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Initial Condensate Composition during Asteroid Impacts

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Abstract

A model has been developed for the chemical composition of early-time condensates forming during planetary impacts at velocities sufficient for complete evaporation of the impactor ($\sim 22 \text{ km s}^{-1}$). Hydrodynamics is approximated as hemispheric expansion of a chondritic impactor described with the help of a new semi-analytic equation of state. The gas phase is a mixture of a large number of molecular and mono-atomic species, whereas the Helmholtz free energy of the condensed phase is approximated as sum of a zero-temperature contribution and an Einstein-Debye solid for the thermal part. Interpolation of the free energy between the states of dense solids and molecular gases is used over the wide range of densities and pressures. Chemical equilibrium calculations, performed in a post-processing step, begin at conditions near the coexistence curve as obtained during hydrodynamic simulations, then the condensed phase contains 31 compound species, among them the most important oxides, sulphides, silicates as well as pure elements occurring in a liquid phase at sufficiently high temperature. The composition of the resulting liquid condensate in terms of major elements is compared to that of spinel inclusions in spherules found worldwide at the K-P boundary.

Key words: Cratering, Earth, Impact Processes, Meteorites

1 Introduction

Impacts of meteorites, asteroids and comets on the earth are capable of causing vaporization of most of the impactor and a comparable or larger volume of target rocks (Pierazzo et al., 1997, 1998). Velocities in large terrestrial or lunar meteorite impacts are sufficient for the vaporisation of silicates; the average impact velocity of near earth objects (NEOs) is $\sim 20 \text{ km s}^{-1}$ (Stuart and Binzel, 2004). In contrast, the average mutual collision velocities of main-belt asteroids of about 5 km s^{-1} (Bottke et al., 1994) are too low for significant evaporation. On the other hand, evaporation of the impactor can be expected during impact on the surfaces of the Galilean satellites, where the relative velocity is greatly enhanced due to the gravitational field of Jupiter (Zahnle et al., 1998). In the case of the Earth, the Cretaceous-Paleogene (K-P) stratigraphic boundary is related to the impact of an extraterrestrial body (Alvarez et al., 1980) forming the Chicxulub crater, and some material has been interpreted as condensation product (Kyte and Bostwick, 1995). The K-P boundary is globally characterised by a layer containing spinel-bearing spherules, where the maximum iridium anomaly has been found (Smit, 1999; Montanari and Koeberl, 2000). Additionally, nanophase iron particles occur which also may have been formed as condensation product in the so-called fireball (Wdowiak et al., 2001). Nanophase dust may result due to a secondary peak in a multi-modal size distribution obtained in a kinetic model of condensation (de Niem, 2002), these calculations did not address the chem-

ical composition. Space weathering on the lunar and asteroidal surfaces is thought to be partly caused by condensation of nanophase iron particles formed in a vapour in meteorite impacts (Keller and McKay, 1993; Hapke, 2001; Sasaki et al., 2002). On the Moon, velocities sufficient to cause significant evaporation of iron-bearing minerals can be reached during impact of meteors of cometary origin or for asteroidal impactors with large orbital eccentricities. Interestingly, meteor showers from 21P/Giacobini-Zinner show chondritic abundance ratios of Na:Fe and Mg:Fe in the spectra, and a temperature of ablation products of about 4000 K has been estimated, see Borovička et al. (2007). However, to infer the meteorite composition from such observations requires consideration of chemical fractionation, see Shaefer and Fegley (2004).

Considerable effort has been made to understand if spinels can form as condensation products from specific impacts, e.g. Chicxulub (Ebel and Grossman, 2005). According to Siret and Robin (2003) direct condensation of solid spinel crystals from the vapour phase is impossible. Earlier Robin et al. (1991) interpreted them as ablation residues during atmospheric entry, necessarily unrelated to the target rock composition. Kyte and Bostwick (1995) found that Ni-rich magnesiowüstite is preserved and intergrown with magnesioferrite spinel in the core of some spinel crystals. Because Ni-rich magnesiowüstite forms at temperatures even higher than 2300 K, they suggested an origin in a hot fireball, where metal oxides dominate the liquid composition relative to silicates. Ebel and Grossman (2005) obtain favourable

conditions for spinel formation in a silicate liquid in equilibrium with the gas phase at temperatures ranging from 1400 to 2400 K. Their vapour plume model assumes complete mixing of the target and impactor components predicted by Pierazzo et al. (1997, 1998), prior to condensation. Calculations of chemical equilibrium by Ebel and Grossman (2005) have been confined to $T < 2400$ K and used a (P, T) path extracted from hydrocode calculations. These hydrocode calculations (Pierazzo et al., 1997, 1998) used a different equation of state (EoS) in the gas phase than the chemical equilibrium solver. A hydrodynamic model of a condensing vapour plume requires an EoS not only in the high-pressure region, where data are available from shock wave experiments along the principal Hugoniot, mainly, but in a wide range of temperatures, pressures and densities. Shock wave experiments do not measure temperature and entropy directly, which are more important than pressure or particle velocity, in the context of condensation. Moreover, experiments corresponding to impact velocities in excess of 15 km s^{-1} are barely feasible with geomaterials. There are a number of laser experiments devoted to impact condensation and evaporation using meteoritic or analogue material, e.g. Moroz et al. (1996); Sasaki et al. (2002) however these experiments do not reproduce all thermodynamic conditions of a planetary impact: pressure, temperature, entropy, and do not lead to a full theoretical understanding of the observed compositions.

In this work, we investigate the simultaneous hydrodynamic, thermodynamic and chemical evolution of impact-created vapour numerically. In the

hydrodynamic runs, thermodynamics is treated consistently up to the point where the coexistence curve of the vapour with the condensed phase is intersected. In Chapter 2 we describe our approach for the equation of state (EoS). Following Thompson and Lauson (1972); Bobrovskii et al. (1974, 1976) and Melosh (2007), we use an interpolation formula for the free energy to generate the EoS. Our equation of state is a semi-analytical development similar to ANEOS (Thompson and Lauson, 1972) with the additional property that it asymptotically approaches a mixture of ideal gases in chemical equilibrium at low densities. This mixture is constructed with some realism, including 26 mono-atomic and 183 molecular species, relevant in work about condensation in the early solar system (Sharp and Huebner, 1990).

