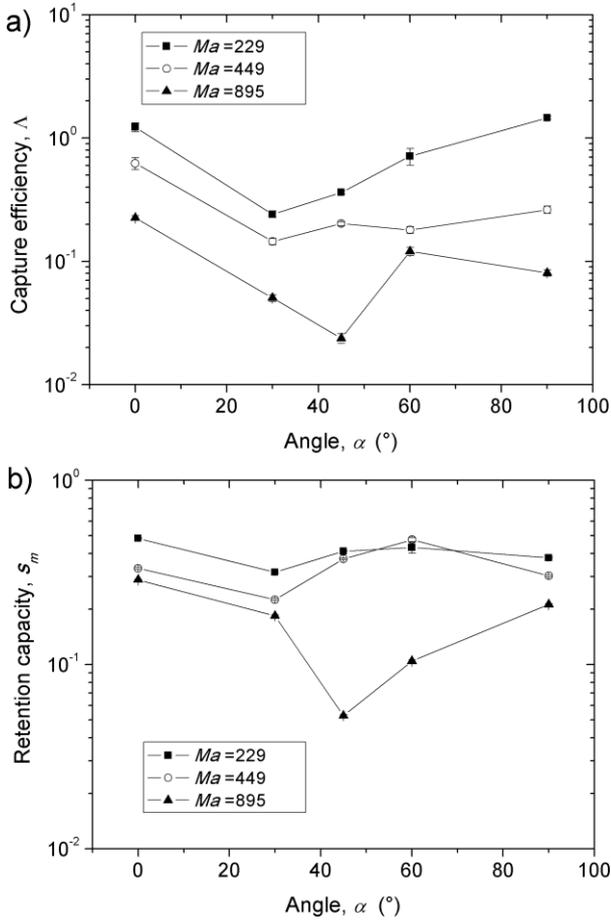
with a scaling law  $\Lambda \propto Ma^{-2}$  [dashed line in Fig. 4a] inherent for phase separating colloids, while there is no clear effect of the particle volume fraction. This is in agreement with the scenario of destructible aggregates [7] where their size and interaction with micropillars depend entirely on Mason number but not on particle concentration, at least in the beginning of separation when the dilute limit applies in the whole volume of the filter. The Mason number dependencies of the retention capacity follow previously found scaling law  $s_m \propto Ma^{-0.6 \pm 0.1}$  but no longer collapse on a single curve for different particle concentrations and show an increase of  $s_m$  with increasing  $\phi_0$  [Fig. 4b]. This is probably because the dilute limit approach is no longer valid for the concentrated deposits and their size is expected to grow with the inlet particle concentration because of enhanced magnetic interactions between nanoparticles that result in larger deposit sizes, as has been previously shown for separation on single collectors [8].

The effect of the array's geometry is shown in Fig.5 where  $\Lambda$  and  $s_m$  versus  $Ma$  dependencies are plotted for square and hexagonal arrays and for two different particle sizes (samples F1 and F2) at constant nano-



**Fig. 5.** The same as in Fig.3 but for different array geometries (square and hexagonal) and for two different samples (F1 and F2) at fixed values of  $H_0=13.5$  kA/m,  $\alpha=0^\circ$ , and  $\phi_0=0.3\%$ . The dashed line in (a) corresponds to a fit of all the data by a single curve  $\Lambda \propto Ma^{-2}$ , while two dashed curves in (b) correspond to the fit of the data for the square and hexagonal arrays by two distinct curves,  $s_m \propto Ma^{-0.6 \pm 0.1}$  and  $s_m \propto Ma^{-0.34 \pm 0.11}$ , respectively.

