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On the notion of thermophoretic velocity

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The phenomenology of thermal diffusion of a particle in a solvent involves the Soret coefficient of the particle/solvent mixture. It is usually considered that the migration velocity of the particle in the solvent is proportional to the Soret coefficient. I show here that this view is wrong because ordinary diffusion contributes to migration if the solvent is not homogeneous. I examine several examples (NaCl in water, polystyrene in ethylbenzene, maghemite nanoparticles) to show that this contribution can be strong enough to change the sign of the migration velocity and vitiate the interpretation of experimental data, the measurement of the Soret coefficient, the comparison of experiment with theory, and inter-experimental comparisons.

Keywords: thermophoresis; thermal diffusion; Soret effect

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§ 1. Introduction

In a binary mixture, thermodiffusion, also called thermal diffusion or the Ludwig-Soret effect, is the partial demixtion induced by the application of a temperature gradient. It is the relative transport of a species, say 1, with respect to the other one, 2. In this paper, the species 1, henceforth called the solute, is taken to be very dilute among a liquid or gaseous medium made up of molecules 2, called the solvent. The Ludwig-Soret effect has been discovered 150 years ago in liquids [1, 2] and some 90 years ago in gases [3]. The variety of mixtures found in soft matter science has recently generated a number of studies [4, 5]. Thermodiffusion of NaCl plays a role in the thermohaline circulation, a key ingredient in global climate warming models [6], and thermodiffusion of DNA could play a major role in the origin of life [7].

The local state of a binary mixture is defined by the temperature T , the pressure p and the mole fractions $x_1 = n_1/n$ and $x_2 = 1 - x_1$ of the components (n_1 and n_2 are the number densities of species 1 and 2, in m^{-3} in SI unit, and $n = n_1 + n_2$ is the total density). Starting from a homogeneous mixture where x_1 and x_2 are independent of position, the gradient of temperature causes a transport of particles 1 relative to 2, directed along or against ∇T in an isotropic medium. Transport is phenomenologically described by the number current density j_1 (in $\text{m}^{-2}\cdot\text{s}^{-1}$ in SI unit). As the ensuing inhomogeneity in the solute density entails a diffusion contribution to the current, j_1 is expressed as

$$j_1 = -Dn(\nabla x_1 + \sigma_T x_1 \nabla T), \quad (1)$$

where D is the particle diffusivity and σ_T is called the Soret coefficient [8-10]. We assume in equation (1) that the species 1 is very dilute in the solvent 2, and this is why j_1 is linear in x_1 . It is also assumed that the medium is in mechanical equilibrium, i.e. at a uniform pressure p . Otherwise, another contribution to j_1 is present, which is proportional to $x_1 \nabla p$ and called the barodiffusion current density [8, 10].

Other expressions for j_1 can be found, where the mass fraction [11] or the volume fraction [12] is used instead of the mole fraction x_1 . It is also possible to express j_1 as a linear combination of ∇n_1 and ∇T , as

$$j_1 = -D\nabla n_1 - DS^* n_1 \nabla T, \quad (2)$$

where

$$S^* = \sigma_T + \beta, \quad (3)$$

and β is the coefficient of thermal expansion of the solvent (see appendix A). We also introduce the dimensionless coefficient

$$\alpha = TS^*. \quad (4)$$

In water in standard conditions, $T\beta = 0,075$; in a perfect gas, $T\beta = 1$. The difference between S^* and σ_T can be important in a gas if α is close to unity. It is often ignored in a liquid.

Thermodiffusion has been studied independently in distinct areas. When the solute 1 is a macromolecule, it is usual to call *thermophoresis* its motion in a temperature gradient, in analogy with electrophoresis, which is the motion of a charged solute in an electric field. Generally speaking, the effect for small molecules 1, or for gaseous or liquid mixtures having comparable proportions of 1 and 2, is called thermodiffusion, while for suspensions of particles in gases or in liquids, it is called thermophoresis [13-19]. Then, DS^* is called the thermophoretic mobility, in analogy with the electrophoretic mobility, and accordingly $-DS^* \nabla T$ is called the thermophoretic velocity. In what follows, I consider a dilute suspension of particles 1 in a solvent 2, and I drop the index 1.