In the third Chapter, using the derived EoS, we simulate the hydrodynamic expansion of an impact-generated vapour plume into a surrounding atmosphere and obtain liquid compositions in a post-processing step. The algorithm is a variant of our Eulerian multi-material volume-of-fluid method (de Niem et al., 2007), adapted to spherical symmetry. Back-reaction of condensation on the hydrodynamics of the expanding cloud is neglected. This is a valid approximation as long as the mass fraction of condensates remains small and the purpose of hydrodynamic simulation is to obtain the thermodynamical state variables at the onset of condensation only. The impactor is modelled as a carbonaceous chondritic object, using the elemental abundances compiled by Lodders (2003, her table 3 column 6) with modifications for elements like oxygen and hydrogen. We start with initial conditions for

density, internal energy and pressure resulting from an impact with a given velocity, using the planar impact approximation (Melosh, 1989). Results are presented for two sets of initial conditions. A post-processing step, obtaining condensate compositions, is invoked when the boundary to the gas-liquid coexistence region is intersected in some computational cell, although the hydrodynamic run is continued until most of the material is affected.

In Chapter 4 we investigate the chemical equilibrium and condensate compositions and compare the overall elemental abundances of the refractive liquid to that of magnesioferrite spinels contained inside spherules from the global Cretaceous-Paleogene boundary layer analysed by Kyte and Bostwick (1995). For a model of the liquid phase as a single ideal solution, depending on initial conditions and composition, condensates begin to form at $T > 4000$ K. The results and some approximations are critically discussed in Chapter 5.

2 Analytical equation of state formulation in impact simulations

2.1 General thermodynamic considerations

Following Thompson and Lauson (1972), our analytical equation of state (EoS) is based on the free energy per unit of mass f as generating thermodynamic potential. In this way, a thermodynamically consistent EoS is

developed. The free energy is the sum of three parts

$$f = f_c + f_E + f_\Psi, \quad (1)$$

where f_c is the zero-temperature ('cold') part. Thermal contributions of the condensed and gaseous phases (Zel'dovich and Raizer, 1967; Anderson, 1989) are denoted by f_E and f_Ψ , respectively. The term f_E is the free energy of an Einstein solid – a collection of 3 harmonic oscillators per atom – and f_Ψ interpolates between the free energy of a mixture of gases and that of the condensed phase. The third term is essential for proper asymptotics in the case of evaporation. It is needed to connect high- and low-density states at super-critical temperatures and to construct the boundary of the two-phase mixture region (Thompson and Lauson, 1972; Bobrovskii et al., 1974; Melosh, 2007). The interpolation term is such that it suppresses the lattice contributions of the condensed phase in the dilute gas limit, see section 2.3. In the region of liquid-vapor coexistence, a Maxwell construction has to be applied (Thompson and Lauson, 1972) if hydrodynamic calculations enter this part of thermodynamic space.

Previous models either did not address the full problem of chemical equilibrium with molecular species (Thompson and Lauson, 1972) in the gas phase, or are specialized to a gas phase with a single molecular species (Bobrovskii et al., 1974, 1976; Melosh, 2007), so chemical equilibrium considerations have been oversimplified. A recent application of the idea of Bobrovskii

et al. (1976) by Ivanov and Deutsch (2002), investigated the decomposition of CaCO_3 relating to the possible climate catastrophe following the Chicxulub impact.

2.2 Zero-temperature part

We use a simple model for the zero-temperature part of the free energy, f_c , distinguishing expansion ($\rho < \rho_0$) and compression ($\rho \geq \rho_0$) where ρ_0 is the density of the condensed phase at $T = 0$ and $P = 0$. Following Bobrovskii et al. (1974, 1976) or Melosh (2007), for expansion ($\rho < \rho_0$), we take a Lennard-Jones-like potential

$$f_c = \frac{A}{\rho_0(\beta - \alpha)} \left(\frac{\eta^{\beta-1} - 1}{\beta - 1} - \frac{\eta^{\alpha-1} - 1}{\alpha - 1} \right), \quad (2)$$

with $\eta := \rho/\rho_0$, A is the bulk modulus at $\rho = \rho_0$, α and β are dimensionless parameters with $\alpha < \beta$ in order that a minimum results at $\rho = \rho_0$. Rather than giving these parameters directly, both ρ_0 and A may be determined by matching the bulk modulus and density at normal conditions. The exponent β is determined, knowing $-f_c(0)$, the energy of vaporisation at $T = 0$, the bulk modulus, and α (default value 5/3). For ($\rho_0 \geq 0$), Eq.(2) is replaced by

$$f_c = \frac{A - 2B}{\rho_0} \ln \eta + \frac{A - B}{\rho_0} \left(\frac{1}{\eta} - 1 \right) + \frac{B}{\rho_0} (\eta - 1), \quad (3)$$

here B is an additional parameter with the dimension of pressure. The pressure follows as the derivative (with minus sign) with respect to volume per unit of mass $v := 1/\rho$

$$P_c = \begin{cases} \frac{1}{(\beta-\alpha)} A (\eta^\beta - \eta^\alpha), & (\rho < \rho_0), \\ A(\eta - 1) + B(\eta - 1)^2, & (\rho \geq \rho_0), \end{cases} \quad (4)$$

note that P_c and its first derivative are continuous at ρ_0 . The expression for P_c in the compression region is simply a quadratic expansion in the deviation from zero-point density, reminiscent of the 'cold' pressure term in Tillotson's EoS (see Melosh (1989) e.g.). The second parameter B can be used to tune the high-pressure asymptotics of the Hugoniot curve, or it may be found from a condition of continuity of second-order derivative of P_c at ρ_0 . No attempt is made to include solid-state phase transitions, here. The authors of ANEOS (Thompson and Lauson, 1972) treat this in a rudimentary way by modification of f_c which we could do as well if a better match of the Hugoniot curve of a given meteorite material is desired. Only the form of the potential $f_c(\rho)$ in expansion is important for the construction of the liquid-vapor coexistence region. The contribution to the internal energy per unit mass obviously is $\epsilon_c = f_c$, because the entropy is zero at $T = 0$.