particle volume fraction ( $\phi_0=0.3\%$ ), field intensity ( $H_0=13.5$  kA/m) and the flow orientation ( $\alpha=0^\circ$ ). Field-induced phase separation is observed for all the experimental data on Fig.5. Again, the data on the capture efficiency collapse on a single master curve  $\Lambda \propto Ma^{-2}$  [dashed line on Fig. 5a], while the data on the retention capacity are regrouped along two different curves corresponding to both considered geometries:  $s_m \propto Ma^{-0.60 \pm 0.10}$  for square arrays and  $s_m \propto Ma^{-0.34 \pm 0.11}$  for hexagonal arrays [dashed curves on Fig. 5b]. The array's geometry does not influence the initial capture efficiency  $\Lambda$  likely because, in the beginning of separation, the nanoparticle trajectories in the vicinity of a given micropillar are expected to be weakly influenced by the geometrical disposition of the neighbouring pillars provided that they occupy only about 10% of the array volume ( $c \approx 0.1$ ). On the other hand, the hexagonal array has a larger retention capacity than the square array (in agreement with observations on Fig.2) likely because hexagonal arrays favour more easily percolation of the primary elliptical deposits, as has been supposed in Section 3.1.



**Fig. 6.** Dependences of the capture efficiency and retention capacity on the angle  $\alpha$  between the flow and the magnetic field for different values of  $Ma$ , at fixed values of  $H_0=13.5$  kA/m,  $\phi_0=0.3\%$ , and for the sample F1 and the square array.

The effect of the flow orientation with respect to the applied magnetic field is inspected on Fig. 6 where  $\Lambda$  and  $s_m$  are plotted as function of the angle  $\alpha$  for different values of Mason number. The capture efficiency exhibits a minimum at some intermediate angles [Fig. 6a]. It can be shown that the change of the field orientation significantly changes the local distribution of Mason numbers in the vicinity of micropillars that affects mechanical stability of the nanoparticle aggregates and modifies their size and therefore their capture efficiency. This scenario has to be studied in detail in order to confirm if it can explain a non-monotonic  $\Lambda$  versus  $\alpha$  function. The effect of the flow orientation on the retention capacity is even less clear because there is a minimum of  $s_m(\alpha)$ -function for  $Ma=895$  but there is no pronounced effect at  $Ma=229$  and 449 [Fig. 6b].

## 4 Conclusions

We presented a detailed experimental study of the effect of different dimensionless parameters on the magnetic separation of medium-sized nanoparticles (40-70 nm) on ordered arrays of magnetizable micropillars. Visualization of suspension flows across micropillar arrays allowed us to follow formation and growth of nanoparticles deposits and extract two major parameters

describing this process – the capture efficiency  $\Lambda$  in the beginning of separation and the retention capacity  $s_m$  of the array. It has been shown that the capture efficiency depends mostly on Mason number and on the mutual orientation between the flow and the magnetic field, being nearly independent of the dipolar coupling parameter (in the range  $0.5 \leq \lambda \leq 3.7$ ), of the nanoparticle volume fraction (at  $0.075 \leq \phi_0 \leq 0.3\%$ ) and on the array's geometry (square or hexagonal). The Mason number behaviour changing from  $\Lambda \propto Ma^2$  to  $\Lambda \propto Ma^{-1}$  has been explained by transition from destructible nanoparticle aggregates (appearing as a result of field-induced phase separation) at  $\lambda \geq 0.5$  to isolated nanoparticles at  $\lambda < 0.5$ . A non monotonic dependence on the angle  $\alpha$  with a minimum of  $\Lambda$  at intermediate angles is less clear and has been tentatively explained by an effect of  $\alpha$  on mechanical stability of aggregates near the micropillars. The retention capacity has also been found to be a decreasing function of Mason number (typically  $s_m \propto Ma^{-0.6}$ ) however it also depends on all other parameters (increases with  $\lambda$  and  $\phi_0$  and is larger for the hexagonal array than for the square array). Tuning the array's geometry and mutual orientation of the flow and of the magnetic field allows generation of particular patterns of nanoparticle deposits minimally affected by the flow and providing a maximized retention capacity. This could be useful for development of microscale magnetic separators for biomedical applications.

For the deeper understanding of the above reported effects, numerical modelling of the separation process incorporating trajectory analysis and field-induced aggregation has to be conducted in future.

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