The point I want to make in this paper is that the wording *thermophoretic velocity* is fallacious. It is drawn from the usual interpretation of the coefficients in a migration-diffusion current equation, also called advection-diffusion or convection-diffusion equation, formally similar to equation (2). Unfortunately, that interpretation is not valid in an inhomogeneous

medium, as occurs here because of the temperature non-uniformity. Stated otherwise, I want to show that a particle does not migrate at the velocity $-DS^*\nabla T$ through the solvent. Likewise, the notion of an effective force $-\alpha\nabla(kT)$, sometimes termed "thermal force", propelling the particle against ($\alpha > 0$) or along ($\alpha < 0$) the temperature gradient with a mobility D/kT inferred from the Nernst-Einstein relation, is misleading. It is drawn from viewing equation (2) as a forced diffusion equation [10]. The incorrectness of the identification of the migration velocity with $-DS^*\nabla T$ is shown in § 2, which is based upon the phenomenological current equation only, with no appeal to any underlying theory or assumption. In § 3, I pick up three applications to the phenomenology of thermophoresis and the experimental determination of S^* . Conclusions are gathered in § 4.

§ 2. The migration velocity

§ 2.1. Derivation of the migration velocity from the current equation

Consider a statistical ensemble of particles in a vessel, and take one space dimension x for simplicity. (In three dimensions the calculation is similar, with Gauss's divergence theorem replacing the integration by parts.) The vessel boundaries are $x = 0$ and $x = L > 0$. For definiteness, a hot source located at $x = 0^-$ and a cold source located at $x = L^+$ establish the temperature gradient $dT/dx < 0$ in the bulk (figure 1).

[Insert figure 1 about here]

Generally speaking, the migration, or drift, velocity v_d is the velocity of the centroid

$$\langle x \rangle = \int x n(x, t) dx \quad (5)$$

of the ensemble of particles, with n being normalized to unity ($\int n(x, t) dx = 1$). To obtain $d\langle x \rangle/dt$, we use the equation of continuity,

$$\frac{\partial n}{\partial t} + \frac{\partial j}{\partial x} = 0, \quad (6)$$

expressing the local conservation of particles. Multiply equation (6) by x and integrate over x . Integration by parts and the vanishing of $xj(x, t)$ at the boundaries of the vessel entail

$$d\langle x \rangle/dt = \int j(x, t) dx. \quad (7)$$

The phenomenological current equation (2) may alternatively be rewritten as

$$j = \left(-DS^* \frac{dT}{dx} + \frac{dD}{dx} \right) n - \frac{d(Dn)}{dx}. \quad (8)$$

The last term in (8) contributes $D(L)n(L, t) - D(0)n(0, t)$ to the right-hand side of (7). Assume that $n(x, t)$ vanishes at the vessel boundaries (the opposite case is examined in § 2.2). Then,

$$\frac{d\langle x \rangle}{dt} = \left\langle -DS^* \frac{dT}{dx} + \frac{dD}{dx} \right\rangle. \quad (9)$$

Relation (9) shows that the sign of $d\langle x \rangle/dt$ is not determined by that of S^* alone. The meaning of the second contribution to $d\langle x \rangle/dt$ in the right-hand side of (9) is easy to understand if we take, for the normalized density profile at time t ,

$$n(x, t) = 1/(x_{II} - x_I) \text{ if } x_I < x < x_{II}, \quad (10)$$

and zero otherwise (it is understood that $0 < x_I$ and $x_{II} < L$). Then, at the same time t ,

$$\frac{d\langle x \rangle}{dt} = \left\langle -DS^* \frac{dT}{dx} \right\rangle + \frac{D(x_{II}) - D(x_I)}{x_{II} - x_I}. \quad (11)$$