2.3 Thermal contribution in the condensed state

In the condensed state, the thermal contribution to the free energy is modeled in the quasi-harmonic approximation as an Einstein solid¹

$$f_E = -\frac{3k_B T}{m} \ln(Z), \quad Z = \frac{\exp(\Theta/(2T))}{\exp(\Theta/T) - 1}, \quad (5)$$

where Z is the partition function of a single harmonic oscillator with frequency ν , and $\Theta := h\nu/k_B$ is the Einstein temperature (analogous to the Debye temperature) in terms of Planck's constant h and the Boltzmann constant k_B ; m is the mean atomic mass. Equation(5) includes the contribution of the ground state. Only the lattice part of the EoS contributes to the entropy in the condensed state, thermal electronic contributions are ignored but the electronic pressure is thought to be included in the 'cold' pressure. The ratio T/Θ is constant along the adiabat as far as additional terms are suppressed in the condensed state, indeed from Eq.(5)

$$s_E = -\left(\frac{\partial f_E}{\partial T}\right)_\rho = \frac{3k_B}{m} \left[\frac{\Theta}{T} \frac{\exp(-\Theta/T)}{1 - \exp(-\Theta/T)} - \ln(1 - \exp(-\Theta/T)) \right], \quad (6)$$

¹A Debye solid is not much different except at very low temperatures $T \ll 300$ K.

and clearly s_E depends on the ratio Θ/T , only. For later reference, we list the lattice contribution to the thermal pressure

$$P_E = \Gamma \frac{3 k_B \Theta}{2 m} \rho \frac{1 + \exp(-\Theta/T)}{1 - \exp(-\Theta/T)}, \quad (7)$$

here the Debye-Grüneisen parameter Γ is (see Landau and Lifshitz (1980), e.g.)

$$\Gamma = \frac{\rho}{\Theta} \frac{d\Theta}{d\rho}. \quad (8)$$

We employ the model of Thompson and Lauson (1972) for Γ :

$$\Gamma = \begin{cases} 1 + (3\Gamma_0 - 2) \left(\frac{\rho}{\rho_0}\right) + (1 - 2\Gamma_0) \left(\frac{\rho}{\rho_0}\right)^2, & \rho < \rho_0, \\ \Gamma_0 \left(\frac{\rho_0}{\rho}\right) + \frac{2}{3} \left(1 - \frac{\rho_0}{\rho}\right)^2, & \rho \geq \rho_0, \end{cases} \quad (9)$$

where Γ_0 is the value at the density ρ_0 . In compression, the leading term gives the experimentally observed $\Gamma \propto \rho^{-1}$ behaviour whereas the quadratic term is required to asymptotically reach the value 2/3 of the Thomas-Fermi model. The low-density expression is simply a quadratic expansion in the density where the two coefficients are determined from continuity of Γ and its first derivative at $\rho = \rho_0$. The theoretical expressions for the Debye-Grüneisen parameter and Θ , see Burakovsky and Preston (2004), e.g., would lead to inconsistencies at low density (Thompson and Lauson, 1972). The

Einstein or Debye temperature following for this model is

$$\Theta = \begin{cases} \Theta_0 \left(\frac{\rho}{\rho_0} \right) \exp \left[\frac{1-2\Gamma_0}{2} \left(\frac{\rho}{\rho_0} \right)^2 + (3\Gamma_0 - 2) \left(\frac{\rho}{\rho_0} \right) - 2\Gamma_0 + \frac{3}{2} \right], & \rho < \rho_0 \\ \Theta_0 \left(\frac{\rho}{\rho_0} \right)^{2/3} \exp \left[\Gamma_0 \left(1 - \frac{\rho_0}{\rho} \right) - \frac{1}{3} \left(3 - 4\frac{\rho_0}{\rho} + \left(\frac{\rho_0}{\rho} \right)^2 \right) \right], & \rho \geq \rho_0 \end{cases} \quad (10)$$

and Θ_0 is the Einstein temperature at the reference density. An indirect dependence of entropy on the 'cold curve' could enter by way of the density dependence of Θ , the above model for Γ avoids this.

2.4 The interpolation formula

The additional contribution to the free energy achieves the interpolation between gaseous and condensed states. It is written in the form (Thompson and Lauson, 1972)

$$f_\Psi = \frac{3}{2} \frac{k_B T}{m} \ln(1 + \Psi), \quad (11)$$

where the function Ψ is determined by consistency in the two limiting cases of a mixture of ideal gases and a solid. A derivation of the interpolation formula can be found in Thompson and Lauson (1972) for mixtures of monoatomic gases. Bobrovskii et al. (1974) or Melosh (2007) extended this to molecular gases in special cases. The general idea was introduced much earlier already, see (Thompson and Lauson, 1972; Bobrovskii et al., 1974, 1976) for the original references. From Eq.(5) the contribution of the Einstein

solid in the limit $T \gg \Theta$ is

$$f_E \sim \frac{3k_B T}{m} \ln \left(\frac{\Theta}{T} \right). \quad (12)$$

For very large temperature as compared to Θ , part of the term f_Ψ has to compensate f_E , so Ψ has to contain a factor $(T/\Theta)^2$. Furthermore, the remaining part of the free energy has to be equal to that of an ideal gas mixture

$$\frac{3}{2} \frac{k_B T}{m} \ln \Psi \rightarrow \frac{3k_B T}{2m} \ln \left(\frac{T}{\Theta} \right)^2 + f^{id}, \quad (13)$$

where f^{id} denotes the Helmholtz free energy of a mixture of ideal gases. The resulting expression for Ψ is

$$\Psi = \exp \left[\frac{2f^{id}}{3(k_B T/m)} \right] \left(\frac{T}{\Theta} \right)^2. \quad (14)$$

In the case of mono-atomic ideal gases, the formula for f^{id} is simple. For the resulting f^{id} arising from chemical equilibrium calculations for a molecular gas, this is outlined in the appendix, in particular for thermochemical parameters in tabulated form. Thompson and Lauson (1972) and also Melosh (2007) express the last equation in terms of quantum-mechanical partition functions of gases. In the special case of mono-atomic ideal gases it can be shown that $\Psi \propto (\rho/m)^{2/3} \lambda^2 T^2 / \Theta^2$, where λ denotes the thermal de Broglie wavelength of an atom (Thompson and Lauson, 1972). The authors of ANEOS treated this special case, additionally setting internal atomic par-

tition functions equal to unity, whereas Bobrovskii et al. (1974) or Melosh (2007) insert vibrational and rotational terms for the internal partition function of molecules. We prefer the use of tabulated thermodynamic data.

The partial derivatives of the complete Helmholtz free energy f with respect to ρ and T can be found with the help of two identities arising from the definition of Ψ :

$$\left(\frac{\partial \Psi}{\partial T}\right)_{\rho} = \frac{2\Psi}{3(k_B T^2/m)} \left(\frac{3k_B T}{m} - \epsilon^{id}\right), \quad (15)$$

$$\left(\frac{\partial \Psi}{\partial \rho}\right)_T = \frac{2\Psi}{3(k_B T/m)\rho} \left(\frac{P^{id}}{\rho} - \Gamma \frac{3k_B T}{m}\right). \quad (16)$$

These identities are valid irrespective of considerations about chemical equilibrium of gases. In other words: the operations of partial derivation of f^{id} and chemical equilibrium constraint can be interchanged. This is not true for second-order derivatives of f^{id} : the partial derivative of the ideal-gas mixture pressure with respect to temperature is constrained by chemical equilibrium, likewise that of the internal energy. These derivatives are evaluated together with the chemical equilibrium calculations implemented in the EoS library. Interestingly, nowhere in the derivation it is actually needed that f^{id} describes a mixture of ideal gases, so the model for the gas phase could easily be generalized. The complete EoS with all partial derivatives necessary in hydrodynamic applications is listed in the appendix.

3 Hydrodynamic simulations

The numerical hydrodynamics algorithm is a modification of our axisymmetric multi-material code (de Niem et al., 2007) valid for (quasi-1D) spherical coordinates. Table 1 shows initial values of state variables resulting from two different sets of condensed-phase EoS parameters.

In the so-called planar impact approximation (Melosh, 1989), assuming the same material for impactor and target, a particle velocity of half the impact speed results. This follows because then the shock speed D_s is identical in both materials, and the pressure P_s is given by $P_s - P_0 = \rho D_s(u_i - u_p) = \rho D_s u_p$ (Zel'dovich and Raizer, 1967), where ρ and P_0 denote the initial density and pressure; u_i and u_p are the impact and particle velocities, respectively. The initial state of the vapor plume is situated on the Hugoniot curve originating at the pre-impact state (Zel'dovich and Raizer, 1967; Melosh, 1989) which we assume at a pressure of $P_0 = 1$ atm, here. Real asteroids of moderate size are porous and may resemble a rubble-pile (Britt et al., 2002). Therefore a typical porosity has been taken into account which leads to a modified initial state of the impactor, in particular the entropy and internal energy are higher for the same value of impact velocity whereas the pressure is lower, as compared to the non-porous case, see Zel'dovich and Raizer (1967).

Two different types of impactors are considered, each corresponding to a distinct set of parameters for the condensed-phase part of the EoS. Param-

eters for the gas-phase part are the same in both cases. In hydrodynamic calculations, the effect of chemistry on the condensed phase is ignored, not so, in the post-processing step (the chemical equilibrium calculations for liquid species). For the first type of impactor, condensed-state EoS parameters have been derived from Bobrovskii et al. (1974). This set of parameters is listed as 'granite' case in Table 2. The remaining parameter B is found, imposing the additional condition of continuity of the second derivative of the pressure at ρ_0 . The bulk properties are similar² to that of the granitic crust below the 2-3 km thick carbonate platform in the case of the Chicxulub impact. Recent work (Bottke et al., 2007) suggests a CM2-type carbonaceous chondrite for the impactor. Therefore the second type of impactor, denoted as the 'dunite' case in Table 2, is a more dense object where density, bulk modulus, and other parameters take values more appropriate for olivine. Values of the parameters are derived from different sources: so the value of the bulk modulus A is from Anderson (1989), the density ρ_0 is typical for olivine. Parameters Θ_0 and Γ_0 are the ANEOS values for dunite from Pierazzo et al. (1997, 1998) where these parameters have the same meaning as in our EoS model. The initial geometry of the vapour plume is that of a half-sphere, with radius corresponding to conservation of mass for a spherical impactor with initial diameter of 10 km, surrounded by a constant-density atmosphere. The atmosphere is taken as an ideal gas with $\gamma = 1.4$, treated as a distinct material. As mentioned, the gas-phase part of the EoS contains a mixture of

²however the gas phase composition is chondritic

mono-atomic and molecular species, details concerning the set of molecular gas species are given in the section on chemical equilibria. The overall composition is taken as chondritic with abundances from Lodders (2003) with some modification for O and H to resemble a carbonaceous chondrite, see Table 3 below.

Results of example hydrodynamic runs are shown in Figs. 1,2, corresponding to the initial values listed in Table 1, and EoS parameters appropriate for the different types of impactors, see Table 2. The volume-of-fluid method keeps the impact-generated vapor products and atmosphere always separate, see Figs. 1,2 where we also display the volume fraction, which equals zero in a computational cell containing atmospheric gas, only. The advantage over a more simple one-material algorithm is that otherwise one would have to take the same EoS for the atmosphere and impactor, the location of the contact discontinuity to the atmosphere could barely be determined, and the distribution of mass of impact-derived vapor over the grid would remain unclear. More realistic conditions near the shock to the atmosphere are obtained in this way. The reason for the rather large but still realistic value of the impact velocity of 22 km s^{-1} used here is that for a lower value, condensation would begin even closer to the critical point, at conditions for density and pressure where the ideal gas approximation made in the chemical equilibrium calculations definitely breaks down.