If the diffusivity is larger on the leading edge $x = x_{II}$ than on the trailing edge $x = x_I$, $d\langle x \rangle/dt$ will, algebraically speaking, exceed the average value of the "thermophoretic velocity" $-DS^*(dT/dx)$ over the particle distribution. No matter how large the packet is, its actual mean velocity $d\langle x \rangle/dt$ is altered by the differential spreading dD/dx , see figure 2. This is known in the study of stochastic processes [20-22][¶] and has been experimentally checked in an inhomogeneous colloidal solution [24]. Therefore, contrary to a widespread belief, the positivity of S^* does not imply that the particles should migrate, on the average, to the cold side. Finally, in the limit $x_I \rightarrow x \leftarrow x_{II}$ of a δ -peaked $n(x, t)$, the velocity is a function of x only,

$$v_d(x) = -DS^* \frac{dT}{dx} + \frac{dD}{dx}. \quad (12)$$

It is the mean velocity of a group of particles released at a definite position x at time t . At later times, the centroid of the group moves at velocity v_d and the group spreads about the centroid.

[Insert figure 2 about here]

The spreading of the group can be obtained from the phenomenological current equation (2). Calculations similar to (5)-(9) throw up

$$\frac{d\langle x^2 \rangle}{dt} - \frac{d\langle x \rangle^2}{dt} = 2\langle D(x) \rangle + 2\langle x v_d(x) \rangle - 2\langle x \rangle \frac{d\langle x \rangle}{dt}. \quad (13)$$

If we consider a normalized δ -peaked n at time t , $n(x, t)$ is identical with $\delta(x - \langle x \rangle)$, so that (i) $\langle D(x) \rangle = D(\langle x \rangle)$ and (ii) the middle term in the right-hand side of (13) is $2\langle x \rangle \langle v_d(x) \rangle$ and cancels the last term. As a result, the instantaneous rate of change of the variance in position is just $2D(x)$ in one dimension. Therefore $D(x)$ retains its usual meaning of half the spreading rate of a packet initially located at position x , and may be thought of as the local diffusivity.

Assume now that the only dependence of D on position is due to $T(x)$. Then, relation (12) can be rewritten as

$$v_d(x) = -D \left(S^* - \frac{d \ln D}{dT} \right) \frac{dT}{dx}. \quad (14)$$

Thus, taking into account the temperature dependence of the diffusivity is tantamount to subtracting $d \ln D / d \ln T$ from TS^* in determining the migration velocity caused by a temperature gradient. Section 3 will show on three specific examples that the correction to S^* may be large enough to change its sign and/or flaw the comparison of experiment with theory and the consistency of different experimental methods aimed at measuring S^* .

[¶] The converse effect is also found, experimentally and theoretically, namely the change in the diffusivity due to an inhomogeneous drift velocity, in charge-carrier transport in a gas or a semiconductor subjected to a high electric field. Because the leading edge drifts at a slower velocity than the trailing edge, the carrier packet is squeezed along the direction of motion, and the longitudinal diffusivity is smaller than the transverse diffusivity. See [23] and references therein.

§ 2.2. The relationship between the migration velocity and the steady state

Consider a solute such that $S^* > 0$ and $v_d < 0$ (we shall see in § 3.1 that NaCl so behaves around 25 °C). Again, the vessel is the one depicted in figure 1. How can we reconcile the direction of the migration velocity with the sign of S^* in the steady state ? Then, $j = 0$ and the density profile, denoted as $n_\infty(x)$, obeys

$$\frac{d \ln n_\infty}{dx} = -S^* \frac{dT}{dx} . \quad (15)$$

The equation governing the profile is formally identical with that of a sedimentation equilibrium due to a force $-\alpha d(kT)/dx > 0$. Equation (15) shows that the positivity of S^* is tantamount to the solute preferentially concentrating in the colder region ($x \rightarrow L$) in the final state. Although the concept of a position-dependent particle velocity $v_d(x) < 0$ is still relevant in the steady state, *it is insufficient* because we are dealing with stochastic motion. In addition to the directed, or average, motion $v_d(x)$, making the so-called orthokinetic contribution to j [25], we have to take into account the fluctuations about the average, making the so-called perikinetic contribution to j . It is because of that contribution that, in the classic sedimentation equilibrium, the suspended particles reach a steady distribution although they everlastingly fall toward the bottom of the vessel. In the present problem, while the solute does drift toward $x = 0$, its higher diffusivity as $x \rightarrow 0$ entails a net backflow toward $x = L$. In this example, because the variation in $D(x)$ outweighs that in $n_\infty(x)$, the perikinetic contribution to j disagrees *in sign* with Fick's law holding in a homogeneous medium where D is independent of position x . Although the solute moves, on the average, to the hot side, much of it does not stay there because it diffuses farther on that side. The larger perikinetic outflow on the hot side causes the depletion near $x = 0$, consistent with $S^* > 0$. The profile $n_\infty(x)$ is determined by both the ortho- and perikinetic contributions to the flow, and this is why v_d may be negative while $-S^*(dT/dx)$ is positive.

In the steady state, the perikinetic contribution locally balances the orthokinetic one, $n v_d(x) - d(Dn)/dx = 0$ (drift without current [24]). The *integral* balance reads

$$\int_0^L v_d(x) n_\infty(x) dx + D(0) n_\infty(0) - D(L) n_\infty(L) = 0. \quad (16)$$

Relation (16) replaces relation (9) which does not hold here as equation (15) prevents $n_\infty(x)$ from vanishing at both boundaries. Relation (16) may be thought of as a bulk migration $\langle v_d \rangle < 0$ being offset by a reflecting effect [22, 26] of the $x = 0$ boundary ; the reflecting effect of the $x = L$ boundary enhances $\langle v_d \rangle$, but it is weaker than at $x = 0$.

§ 3. Applications

§ 3.1. NaCl in water

To show the practical implications of our relation (14), we now consider three examples of very different natures. The first one deals with the interpretation of S^* in a solution first studied by Soret [2], namely the aqueous solution of NaCl. The thermal diffusions of Na^+ and Cl^- are coupled because the solution cannot significantly deviate from local electroneutrality, so that one S^* coefficient is used for NaCl as a whole [8], although it is dissociated into ions. Similarly, the coupling of ordinary diffusions of Na^+ and Cl^- is reflected in a single diffusivity D , the so-called ambipolar diffusivity [27]. At $0.5 \text{ mol}\cdot\text{L}^{-1}$, it is found [28] that thermodiffusion of Na^+ and Cl^- has a $TS^* = +0.3$ at 25°C , whose sign changes at 12°C . To determine the correction implied by relation (14), we have to determine the ambipolar diffusivity D of NaCl. It is given by $2/D = 1/D_+ + 1/D_-$ [27] and the ionic diffusivities D_+ and D_- can be obtained from the Nernst-Einstein relation $D_\pm = kT\mu_\pm$, where $\mu_\pm$ are the ionic mobilities. In water at 25°C at standard pressure, it has been experimentally found that $d\ln\mu_+/dT = 0.022 \text{ K}^{-1}$ for Na^+ and $d\ln\mu_-/dT = 0.020 \text{ K}^{-1}$ for Cl^- [29]. We thus get $d\ln D/d\ln T = +7.3$, meaning that $D \propto T^{7.3}$, near 25°C . This is a very strong temperature dependence. From relation (14), the correction to TS^* is more than twenty times larger than $TS^* = +0.3$, with an opposite sign. This upsets the direction of the migration of the Na^+ and Cl^- ions and the usual view held in studies of the thermohaline circulation in oceans [28]. The actual migration is towards the warmer temperatures. The incorrect interpretation is of no concern if the phenomenological equation (1) or (2) is correctly encoded in a computer programme. But, if physical reasoning is used, it entails qualitatively wrong conclusions.

More generally speaking, whenever TS^* crosses the zero value, the diffusivity gradient changes the transition temperature from a "thermophobic" to a "thermophilic" behaviour. As a recent example involving proteins (top curve in figure 1 of [30]), TS^* varies from -3.0 to $+3.0$ as T spans the $280\text{--}310 \text{ K}$ range, and vanishes at 290 K . The measurement of $D(T)$ is not reported, but we may estimate $d\ln D/d\ln T = 1 - d\ln\eta/d\ln T$ from the Stokes-Einstein formula $D = kT/6\pi\eta R$ which is usually good for large-size spherical particles (η is the solvent viscosity and R is the radius of the particle). We get $d\ln D/d\ln T = +8.2$ in water in standard conditions. (It is worthy of remark that even the temperature dependence $d\ln D/d\ln T = 7.3$ of the diffusivity of the small-size Na^+ and Cl^- ions computed above is well described by this formula.) Then, according to our relation (14), the protein migration is thermophilic throughout the $280\text{--}310 \text{ K}$ range.