The most obvious feature of the solution is a spatially nearly linear velocity up to the radius where the shocked atmospheric gas begins to decelerate

impact-derived vapor. Due to the decelerating effect of the atmosphere, the maximum of velocity decreases monotonously with time. The distribution of density, pressure and temperature are more complicated, initially. Temperature and pressure develop a local maximum near the shock front. After the highly compressed material has expanded for a while, the region interior to the contact discontinuity to the atmosphere (C.D.), where the volume fraction jumps from one to zero, takes a more flat temperature- and pressure profile. An exception from this behaviour occurs near the shock front: here impact-derived material piles up at late time. This phenomenon mainly appears due to the approximation of constant initial density for the atmosphere which does not hold in the actual geometry where the atmosphere is vertically stratified. The impact-produced vapor reaches the largest temperatures at the C.D., and the thermodynamic path there is different from that in the interior. This does not play a major role at the time where most of the mass enters the coexistence region, i.e. at the times of the two last curves shown in Figs. 1,2. There are barely differences in the two simulation cases although the initial pressure differs (cf. Table 1) by about 100 GPa. The speed of expansion is almost the same as it is found by comparing the position of the C.D. and shock front. The value of the entropy of shocked material is comparable in both cases. Similiar thermodynamic conditions should be reached at the onset of condensation.

The main purpose of the hydrodynamic runs is to obtain the thermodynamic conditions during condensation. In Figs. 3,4 we display the ther-

modynamic history of computational cells in (T, ρ) space, for the 'granite' and 'dunite' runs, respectively. Vapor is supersaturated in the region above the coexistence curve. There are two ways to obtain the coexistence curve: a Maxwell construction using the EoS, or from the (dis)appearance of the condensed phase in the chemical equilibrium solver. Ideally, both methods should give the same curve. However differences exist despite the gas phase species are the same in both cases. Firstly, the condensed phase in the chemical equilibrium solver is a liquid solution containing many species, see next section, so the thermal part of the free energy is more realistic. Secondly, a 'cold' pressure is absent in the chemical equilibrium calculations assuming ideality of the gas phase. The Maxwell construction is a standard procedure which seeks a solution for the densities of two phases which simultaneously satisfy equality of pressure and chemical potential $\mu = f + P/\rho$ at given temperature (Landau and Lifshitz, 1980). At the phase boundary – at points where the mole fraction of condensed species is zero – only a single liquid (or solid) phase can coexist with the gas. This is a special case in more general multi-phase chemical equilibria treated in the next section.

Each symbol in Figs. 3,4 entering the supersaturated region represents a computational cell where condensation starts. In the 'granite' run, after ~ 2.8 seconds, the first few points approach the coexistence curve from below and the temperature is ~ 5000 K. Later, more and more cells move into the supersaturated vapor region. Finally, after a time of ~ 3.2 seconds, nearly all material is inside the mixed-phase region, the minimum temperature of

points close to the coexistence curve is ~ 4450 K. Fig. 4 shows the situation in the 'dunite' case. Here condensation starts after 3.8 seconds with a maximum temperature at the coexistence curve of about 4800 K. The interval of densities and temperatures occupied by the grid cells is comparable to the first case. After a time of about 4.2 seconds, most of the material has moved into the supersaturated region where now the lowest temperature at the coexistence curve is about 4350 K. There is a small number of data points at each time step that escapes towards very high temperatures. These correspond to cells close to the C.D. because only here such extremes can be reached. The lower temperatures in the 'dunite' case seem to be caused in part by the slower expansion time scale for this case, although it is clear that there is no unique value where the thermodynamic path intersects the coexistence curve as it would be in an isentropic situation. The general result in both cases is that condensation occurs under extreme thermodynamic conditions, temperatures above 4000 K, and it takes not much time, and the radius of the vapor plume when most of the material is super-saturated is about 38 km and 49 km in the 'granite' and 'dunite' cases, respectively, see Figs. 1,2.

4 Chemical equilibrium and condensate compositions

We use chemical equilibrium calculations as a post-processing step where the coexistence curve of the vapor with liquid or other condensed phases is intersected in a given grid cell. The hydrodynamic simulation is continued, treating the material in a cell containing condensate with the EoS of the metastable vapor. This approximation is not too strong as long as the degree of condensation –the mass fraction of the condensate– remains low. The purpose is to understand the origin of the most refractory condensates whereas it is not intended to predict the equilibrium liquid composition at low temperature³.

4.1 Method and source of data

We approximate the multi-component liquid that forms when the impact-derived vapor starts to condense as a single ideal solution of a condensible subset of 26 elements and of 31 condensed-phase compounds. A model of the liquid phase as a single ideal solution is only the first approximation to the actual behaviour, but non-ideal solution models such as those developed by Navrotsky (1986), Ghiorso et al. (1983), Hirschmann (1991) or Sack and Ghiorso (1991) require experimental data in the temperature range of application. A better model requires knowledge of the activities of liquid

³far away from the coexistence curve

components at the high temperatures involved. To first order, the liquid composition at such high temperatures and pressures as encountered in our simulations is controlled by the free enthalpy of the end-members.

The elements in the gas phase are H, C, N, O, F, Na, Mg, Al, Si, P, S, Cl, K, Ca, Sc, Ti, V, Cr, Mn, Fe, Ni, Cu, Br, Sr, Y, Zr, additionally the gas contains 183 molecular compounds listed in table 1 of Sharp and Huebner (1990). The end-members of the liquid solution are a subset of the species listed in table 2 of Sharp and Huebner (1990), with the distinction that we consider the liquid state where data are available in the appropriate temperature range, whereas Sharp and Huebner (1990) solved the problem of condensation of solids from a gas of solar composition. The JANAF data (Chase, 1998) contain liquid-phase thermochemical parameters for a subset of compounds from table 2 of Sharp and Huebner (1990): CaO, FeO, FeS, MgO, TiN, VN, ZrN, NiS, TiO, VO, NiS₂, SiO₂, TiO₂, ZrO₂, Al₂O₃, Cr₂O₃, MgSiO₃, MgTiO₃, Ni₃S₂, Ti₂O₃, V₂O₃, K₂SiO₃, Na₂SiO₃, MgAl₂O₄, Mg₂SiO₄, V₂O₅, MgTi₂O₅, Ti₃O₅, Ti₄O₇; data for MgFe₂O₄ and FeAl₂O₄ are from Sack and Ghiorso (1991). We also include a condensible subset of the 26 elements within the liquid solution in the respective temperature range. For elements, thermochemical parameters are JANAF data, except for *C* and *Y*, here we utilised the program COACH/THERMODATA (available online at <http://thermodata.online.fr/activity.html#logiciels>). Data for some molecular gases listed in table 1 of Sharp and Huebner (1990) are absent in the

NIST/JANAF data, in such cases we used the data of Tsuji (1973)⁴ as did Sharp and Huebner (1990). In these cases where only the approximation of Tsuji (1973) is available, ΔH_C^0 , $\Delta c_{p,C}$ for molecules, with respect to atomic gases as standard state are obtained by differentiation of the respective approximating expressions for the equilibrium constant for dissociation, i.e.

$$\frac{d \ln K_C}{dT} = \frac{\Delta H_C}{RT^2}, \quad \Delta c_{p,C} = \frac{d\Delta H_C}{dT}. \quad (17)$$

These quantities are required to evaluate partial derivatives of the pressure and internal energy of the ideal-gas mixture in chemical equilibrium, in the calculation of EoS derivatives in the hydrocode. For consistency of the EoS we have obtained all parameters for the molecular species from the NIST/JANAF data, where possible.