§ 3.2. Thermal field-flow fractionation

The second application of our relation (14) is the measurement of S^* through thermal field-flow fractionation, a high-resolution technique that uses thermophoresis to separate and characterise objects [17, 31]. The solution flows between a hot wall and a cold wall whose

temperature difference is ΔT , along a direction parallel to the walls. What is measured is the shift Δx of a solute injected at a definite position x , after a time Δt has elapsed. From the thermophoretic velocity $U_T \equiv \Delta x / \Delta t$ thus measured, a thermophoretic mobility is defined and computed as $D_T \equiv -U_T / (\Delta T / \Delta x)$. Then, it is compared to a theoretical prediction of that mobility. The experimentally defined quantity corresponds to our $-v_d / (dT/dx) = DS^* - dD/dT$ according to relation (14), whereas the theoretical quantity is DS^* . Thus, the comparison between both quantities is flawed. The extent of the error depends on the values of the parameters. The values $TS^* \approx 45$ measured for polystyrene in ethylbenzene around 310 K (figure 9 in [31]) are not much affected by $d \ln D / d \ln T \approx 4.7$. However, this correction (10 %) is larger than the correction to the velocity profile of the flow between the hot and cold walls, which is also due to the temperature dependence of η and is typically 4 % [32].

§ 3.3. Maghemite nanoparticles

The values of D and S^* of $\gamma\text{-Fe}_2\text{O}_3$ nanoparticles have been measured by another experimental method, namely forced Rayleigh scattering [12, 33] where a gradient of T is that of a temperature grating created by a light-intensity grating. The phenomenology of the method rests upon equation (6) to describe the initial rise and the subsequent relaxation of n following a light pulse. In equation (6), the current density is inputted with the pattern (2) in which D and S^* , or D and DS^* , are treated as adjustable parameters. The method is immune from the incorrect understanding of the migration velocity because the current density is not viewed according to the pattern (8). Values of TS^* such as +12.5 (in cyclohexane) and -4.17 (in water) were obtained (table 4 in [33]). If the same colloidal particles had been studied by means of thermal field-flow fractionation, values of +8.0 and -12.47 would have been obtained owing to relation (14). In this example, it is clear that the incorrect interpretation of the velocity would cause an important discrepancy between different experimental methods aimed at measuring S^* . *A contrario*, we notice that values of S^* consistent with those derived from forced Rayleigh scattering have been obtained from thermal-lens measurements [34]. Agreement is achieved because neither method identifies $-DS^* \nabla T$ with a migration velocity.

§ 4. Conclusions

This paper has shown that the measure of partial demixtion $\sigma_T \approx S^*$ and the migration velocity v_d are not proportional to each other. They should be conceived of as distinct concepts. σ_T refers to the static enrichment of one side relative to the other induced by ∇T , whereas v_d is a dynamic quantity. Their non-proportionality is shown to be due to the inevitable temperature dependence of the diffusivity. What matters in the correction is not the absolute value of D , but its relative rate of change with T . The correction can be very important if diffusion is

thermally activated*. The reader is also warned about the semantic gap between the notions of *transport* (entified in j) and of *motion* (entified in dx/dt). They are linked through relation (7).

The conceptual confusion is strengthened in the "non-Brownian approximation" sometimes used in colloidal or micellar systems. That approximation consists in neglecting D , or the diffusion current, in a sedimentation experiment when the Péclet number assessing the relative importance of migration over diffusion is large [17, 25]. The limit $D \rightarrow 0$ of a "non-Brownian particle" is often envisaged at a large R . However, removing the Fick term in equation (2) suppresses the $d \ln D / d \ln T$ correction in (14) and entails a wrong value of the sign of the migration velocity in an aqueous solution of NaCl at 0.5 mol·L⁻¹ at 25 °C. Therefore, the non-Brownian approximation should be avoided in studying thermophoresis. At any rate, a better approximation consists in decomposing j according to equation (8) and removing the total derivative, i.e. the perikinetic contribution to the flow. The latter cannot be dismissed in the steady state, however, as the discussion in § 2.2 has shown. More broadly speaking, because the Nernst-Einstein relation between D and mobility μ always holds[#] and because the response to a force, whether of thermal origin or not, involves the mobility μ , it is hazardous to put $D = 0$ while retaining μ in thermodiffusion studies.

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In summary, the view of the Soret coefficient σ_T , or of the thermophoretic mobility DS^* , as being proportional to a particle velocity, is erroneous. The error is rooted in the fact that, when a medium is inhomogeneous (owing to a temperature gradient or whatever reason), the coefficient of n in the phenomenological current equation does not have its usual meaning. This can vitiate interpretations of experiment, experimental measurements, theoretical calculations, comparisons of experiment with theory and cross-experimental comparisons. This finding should help to remove discrepancies in the physics of thermophoresis whenever $|T\sigma_T|$ is not very large.

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Appendix A

To obtain equation (2), we rewrite equation (1) as

$$\mathbf{j}_1 = -D \nabla n_1 + Dx_1 \nabla n - D\sigma_T n_1 \nabla T. \quad (\text{A } 1)$$

We notice that $n = 1/v$, where $v = v(T, p, x_1)$ is the volume per particle, and

* Unpublished data of G. Demouchy and A. Bourdon on ionic-coated maghemite nanoparticles show a $D(T)$ dependence larger than expected from the temperature dependence of the solvent viscosity in the Stokes-Einstein formula with a T -independent radius R . The thermally activated nature of the weak acid-base equilibrium of the citrate ions coating the nanoparticle surface is suspected to alter the hydrodynamic radius.

[#] An activity correction to $D/kT\mu$ is due in a non-ideal solution. See [10], p. 774; or [27], pp. 450-452.

$$\nabla v = (\partial v / \partial T)_{p, x_1} \nabla T + (\partial v / \partial x_1)_{p, T} \nabla x_1. \quad (\text{A } 2)$$

In the right-hand side of (A 2), we recognize the coefficient of thermal expansion $\beta = (1/v)(\partial v / \partial T)_{p, x_1}$ of the solution. Since $\nabla n = -(\nabla v)/v^2$, equation (A1) becomes

$$\mathbf{j}_1 = -D \nabla n_1 - D x_1 [\beta n \nabla T + (\partial v / \partial x_1)_{p, T} (\nabla x_1)/v^2] - D \sigma_T n_1 \nabla T. \quad (\text{A } 3)$$

The right-hand side of (A 3) contains a $x_1 \nabla x_1$ term which is quadratic in x_1 . Since we are interested in the limit $x_1 \rightarrow 0$, we drop that term. Similarly, in the limit $x_1 \rightarrow 0$, β is the coefficient of thermal expansion of the pure solvent. To first order in n_1 or x_1 , (A 3) yields equation (2).