The chemical equilibrium solver is based on the SOLGASMIX algorithm which has been described in detail by Weber (1998), recently. An advantage is its robustness and simplicity for multi-phase problems. The low speed of convergence prevents its direct implementation into the hydrodynamic EoS⁵. Our implementation of the algorithm is a simplification to two mixture phases which may be gases, liquid or solid solutions, although generalisation to include a number of stoichiometric solid phases is straightforward. The initial guess for a two-phase gas-liquid equilibrium is provided by a solution for the gas phase alone.

⁴and in the parametrisation of Tsuji (1973)

⁵where a more direct Newton method is applied

The initial abundances of the vapor plume are taken from Lodders (2003, her table 3 column 6) who gave these data for primitive CI chondrites. However the hydrogen abundance is reduced to simulate a dry carbonaceous chondrite, see table 1-1 in Anderson (1989) for the water content of chondrites, e.g. The oxygen abundance is reduced by a factor of two relative to CI chondrites, consequently the abundances of the other elements increase such that a composition more typical for CM, CO, and CV carbonaceous chondrites results. The overall composition is given in table 3 for reference.

4.2 Results

Fig. 5 shows the elemental composition of the liquid condensate, as a function of temperature, beginning at the saturation point, corresponding to the highest temperatures shown in the diagram. The liquid mole fraction approaches zero directly at the coexistence curve, corresponding to the highest temperature, and increases with decreasing temperature; it reaches about 60 % at the lowest temperature shown in Figs. 5,6. The pressure is kept constant, a value of ~ 50 atm is typical for the hydrodynamic simulations. The abundance of each element displayed in Fig. 5 is obtained as the sum over all liquid compounds containing that particular element, including pure elements, if present. Complementary, Fig. 6 displays abundances of individual compounds, except pure elements, over the same temperature range. At the highest temperature Al is the most abundant element besides oxygen, followed by Mg, Fe, Ca, Si. Most metals develop a local maximum abundance

at some temperature, and later their content in the liquid is decreasing. Fe dominates over some interval of temperatures, later Mg crosses the curve of Fe. As Fig. 6 shows, the most abundant liquid compound species at the highest temperatures are FeO, MgO, MgAl_2O_4 , CaO, and Al_2O_3 ; pure metals go into solution as well. Initially few MgSiO_3 , SiO_2 , Mg_2SiO_4 , and metallic Si is dissolved, and abundances of silicates increase slowly with growing liquid mole fraction. There is also some FeS, always below the fraction of MgSiO_3 . Sulphides are very susceptible to the amount of oxydation and would be suppressed for a less reduced primitive chondritic impactor.

4.3 Comparison with spinel inclusions in K-P spherules

In the following, we compare the overall elemental abundances of the liquid with that of magnesioferrite spinels contained inside spherules from the global K-P boundary layer analysed by Kyte and Bostwick (1995). The matrix material of the spherules is mostly altered and lost, and the spinels are the residues that preserve compositional information about the impact event. The spherule layer is correlated with the maximum concentration of platinum-group elements (Kyte and Bostwick, 1995). We assume that the spinels crystallised from a liquid with an overall composition quenched shortly after the onset of condensation. Condensation in impact and explosion phenomena does not occur in equilibrium, and the condensate mass fraction typically can not reach more than about 50 percent (Raizer, 1960; Zel'dovich and Raizer, 1967). Therefore we think that the overall composi-

tion of primary condensates resembles that obtained in chemical equilibrium calculations shortly after crossing the liquid-vapor coexistence curve, when the condensate mass fraction is small. Our calculations do not indicate the presence of large amounts of silicate liquid, so the spinels could originate in a slag mixture dominated by pure metals and oxides.

Data of electron-microprobe analyses of spinel compositions have been obtained from GSA Data repository item 2005050, table DR1 (available online at www.geosociety.org/pubs/ft2005.htm). The spherules containing these spinels come from a wide range of geographic positions in the Pacific, south Atlantic, Indian ocean and Europe (Kyte and Bostwick, 1995). In Fig. 7 the composition of spinels is displayed together with that from our chemical equilibrium calculations corresponding to Fig. 5. The data scatter over a considerable range in composition for all elements except for oxygen⁶. To visualise the sense of compositional change with growing liquid fraction or, equivalently, decreasing temperature, the calculated values are shifted to the right in proportion to the liquid fraction. Compositions obtained in chemical equilibrium calculations for a pressure of 50 atmospheres are roughly compatible with the data from the Pacific K-P sites for such elements as Fe, Ni, Fe, Al, Cr, Ti, Mn, whereas there is great discrepancy for Ca and less for Si. The abundance of Mg is slightly overestimated by the model. The Ca initially contained in the metal-rich primary condensate will form separate minerals or be incorporated into silicate. A recent study by Cruz et al. (2005)

⁶its abundance has not been measured but is calculated assuming stoichiometric spinels

for the system $\text{SiO}_2\text{-NiO-FeO}$ compared Gibbs free energy of mixing of the two metal oxides in silicates with that of CaO . For example, at $T = 1873$ K the metal oxides showed a very similar near-ideal behavior in solution with SiO_2 , whereas Ca^{2+} incorporation into a SiO_4 network is preferred, i.e. the Gibbs free energy of mixing is strongly more negative than for the metals. The data for Si given by Kyte and Bostwick (1995) probably do not characterise the spinel phase, these minor amounts may also reflect some olivine contamination. In Fig. 8 we also display a comparison of the data with calculations for the European K-P sites Caravaca and Furlo. In contrast to the marine K-P sites the Cr and Ni abundances are underestimated by the model and the data for Cr are at least an order of magnitude higher than calculated.