References

- [1] C. Ludwig, S. B. Akad. Wiss. Wien **20** 539 (1856).
- [2] Ch. Soret, Arch. Sci. Phys. Nat. **2** 48 (1879); C. R. Séances Hebd. Acad. Sci. **91** 289 (1880); Arch. Sci. Phys. Nat. **4** 209 (1880).
- [3] S. Chapman and F. W. Dootson, Phil. Mag. **33** 248 (1917).
- [4] W. Köhler and S. Wiegand (editors), *Thermal Nonequilibrium Phenomena in Fluid Mixtures*, Proceedings of the Fourth International Meeting on Thermodiffusion (Springer, Berlin, 2002).
- [5] A. Shapiro (editor), Selected Papers from the Fifth International Meeting on Thermodiffusion, Phil. Mag. **83** 1965-2219 (2003).
- [6] W. S. Broecker, *Science* **278** 1582 (1997).
- [7] D. Braun and A. Libchaber, Phys. Biol. **1** P1 (2004).
- [8] R. Haase, *Thermodynamics of Irreversible Processes* (Addison-Wesley, Reading, MA, 1969), pp. 357 and 370.
- [9] E. L. Cussler, *Diffusion: Mass transfer in fluid systems*, 2nd edition (Cambridge University Press, Cambridge, MA, 1997), p. 522.
- [10] R. Byron Bird, Warren E. Stewart, and Edwin N. Lightfoot, *Transport phenomena*, 2nd edition (Wiley, New York, 2002), p. 770.
- [11] L. D. Landau and E. M. Lifshitz, *Fluid Mechanics* (Pergamon, Oxford, 1959) (original Russian edition, Mir, Moscow, 1954), section 58.
- [12] J. Lenglet, A. Bourdon, J.-C. Bacri and G. Demouchy, Phys. Rev. E **65** 031408 (2002).
- [13] G. S. McNab and A. Meisen, J. Coll. Interf. Sci. **44** 339 (1973).
- [14] J. L. Anderson, Annu. Rev. Fluid Mech. **21** 61 (1989).
- [15] F. Zheng, Adv. Coll. Interf. Sci. **97** 255 (2002).
- [16] E. J. Davis, "Thermophoresis of particles", in *Encyclopedia of Surface and Colloid Science*, vol. 4 (Marcel Dekker, New York, 2002), pp. 5365-5375.
- [17] A. Regazzetti, M. Hoyos and M. Martin, J. Phys. Chem. B **108** 15285 (2004).
- [18] S. Wiegand, J. Phys. Condens. Matter **16** R357 (2004).

- [19] S. Nader Rasuli and Ramin Golestanian, *J. Phys. Condens. Matter* **17** S1171 (2005).
- [20] N. G. van Kampen, *J. Phys. Chem. Solids* **49** 673 (1988).
- [21] R. Collins and T. Takemori, *J. Phys. Condens. Matter* **1** 3801 (1989).
- [22] N. G. van Kampen, *Stochastic Processes in Physics and Chemistry*, 2nd edition (North-Holland, Amsterdam, 1992).
- [23] E. Bringuier, *Phys. Rev. B* **58** 4543 (1998).
- [24] P. Lançon, G. Batrouni, L. Lobry and N. Ostrowsky, *Europhys. Lett.* **54** 28 (2001).
- [25] Theo G. M. Van de Ven, *Colloidal Hydrodynamics* (Academic, London, 1989).
- [26] R. Collins, S. R. Carson and J. A. D. Matthew, *Am. J. Phys.* **65** 230 (1997).
- [27] W. M. Deen, *Analysis of Transport Phenomena* (Oxford University Press, New York, 1998), p. 457.
- [28] D. R. Caldwell, *J. Phys. Chem.* **77** 2004 (1973).
- [29] Yakov I. Gerasimov (editor), *Physical Chemistry*, vol. 2 (Mir, Moscow, 1974), p. 409.
- [30] S. Iacopini and R. Piazza, *Europhys. Lett.* **63** 247 (2003).
- [31] M. Martin, C. Van Batten and M. Hoyos, in reference [4], pp. 250-284.
- [32] A. C. van Asten, H. F. M. Boelens, W. Th. Kok, P. S. Williams and J. C. Giddings, *Sep. Sci. Technol.* **29** 513 (1994).
- [33] G. Demouchy, A. Mezulis, A. Bée, D. Talbot, J.-C. Bacri and A. Bourdon, *J. Phys. D: Appl. Phys.* **37** 1417 (2004).
- [34] S. Alves, G. Demouchy, A. Bée, D. Talbot, A. Bourdon and A. M. Figueiredo Neto, in reference [5], pp. 2059-2066.

Figure captions

Figure 1. A binary fluid mixture is contained in a vessel bounded at $x = 0$ and L . A temperature gradient $dT/dx < 0$ is applied from the top ($x = L$) to the bottom ($x = 0$).

Figure 2. In the thermophoresis of a finite packet, the temperature-induced gradient of diffusivity D (double arrow) contributes to the drift velocity v_d (simple arrow).

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1310x1853mm (96 x 96 DPI)

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