5 Discussion

The EoS model combined with typical velocities for the impact of an asteroidal body leading to evaporation causes very large temperatures and pressures at the onset of condensation. This happens at least for impact velocities not much larger than 22 km s^{-1} and a chondritic chemical composition of the impactor as that given in table 3. A substantially larger velocity is not typical for asteroidal impactors and the effect of shock compression in the case of the planar impact approximation already is an upper limit corresponding to a 90 degrees impact. Even considering porosity of the impactor

the additional entropy produced in the primary shock wave does not seem to be sufficient for the condensates to appear at much lower temperatures and pressures although it lowers the impact velocity required to vaporise the impactor. It is clear that an ideal solution is a poor approximation at lower temperature where liquid immiscibility will tend to separate in particular metal oxides, silicates and pure metal. Several processes have been neglected, so the appearance of a silicate liquid at lower temperatures and the liquid immiscibility leading to separation of metal-rich phases from silicates and, most importantly, the crystallisation of spinels.

At liquid fractions not far away from the coexistence curve of the two-phase mixture a range of compositions appears that corresponds – at least qualitatively – to that measured in magnesioferrite spinels by Kyte and Bostwick (1995). Therefore we suggest that the spinels originated in such a liquid. In the phase diagram of Phillips, Sōmiya, and Muan (1961), with MgO and Fe_2O_3 as end-members, a solid mixture of magnesiowüstite and magnesioferrite exists over a broad composition range. More detailed investigations of equilibrium in a cooling refractive liquid of the composition we obtained here would show that certain amount of oxydation is necessary to produce abundant spinel. This could be achieved during later reaction with atmospheric air. Krawitz and Cohen (1974) state that ‘even when magnesiowüstite is rapidly cooled in a reducing atmosphere, a small volume fraction of spinel forms’.

The present model does not require a mixture with other materials such

as target rocks of sedimentary or crustal origin. Processes of diffusion required to achieve homogeneous mixing with target material in the gas phase take much longer than the short time interval available until the impactor-derived refractory material condenses. This is supported by the large Péclet number $Pc = vL/D$, measuring the ratio of advective to diffusive effects; here v is a typical flow velocity, L the length scale (e.g. the projectile diameter) and D (of the order $10^{-5}m^2s^{-1}$) the coefficient of interdiffusion of two given gas species. The hydrodynamic simulations show that there is an interval of densities, temperatures, and consequently pressures, where different parts of the vapor plume cross the coexistence curve, and there is no single thermodynamic path for the condensates. In view of the complexity of the problem of chemical composition in planetary impact the overall agreement of the model with spinel elemental composition is satisfactory.

Recently, the chondritic meteorites Gujba and Hammadah al Hamra HH237, belonging to the group of Bencubbin-like meteorites (Greshake et al., 2002; Rubin et al., 2003), have been hypothesized to result from a giant impact in the early solar system (Krot et al., 2005). Formation ages of these meteorites are ~ 5 Myr later than those of calcium-aluminium-rich inclusions (CAI's) (Krot et al., 2005). Gujba and HH237 are characterized by abundant Fe-Ni metal globules, Fe-Ni sulphide nodules, ferromagnesian pyroxene and olivine, and glassy or fine-grained silicate material (Rubin et al., 2003; Krot et al., 2005). As shown in this work, a metal-rich condensate containing abundant Fe-Ni, but also metal oxides and -sulphides, is the natural outcome

in vaporising collisions. A detailed comparison of the model with the data of Rubin et al. (2003) is planned for the future.

Complete vaporisation in collisions of massive protoplanets not necessarily requires the large impact velocity of 22 km s^{-1} used in this work. However modeling condensation at conditions even closer to the liquid-vapour critical point is barely feasible because of the lack of knowledge of activities of liquid components at such high P, T . Relative velocities leading to evaporation are not characteristic for the current asteroid population (Bottke et al., 1994), but may have occurred among a lost population of mars-sized objects.

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7 Appendix

7.1 Complete EoS with partial derivatives

In hydrodynamic applications, in addition to the pressure and internal energy, given as function of density and temperature, the partial derivatives

of pressure and internal energy are required since most algorithms need the sound speed. Moreover, the internal energy per unit mass ϵ is given rather than the temperature, the latter has to be found numerically from ϵ and ρ , during the solution of the energy equation. With the help of Eqs.(1,16) and the usual thermodynamic relation (Landau and Lifshitz, 1980)

$$P = - \left(\frac{\partial f}{\partial v} \right)_T, \quad (18)$$

the total pressure P is found

$$P = P_E + \left(P^{id} - 3\Gamma \frac{k_B T \rho}{m} \right) \frac{\Psi}{1 + \Psi} + P_c(\rho), \quad (19)$$

where P_E is given by Eq.(7) above and P^{id} is the pressure of the ideal gas mixture of molecules in chemical equilibrium; $m := \sum_a c_a m_a$ in terms of the atomic masses m_a and fixed overall abundance of the elements, c_a . In the condensed state, at not too large a temperature, the term proportional to Ψ is negligible. For large values of Ψ as in the high-temperature or dilute gas limits (where Θ is negligible), the first term P_E in Eq.(19) is compensated by $-(3\Gamma k_B T \rho / m)$. The internal energy per unit mass is evaluated with the help of Eq.(15) and $\epsilon = f + Ts$ where the entropy is $s = -(\partial f / \partial T)_v$, with the result

$$\epsilon = \epsilon_E + \left(\epsilon^{id} - \frac{3k_B T}{m} \right) \frac{\Psi}{1 + \Psi} + \epsilon_c(\rho), \quad (20)$$

with ϵ_E following from Eqs.(5,6) as

$$\epsilon_E = f_E + T s_E = \frac{3}{2} \frac{k_B \Theta}{m} \frac{1 + \exp(-\Theta/T)}{1 - \exp(-\Theta/T)}. \quad (21)$$

Beginning with the temperature derivative of P , using Eq.(19), we find

$$\begin{aligned} \left(\frac{\partial P}{\partial T} \right)_\rho &= \Gamma \frac{3k_B \rho}{m} \frac{\Theta^2}{T^2} \frac{\exp(-\Theta/T)}{(1 - \exp(-\Theta/T))^2} + \\ &+ \left[\left(\frac{\partial P^{id}}{\partial T} \right)_\rho - \Gamma \frac{3k_B \rho}{m} \right] \frac{\Psi}{(1 + \Psi)} + \\ &+ \left[\frac{P^{id}}{T} - \Gamma \frac{3k_B \rho}{m} \right] \left[2 - \frac{2}{3} \frac{\epsilon^{id}}{(k_B T/m)} \right] \frac{\Psi}{(1 + \Psi)^2}, \end{aligned} \quad (22)$$

where Eq.(15) has been used in the last term. The derivative with respect to density is found with the help of Eq.(16)

$$\begin{aligned} \left(\frac{\partial P}{\partial \rho} \right)_T &= \left(\frac{\partial P_E}{\partial \rho} \right)_T + \frac{dP_c}{d\rho} + \\ &+ \left[\left(\frac{\partial P^{id}}{\partial \rho} \right)_T - \left(\Gamma + \rho \frac{d\Gamma}{d\rho} \right) \frac{3k_B T}{m} \right] \frac{\Psi}{(1 + \Psi)} + \\ &+ \frac{2}{3(k_B T/m)\rho^2} \left[P^{id} - \Gamma \frac{3k_B T \rho}{m} \right]^2 \frac{\Psi}{(1 + \Psi)^2}, \end{aligned} \quad (23)$$

here the part due to the Einstein solid is

$$\left(\frac{\partial P_E}{\partial \rho} \right)_T = \left(\Gamma + \rho \frac{d\Gamma}{d\rho} \right) \epsilon_E + \Gamma^2 (\epsilon_E - c_{v,E} T). \quad (24)$$

The specific heat per unit mass amounts to

$$c_v = c_{v,E} + \left[\left(\frac{\partial \epsilon^{id}}{\partial T} \right)_\rho - 3 \frac{k_B}{m} \right] \frac{\Psi}{(1 + \Psi)} + \frac{2}{3} \frac{1}{(k_B T^2)/m} \left[\epsilon^{id} - 3 \frac{k_B T}{m} \right]^2 \frac{\Psi}{(1 + \Psi)^2}, \quad (25)$$

here the contribution of the Einstein solid to the specific heat is

$$c_{v,E} := \frac{3k_B}{m} \frac{\Theta^2}{T^2} \frac{\exp(-\Theta/T)}{(1 - \exp(-\Theta/T))^2}. \quad (26)$$

Clearly, the third terms in the expressions for the derivatives of pressure and internal energy vanish in the dilute gas limit $\Psi \rightarrow \infty$ where $\Psi/(1 + \Psi)^2 \rightarrow 0$. There is a negative part in the second term of the formula for the specific heat which does not vanish but annihilates the first term (in the Dulong-Petit limit when $\Theta/T \rightarrow 0$).

7.2 Evaluation of Ψ from tabulated data

It is necessary to evaluate the function Ψ from tabulated thermochemical parameters. These are given for atomic and molecular species as those of an ideal gas at the standard state, leading to a molar Helmholtz free energy

$$F^{id} = \sum_a N_a \left\{ \left[H_a^0 - T S_a^0 + RT \ln \left(\frac{RT N_a}{V P_{ref}} \right) \right] - RT \right\} + \sum_C N_C \left\{ \left[H_C^0 - T S_C^0 + RT \ln \left(\frac{RT N_C}{V P_{ref}} \right) \right] - RT \right\}, \quad (27)$$

where H_a^0 , S_a^0 refer to one mole and depend on T only, P_{ref} is a reference pressure (usually one atmosphere), and R denotes the universal gas constant $R = N_A k_B$ in terms of Avogadro's number N_A . Here N_a , N_C denote numbers of moles of mono-atomic and molecular gases, respectively. The expressions in the square brackets are the chemical potentials on a molar basis. The law of mass action and the EoS of an ideal gas can be used to show that in chemical equilibrium

$$F^{id} = \sum_a N_a^0 \left[H_a^0 - T S_a^0 + RT \ln \left(\frac{P_a}{P_{ref}} \right) \right] - P^{id} V, \quad (28)$$

where P_a is the partial pressure of element a obtained as solution of chemical equilibrium. Using Eq.(14), the function Ψ can be expressed as

$$\Psi = \left(\frac{T}{\Theta} \right)^2 \exp \left\{ \frac{2}{3} \sum_a c_a \left[\frac{G_a^0}{RT} + \ln \left(\frac{P_a}{P_{ref}} \right) \right] - \frac{2}{3} \frac{P^{id}}{(RT/M)\rho} \right\}, \quad (29)$$

here $G_a^0 := H_a^0 - T S_a^0$ is the molar Gibbs enthalpy of element a at standard pressure.

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Table 1: Initial state of highly shocked vapor-plume material. The two cases use different Eos parameters given in table 2.

Case	u_i [km s ⁻¹]	ρ [g cm ⁻³]	P [GPa]	T [K]	S [J/kg K]	porosity %
'granite'	22	4.6416	205.32	51106	5752.1	50
'dunite'	22	4.6115	303.37	50907	5733.3	50

Table 2: EoS parameters for the condensed-phase part. See text for details.

Parameter	Units	'granite' case	'dunite' case
ρ_0	gcm ⁻³	2.59	3.3
A	GPa	36.208	129.0
B	GPa	68.444	527.73
α		5/3	5/3
β		3.1139	7.5151
Γ_0		2/3	0.82
Θ_0	K	600.0	661.5

Table 3: Abundances of elements in the initial vapor plume.

	atom %		atom %
H	7.35133	Ca	0.67075
C	8.68136	Sc	0.00038
N	0.62212	Ti	0.02724
O	42.44063	V	0.00324
F	0.00945	Cr	0.14763
Na	0.64690	Mn	0.10304
Mg	11.69090	Fe	9.70180
Al	0.93471	Ni	0.53729
Si	11.23901	Cu	0.00592
P	0.08803	Br	0.00127
S	5.00065	Sr	0.00262
Cl	0.05885	Y	0.00005
K	0.04018	Zr	0.00013

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